## ELECTRONIC SUPPLEMENTARY INFORMATION



Figure S1: IR spectra of $\mathrm{FePO}_{4}$ catalyst


Figure S2 : TEM micrograph $($ scale $=100 \mathrm{~nm})$ of $\mathrm{FePO}_{4}$ catalyst


Figure S3: Time on line studies over the fresh catalysts at a temperatures of $350^{\circ} \mathrm{C}$ and $550{ }^{\circ} \mathrm{C}$ at a carbon to oxygen ratio of $8: 3, \mathrm{GHSV}=5000 \mathrm{~h}^{-1}$


Figure S4: Effect of temperature on the conversion of $n$-octane and selectivity towards products over $\mathrm{Fe}_{2} \mathrm{P}_{2} \mathrm{O}_{7}$ phase at a carbon to oxygen ratio of $8: 3, \mathrm{GHSV}=5000 \mathrm{~h}^{-1}$


Figure S5 : Time on line studies over the "deactivated" catalyst catalysts at a temperatures of 350 ${ }^{\circ} \mathrm{C}$ and $550^{\circ} \mathrm{C}$ at a carbon to oxygen ratio of $8: 3, \mathrm{GHSV}=5000 \mathrm{~h}^{-1}$


Figure S6 : Time on line studies over the "regenerated" catalyst catalysts at a temperatures of 350 ${ }^{\circ} \mathrm{C}$ and $550^{\circ} \mathrm{C}$ at a carbon to oxygen ratio of $8: 3, \mathrm{GHSV}=5000 \mathrm{~h}^{-1}$

## S1: Analysis of products and Calculations:

The products of the catalysed reactions were expressed as conversion, selectivity and yield. Conversion is a measure of the amount of feed introduced into the reactor that is converted into products:

$$
\text { Conversion }(\mathrm{mol} \%)=\frac{\text { moles of } n \text {-octane in }- \text { moles of } n \text {-octane out }}{\text { moles of } n \text {-octane in }} \times 100
$$

The selectivity towards a product may be defined as the ratio of that product formed to the total moles of products formed, based on carbon atoms:

$$
\text { Selectivity }(\mathrm{mol} \%)=\frac{\text { total moles carbon of product component }}{\text { total moles carbon of all product components }} \times 100
$$

The yield is the molar fraction of a particular product formed to the total number of moles of feed introduced:

$$
\text { Yield }(\mathrm{mol} \%)=\frac{\text { Selectivity of product component } \times \text { conversion }}{100}
$$

The gas hourly space velocity (GHSV) was calculated as follows:

$$
\text { Gas hourly space velocity, GHSV }\left(h^{-1}\right)=\frac{\text { total flow rate into the reactor }}{\text { volume of the catalyst used }}
$$

The carbon balance of each reaction was determined as below :

$$
\text { Carbon balance }=\frac{\text { moles of carbon in }}{\text { moles of carbon out }} \times 100
$$

## S2. Calculation of response factors (RF):

Assign $n$-octane a RF of 1 and calculate all other Response Factors relative to this:
Mass of $n$-octane in standard solution $=0.0073 \mathrm{~g}$
Mass of trans-2-octene in standard solution $=0.00715 \mathrm{~g}$
Injection volume $=0.1 \mu \mathrm{l}$
Peak area of $n$-octane $=46684.56$
Peak area of trans-2-octene $=51712.54$

The RF of $n$-octane was considered as 1 and Response Factor calculations was carried out relative to $n$-octane

Mass of $n$-octane in standard solution $=0.0075$
Mass of trans 2-octene in standard solution $=0.00715$
Injection volume $=0.1 \mu \mathrm{~L}$
Peak area of $n$-octane $=46684.56$
Peak area of trans-2-octene $=50712.21$
peak area of trans-2-octene $\times$ mass of $n$-octane
Response factor of trans-2-octene $=$ mass of trans-2-octenexpeak area of n-octane

