

SUPPLEMENTARY INFORMATION FOR:

UVC based advanced oxidation processes for simultaneous removal of microcontaminants and pathogens from simulated municipal wastewater at pilot plant scale

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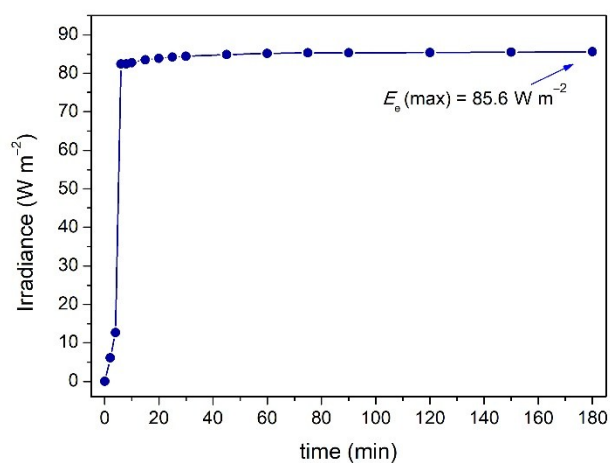


Fig. S1 – Irradiance profile of the UV-C lamp measured during 180 min in distilled water (maximum value 85.6 W m⁻²).

Table S1 – Chromatographic parameters: retention time, wavelength of maximum absorbance and area of each microcontaminant peak at 100 µg L⁻¹.

Microcontaminant	Retention time (min)	λ (nm)	Area - 100 µg L ⁻¹ (a. u.)
Acetaminophen (ACT)	2.48	245	18.2
Caffeine (CAF)	3.60	270	14.0
Carbamazepine (CBZ)	3.94	270	5.5
Trimethoprim (TMP)	5.01	267	20.0
Sulfamethoxazole (SMX)	7.2	267	8.7
Diclofenac (DCF)	10.6	280	9.7

Table S2 – Photochemical properties of the microcontaminants and experimental degradation percentages under UVC irradiation

Microcontaminant	Chemical structure	* $A_{254\text{ nm}}$ (a. u.)	$\epsilon_{254\text{ nm}}$ [1] ($10^3\text{ M}^{-1}\text{ cm}^{-1}$)	[1] $\Phi_{254\text{ nm}}$ ($10^{-2}\text{ mol Es}^{-1}$)	*Deg. (%)
DCF		0.023	6.1	22.2	~100% (200 min)
SMX		0.064	16.5	5.8	~100% (30 min)
ACT		0.056	6.6	4.6	75% (180 min)
TMP		0.017	2.9	0.6	40% (180 min)
CAF		0.022	4.2	0.3	30% (180 min)
CBZ		0.026	5.5	0.2	20% (180 min)

$\epsilon_{254\text{ nm}}$ ($\text{M}^{-1}\text{ cm}^{-1}$) = molar absorptivity coefficient

$\Phi_{254\text{ nm}}$ (mol Es^{-1}) = quantum efficiency

*Experimental values obtained in this work

[1] H. W. Yu, M. Park, S. Wu, I.J. Lopez, W. Ji, J. Scheideler, S. A. Snyder, Strategies for selecting indicator compounds to assess attenuation of emerging contaminants during UV advanced oxidation processes. Water Research, 2019. 166: p. 115030. doi: 10.1016/j.watres.2019.115030.

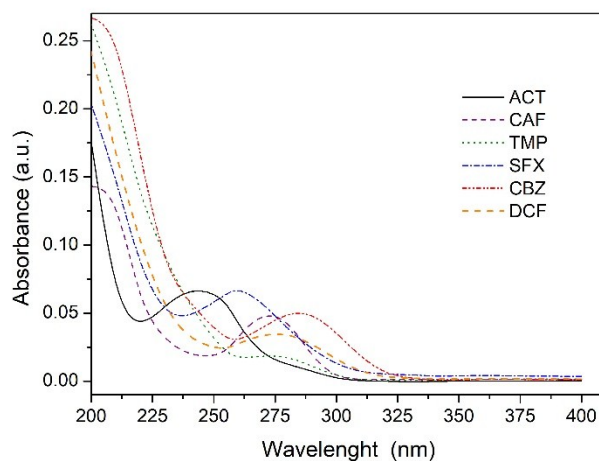


Fig. S2 – UV absorption spectrum of each microcontaminant. This measurement was carried out using 1 mg L^{-1} of each compound dissolved in distilled water between 200–400 nm. The obtained absorbance at 254 nm can be seen in Table S2 above.

