

Supplementary Data

Bioinspired Succinyl- β -cyclodextrin Membranes for Enhanced Uranium Extraction and Reclamation

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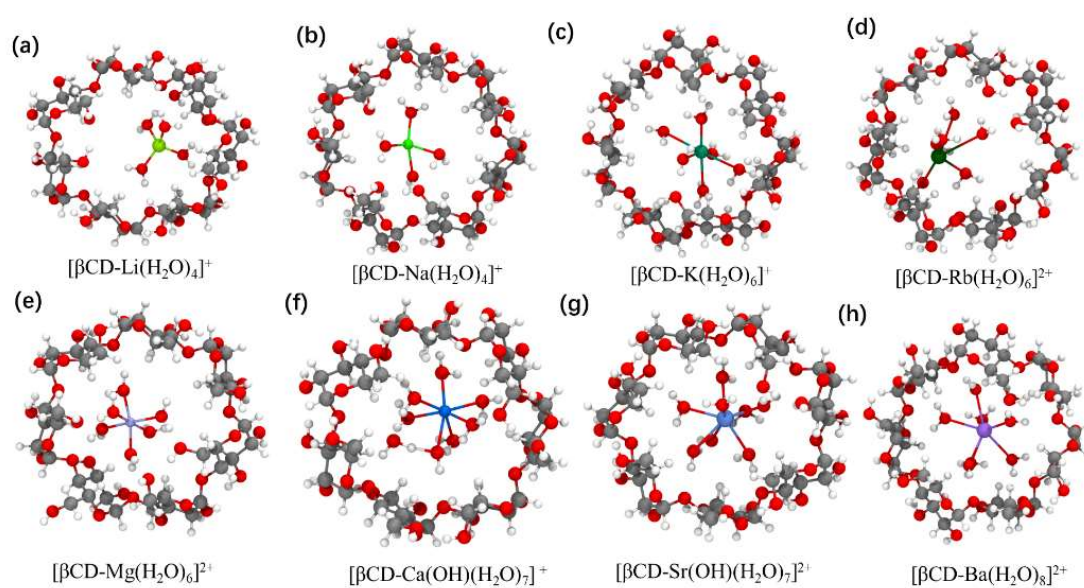


Fig. S1 Optimized structures of β CD-hydrated metal ions complexes.

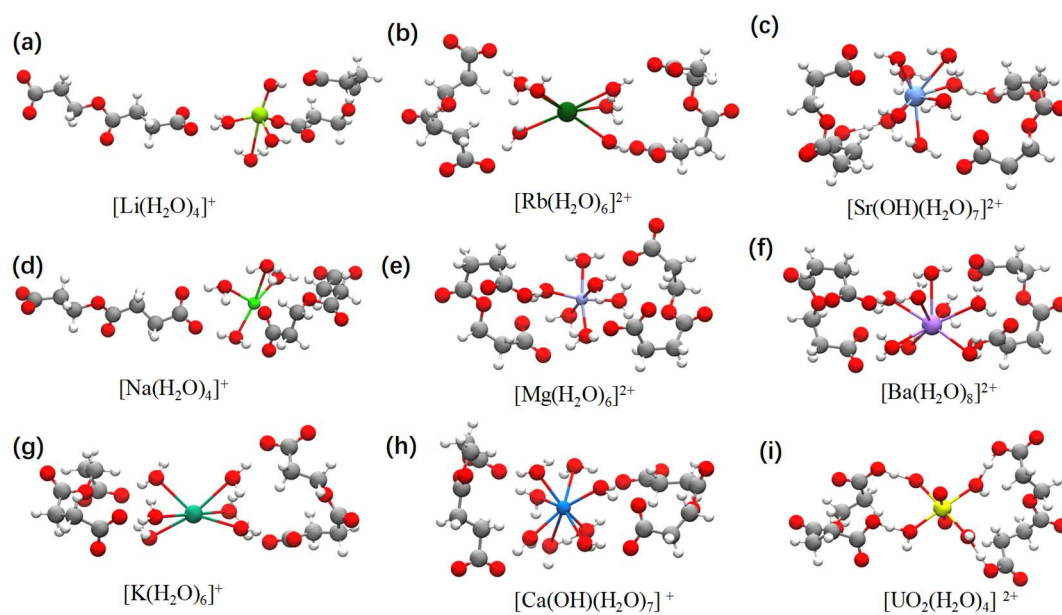


Fig. S2 Optimized structures of succinate, 1-(2-carboxyethyl) ester-hydrated metal ions complexes

