

Supporting Document

Table 1SD Pseudo steady-state influent and effluent characteristics (10 samples)

Parameter	Influent (mg/L)	Effluent (mg/L)
	Average±SD	Average±SD
TCOD	571±171	188±88
SCOD	214±120	92±77
Methanol	141±112	
NO₂-N	48±16	9.2±16
Total N	95±17	27±18
Soluble N	72±16	23±18
Total P	6.9±3.2	1.8±0.9
Soluble P	1.3±0.5	0.4±0.38
NH₃-N	21.2±3	11.5±2.6
Alkalinity (CaCO₃/L)	228±41	487±86
TSS	340±80	96±24
VSS	250±76	62±14
Bioreactor parameters		
MLSS	4439±190	
MLVSS	3392±125	
SRT	17.4	

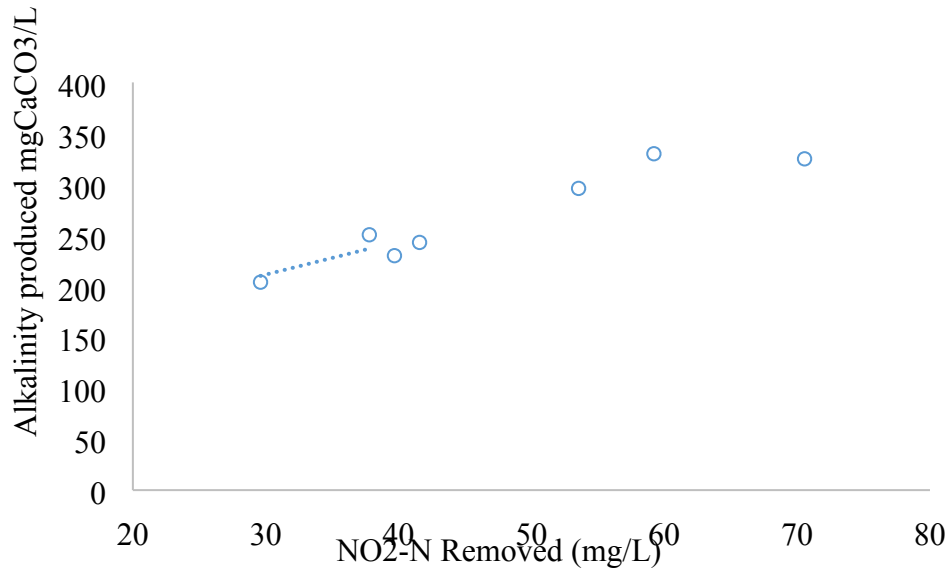


Figure 1SD. Relation between the alkalinity produced and nitrogen removed in the SBR (influent and effluent data, room temp. 25°C)