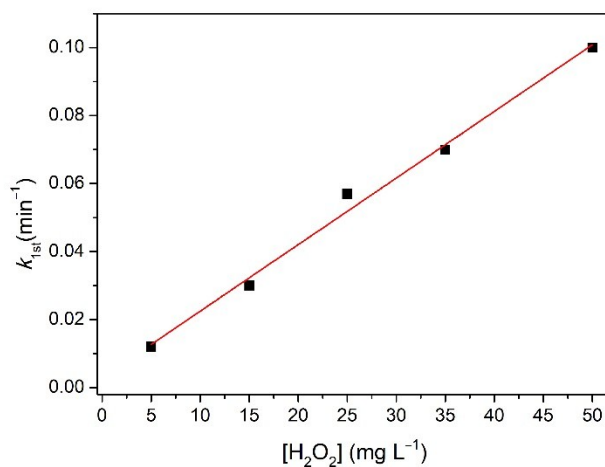


Fig. S3 – Pseudo first order kinetic constant (k_{1st}) as a function of H_2O_2 concentration ($[\text{H}_2\text{O}_2]$) for UVC/ H_2O_2 process. The obtained slope and R^2 for the linear regression were $0.00196 \text{ L (mg min)}^{-1}$ and 0.990, respectively.

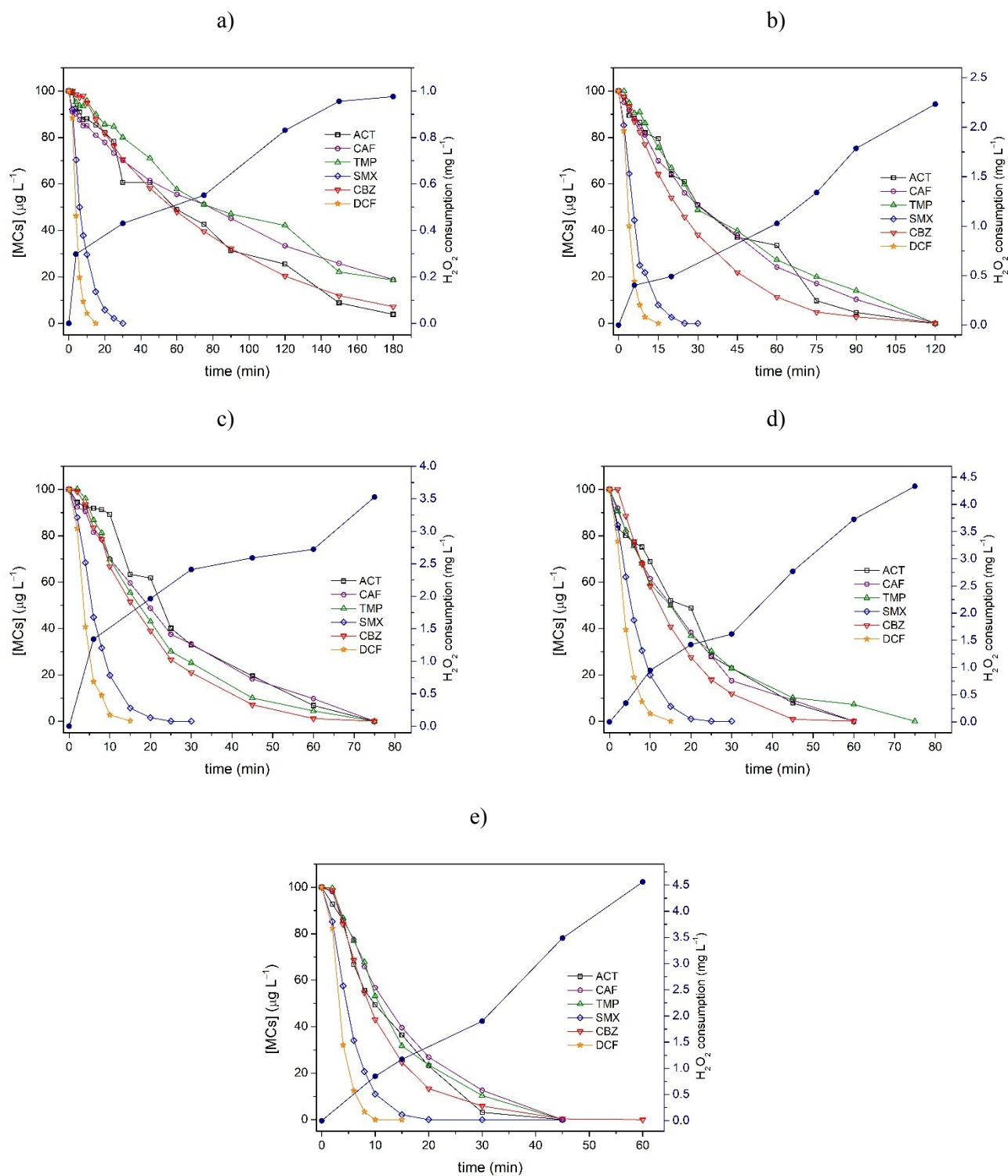


Fig. S4 – Degradation profile of each MCs and H_2O_2 consumption for the UVC/ H_2O_2 process: a) 5 $mg L^{-1}$, b) 15 $mg L^{-1}$, c) 25 $mg L^{-1}$, d) 35 $mg L^{-1}$, and e) 50 $mg L^{-1}$.

Table S3 – Pseudo first-order kinetic constants (k_{1st}) for the UVC/H₂O₂ process during degradation of MCs. The values in parentheses correspond to the coefficient of determination (R^2).

