

Supporting Information

**Production of Renewable Oleo-Furan Surfactants by
Cross-Ketonization of Biomass-Derived Furoic Acid and
Fatty Acids**

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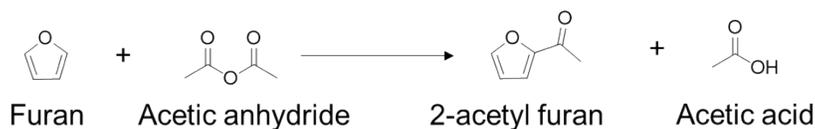
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Thermochemistry calculations

a. Acylation of furan with acetic anhydride

All ΔG calculations were done at the G4 level

Furan:acetic anhydride molar ratio = 1:1



Temp (° C)	ΔG (T) (kcal/mol)	K_{eq}	Furan Conversion (%)
150	-4.65	253.58	94.09
200	-4.58	130.14	91.94
250	-4.50	75.87	89.70

b. Acylation of furan with acetic acid or lauric acid

All ΔG calculations were done with m062-x functional and 6-311G(2df, β) basis set

Furan:acid molar ratio = 1:1

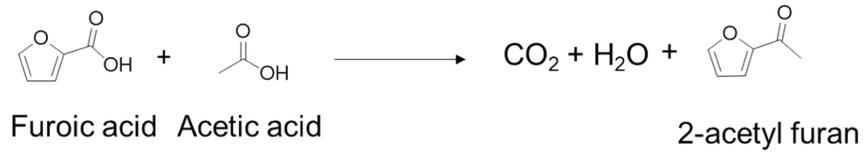


Temp (° C)	ΔG (T) (kcal/mol)		K_{eq}		Furan Conversion (%)	
	Acetic	Lauric	Acetic	Lauric	Acetic	Lauric
150	10.81	11.31	2.59e-6	1.42e-6	0.16	0.12
200	10.97	11.48	8.75e-6	4.92e-6	0.29	0.22
250	11.07	11.65	2.35e-5	1.34e-5	0.48	0.37

c. Cross-ketonization of 2-furoic acid with acetic acid

All ΔG calculations were done at the G4 level

Furoic acid:acetic acid molar ratio = 1:1



Temp (° C)	ΔG (T) (kcal/mol)	K_{eq} (M)	Furoic acid conversion
150	-14.1823	2.11E+07	100
200	-15.8396	2.07E+07	100
250	-17.4912	2.03E+07	100

Calibration

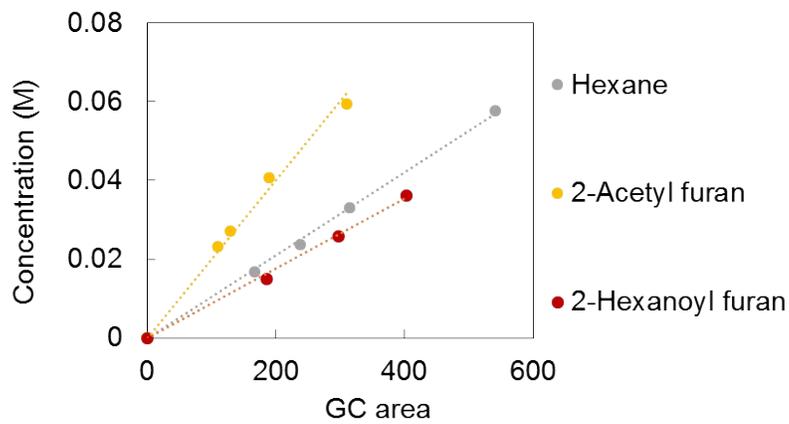
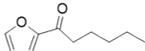


Figure S.1. GC calibration curves for chemical standards (●) hexane, (●) 2-acetyl furan, and (●) 2-hexanoyl furan.

Table S.1. Effective carbon number calculation for 2-dodecanoyl furan.

