

1

Supporting Information

2 **In-situ sulfation of Cu/TiO₂ catalysts for catalytic combustion of dichloromethane**

3 Qingji Ying^a, Yue Liu^{a*}, Yaoyu Zhang^a, and Zhongbiao Wu^{a,b}

4 ^aDepartment of Environmental Engineering, Zhejiang University, 866 Yuhangtang

5 Road, Hangzhou, 310058, P. R. China.

6 ^bZhejiang Provincial Engineering Research Center of Industrial Boiler & Furnace Flue

7 Gas Pollution Control, 866 Yuhangtang Road, Hangzhou, 310058, P. R. China.

8

9

10

11

12

13

14

15

16

17

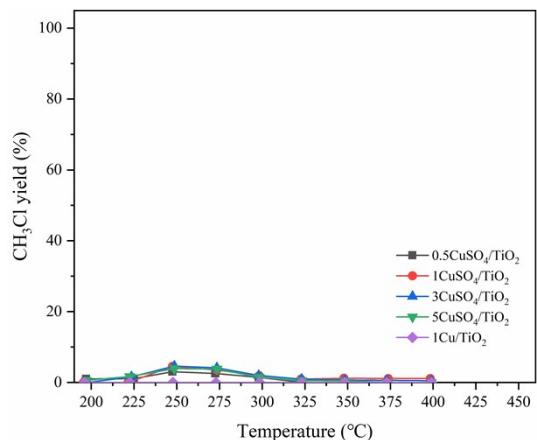
18

19

20

21 ***Corresponding author:**

22 Tel: +86 571 87953088; Fax: +86 87953088; E-mail address: yueliu@zju.edu.cn

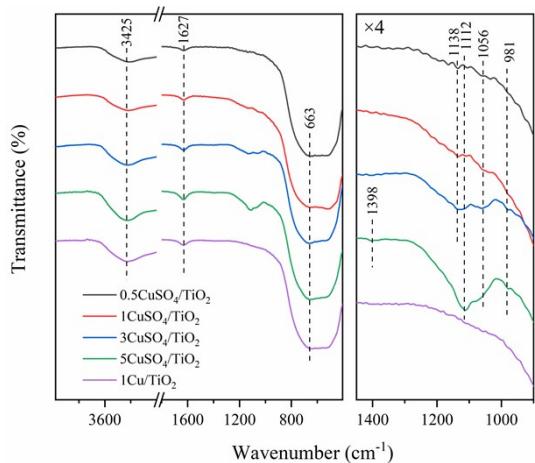


23

24 **Fig. S1.** MCM yield during the catalytic oxidation process. Gas composition: 1000

25 ppm DCM, 10% O₂ and N₂ balance; GHSV = 30,000 mL g⁻¹ h⁻¹.