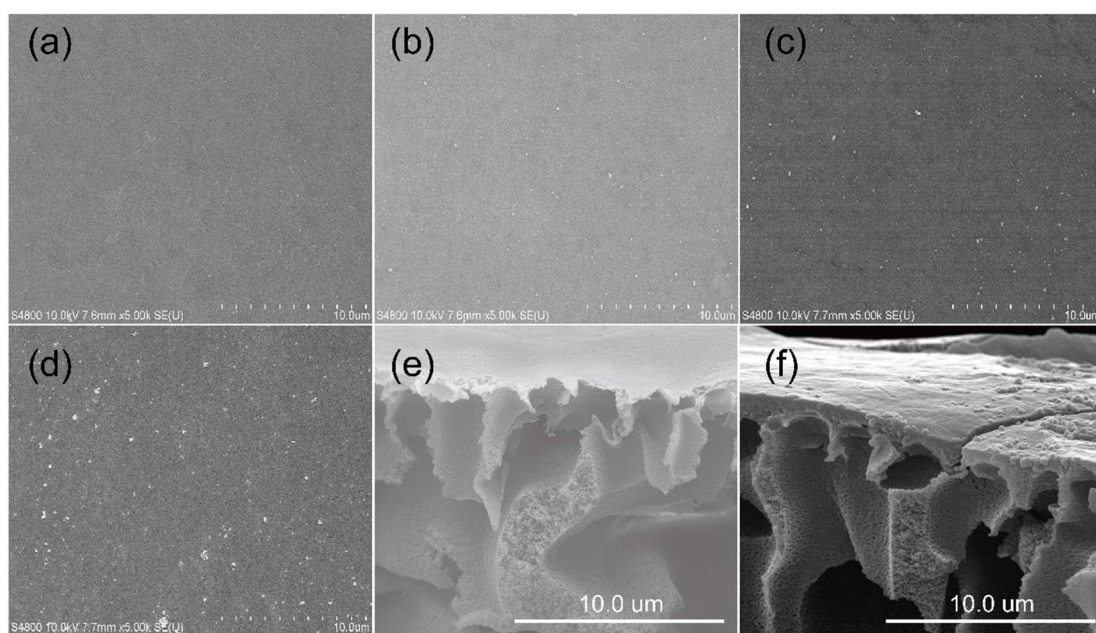


Fig. S3 SEM of (a) DA-PAN, (b) S β CDM-1, (c) S β CDM-2, (d) S β CDM-5, MAG $\times 10000$. (f) cross-section of (e) PAN and (f) S β CDM.



Fig. S4 Marine field study site location at Qingdao on the local map of the Yellow Sea in China. Image was acquired from Maps of World.

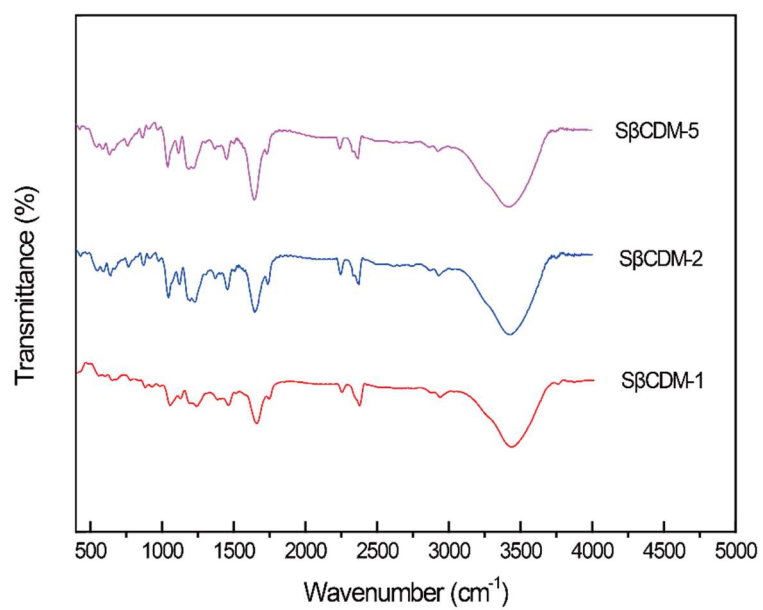


Fig. S5 XPS spectra of SβCDM-1, SβCDM-2 and SβCDM-5.

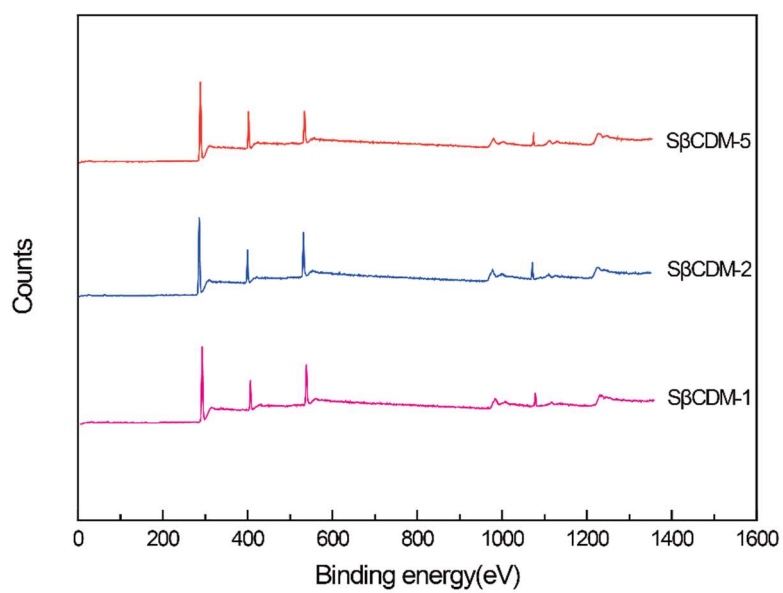


Fig. S6 FT-IR spectra of SβCDM-1, SβCDM-2 and SβCDM-5.