Compound	Compound structure	Number of C	Calibrated slope	Theoretical slope	Effective carbon
hexane		6	1.05E-04	N/A	6
2-acetyl furan		6	2.00E-04	N/A	3.15
2-hexanoyl furan		10	8.83E-05	8.83E-05	7.15
2-dodecanoyl furan		16	N/A	4.80E-05	13.15

Catalyst screening at 300 °C

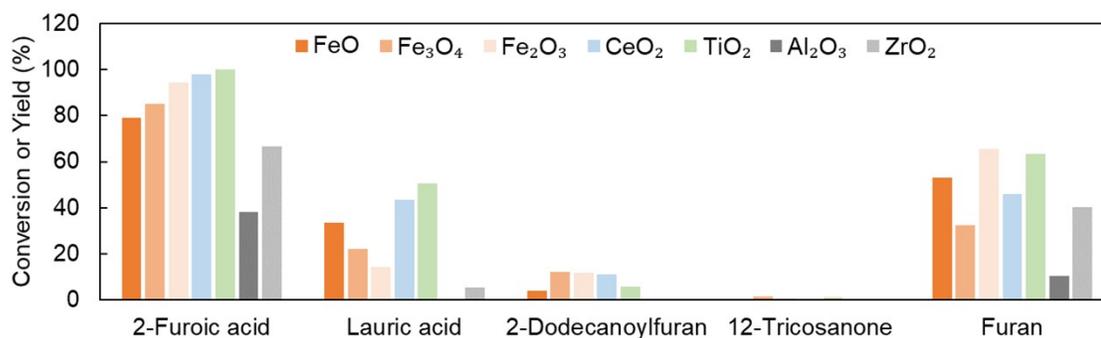


Figure S.2. Performance of various commercial metal oxides in the reaction of 2-furoic acid with lauric acid in n-dodecane. Reaction conditions: 0.05 M lauric acid, 0.25 M 2-furoic acid, 0.2 g catalyst, 300 °C, 90 min, 20 bar N₂, 800 rpm. The pressure at reaction temperature is 40 bar.

Tests at various FA:LA ratios

The activity, at various lauric:acid molar ratios over Fe₃O₄, as a case study catalyst, suggests that the cross-ketonization is favored as higher furoic acid:lauric acid ratios (Figure S.3); therefore a lauric acid:furoic acid molar ratio of 1: 5 was chosen for the initial screening.

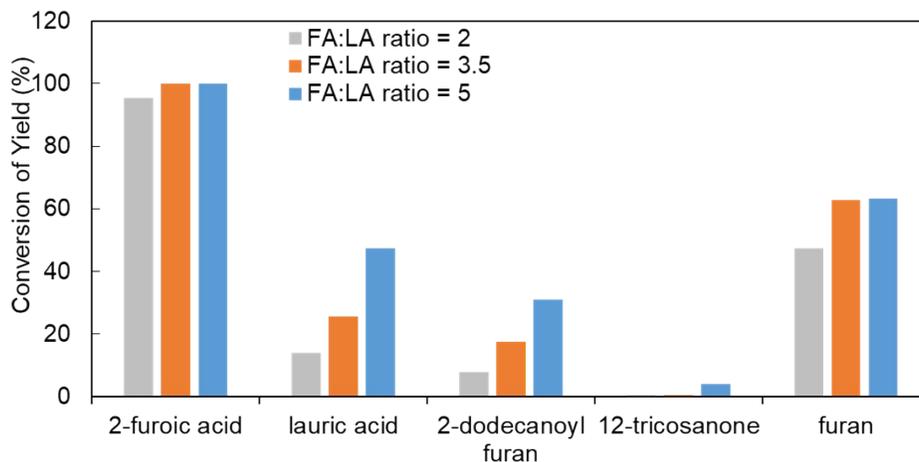


Figure S.3. Acid conversion and product yield at various furoic acid (FA) to lauric acid (LA) molar ratios, with the LA concentration constant at 0.05 M over the Fe_3O_4 catalyst. Reaction conditions: 0.05 M lauric acid, [0.1-0.25] M 2-furoic acid, 0.2 g Fe_3O_4 , 316 °C, 90 min.

