# **Supporting Information**

## Platform Selection of Engineered Nanomaterials for Water Decontamination Applications

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#### Search terms for Figure 1:

NM:

(TITLE-ABS-KEY (nanomaterial OR nano AND material OR nanoparticle OR nano AND particle ) AND TITLE-ABS-KEY (water AND remediation OR decontamination OR water AND treatment OR water OR decontamination ))

#### NM@S:

(TITLE-ABS-KEY(nanomaterial OR nano material OR nanoparticle OR nano particle) AND TITLE-ABS-KEY(Water Remediation OR decontamination OR water treatment OR water OR decontamination)AND TITLE-ABS-KEY(embedded OR infused OR incorporated OR affixed OR impregnated OR immobilized OR modified OR functionalized)) **Table S1.** Literature used for evaluation of the efficiency criterion for selected supports for metal oxide nanoadsorbents. The table summarizes the calculations and assumptions taken into account when adsorption performance of the supported nanomaterial (NM@S) was normalized to the performance of the nanomaterial in suspended form (NM).

| Article                              | Platform group     | Nanoadsorbent                    | Adsorbate | Nanoadsorbent  | Nanoadsorbent performance on                         | NM@S/NM | Assumptions                                      |
|--------------------------------------|--------------------|----------------------------------|-----------|--|--|---------|--|
|                                      |                    |                                  |           | performance (NIVI)                                     | substrate (NM@S)                                     | 0.000   |  |
| O. Inirunavukkarasu, Arsenic         | Natural media      | α-геоон                          | AS (III)  | 23 mg/g FeOOH -  | 41.1ug/gNM@S/45mgFe/gNM@                             | 0.026   | Iron oxide content 45                            |
| removal from drinking water using    | Bead - Sand        |                                  |           |  | 5*65Fe/100FeO(OH)=0.59mgAs/g                         |         | mg/g (4.5%)                                      |
| Iron oxide-coated sand, 2003,        |                    |                                  |           |  | FeOOH  | 0.700   | pH 7.6   |
| Water, Air, and Soil Pollution       |                    |                                  | As(V)     | 1.14 mg/g FeOOH <sup>3</sup>                           | 42.6ug/gNM@S/45mgFe/gNM@                             | 0.539   | phase: combination of                            |
|                                      |                    |                                  |           |  | S*65Fe/100FeO(OH)=0.615mgAs/                         |         | goethite and nematite                            |
|                                      |                    |                                  |           |  |  | 0.420   |  |
| S.Lee, Iron oxide nano-particles-    | Natural media      | Iron oxide                       | Cd(II)    | 7.4 mg/g Iron oxide 5                                  | 0.5282/5./*0.65*1000=60.23                           | 8.139   | pH 4 and not 5 as in                             |
| immobilized-sand material in the     | Bead - Sand        |                                  |           |  | mg/g Iron oxide                                      |         | the NM@S paper                                   |
| treatment of Cu(II), Cd(II) and      |                    |                                  |           |  |  |         |  |
| Pb(II) contaminated waste waters,    |                    |                                  | Pb(II)    | 22.83 mg/g Iron oxide                                  | 2.0877/5.7*0.65*1000=238.07                          | 10.43   |  |
| 2012, Chemical Engineering           |                    |                                  |           | 5  | mg/g Iron oxide                                      |         |  |
| Journal <sup>4</sup>                 |                    |                                  |           |  |  |         |  |
| S. Kundu, Adsorptive removal of      | Natural media -    | Fe <sub>3</sub> O <sub>4</sub>   | As(III)   | 2.63 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>3</sup>  | 0.69*0.2353=0.16 mg/g Fe <sub>3</sub> O <sub>4</sub> | 0.061   |  |
| As(III) from aqueous solution using  | Cement             |                                  |           |  |  |         |  |
| iron oxide coated cement (IOCC):     |                    |                                  |           |  |  |         |  |
| Evaluation of kinetic, equilibrium   |                    | Fo 0                             |           | 2.62  mg/g  Eq.  0.3                                   | 2 86*0 025*221/55 8-0.4 mg/g                         | 0.152   |  |
| and thermodynamic models             |                    | re <sub>3</sub> O <sub>4</sub>   | AS(V)     | 2.05 mg/g Fe <sub>3</sub> O <sub>4</sub>               | 5.80° 0.025° 251/55.8–0.4 mg/g                       | 0.152   |  |
| Sanghamitra, 2006, Separation and    |                    |                                  |           |  | Fe304  |         |  |
| Purification Technology <sup>6</sup> |                    |                                  |           |  |  |         |  |
| A. Yurum, Fast deposition of         | Granular activated | α-Fe <sub>2</sub> O <sub>3</sub> | As(V)     | 0.827 mg/g Fe <sub>2</sub> O <sub>3</sub> <sup>8</sup> | 136.37 mg/g Fe <sub>2</sub> O <sub>3</sub>           | 164.897 | Took the oxidized                                |
| porous iron oxide on activated       | carbon             |                                  |           |  |  |         | activated carbon.                                |
| carbon by microwave heating and      |                    |                                  |           |  |  |         | WT%(Fe)=20.37%                                   |
| arsenic (V) removal from water,      |                    |                                  |           |  |  |         | Assumption: Same pH                              |
| 2014, Chemical Engineering           |                    |                                  |           |  |  |         | range (pH=6.27 for                               |
| Journal <sup>7</sup>                 |                    |                                  |           |  |  |         | N <sub>ads</sub> -S, pH=7 for N <sub>ads</sub> ) |
| A.M. Cooper, The effect of carbon    | Granular activated | δ -FeOOH                         | As(V)     | 7 mg/g δ-FeOOH <sup>10</sup>                           | 45.1 mg/g FeOOH                                      | 6.443   | Assumption:                                      |
| type on arsenic and                  | carbon             |                                  |           |  |  |         | The same N <sub>ads</sub> phase                  |
| trichloroethylene removal            |                    |                                  |           |  |  |         | in both articles                                 |
| capabilities of iron (hydr)oxide     |                    |                                  |           |  |  |         | The same condition                               |
| nanoparticle-impregnated             |                    |                                  |           |  |  |         | used to measure the                              |
| granulated activated carbons,        |                    |                                  |           |  |  |         | adsorption capacity.                             |
| 2010, Journal of Hazardous           |                    |                                  |           |  |  |         |  |
| Materials <sup>9</sup>               |                    |                                  |           |  |  |         |  |