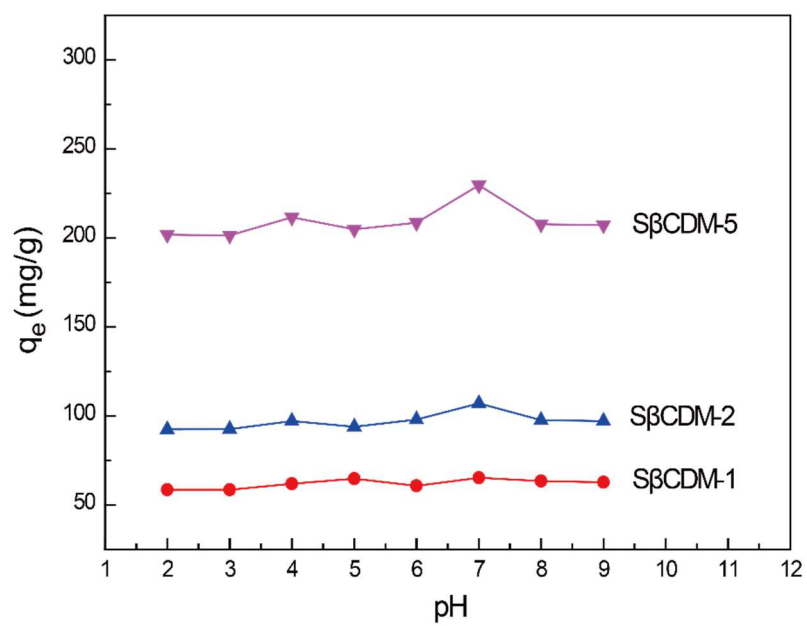


Fig. S7 Effect of pH on U(VI) uptakes of SβCDM-1, SβCDM-2 and SβCDM-5.

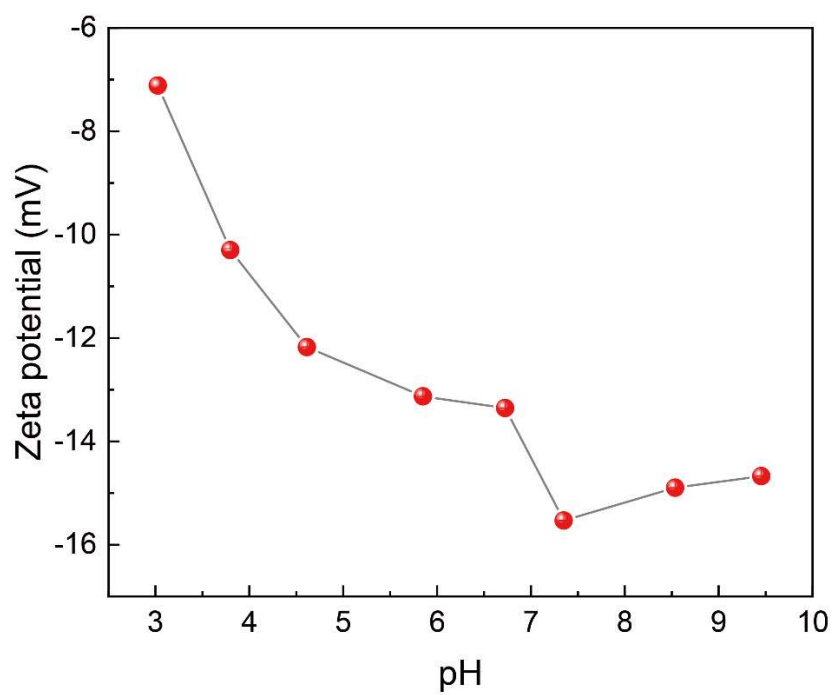


Fig. S8 Zeta potential of SβCDM at different pH.