External mass transfer tests

The activity (demonstrated for FeO) vs. the stirring speed from 600 to 1000 rpm, shown in Fig. S.4, indicates no external mass transfer limitations.

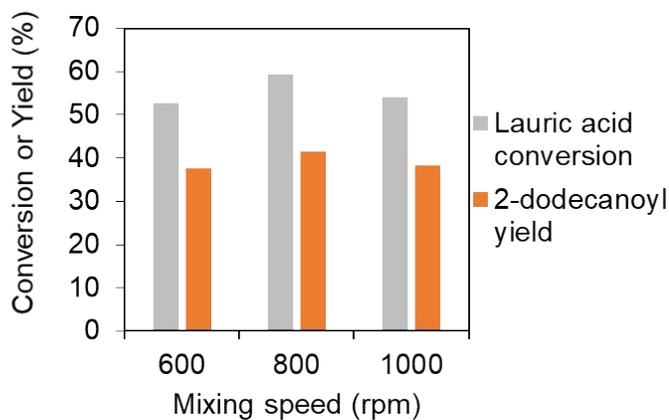


Figure S.4. Lauric acid conversion and 2-dodecanoyl yield at various mixing speeds. Reaction conditions: 0.05 M lauric acid, 0.25 M 2-furoic acid, 0.2 g FeO , 316 °C, 90 min.

Carbon balance analysis

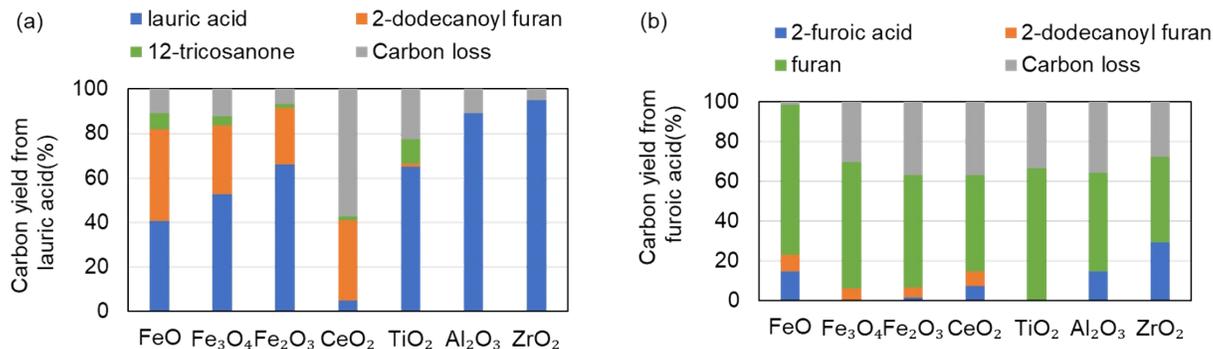


Figure S.5. Carbon balance for lauric acid and furoic acid in the catalyst screening experiments. Reaction conditions: 0.05 M lauric acid, 0.25 M 2-furoic acid, 0.2 g catalyst, 316 °C, 90 min, 20 bar N₂, 800 rpm.

Activity of the homogeneous Fe species

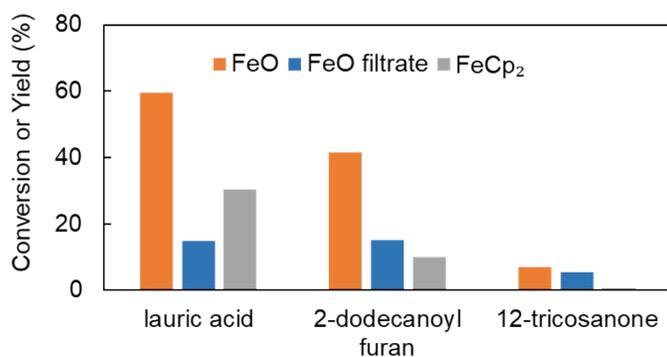


Figure S.6. Comparison of activity for cross-ketonization between FeO, its filtrate after the reaction, and homogeneous ferrocene (FeCp₂). Reaction conditions: 0.05 M lauric acid, 0.25 M 2-furoic acid, 0.2 g FeO or FeCp₂, 316 °C, 90 mins.