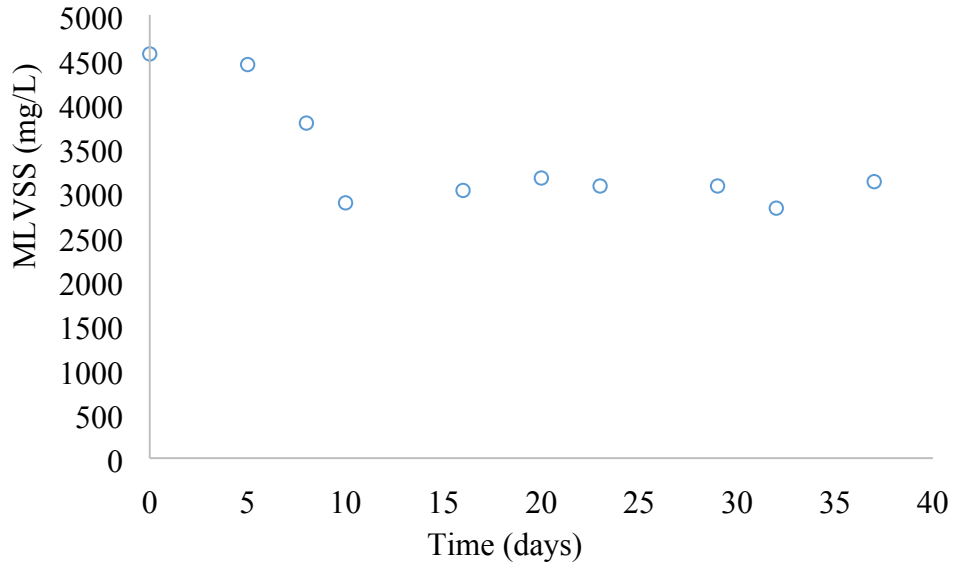


Figure 2SD. MLSS concentration in the SBR during pseudo-steady-state operation (room temp. 25°C)

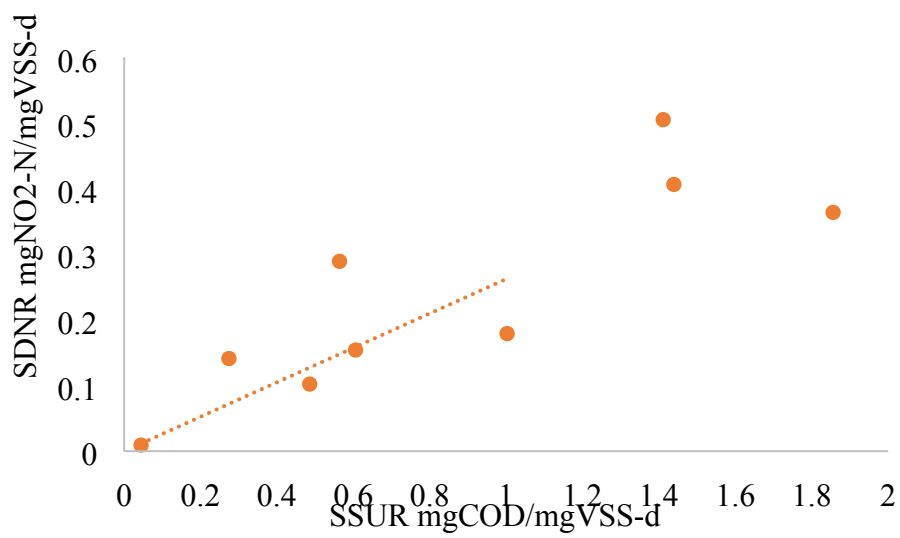
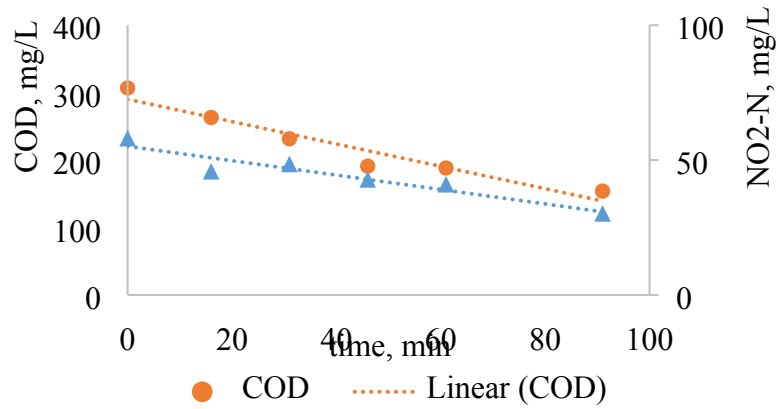
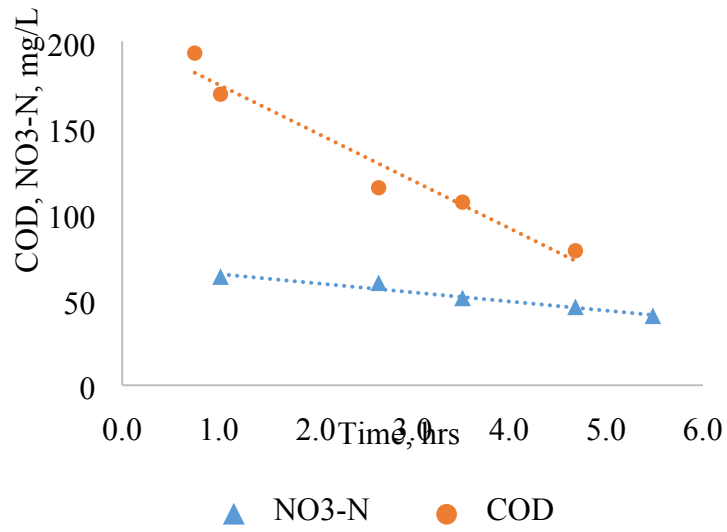