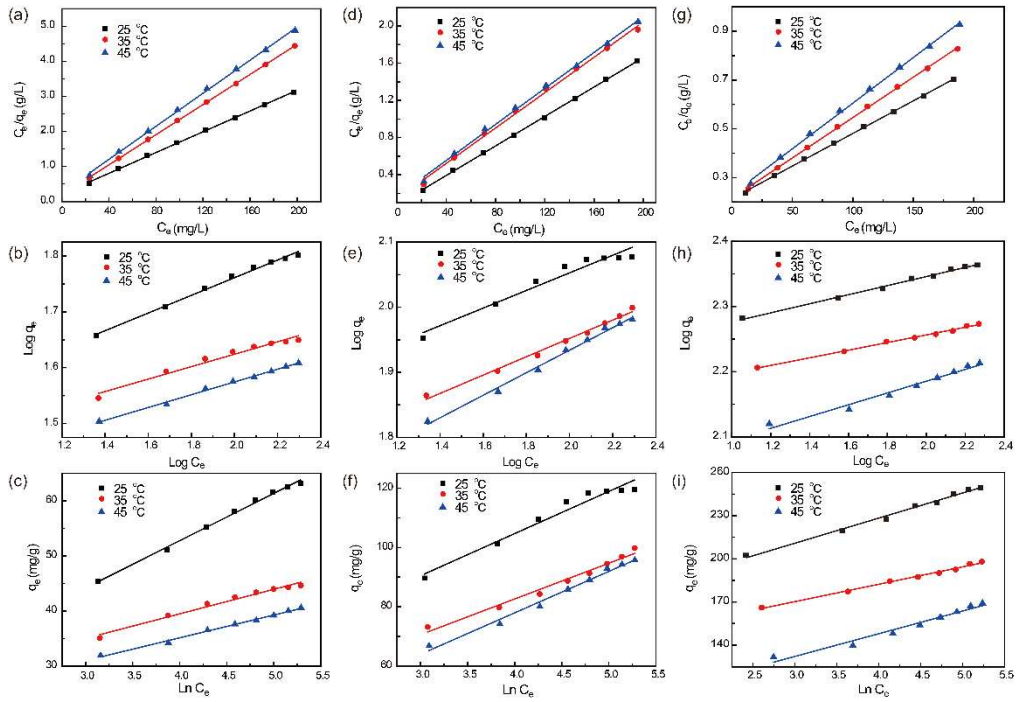


Fig. S9 (a) Langmuir isotherms, (b) Freundlich isotherms and (c) Temkin isotherms for U(VI) onto SβCDM-1 at 25°C, 35°C and 45°C. (d) Langmuir isotherms, (e) Freundlich isotherms and (f) Temkin isotherms for U(VI) onto SβCDM-2 at 25°C, 35°C and 45°C. (g) Langmuir isotherms, (h) Freundlich isotherms and (i) Temkin isotherms for U(VI) onto SβCDM-5 at 25°C, 35°C and 45°C.

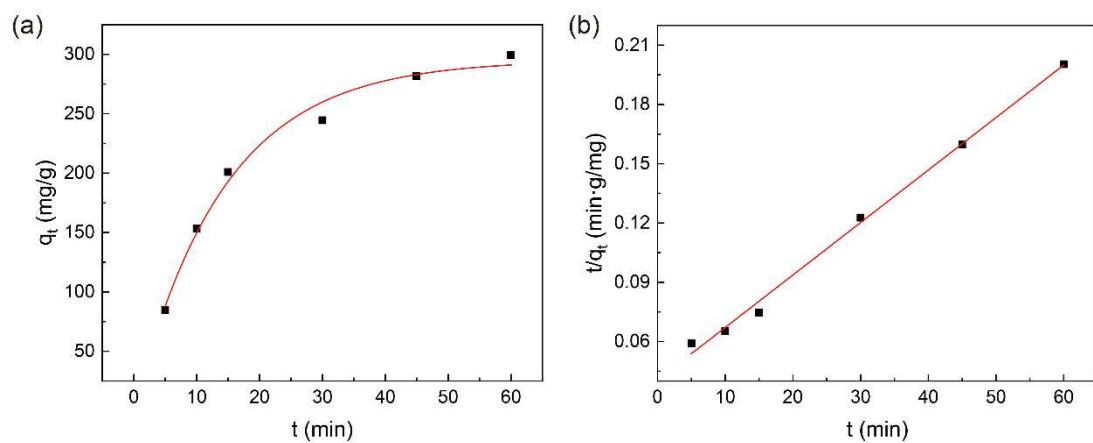


Fig. S10 (a) Pseudo-first-order kinetic model and (b) pseudo-second-order kinetic model fit for the adsorption of U(VI) onto S β CDM.

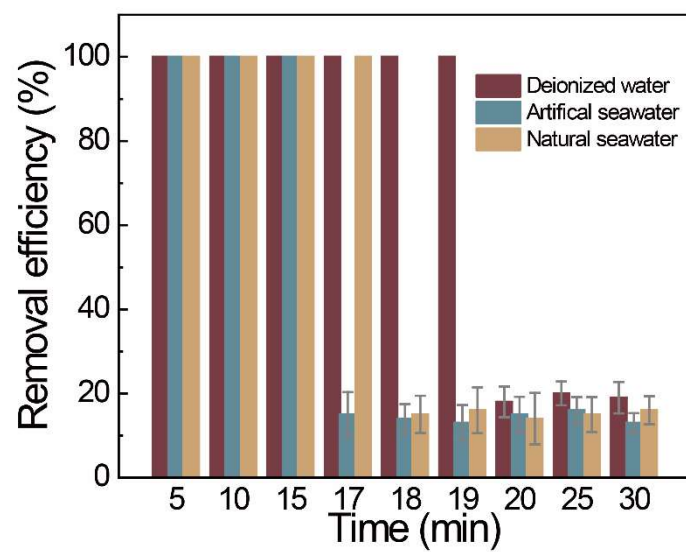


Fig. S11 Removal efficiency of U(VI) at different times in a dynamic system in deionized water, artificial seawater and natural seawater.