| K. Hristovski, Effect of synthesis<br>conditions on nano-iron<br>(hydr)oxide impregnated<br>granulated activated carbon, 2009,<br>Chemical Engineering Journal <sup>11</sup> | Granular activated<br>carbon | Amorphous<br>FeOOH                       | As(V)   | 7 mg/g Amorphous<br>FeOOH <sup>12</sup>  | 21.7 mg/g Amorphous FeOOH                                     | 3.100   | Assumption:<br>Adsorption capacity:<br>the average amount of<br>adsorption capacity<br>(15.2-28.2 mg/g<br>amorphous FeOOH)  |
|--|------------------------------|--|---------|--|---|---------|---|
| M. Jain, Development of iron oxide/activated carbon  | Activated carbon             | Fe <sub>3</sub> O <sub>4</sub> magnetite | Cr(IV)  | 5.5 mg/g Fe <sub>3</sub> O <sub>4</sub>  | 8.06/0.184*0.72 =31.54 mg/g<br>Fe <sub>3</sub> O <sub>4</sub> | 5.727   | Phase: magnetite  |
| nanoparticle composite for the<br>removal of Cr(VI), Cu(II) and Cd(II)   |                              |  | Cu(II)  | 2.7 mg/g Fe <sub>3</sub> O <sub>4</sub>  | 3.2/0.184*0.72=12.52 mg/g<br>Fe <sub>3</sub> O <sub>4</sub>   | 4.637   |   |
| Water Resources and Industry <sup>13</sup>   |                              |  | Cd(II)  | 0.09 mg/g Fe <sub>3</sub> O <sub>4</sub>                                       | 2.15/0.184*0.72=8.41 mg/g<br>Fe <sub>3</sub> O <sub>4</sub>   | 93.444  |   |
| D.Mohan, Cadmium and lead<br>remediation using magnetic oak  | Carbon biochar               | Fe <sub>3</sub> O <sub>4</sub> magnetite | Cd(II)  | 0.09 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>13</sup>                         | 7.4/0.513*0.72=10.39 mg/g<br>Fe <sub>3</sub> O <sub>4</sub>   | 115.444 | pH=5  |
| wood and oak bark fast pyrolysis<br>bio-chars,2014, Chemical   |                              |  | Cd(II)  | 0.09 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>13</sup>                         | 2.87/0.806*0.72=2.56 mg/g<br>Fe <sub>3</sub> O <sub>4</sub>   | 28.444  |   |
| Engineering Journal <sup>14</sup>  |                              |  | Pb(II)  | 22.89 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>15</sup>                        | 30.2/0.513*0.72=42.39 mg/g<br>Fe <sub>3</sub> O <sub>4</sub>  | 1.852   |   |
|  |                              |  | Pb(II)  | 0.1105mmol/g*207.2=<br>22.89 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>15</sup> | 10.13/0.806*0.72=9.05 mg/g<br>Fe <sub>3</sub> O <sub>4</sub>  | 0.395   |   |
| S.M, Miller, Novel, bio-based,<br>photoactive arsenic sorbent: TiO <sub>2</sub> -<br>impregnated chitosan bead, 2010,<br>Water Research<br>P.A. Nishad, Enhancing the        | Chitosan beads               | TiO <sub>2</sub>                         | As(III) | 3 mg/g TIO <sub>2</sub>  | 2.099/0.298 =7.04 mg/g TiO <sub>2</sub>                       | 2.347   | Data for NM is taken<br>from fig. 4 in article,<br>so we assume the<br>experiment conditions<br>are the same as for<br>the NM@S.<br>In article mentioned<br>that TiO <sub>2</sub> mass is<br>29.8%.<br>Assumption:<br>pH is similar (pH-3.3<br>for N <sub>ads</sub> and pH=4.3 for<br>NM@S).<br>Same NM used. <sup>17</sup><br>The ration between<br>N <sub>ads</sub> to S is given (1:5) |
| nano titania -chitosan beads using<br>epichlorohydrin as the crosslinker,<br>2017, Journal of Hazardous<br>Materials <sup>16</sup>   |                              |  | As (V)  | 5.5 mg/g TIO <sub>2</sub>  | 2.050/0.298 = 6.88 mg/g TiO <sub>2</sub>                      | 1.251   |   |
| P.A. Nishad, Nano-titania-<br>crosslinked chitosan composite as<br>a superior sorbent for antimony   | Chitosan beads               | TiO <sub>2</sub>                         | Sb(III) | 173.2 μmol/g TiO <sub>2</sub>  | 170.3 6 = 1021.8 μmol/g                                       | 5.9     | pH=6.9<br>NM to S ration is 1:5   |
| (III) and (V), 2014, Carbohydrate  |                              |  | Sv(III) | 187.7 μmol/g TiO <sub>2</sub>  | 1089 μmol/g TiO <sub>2</sub>                                  | 5.802   | pH=3.06   |