Table A2.4 Relative response factor of trans 2-octene

| Injection <br> volume ( $\boldsymbol{\mu l}$ ) | Amount of <br> trans 2- <br> octene | Peak area of <br> trans 2- <br> octene | Amount of <br> $\boldsymbol{n}$-octane <br> injected | Peak area of <br> $\boldsymbol{n}$-octane | Relative <br> response <br> factor (RF) |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 0.1 | 0.00071 | 51714,89 | 0.000703 | 46684.56 | 0.91 |
| 0.2 | 0.00153 | 113606.4 | 0.001416 | 94552.7 | 0.9 |
| 0.3 | 0.00225 | 158300.4 | 0.002109 | 136843.9 | 0.91 |
| 0.4 | 0.00285 | 229129.7 | 0.002813 | 205058.5 | 0.91 |

Average response factor of trans 2-octene $=0.91$

Table S1. Retention times, Response factors and gradient of the calibration graph of compounds

| Component | R. T. (min) | R.F | Equation (y=..) |
| :---: | :---: | :---: | :---: |
| 1-pentene | 2.432 | 0.93 | $1.01 \mathrm{E}+14$ |
| 2-methyl-2-propanol | 2.477 | 0.72 | $8.13 \mathrm{E}+14$ |
| $n$-Pentane | 2.37 | 0.76 | $8.81 \mathrm{E}+14$ |
| 1-hexene | 3.52 | 0.95 | $1.36 \mathrm{E}+14$ |
| $n$-Hexane | 3.692 | 0.93 | $1.32 \mathrm{E}+14$ |
| Methylcyclopentane | 4.311 | 0.92 | $1.24 \mathrm{E}+14$ |
| $n$-Heptane | 6.98 | 0.91 | $1.63 \mathrm{E}+14$ |
| 2, 4-dimethylhexane | 8.97 | 0.94 | $1.79 \mathrm{E}+14$ |
| Toluene | 10.47 | 1.12 | $1.57 \mathrm{E}+14$ |
| 4-methylheptane | 11.72 | 1.14 | $1.83 \mathrm{E}+14$ |
| 1,7-octadiene | 12.52 | 0.90 | $1.85 \mathrm{E}+14$ |
| 1-octene | 13.8 | 0.98 | $1.90 \mathrm{E}+14$ |
| 3-octene | 14.9 | 0.98 | $1.75 \mathrm{E}+14$ |
| Trans-4-octene | 14.53 | 0.97 | $1.83 \mathrm{E}+14$ |
| $n$-Octane | 15.26 | 1 | $1.82 \mathrm{E}+14$ |
| Trans-2-octene | 15.59 | 0.94 | $1.79 \mathrm{E}+14$ |
| 1,3-octadiene | 16.523 | 0.92 | $1.54 \mathrm{E}+14$ |
| Ethyl cyclohexane | 16.92 | 0.90 | $1.87 \mathrm{E}+14$ |
| Propyl cyclopentane | 16.93 | 10.95 | $1.75 \mathrm{E}+14$ |
| Ethyl benzene | 17.58 | 1.13 | $1.93 \mathrm{E}+14$ |
| Styrene | 18.34 | 1.17 | $1.75 \mathrm{E}+14$ |
| xylene | 18.49 | 1.15 | $1.92 \mathrm{E}+14$ |


| cis-cyclooctene | 18.829 | 1.20 | $1.78 \mathrm{E}+14$ |
| :--- | :--- | :--- | :--- |
| cyclooctane | 19.16 | 1.16 | $1.90 \mathrm{E}+14$ |
| cis.cis-1,5-cyclooctadiene | 19.52 | 1.12 | $1.84 \mathrm{E}+14$ |
| 4-octanone | 20.839 | 0.73 | $1.32 \mathrm{E}+14$ |
| 3-octanone | 21.28 | 0.91 | $1.87 \mathrm{E}+14$ |
| 2-octanone | 21.394 | 0.84 | $1.80 \mathrm{E}+14$ |
| 3-octanol | 21.83 | 0.76 | $1.51 \mathrm{E}+14$ |
| octanal | 21.84 | 0.71 | $1.40 \mathrm{E}+14$ |
| 2-octanol | 21.992 | 0.78 | $1.61 \mathrm{E}+14$ |
| octene oxide | 22.244 | 0.85 | $1.28 \mathrm{E}+14$ |
| benzyl alcohol | 22.765 | 0.89 | $1.86 \mathrm{E}+14$ |
| 1-octanol | 24.446 | 0.85 | $1.23 \mathrm{E}+14$ |
| octanoic acid | 26.396 | 0.61 |  |