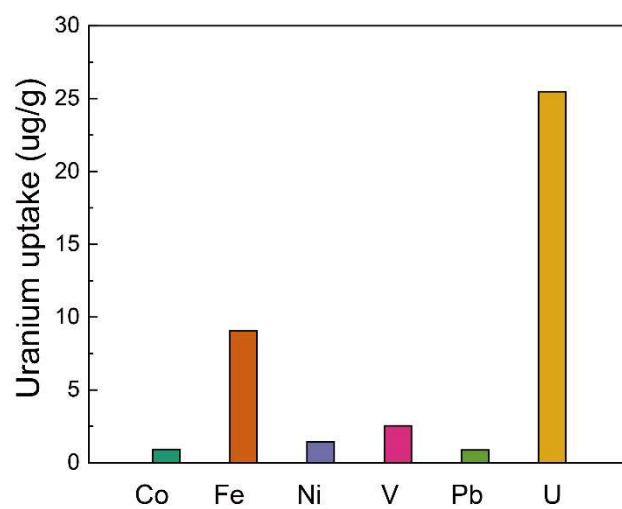


Fig. S12 Average adsorption capacities (ug/g) of Co, Fe, Ni, V, Pb and U for S β CDM during d with natural seawater for 8 days.

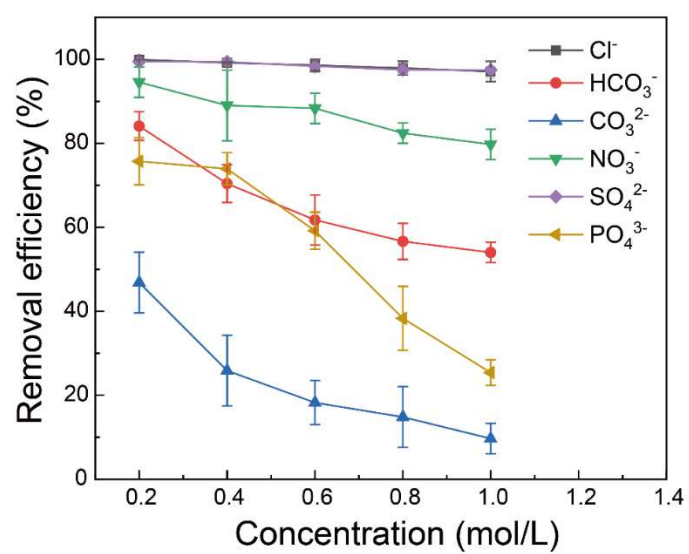


Fig. S13 Effect of different anions and their concentrations on removal efficiency of U(VI) in 100 mg/L uranium solution.

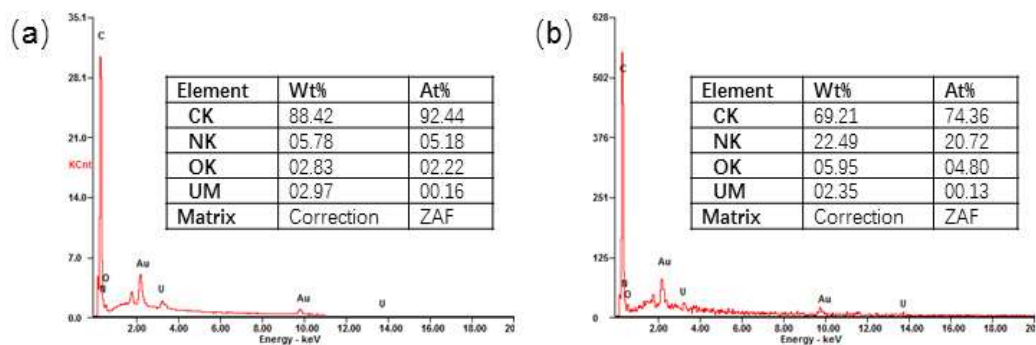


Fig. S14 EDS data of S β CDM and S β CDM-R10 adsorbed U(VI).