Fe leaching test

Table S.2. Fe content in pure dodecane and post-reaction filtrates of iron oxides measured by ICP.

	FeO	Fe ₂ O ₃	Fe ₃ O ₄
Run 1	70 ppm	10 ppm	10 ppm
Run 2	35 ppm	15 ppm	12 ppm
Run 3	94 ppm	14 ppm	9 ppm
Dodecane	10 ppm		

The Fe concentration detected in the post-reaction filtrates of Fe_3O_4 and Fe_2O_3 is comparable to that of pure dodecane, indicating that the Fe species are at the measurement noise level.

Reduction profile of the Fe_xO_y catalysts

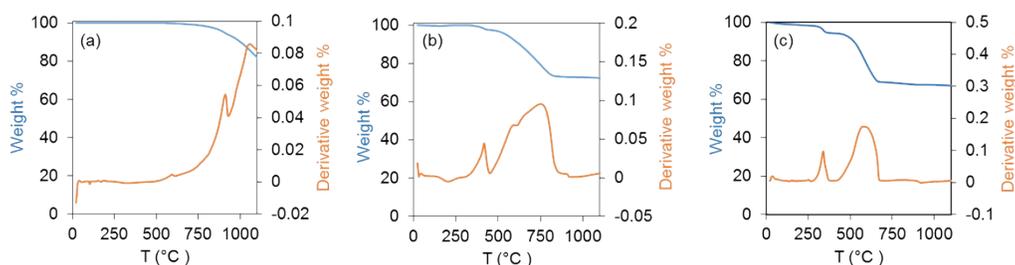


Figure S.7. H_2 TPR-TGA profiles of iron oxides: FeO (a), Fe_3O_4 (b), and Fe_2O_3 (c).

Induction period in catalyst activity

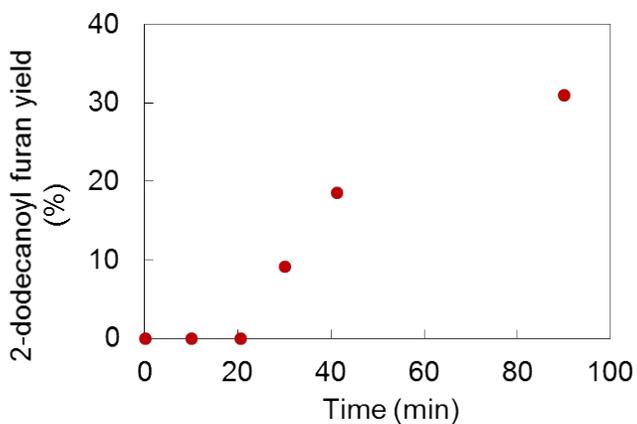


Figure S.8. Time evolution of 2-dodecanoyl furan formation over Fe_3O_4 . Reaction conditions: 0.05 M lauric acid, 0.25 M 2-furoic acid, 0.2 g Fe_3O_4 , 316 °C.

Oxidation state of Fe of the surface of Fe₃O₄

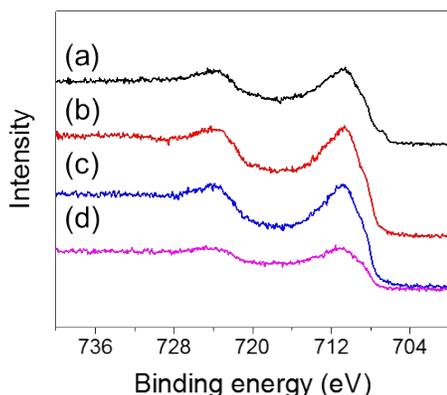


Figure S.9. XPS spectra of Fe 2p_{3/2} of Fe₃O₄ catalyst pretreated in H₂ (a), pure dodecane (b), 0.05 M lauric acid in dodecane (c), and 0.25 M furoic acid in dodecane (d). Reaction conditions: 0.2 g Fe₃O₄, 316 °C, 30 min.