| Polymers <sup>17</sup>  |                    |   | Sb(V)             | 799.1 μmol/g TiO <sub>2</sub>                              | 1215 μmol/g TiO <sub>2</sub>  | 1.519 | pH=3.33  |
|---|--------------------|---|-------------------|--|---|-------|--|
| J. Yamani, Enhanced arsenic<br>removal using mixed metal oxide<br>impregnated chitosan beads, 2012,<br>Water Research <sup>18</sup>   | Chitosan beads     | Al <sub>2</sub> O <sub>3</sub>              | As(V)             | 12 mg/g Al <sub>2</sub> O <sub>3</sub>                     | 8.4 mg/g Al <sub>2</sub> O <sub>3</sub>                                     | 0.7   |  |
| A. I. Zouboulis, Arsenic Removal<br>Using Iron Oxide Loaded Alginate<br>Beads, 2002, Industrial and<br>Engineering Chemistry Research <sup>19</sup>   | Alginate beads     | Hydrous FeO(OH)                             | As(V)             | 9 mg As / g-Fe <sup>20</sup>                               | 5.79 mg As / g-Fe   | 0.643 | Assumption:<br>Same N <sub>ads</sub> phase and<br>experiment<br>conditions.  |
| J. Min, Removal of Selenite and<br>Chromate Using Iron(III)-Doped<br>Alginate Gels, 1999, Water<br>Environment Research <sup>21</sup>   | Alginate gel beads | Iron oxyhydroxide<br>Fe(OH)₃                | Se(IV)            | 2.4 mg / g-Fe <sup>22</sup>                                | 0.15 g Se(IV) / g-Fe  | 0.062 |  |
| W. Biftu, Synthesis of nanoZrO <sub>2</sub> via<br>simple new green routes and its<br>effective application as adsorbent<br>in phosphate remediation of water<br>with or without immobilization in<br>Al-alginate beads,2020, Water<br>Science & Technology <sup>23</sup> | Al-alginate beads  | nZrO <sub>2</sub>                           | PO4 <sup>3-</sup> | 126.2 mg/g - nZrO <sub>2</sub>                             | 173.0 mg/g nZrO <sub>2</sub> -Al-alginate =<br>24.22 mg/g nZrO <sub>2</sub> | 0.192 | 1.5 g of nano ZrO2<br>was added =><br>1.5/173= 86 => 86%<br>Al-alginate beads<br>and 14% NM  |
| R. Pineda, Removal of Arsenic from<br>Aqueous Solutions with Alginate<br>Based-Magnetic Nanocomposites,<br>2009, Clean Technology <sup>24</sup>   | Alginate           | Magnetite (Fe <sub>3</sub> O <sub>4</sub> ) | As(V)             | 11-17 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>25,26</sup> | 1.1 mg/g  | 0.418 | Assumption:<br>Same N <sub>ads</sub> phase and<br>experiment<br>conditions.<br>For NM@S/NM<br>calculation we took<br>the NM average  |
|   |                    |   | As(III)           | 20-22 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>25,26</sup> | 1.04 mg/g   | 0.495 | Assumption:<br>Same N <sub>ads</sub> phase and<br>experiment<br>conditions.<br>For NM@S/NM<br>calculation we took<br>the NM average  |
| J. Elton, Titanium Dioxide-Based<br>Hybrid Ion-Exchange Media for<br>Simultaneous Removal of Arsenic<br>and Nitrate, 2013, Novel Solutions<br>to Water Pollution <sup>27</sup>  | Ion-Exchange beads | TiO <sub>2</sub>                            | As                | 7 mg/g TiO <sub>2</sub> <sup>28</sup>                      | —<br>9.95 mg/g TiO <sub>2</sub>   | 1.421 | MW(Ti)=47.8 g/mol<br>MW(TiO <sub>2</sub> )=79.8 g/mol<br>Assumption:<br>Same N <sub>ads</sub> phase and<br>experiment<br>conditions. |