Figure 3SD Relation between SDNR and SSUR to estimate the yield coefficient-Post denitrification (kinetic study in the post-denitrification SBR, room temp. 25°C)



(a)



(b)

Figure 4SD Denitrification rates for (a) nitrite and (b) nitrate with MWW as a sole carbon source (batch kinetics, room temp. 25°C)

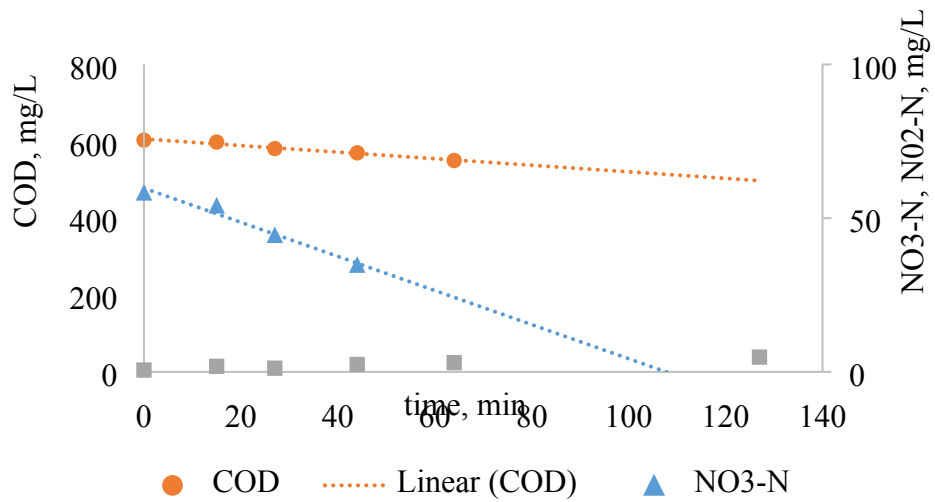
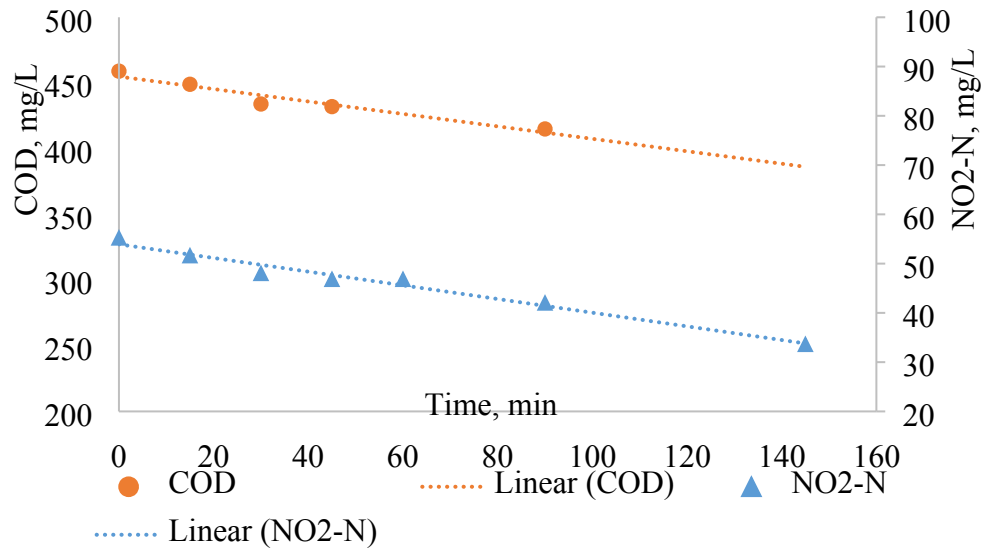


