

## **Sewage treatment at 4 °C in anaerobic upflow reactors with and without a membrane – performance, function and microbial diversity**

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Supplementary material

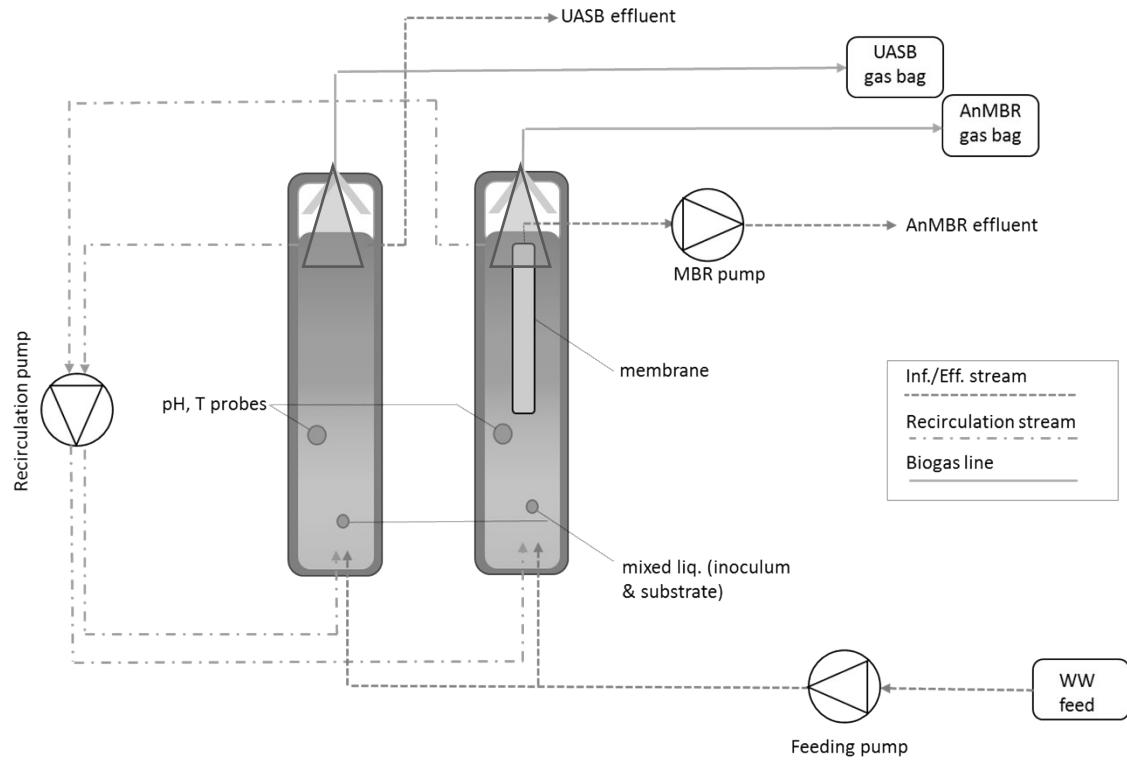


Figure S1 – Process scheme, as described by Petropoulos et al. (2019).