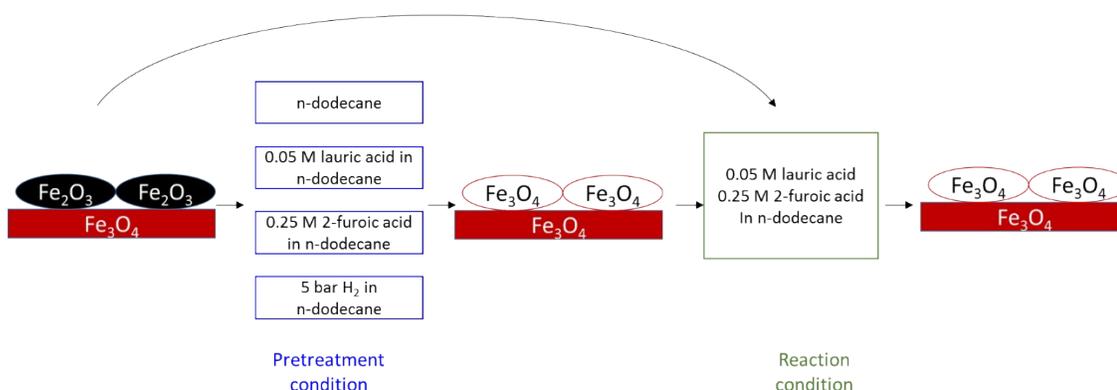


Figure S.10. Iron oxidation state on the surface of Fe₃O₄ before and after pretreatment and reaction as shown by XPS.

Acidity measurement of the fresh oxides

Pyridine Fourier transform infrared (FT-IR) spectroscopy was conducted on an FT-IR Spectrometer (Nicolet 8700) equipped with a MCT detector (128 scans at a spectral resolution of 2 cm⁻¹). The catalyst sample was pressed to a thin pellet before analysis. FeO, Fe₂O₃, Fe₃O₄, or CeO₂ was mixed with SiO₂ at a mass ratio of 1:4 before being pressed. The pellet was heated to 300 °C for 1 h under vacuum of approximately 10⁻⁵ Pa to remove adsorbed water and impurities. The sample was then cooled to 150 °C, at which the background was scanned. Pyridine (>99%, Sigma Aldrich) was adsorbed on the sample for 10 min. The sample was then evacuated under vacuum for 20 min, and the spectra were collected.

The peaks corresponding to Lewis acid sites and Brønsted acid sites are labeled as LS and BS, respectively, in Figure S.11 below.