## S2. Determination of moles of trans 2-octene from a liquid organic sample

Mass of the organic layer $=1.786 \mathrm{~g}$ Percentage peak area of trans 2 -octene $=0.91$ Calculated Response Factor $=1.0519$

Corrected area $=$ Percentage peak area $\div$ Response factor $=0.91 \div 1.0519=0.9677$ corrected area

Normalised area $(\%)=\overline{\text { Sum of corrected areas of all the products in sample }} \times 100$

$$
=0.866
$$

(g)

Mass
= normalised are
Component

$$
\begin{aligned}
& \frac{100}{1} \times \quad \text { mass of organic layer } \\
= & \frac{(0.8601 \times 1.786)}{100}=0.01525 \mathrm{gm}
\end{aligned}
$$

mass of component
Moles component out (moles) $=\overline{\text { molar mass of component }}$

$$
=\frac{0.01525}{112.21}=0.000135
$$

Moles of carbon out $=$ moles component out $\times$ carbon number

$$
=0.001087 \text { moles of carbon }
$$

## S3. Determination of moles of butane from a gaseous organic sample

The gaseous samples were identified with the help of GCMS and their quantification was carried out by using methane as a standard gas by using the equation below

Initially, the constant was derived by using equation
Constant $=(\operatorname{Rf}$ of methane/Area of methane $) \times$ Vol. $\%$ of methane
The values obtained by injecting $0.2 \mu \mathrm{~L}$ in the GC-FID are
Injection volume $=0.2 \mu \mathrm{~L}$ Methane area $=90000$
Methane $\mathrm{Rf}=1$
Constant $=(1 / 90000) \times 0.02$

$$
=2.22 \times 10^{-7}
$$

Ethylene area from gaseous sample from reaction=17629.91 Corrected area= Area/ Rf

$$
\begin{aligned}
& =17629.91 / 1 \\
& =17629.91
\end{aligned}
$$

Further, the corrected area was entered in the following formula to get the Mol. \%, Mol. \% = Corrected area $\times$ constant $\times$ (molecular weight of methane/ molecular weight of unknown)

Mol. $\%=17629.91 \times 2.22 \times 10^{-7} \times(16 / 28) \mathrm{Mol} \%=0.223871 \%$

Then, the volume of gas out was calculated from Mol. \% Volume of gas out= Mol. $\% \times$ gas out $/$ min

$$
=0.223 \% \times 67 \mathrm{~mL} / \mathrm{min}
$$

$$
=0.0538 \mathrm{~mL} / \mathrm{min}
$$

Moles out were calculated by using ideal gas equation

$$
\mathrm{PV}=\mathrm{nRT}
$$

Where,
$\mathrm{P}=10000 \mathrm{~Pa}$
$\mathrm{V}=0.0538 \mathrm{ml} / \mathrm{min}$
$\mathrm{R}=8.314 \mathrm{~L} \mathrm{kPa} \mathrm{K}{ }^{-1} \mathrm{~mol}^{-1} \mathrm{~T}=298 \mathrm{~K}$
Number of moles of ethylene $=100000 \mathrm{~Pa} \times 0.0538 \mathrm{ml} / \mathrm{min} \times 0.000001 /(8.314 \mathrm{kPa}$ $\mathrm{K}^{-1}$

$$
\begin{aligned}
& \left.\mathrm{mol}^{-1} \times 298 \mathrm{~K}\right) \\
= & 0.00000217 \\
= & 0.00000217 \times \\
= & 0.00000434
\end{aligned}
$$

Moles of Carbon $\quad=0.00000217 \times 2$

Total moles of Carbon $\quad=0.00000434 \times$ Reaction time $(\mathrm{min}$.
$=0.00000434 \times 120 \mathrm{~min}$.
$=0.00052$