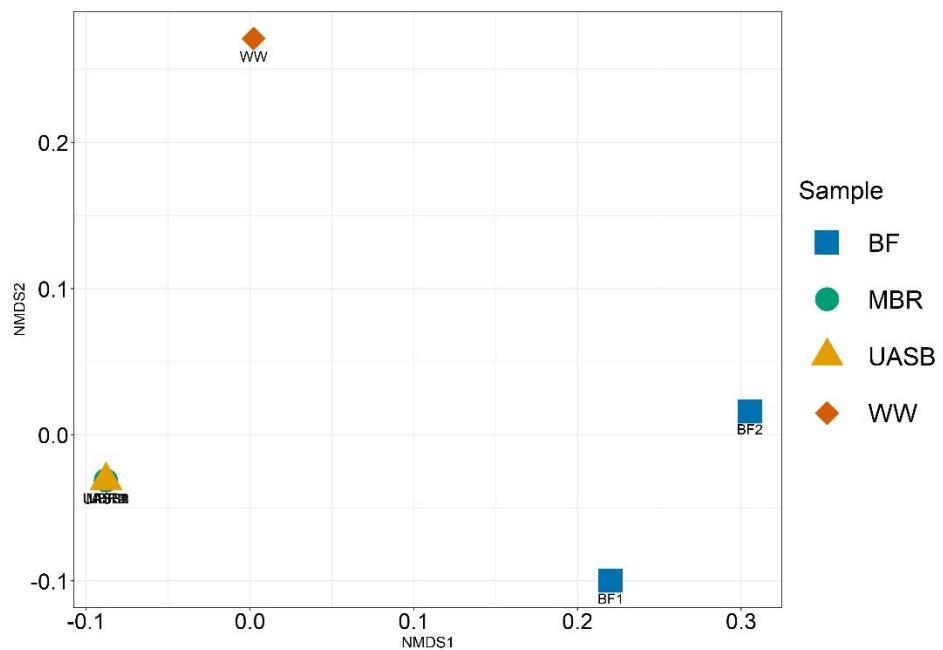
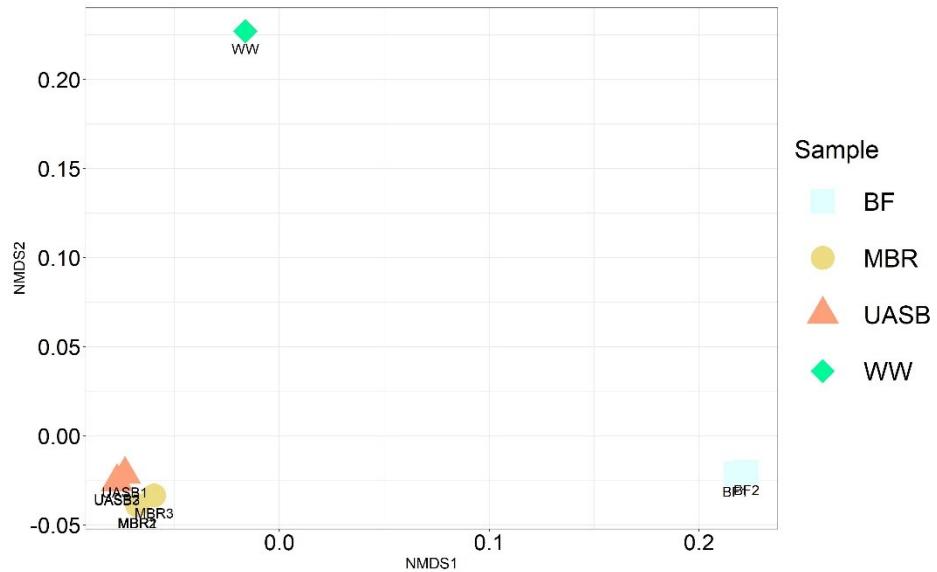


Figure S2 – NMDS plots for total bacteria (up) and archaea (bottom)