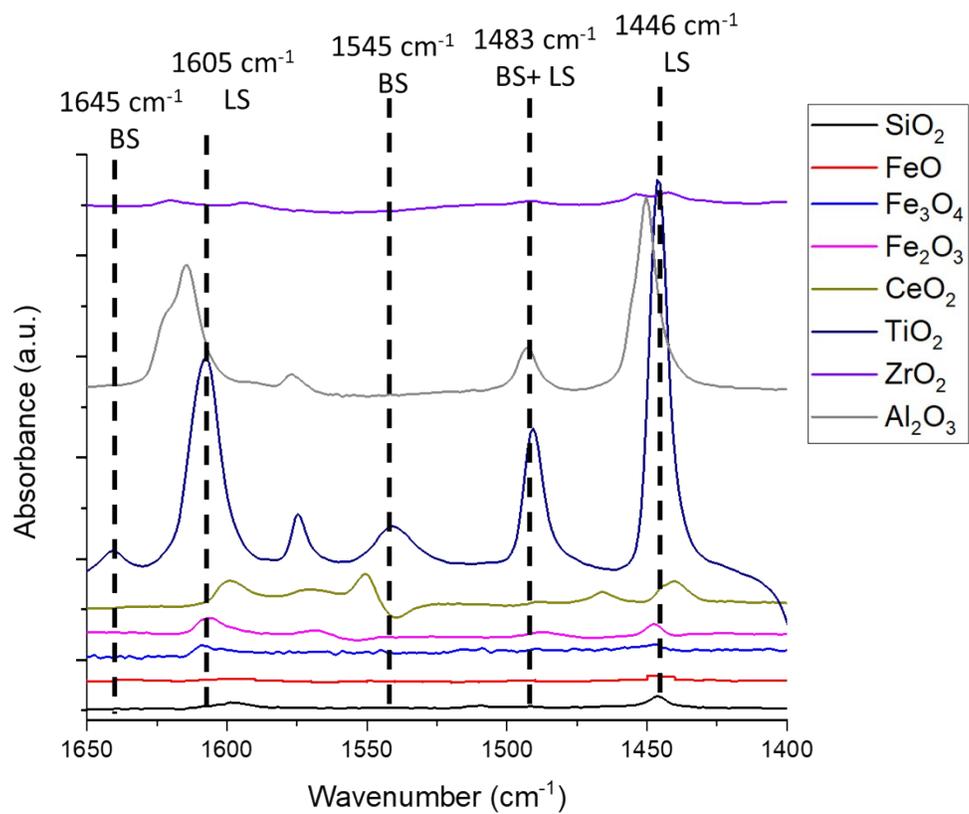


Figure S.11. IR spectra of pyridine adsorption on the fresh metal oxide catalysts.

Isotopic tracing

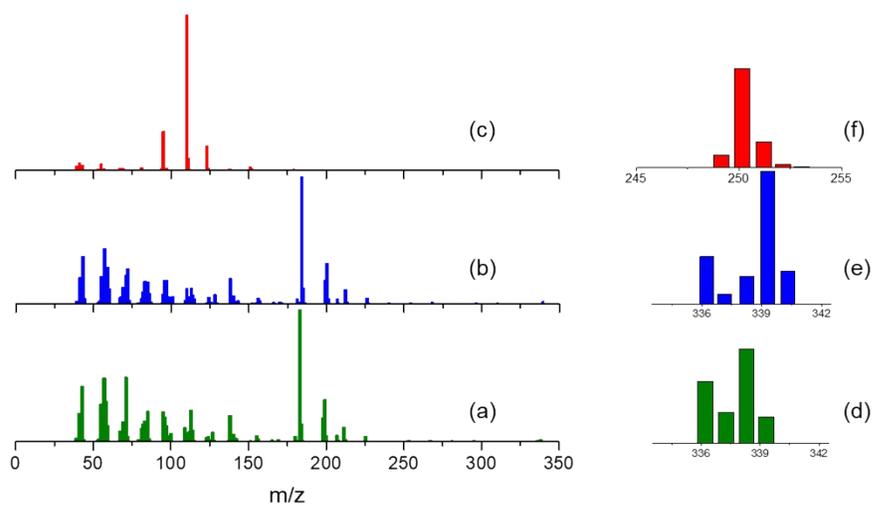


Figure S.12. GCMS spectra of (a) 12-tricosanone from reaction starting with unlabeled lauric, (b) 12-tricosanone from reaction starting with ^{13}C -C1 lauric acid, and (c) 2-dodecanoyl furan from reaction starting with ^{13}C -C1 lauric acid, and their respective zoomed in region in (d), (e), and (f).

N_2 physisorption data of the catalysts

Table S.3. BET surface areas and micropore volumes of fresh oxide catalysts and the spent iron oxides after cross-ketonization reactions.

	Fresh catalyst							Spent catalyst		
	FeO	Fe ₃ O ₄	Fe ₂ O ₃	CeO ₂	TiO ₂	Al ₂ O ₃	ZrO ₂	FeO	Fe ₃ O ₄	Fe ₂ O ₃
BET surface area (m²/g)	0.1	8.8	34.3	75.4	84.5	79.0	104.5	18.7	9.1	17.7
Micropore volume (cm³/g)	2.83e-4	2.18e-2	7.58e-2	0.23	0.27	0.33	0.62	8.43e-2	2.29e-2	8.53e-2