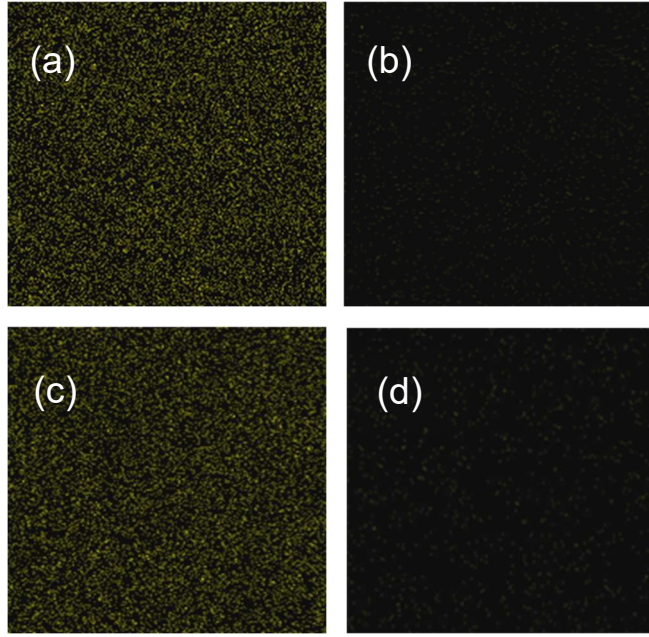


Fig. S15 U distribution mapping of (a) $S\beta$ CDM-U, (b) desorbed $S\beta$ CDM-U, (g) $S\beta$ CDM-R10 with U and (h) desorbed $S\beta$ CDM-R10.

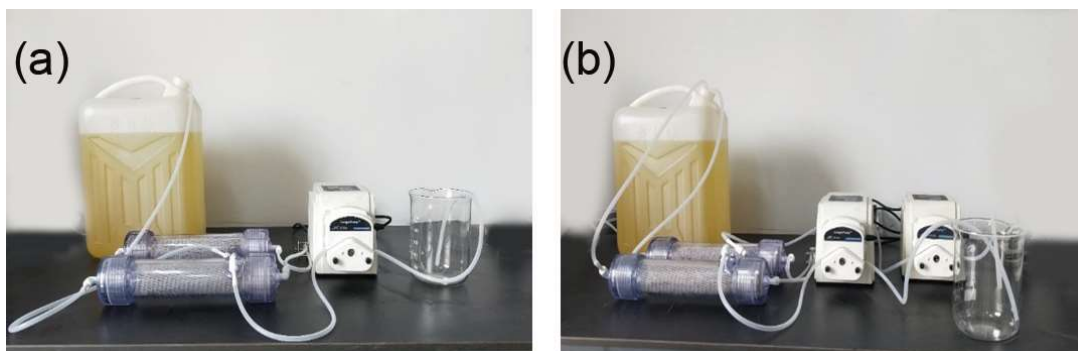


Fig. S16 (a) Series connection and (b) parallel connections of hollow fiber S β CDM modules.

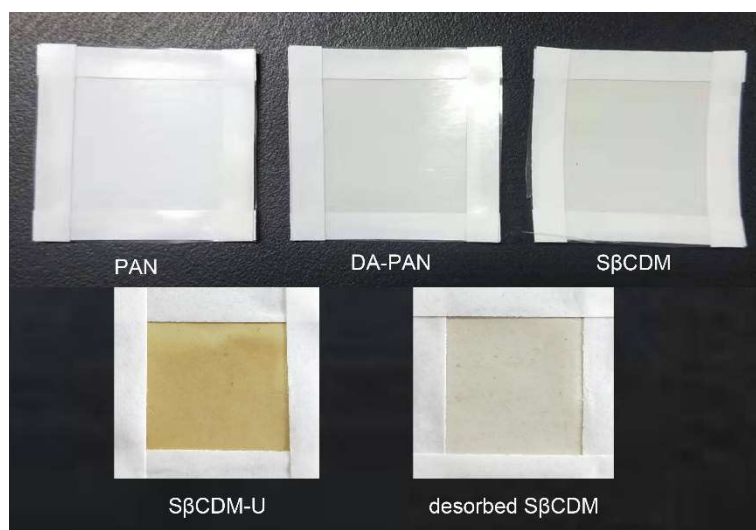


Fig. S17 Photos of different membranes.