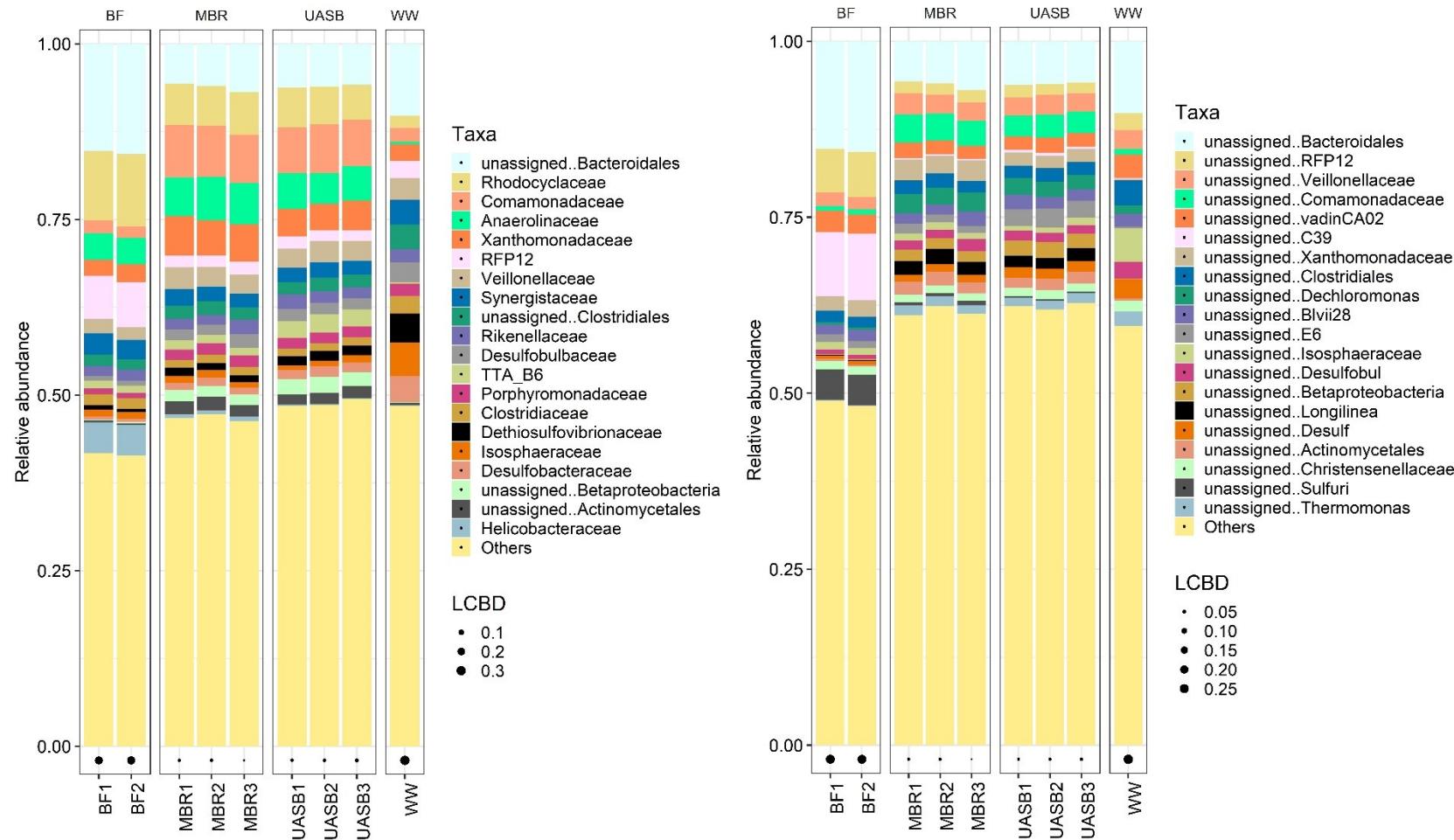


Figure S3 - Bar plot for total bacteria at a family (left) and species level (right); the plot shows the top 20 most abundant taxa whilst the rest are displayed as a group of 'others'; dots stand for the LCBD rate of the community; (WW stands for wastewater; BF stands for biofilm; UASB stands for the Upflow Anaerobic Sludge Blanket reactor; MBR stands for the Anaerobic Membrane Bio-Reactor).