|  |                    |                                  |    |                                  | —<br>14.92 mg/g TiO <sub>2</sub> | 2.131 | MW(Ti)=47.8 g/mol<br>MW(TiO <sub>2</sub> )=79.8 g/mol<br>Assumption:<br>Same N <sub>ads</sub> phase and<br>experiment<br>conditions.  |
|--|--------------------|----------------------------------|----|----------------------------------|----------------------------------|-------|---|
|  |                    |                                  |    |                                  | —<br>16.36 mg/g TiO <sub>2</sub> | 2.336 | MW(Ti)=47.8 g/mol<br>MW(TiO <sub>2</sub> )=79.8 g/mol<br>Assumption:<br>Same N <sub>ads</sub> phase and<br>experiment<br>conditions.  |
| M. Gifford, Ranking traditional and<br>nano-enabled sorbents for<br>simultaneous removal of arsenic<br>and chromium from simulated<br>groundwater, 2017, Science of the<br>Total Environment <sup>29</sup> | Ion-Exchange beads | TiO <sub>2</sub>                 | As | 107.5 μmol/g TiO <sub>2</sub>    | 12.4/0.16                        | 0.721 | From J. Elton et al.<br>assuming mass of<br>synthesized TiO <sub>2</sub> @S is<br>11-21% (16% avg) <sup>27</sup> .  |
|  |                    |                                  | Cr | 5.7 μmol/g Fe(OH)2               | <br><br>Fe(OH) <sub>2</sub>      | 8.246 | From K. Hristovski el<br>al. assuming that mass<br>of amorphous iron<br>(hydro)oxide<br>synthesized is 16% of<br>Fe <sup>30</sup> .<br>Mw(Fe) = 55.8 g/mol<br>Mw(Fe(OH) <sub>2</sub> ) = 89.8<br>g/mol  |
|  |                    | amorphous<br>Fe(OH) <sub>2</sub> | As | 172.1 μmol/g Fe(OH) <sub>2</sub> | —<br>—<br>Fe(OH)2                | 0.341 | From J. Elton et al.<br>assuming mass of<br>synthesized TiO <sub>2</sub> @S is<br>11-21% (16% avg) <sup>27</sup> .<br>From K. Hristovski el<br>al. assuming that mass<br>of amorphous iron<br>(hydro)oxide<br>synthesized is 16% of<br>Fe <sup>30</sup> .<br>Mw(Fe) = 55.8 g/mol<br>Mw(Fe(OH) <sub>2</sub> ) = 89.8<br>g/mol<br>From K. Hristovski el<br>al. assuming that mass |