UV-C/H ₂ O ₂ (mg L ⁻¹)	k_{1st} (10 ⁻² min ⁻¹)					
	ACT	CAF	TMP	SFX	CBZ	DCF
5	1.7 (0.97)	0.9 (0.99)	1.0 (0.99)	15.5 (0.99)	1.45 (0.97)	32.1 (0.94)
15	3.3 (0.97)	2.4 (0.99)	2.2 (0.99)	18.5 (0.99)	4.0 (0.99)	37.2 (0.97)
25	4.4 (0.97)	4.0 (0.99)	5.4 (0.99)	21.5 (0.98)	7.1 (0.97)	44.4 (0.96)
35	5.5 (0.98)	5.4 (0.99)	4.6 (0.99)	22.5 (0.97)	9.9 (0.94)	35.0 (0.98)
50	11 (0.93)	7.1 (0.99)	8.0 (0.99)	26.4 (0.97)	12.3 (0.98)	43.4 (0.95)

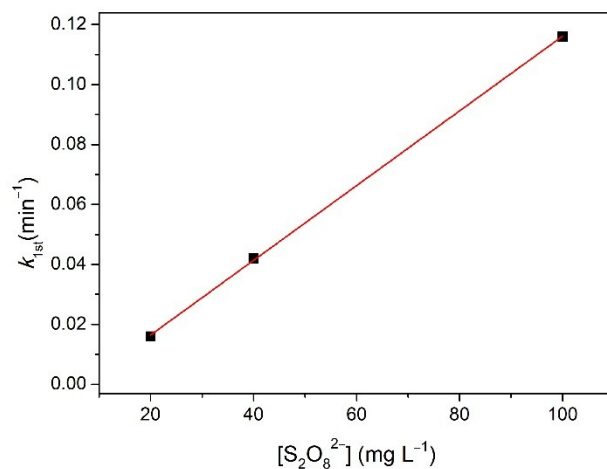


Fig. S5 – Pseudo first order kinetic constant (k_{1st}) as a function of S₂O₈²⁻ concentration ([S₂O₈²⁻]) for UVC/S₂O₈²⁻ process. The obtained slope and R^2 for the linear regression were 0.00125 L (mg min)⁻¹ and 0.999, respectively.