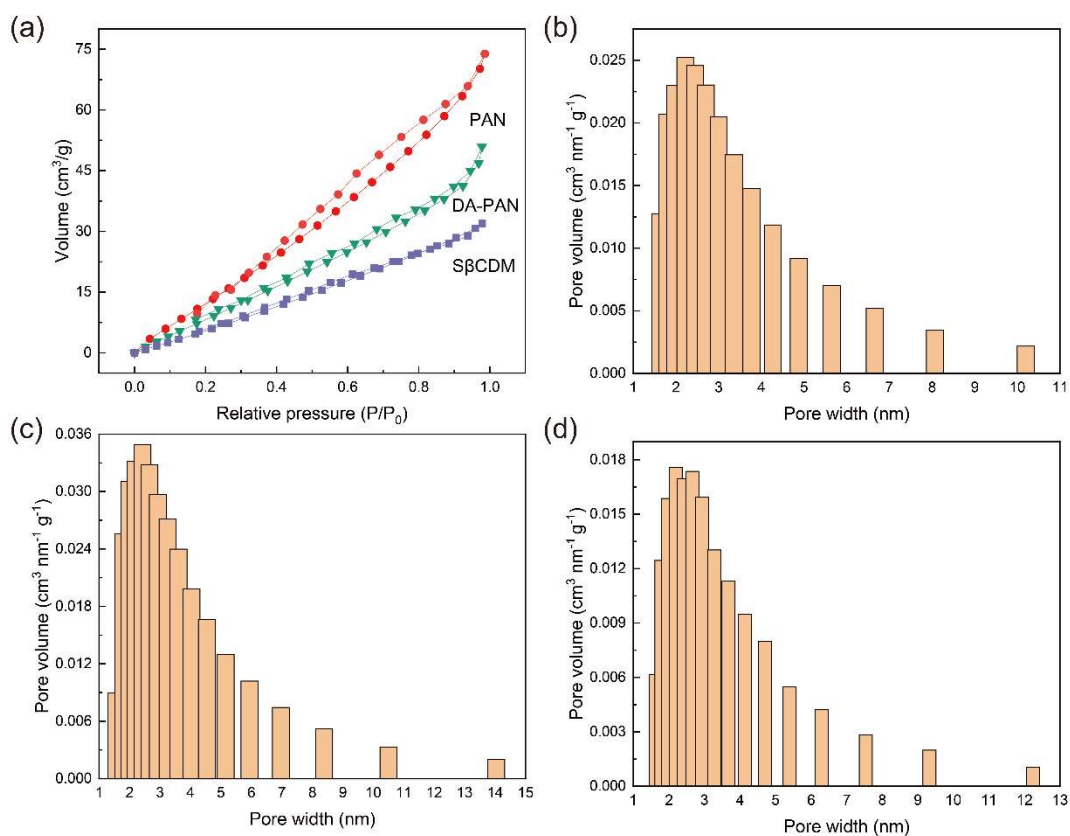


Fig. S18 (a) The N_2 adsorption/desorption isotherms. Pore size distributions of (b) PAN, (c) DA-PAN and (d) S β CDM.

Table S1. Roughness of S β CDMs.

membranes	Rq (nm)
S β CDM-1	14.9
S β CDM-2	15.5
S β CDM-5	16.8

Table S2. Adsorption isotherm parameters obtained from the Langmuir, Freundlich and Temkin models in the adsorption of U(VI) onto S β CDMs.

	Isotherms	Parameters	Temperature		
			25 °C	35 °C	45 °C
SβCDM	Langmuir	q_{max} (mg/g)	378.8	304.9	270.3
		K_L (g/mg)	0.1277	0.1572	0.0919
		R^2	0.9996	0.9995	0.9986
	Freundlich	$1/n$	0.08986	0.07154	0.1064
		$K_f((\text{mg/g}) \text{ L/mg}^{1/n})$	10.59	10.07	8.735
		R^2	0.9926	0.9929	0.9866
	Temkin	a	224.6	212.0	146.3
		b	23.29	16.11	21.06
		R^2	0.9899	0.9930	0.9625
SβCDM-5	Langmuir	q_{max} (mg/g)	227.3	215.4	182.0
		K_L (g/mg)	0.0089	0.0067	0.0068
		R^2	0.9980	0.9958	0.9947
	Freundlich	$K_f((\text{mg/g}) \text{ L/mg}^{1/n})$	2.205	2.049	1.931
		$1/n$	0.1335	0.1398	0.1423
		R^2	0.9808	0.9842	0.9710
	Temkin	a	98.08	78.92	67.20
		b	28.65	26.27	23.79
		R^2	0.9757	0.9691	0.9517
SβCDM-2	Langmuir	q_{max} (mg/g)	114.3	91.25	88.86
		K_L (g/mg)	0.0107	0.0071	0.0060
		R^2	0.9995	0.9965	0.9517
	Freundlich	$1/n$	0.1351	0.1407	0.1729
		$K_f((\text{mg/g}) \text{ L/mg}^{1/n})$	1.616	1.445	1.331
		R^2	0.9463	0.9898	0.9923
	Temkin	a	47.81	34.45	22.06

		b	14.22	12.05	13.97
		R^2	0.9804	0.9905	0.9940
SβCDM-1	Langmuir	q_{max} (mg/g)	61.04	41.37	37.94
		K_L (g/mg)	0.0071	0.0119	0.0093
		R^2	0.9992	0.9999	0.9989
	Freundlich	K_f ((mg/g) L/mg ^{1/n})	1.153	1.104	1.044
		$1/n$	0.1583	0.1115	0.1145
		R^2	0.9917	0.9656	0.9952
	Temkin	a	18.41	21.65	18.59
		b	8.591	4.459	4.134
		R^2	0.9952	0.9769	0.9935

Table S3. Porous structure parameters of PAN, DA-PAN and S β CDM

Adsorbent	S_{BET} (m²/g)	V_{tot} (cm³/g)	D_p (nm)
PAN	88.094	0.114	5.187
DA-PAN	66.292	0.079	4.748
S β CDM	51.979	0.049	3.804

S_{BET} : BET surface area; V_{tot} : Total pore volume; D_p : Average pore size.