|   |                    |                                |                   |   |  |       | of amorphous iron<br>(hydro)oxide<br>synthesized is 16% of<br>Fe <sup>30</sup> .<br>Mw(Fe) = 55.8 g/mol<br>Mw(Fe(OH) <sub>2</sub> ) = 89.8<br>g/mol                     |
|---|--------------------|--------------------------------|-------------------|---|--|-------|---|
| J. Wang, Hydrous ferric oxide-  | Ion-Exchange beads | Amorphous                      | As(III)           | 28.0 mg/g Fe(OH) <sub>2</sub> <sup>16</sup>           | 225*0.65=146.25 mg/g Fe(OH) <sub>2</sub>                                       | 4.223 |   |
| resin nanocomposites of tunable   |                    | Fe(OH)₂                        |                   |   | 200*0.65=130 mg/g Fe(OH) <sub>2</sub>  | 4.643 |   |
| structure for arsenite removal:   |                    |                                |                   |   | 190*0.65=123.5 mg/g Fe(OH) <sub>2</sub>  | 4.411 |   |
| Effect of the nost pore structure,  |                    |                                |                   |   | 200*0.65=130 mg/g Fe(OH) <sub>2</sub>  | 4.643 |   |
| Materials <sup>31</sup>   |                    |                                |                   |   | 175*0.65=113.75 mg/g Fe(OH) <sub>2</sub>                                       | 4.063 |   |
| Q. Su, Fabrication of polymer-<br>supported nanosized hydrous<br>manganese dioxide (HMO) for<br>enhanced lead removal from<br>waters, 2009, Science of the Total<br>Environment <sup>32</sup>                                     | Ion-Exchange beads | Mn(OH) <sub>2</sub>            | Pb(II)            | 352.55 mg/g Mn(OH) <sub>2</sub>                       | 395 mg/g /(7.33%Mn*55/89Mn<br>in MN(OH)2)= 3381.85 mg/g<br>Mn(OH) <sub>2</sub> | 9.592 |   |
| L. Zhang, Removal of phosphate<br>from water by activated carbon<br>fiber loaded with lanthanum oxide,<br>2011, Journal of Hazardous<br>Materials <sup>33</sup>   | Carbon fibers      | LaO                            | PO4 <sup>3-</sup> | 46.95 mg/g LaO <sup>34</sup>                          | 5.85/0.1178 = 49.66 mg/g LaO   | 1.058 | WT%(LaO)=11.78%<br>Assumption:<br>Same LaO phase and<br>experiment condition  |
| J. Zhang, Synthesis of magnetic<br>iron oxide nanoparticles onto<br>fluorinated carbon fabrics for<br>contaminant removal and oil-<br>water separation, 2017,<br>Separation and Purification<br>Technology <sup>35</sup>          | Carbon fibers      | Fe <sub>3</sub> O <sub>4</sub> | Cu(II)            | 8.9 mg/g Fe <sub>3</sub> O <sub>4</sub> <sup>36</sup> | 62.5 mg/g Fe <sub>3</sub> O <sub>4</sub>                                       | 7.022 | pH=5  |
| Q. Zhou, Phosphorus removal from<br>wastewater using nano-<br>particulates of hydrated ferric<br>oxide doped activated carbon fiber<br>prepared by Sol–Gel method,<br>2012, Chemical Engineering<br>Journal journal <sup>37</sup> | Carbon fibers      | FeOOH                          | P                 | 139.5 mg/g FeOOH <sup>38</sup>                        | 12.86/0.44=29.227 mg/g FeOOH   | 0.21  | From fig2 WT%<br>(FeOOH)=44<br>12.86 mg/g-NM@S<br>12.86/0.44 = 29.227<br>mg/g FeOOH<br>pH range of 2.0–6.0<br>assume: amorphous<br>phase, FeOOH<br>adsorption capacity: |