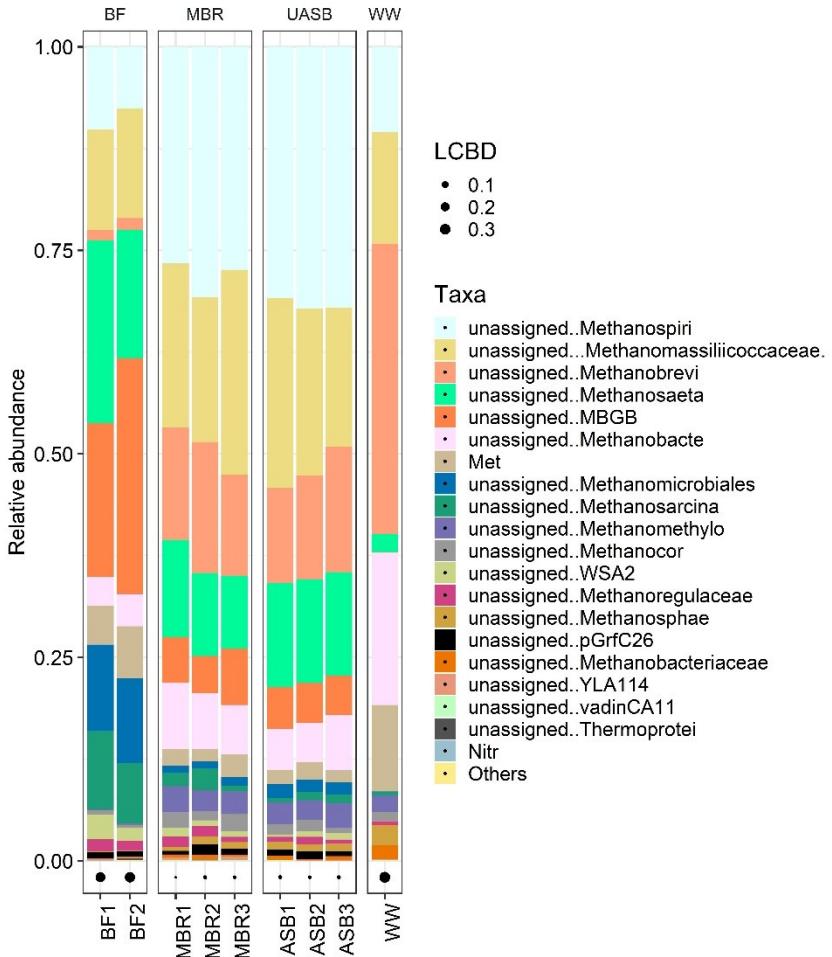
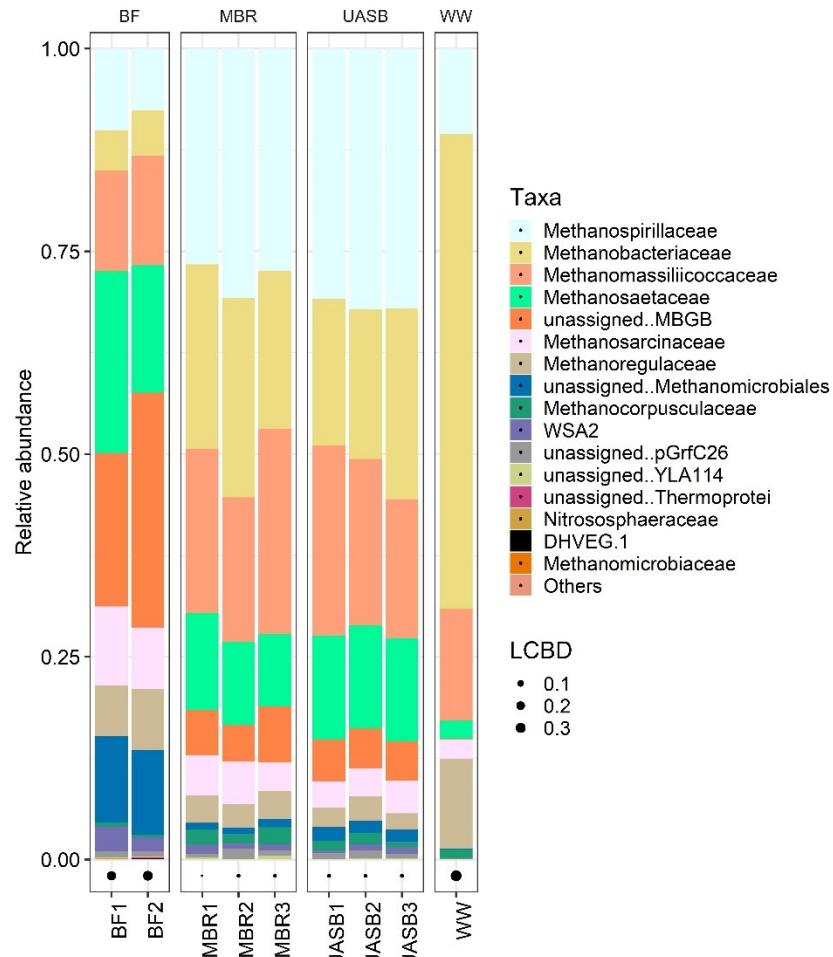