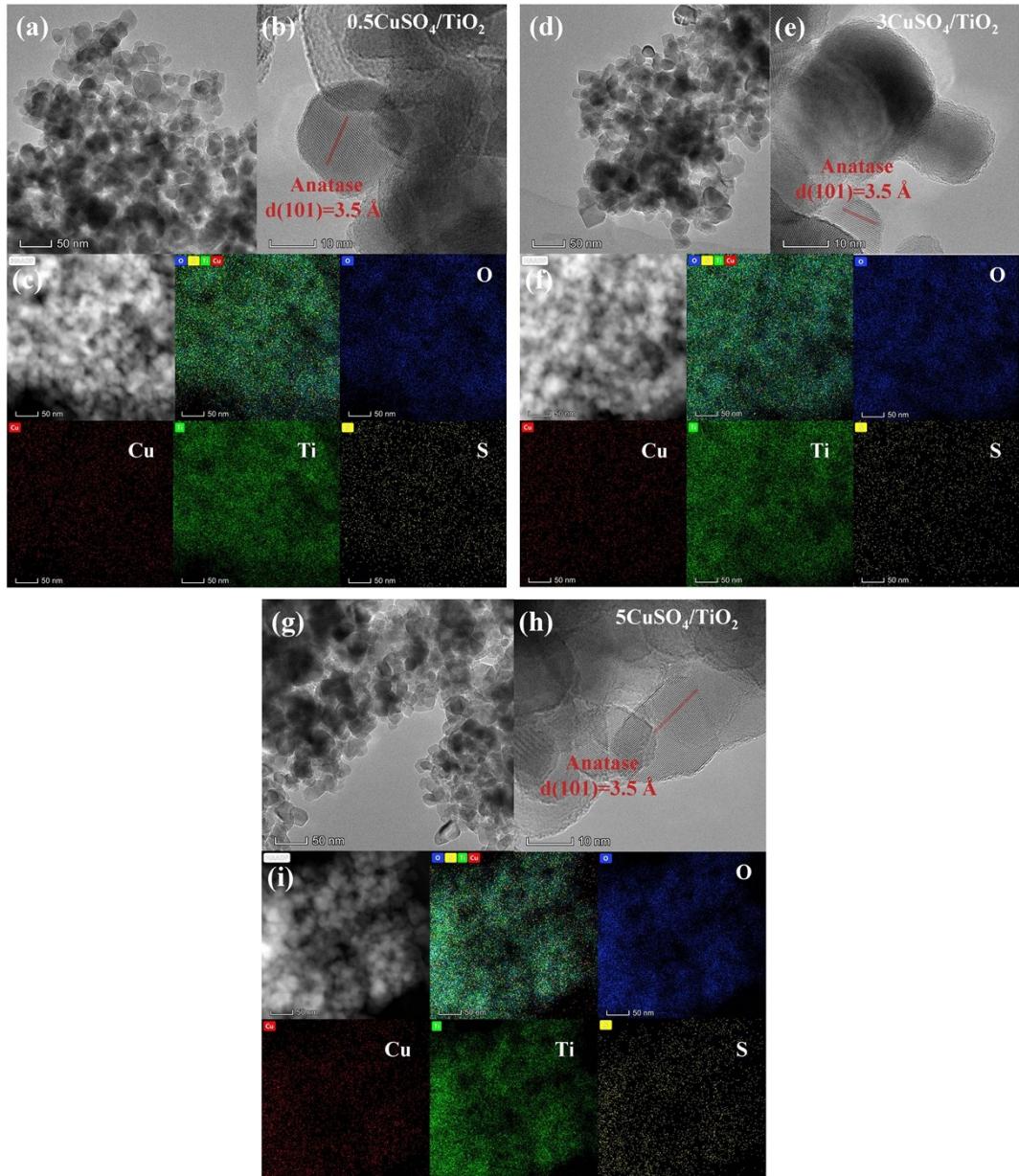
26

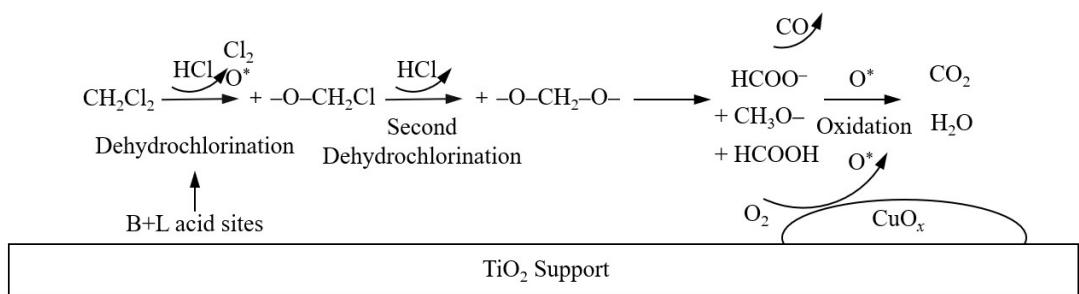


27

28 **Fig. S2.** FT-IR spectra of $1\text{Cu}/\text{TiO}_2$ and $x\text{CuSO}_4/\text{TiO}_2$ samples.

29





35

36 **Scheme S1.** The possible reaction mechanism for the catalytic combustion of DCM

37 over the $\text{CuSO}_4/\text{TiO}_2$ catalyst.

Table S1. Catalytic activity in DCM oxidation over various catalysts.

Entry	Catalyst	Reaction conditions	T ₉₀	Reference
1	1CuSO ₄ /TiO ₂	1000 ppm DCM+10% O ₂ , 30000 ml g _{cat} ⁻¹ h ⁻¹	270 °C	This work
2	Ce/TiO ₂	1000 ppm DCM+10% O ₂ , GHSV = 30000 h ⁻¹	320 °C	26
3	Cr _{0.1} Ti _{0.9}	1000 ppm DCM, 30000 ml g _{cat} ⁻¹ h ⁻¹	320 °C	52
4	SO ₄ ²⁻ /Fe ₂ O ₃ -II	750 ppm DCM+10% O ₂ , GHSV = 30000 h ⁻¹	305 °C	21
5	PO _x -CeO ₂ -0.05	500 ppm DCM, 15000 ml g _{cat} ⁻¹ h ⁻¹	275 °C	19
6	Ru/Ti _{0.6} Sn _{0.4}	1000 ppm DCM+10% O ₂ , 30000 ml g _{cat} ⁻¹ h ⁻¹	295 °C	43
7	Ru/Ti	1000 ppm DCM+10% O ₂ , GHSV = 30000 h ⁻¹	305 °C	53