|   |                             |  |        |  |  |       | 134-145 mg/g <sup>38</sup> , we   |
|---|-----------------------------|--|--------|--|--|-------|---|
|   |                             |  |        |  |  |       | took the average  |
| Y. Zheng, Adsorptive removal of<br>arsenic from aqueous solution by a<br>PVDF/zirconia blend flat sheet<br>membrane, 2011, Journal of<br>Membrane Science <sup>39</sup>                     | Carbon fibers               | Zr(OH)4                                  | As     | 38.9 mg/g Zr(OH) <sub>4</sub>                    | 43 mg/g mg/g Zr(OH)₄   | 1.105 |   |
| K.E. Greenstein, Performance  | Polymeric fibers            | α-Fe <sub>2</sub> O <sub>3</sub>         | As(V)  | 17 mg/g $\alpha$ -Fe <sub>2</sub> O <sub>3</sub> | 9.3 mg/g α-Fe <sub>2</sub> O <sub>3</sub>  | 0.547 |   |
| comparison of hematite (P-Fe <sub>2</sub> O <sub>3</sub> )-   |                             |  | Cu(II) | 70 mg/g α-Fe <sub>2</sub> O <sub>3</sub>         | $35 \text{ mg/g} \alpha$ -Fe <sub>2</sub> O <sub>3</sub>   | 0.5   |   |
| polymer composite and core-shell  |                             |  | Cr(VI) | 9.5 mg/g α-Fe <sub>2</sub> O <sub>3</sub>        | 7.3 mg/g $\alpha$ -Fe <sub>2</sub> O <sub>3</sub>  | 0.768 |   |
| nanofibers as point-of-use<br>filtration platforms for metal<br>sequestration, 2019, Water<br>Research <sup>40</sup>  |                             |  | Pb(II) | 94 mg/g α-Fe <sub>2</sub> O <sub>3</sub>         | 57 mg/g α-Fe <sub>2</sub> O <sub>3</sub>   | 0.606 |   |
| K.T. Peter, Functionalized polymer-   | Polymeric fibers            | Ferrihydrite iron                        | Cr     | 19 mg-Cr/g-Fh                                    | 17 mg-Cr/g-Fh  | 0.89  |   |
| iron oxide hybrid nanofibers:<br>Electrospun filtration devices for<br>metal oxyanion removal, 2017,<br>Water Research <sup>41</sup>  | (polyacrylonitrile,<br>PAN) | oxide                                    | As     | 31 mg-As/g-Fh                                    | 26 mg-As/g-Fh  | 0.84  |   |
| K.T. Peter , Surfactant-assisted  | Polymeric fibers            | Amorphous Fe <sub>2</sub> O <sub>3</sub> | Pb     | 13 mg-Pb/g-Fe <sub>2</sub> O <sub>3</sub>        | 27 mg-Pb/g-Fe <sub>2</sub> O <sub>3</sub>  | 2.08  |   |
| fabrication of porous polymeric   | (PAN)                       |  | Cu     | 75 mg-Cu/g-Fe <sub>2</sub> O <sub>3</sub>        | 25 mg-Cu/g-Fe <sub>2</sub> O <sub>3</sub>  | 0.33  |   |
| nanofibers with surface-enriched  |                             |  | Cd     | 105 mg-Cd/g-Fe <sub>2</sub> O <sub>3</sub>       | 100 mg-Cd/g-Fe <sub>2</sub> O <sub>3</sub>   | 0.95  |   |
| iron oxide nanoparticles:   | Polymeric fibers            | Amorphous Fe <sub>2</sub> O <sub>3</sub> | Pb     | 13 mg-Pb/g-Fe <sub>2</sub> O <sub>3</sub>        | 101 mg-Pb/g-Fe <sub>2</sub> O <sub>3</sub>   | 7.77  |   |
| removal of motal cations 2018   | (PAN-based)                 |  | Cu     | 75 mg-Cu/g-Fe <sub>2</sub> O <sub>3</sub>        | 170 mg-Cu/g-Fe <sub>2</sub> O <sub>3</sub>   | 2.27  |   |
