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# **Supplementary Information**

# **1. Experimental Section**

## 1.1 Sample preparation

The carbon nanotubes (CNTs, average outer diameter >50 nm, length 0.5-2 µm) used were multi-walled carbon nanotubes (purchased from Chengdu Organinc Chemicals Co. Ltd.). The Ni/Mo<sub>2</sub>C/CNTs catalysts were synthesized by a simple and environmentally friendly carburization method according to our previous study.<sup>16,18</sup> This method did not require the passivation step for preparing Mo<sub>2</sub>C. The Ni/Mo<sub>2</sub>C/CNTs catalysts with different Ni/Mo molar ratios were prepared in two steps. In the first step, the precursors with theoretical loadings of 11.6 wt% Ni and a molar ratio of Ni/Mo=0.5, 1, 1.5 and 2 were prepared by two-step impregnation method with a Mo-first impregnation sequence. The first impregnation was followed by drying at 70 °C overnight and calcination at 350 °C in Ar for 1 h, and the second impregnation was followed only by drying at 70 °C overnight. In the second step, these samples were heated in a quartz reactor under a flow of Ar (50 ml min<sup>-1</sup>). The temperature was increased linearly at a rate of 10 °C min<sup>-1</sup> from room temperature (RT) to 850 °C, followed by cooling to RT under Ar flow. Then, the products were taken out for further use.

### 1.2 Sample characterization

X-ray diffraction (XRD) was conducted using an X-ray diffractometer (X'Pert Pro MPD) equipped with a Cu K $\alpha$  source. BET surface areas of the samples were measured by a surface area analyzer (NOVA4200). TEM images were acquired using a transmission electron microscope (Philips Tecnal 10). Methane temperature-programmed surface reaction (CH<sub>4</sub>-TPSR) study was performed using a flow of 6%CH<sub>4</sub>/Ar (50 ml min<sup>-1</sup>). Prior to the reaction, the sample was heated to 850 °C under Ar, followed by cooling to RT under Ar, and then was heated under the reactant gas from RT to 850 °C at a rate of 10 °C min<sup>-1</sup>. The evolution of gasphase products during reaction was monitored using gas chromatography (GC).

#### 1.3 Sample performance tests

Catalytic activities of Ni/Mo<sub>2</sub>C/CNTs catalysts for DRM were evaluated in a micro-reactor with an inner diameter of 10 mm at atmospheric pressure. Prior to the reaction, the sample was preheated with Ar at 850 °C for 30 min. Then CH<sub>4</sub> and CO<sub>2</sub> mixture with a molar ratio of 1:1 was allowed to pass through the catalyst (60-80 mesh) at a flow rate of 40 ml min<sup>-1</sup> (GHSV=60000 cm<sup>3</sup> g<sup>-1</sup> h<sup>-1</sup>). The exit gas stream from the reactor passed through a cold trap to remove water. The flow rates were measured with a soap bubble flow meter. The gas-phase products were analyzed by on-line gas chromatography (GC) equipped with a thermal conductivity detector and a TDX-01 (60-80 mesh) packed column (300 mm×2 mm i.d.). The external standard method was used to quantitative analysis. Linear relationship was obtained between values of peak area and volume concentration of gases in the range of 0.1-100 vol.%. The molar fraction for the products and reactants was determined on the basis of peak area-volume concentration curve and taken into account in the calculation of the conversion and product distribution. The conversions of CH<sub>4</sub> and CO<sub>2</sub>, and selectivity

of H<sub>2</sub> were defined respectively as follows: CH<sub>4</sub> conversion (%)= (moles of CH<sub>4</sub> converted)/(moles of CH<sub>4</sub> introduced); CO<sub>2</sub> conversion (%)= (moles of CO<sub>2</sub> converted)/(moles of CO<sub>2</sub> introduced); H<sub>2</sub> selectivity (%)= (moles of H<sub>2</sub> produced)/(2× moles of CH<sub>4</sub> converted). When the test was over, the used sample was cooled to RT under Ar flow. Then, the used samples were taken out for further characterization.

## 2. Results



Fig. S1 XRD patterns of the sample contained MoNi<sub>4</sub> phase before and after CH<sub>4</sub> carburization.

Table S1 Comparison of DRM catalytic activity and stability for as-prepared and literature

Catalyst	Ni:Mo	Temperature	GHSV	CH <sub>4</sub> conversion	Catalytic	Ref.
	ratio	(°C)	(cm <sup>3</sup> g <sup>-1</sup> h <sup>-1</sup> )	rate <sup><math>b</math></sup> (mol g <sup>-1</sup> h <sup>-1</sup> )	stability (h)	
Ni/Mo <sub>2</sub> C/CNTs	1:1	850	60000	0.96	36	This work
Ni/Mo <sub>2</sub> C/CNTs	1:2	850	60000	0.98	22	This work
Ni/Mo <sub>2</sub> C	1:2	850	18000	0.32	13	19
Ni/Mo <sub>2</sub> C	1:5	850	3800 <sup>a</sup>	0.07	2	22
Ni/Mo <sub>2</sub> C	1:2	800	12000	0.22	23	27
Ni/Mo <sub>2</sub> C	1:1	800	12000	0.21	4	27
Ni/Mo <sub>2</sub> C/La <sub>2</sub> O <sub>3</sub>	1:2	800	12000	0.13	50	30
Ni/Mo <sub>2</sub> C/Al <sub>2</sub> O <sub>3</sub>	1.6:1	700	20000 <sup>a</sup>	0.04	5	7
Ni/Mo <sub>2</sub> C/SBA-15	1:4	800	8000	0.17	180	24

reported Ni/Mo<sub>2</sub>C catalysts.

<sup>*a*</sup> Unit is h<sup>-1</sup>

 $^{\it b}$  Calculated by the  $\rm CH_4$  conversion at the reaction time of 1 h.