Figure S4 - Bar plot for total Archaea at a family (left) and species (right) level; the plot shows the top 20 most abundant taxa whilst the rest are displayed as a group of 'others'; dots stand for the LCBD rate of the community; (WW stands for wastewater; BF stands for biofilm; UASB stands for the Upflow Anaerobic Sludge Blanket reactor; MBR stands for the Anaerobic Membrane Bio-Reacter).

Table S1 - Net energy consumption and production from the methane produced at the AnMBR and the UASB during the steady methane peak periods (85-181)

General			
Steady period (days):	85-181		
Days:	85, 96, 130, 167, 181		
Observations (n):	5		
Energy production	MBR	UASB	
Reactor ID:			
mmol CH <sub>4</sub> .HRT <sup>-1</sup> (or mmol.L <sub>wastewater</sub> <sup>-1</sup> )	0.66	0.68	
mmol CH <sub>4</sub> .m <sub>wastewater</sub> <sup>-3</sup>	662.60	680.00	
mol CH <sub>4</sub> .m <sub>wastewater</sub> <sup>-3</sup>	0.66	0.68	
m <sup>3</sup> CH <sub>4</sub> .m <sup>-3</sup> WW	0.02	0.02	at STP 25°C
KWh.m <sup>-3</sup>	0.16	0.16	1.0 m <sup>3</sup> CH <sub>4</sub> :10.0 kWh
Actual KW.m <sup>-3</sup>	0.099	0.101	61.8% CHP efficiency (Li et al., 2011)
Energy use			
Minimum membrane operation (kWh.m <sup>-3</sup> )	0.30	0.00	Judd, 2010
Pumping wastewater (kWh.m <sup>-3</sup> )	0.02	0.02	Bodik and Kubaska, 2013
Mixing via pumping (kWh.m <sup>-3</sup> )	0.02	0.02	Bodik and Kubaska, 2013
Fouling mitigation via effluent pumping (kWh.m <sup>-3</sup> )	0.02	0.00	Bodik and Kubaska, 2013
Dissolved CH <sub>4</sub> strip (kWh.m <sup>-3</sup> )	0.05	0.05	McCarty et al., 2011
Total energy demand (kWh.m <sup>-3</sup> )	0.410	0.090	
Net energy			
Energy net (kWh.m <sup>-3</sup> )	-0.3113	0.0113	

\* Standard error for the gas production at normal operation regime (SO<sub>4</sub> reduction in) of 0.04 and 0.08 mmol CH<sub>4</sub>.HRT<sup>-1</sup> for AnMBR and UASB respectively

\*\* In the absence of SO<sub>4</sub> the methane rate was 0.82±0.16 and 1.06±0.17 mmol CH<sub>4</sub>.HRT<sup>-1</sup> corresponding to -0.288±0.024 and 0.0664±0.025 kW.m<sup>-3</sup> for the AnMBR and the UASB respectively

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