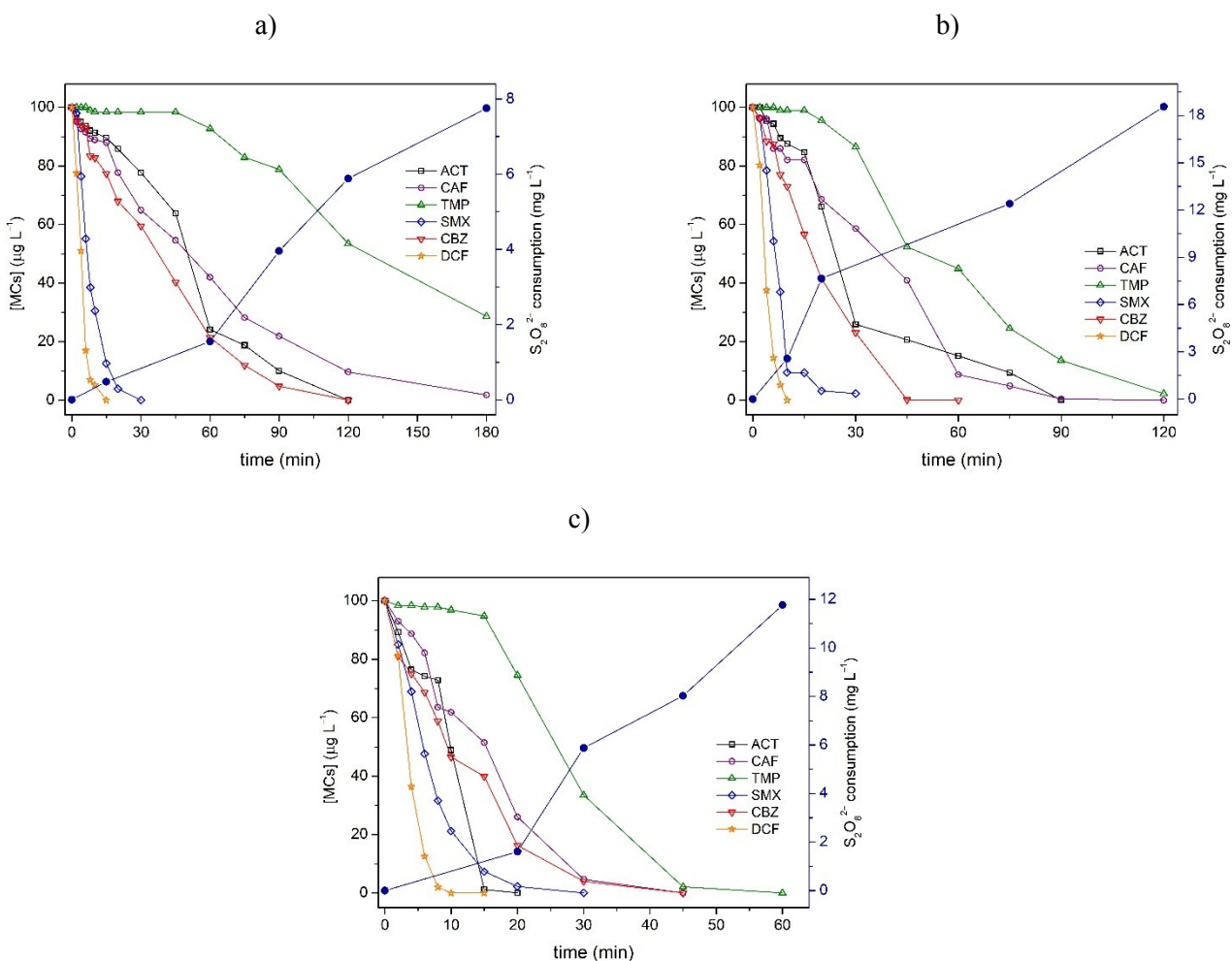


Fig. S6 – Degradation profile of each MCs and H_2O_2 consumption for the UVC/ $\text{S}_2\text{O}_8^{2-}$ process: a) 20 mg L^{-1} , b) 40 mg L^{-1} , and c) 100 mg L^{-1} .

Table S4 – Pseudo first-order kinetic constants (k_{1st}) for the UVC/ $\text{S}_2\text{O}_8^{2-}$ process during degradation of MCs. The values in parentheses correspond to the coefficient of determination (R^2).