Preparation of artificial seawater

Artificial seawater was prepared according to the Mocledon artificial seawater [1], the constituent parts and their concentration were shown in Table S4.

Table S4. Constituent parts in Mocledon artificial seawater.

Constituent parts	Concentration (g/L)
NaCl	26.73
MgCl ₂	2.26
MgSO ₄	3.25
CaCl ₂	1.15
NaHCO ₃	0.20
KCl	0.72
NaBr	0.0580
H ₃ BO ₃	0.0580
Na ₂ SiO ₃	0.0035
KAl(SO ₄) ₂ ·12H ₂ O	0.0230
LiNO ₃	0.0013
NH ₄ H ₂ PO ₄	0.0040

Table S5. Elements in natural seawater.

Elements	Concentration (mg/L)
K	7.4×10^2
Na	8.2×10^3
Ca	3.4×10^2
Mg	1.0×10^2
Fe	6.4×10^{-3}
Ni	1.8×10^{-2}
Co	8.4×10^{-4}
V	2.8×10^{-3}
U	3.5×10^{-3}

Table S6. EXAFS Parameters of S β CDM-U at k₃-Weighted L₃ Edge.

	shell	CN	R (Å)	σ^2	ΔE_0 (eV)	R-factor
SβCDM-U	U-O _{ax}	1.9	1.78	0.002	7.38	0.031
	U-O _{eq}	4.8	2.31	0.011		

Table S7. Calculated Gibbs free energies for complex formation in a water environment.

Metal cation	Aqua complex	Calculated Volum ($\text{\AA}^3$)
Li^+	$[\text{Li}(\text{H}_2\text{O})_4]^+$	104.5
Na^+	$[\text{Na}(\text{H}_2\text{O})_4]^+$	112.1
K^+	$[\text{K}(\text{H}_2\text{O})_6]^+$	162.8
Rb^+	$[\text{Rb}(\text{H}_2\text{O})_6]^{2+}$	168.7
Mg^{2+}	$[\text{Mg}(\text{H}_2\text{O})_6]^{2+}$	144.2
Ca^{2+}	$[\text{Ca}(\text{OH})(\text{H}_2\text{O})_7]^+$	196.5
Sr^{2+}	$[\text{Sr}(\text{OH})(\text{H}_2\text{O})_7]^+$	204.0
Ba^{2+}	$[\text{Ba}(\text{H}_2\text{O})_8]^{2+}$	218.7
UO_2^{2+}	$[\text{UO}_2(\text{H}_2\text{O})_4]^{2+}$	147.0

Table S8. The composition of hydrated metal ions in aqueous solution.

Aqua complex	ΔG^{Aqua} (Kcal/mol)
SCE-[Li(H ₂ O) ₄] ⁺	-55.33
SCE-[Na(H ₂ O) ₄] ⁺	-55.58
SCE-[K(H ₂ O) ₆] ⁺	-47.35
SCE-[Rb(H ₂ O) ₆] ²⁺	-42.37
SCE-[Mg(H ₂ O) ₆] ²⁺	-78.56
SCE-[Ca(OH)(H ₂ O) ₇] ⁺	-54.40
SCE-[Sr(OH)(H ₂ O) ₇] ⁺	-60.31
SCE-[Ba(H ₂ O) ₈] ²⁺	-75.99
SCE-[UO ₂ (H ₂ O) ₄] ²⁺	-265.00

Table S9. Adsorption operation conditions of reported studies on adsorbents for U(VI) in Fig. 11d.

Adsorbents	Operation conditions
GONRs/CTS	$M = 15 \text{ mg}$, $\text{pH} = 5.0$, $C_0 = 50 \text{ mg}\cdot\text{L}^{-1}$, $t = 24 \text{ h}$.
OMS-2 nanowires	$C[\text{U(VI)/Eu(III)}]_{\text{initial}} = 20 \text{ mg}\cdot\text{L}^{-1}$, $I = 0.01 \text{ M KNO}_3$ and $T = 293 \text{ K}$.
CS-CNTs	$C_0 = 15\text{-}100 \text{ mg L}^{-1}$; SD (sorbent dosage) = 0.5 g L^{-1} ; $\text{pH} = 4.0$; $T = 298 \text{ K}$
CS-Fe	$T = 298 \text{ K}$, $C_{\text{U(VI), initial}} = 30 \text{ mg/L}$, Sorbent dosage (SD) = 0.4 g/L
PCTM@PDA@ZIF-8	$20 \text{ mg}\cdot\text{L}^{-1}$, $[\text{m/V}] = 0.075 \text{ g/L}$

Reference

- [1] H. Yue, C. Ling, T. Yang, X. Chen, Y. Chen, H. Deng, Q. Wu, J. Chen, G.-Q. Chen, A seawater-based open and continuous process for polyhydroxyalkanoates production by recombinant *Halomonas campaniensis* LS21 grown in mixed substrates, *Biotechnology for Biofuels*, 7 (2014).