Figure 5SD Denitrification rates for (a) nitrite and (b) nitrate with methanol as a sole carbon source (batch kinetics, room temp. 25°C)

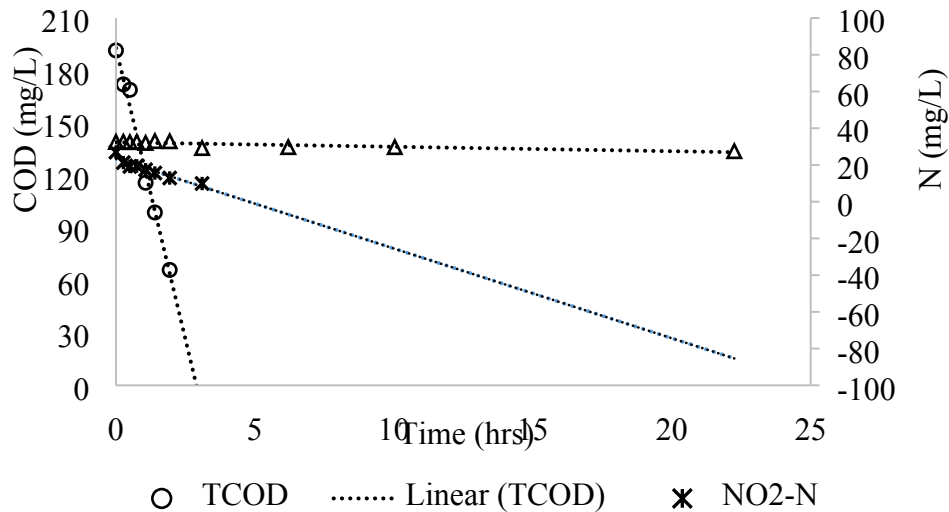


Figure 6SD Denitrification rates of a mixture of nitrite and nitrate with MWW(B2)

Table 2SD Pre and post denitrification cost calculation

Pre-denitrification:

Step-1 Assume

- The bioreactor volume ($V_1=1000 \text{ m}^3$)
- $MLVSS=3000 \text{ mg/L}$

Step-2 Calculate the nitrite mass removed per day under pre-denitrification scenario

- Consider maximum nitrite SDNR of 0.52 mgN/mgVSS-d (based on this study, carbon source MWW+methanol)
- $NO_2\text{-N} = 0.52 \text{ mgNO}_2\text{-N/mgVSS-d} \times 3000 \text{ mgVSS/L} \times 1000 \text{ m}^3 = 1560 \text{ gNO}_2\text{-N/d}$

Step -3 Estimate the equivalent post denitrification tank volume

- Consider maximum nitrite SDNR of $0.38 \text{ mgNO}_2\text{-N/mgVSS-d}$ (based on this study, Carbon source – methanol only)
- $V_2 = 1560 \text{ gNO}_2\text{-N}/(0.38 \text{ mgNO}_2\text{-N/mgVSS-d} \times 3 \text{ gVSS}) = 1368.42 \text{ m}^3$

Step -4 Calculate percent saving

$\% \text{ Savings (equipment, power and volume)} = 100 \times (1368.42 - 1000)/1000 = 36.8\%$