UV-C/ $\text{S}_2\text{O}_8^{2-}$ (mg L^{-1})	k_{1st} (10^{-2} min^{-1})					
	ACT	CAF	TMP	SFX	CBZ	DCF
20	2.5 (0.96)	2.1 (0.99)	0.9 (0.98)	16.5 (0.97)	3.1 (0.96)	33.1 (0.96)
40	3.4 (0.97)	3.8 (0.91)	3.6 (0.94)	14.6 (0.95)	4.9 (0.98)	38.1 (0.96)
100	6.0 (0.85)	9.6 (0.91)	8.1 (0.81)	19.5 (0.98)	10.3 (0.95)	48.4 (0.98)

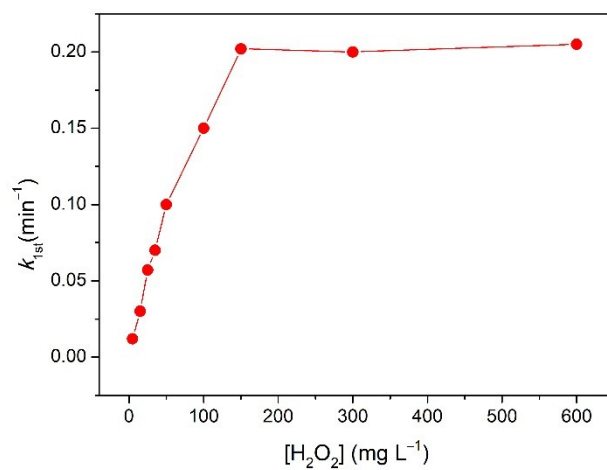


Fig. S7 – Pseudo first order kinetic constant (k_{1st}) as a function of H_2O_2 concentration ($[H_2O_2]$) for UVC/ H_2O_2 process.

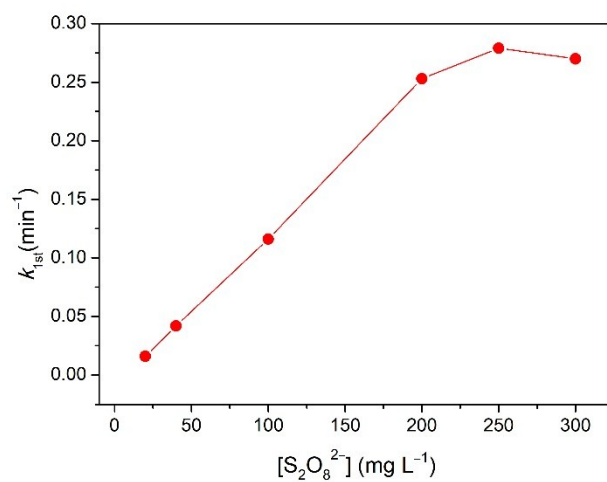


Fig. S8 – Pseudo first order kinetic constant (k_{1st}) as a function of $S_2O_8^{2-}$ concentration ($[S_2O_8^{2-}]$) for UVC/ $S_2O_8^{2-}$ process.

Table S5 – Radical self-scavenging reactions involved in UVC/H₂O₂ and UVC/S₂O₈²⁻ processes.

Reactions	Rate constants	Reference
$2\text{OH}^\bullet \rightarrow \text{H}_2\text{O}_2$	$k = 5.5 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$	[2]
$\text{H}_2\text{O}_2 + \text{OH}^\bullet \rightarrow \text{H}_2\text{O} + \text{HO}_2^\bullet \leftrightarrow \text{O}_2^{\bullet-} + \text{H}^+$	$k = 2.7 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$	[3]
$\text{HO}^\bullet + \text{O}_2^{\bullet-} \rightarrow \text{HO}^- + \text{O}_2$	$k = 8.0 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$	[4]
$\text{HO}^\bullet + \text{HO}_2^\bullet \rightarrow \text{H}_2\text{O} + \text{O}_2$	$k = 7.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$	[5]
$\text{SO}_4^{\bullet-} + \text{S}_2\text{O}_8^{2-} \rightarrow \text{HO}^\bullet + \text{SO}_4^{2-} + \text{S}_2\text{O}_8^{\bullet-}$	$k = 6.1 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$	[6]
$\text{SO}_4^{\bullet-} + \text{SO}_4^{\bullet-} \rightarrow \text{S}_2\text{O}_8^{2-}$	$k = 4.0 \times 10^8 \text{ M}^{-1} \text{ s}^{-1}$	[7]
$\text{SO}_4^{\bullet-} + \text{H}_2\text{O} \rightarrow \text{OH}^\bullet + \text{SO}_4^{2-} + \text{H}^+$	$k < 3 \times 10^8 \text{ s}^{-1}$	[7]

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