| Environmental Science <sup>42</sup>   |                             |  | Cd     | 105 mg-Cd/g-Fe <sub>2</sub> O <sub>3</sub>       | 57 mg-Cd/g-Fe <sub>2</sub> O <sub>3</sub>  | 0.54  |   |
| X.Zhang, Preparation, performance<br>and adsorption activity of TiO <sub>2</sub><br>nanoparticles entrapped PVDF<br>hybrid membranes, 2012, Applied<br>Surface Science <sup>43</sup>        | PVDF membrane               | TiO <sub>2</sub>                         | Cu(II) | 6.86 mg/g TiO <sub>2</sub> <sup>44</sup>         | 86 ug/cm <sup>2</sup> / (1.087*1.78)g/cm <sup>3</sup><br>density of pVDF and added<br>weiget by TiO2 / 0.1 cm thick<br>mem / 8.76% TIO2 = 0.5 mg/g<br>TiO2 | 0.073 | 8.74% loaded TiO <sub>2</sub><br>20mm×20mm<br>membrane area<br>(4cm <sup>2</sup> )<br>pH>7 (for pH>7<br>adsorption is the<br>same)<br>Lagergren model |
| B. Gohari, Polyethersulfone<br>Membranes Prepared with<br>3-Aminopropyltriethoxysilane<br>Modified Alumina Nanoparticles<br>for Cu(II) Removal from Water,<br>2018, ACS OMEGA <sup>45</sup> | PES membrane                | γ-alumina                                | Cu(II) | 51.3 mg/g  | $\frac{44.84\frac{mg}{g}}{0.05} = 896.8 \text{ mg/g}$  | 17.48 | 5% alumina  |
| X. Zhang, Preparation,<br>performances of PVDF/ZnO hybrid   | PVDF membrane               | hexagonal ZnO                            | Cu(II) | 54.3 mg/g <sup>47</sup>                          | 87.5 ug/cm <sup>2</sup> / (1.05*1.78)g/cm <sup>3</sup><br>density of pVDF and added  | 0.172 |   |

| membranes and their applications            |               |                     |                 |               | weiget by ZnO / 0.1 cm thick |       |  |
|---|---------------|---------------------|-----------------|---------------|------------------------------|-------|--|
| in the removal of copper ions,              |               |                     |                 |               | mem / 5% ZnO = 9.35 mg/g ZnO |       |  |
| 2014, Applied Surface Science <sup>46</sup> |               |                     |                 |               |                              |       |  |
| L. Chen, In situ formation of               | PVDF membrane | La(OH) <sub>3</sub> | PO <sub>4</sub> | 61.7 mg /g-La | 256.6 mg/g-La                | 4.159 |  |
| La(OH)3-poly(vinylidene fluoride)           |               |                     |                 |               |                              |       |  |
| composite filtration membrane               |               |                     |                 |               |                              |       |  |
| with superior phosphate removal             |               |                     |                 |               |                              |       |  |
| properties, 2018, Chemical                  |               |                     |                 |               |                              |       |  |
| Engineering Journal 48                      |               |                     |                 |               |                              |       |  |

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