

## **Sewage treatment at 4 °C in anaerobic upflow reactors with and without a membrane – performance, function and microbial diversity**

Evangelos Petropoulos<sup>\*1</sup>, Burhan Shamurad<sup>1</sup>, Shamas Tabraiz<sup>1</sup>, Yongjie Yu<sup>1</sup>, Russell Davenport<sup>1</sup>, Thomas P. Curtis<sup>1</sup>, Jan Dolfig<sup>1, 2</sup>

<sup>1</sup>Newcastle University, School of Engineering, Newcastle upon Tyne, NE1 7RU, UK

<sup>2</sup>Northumbria University, Faculty Engineering and Environment, Newcastle upon Tyne, NE1 8QH, UK

Supplementary material

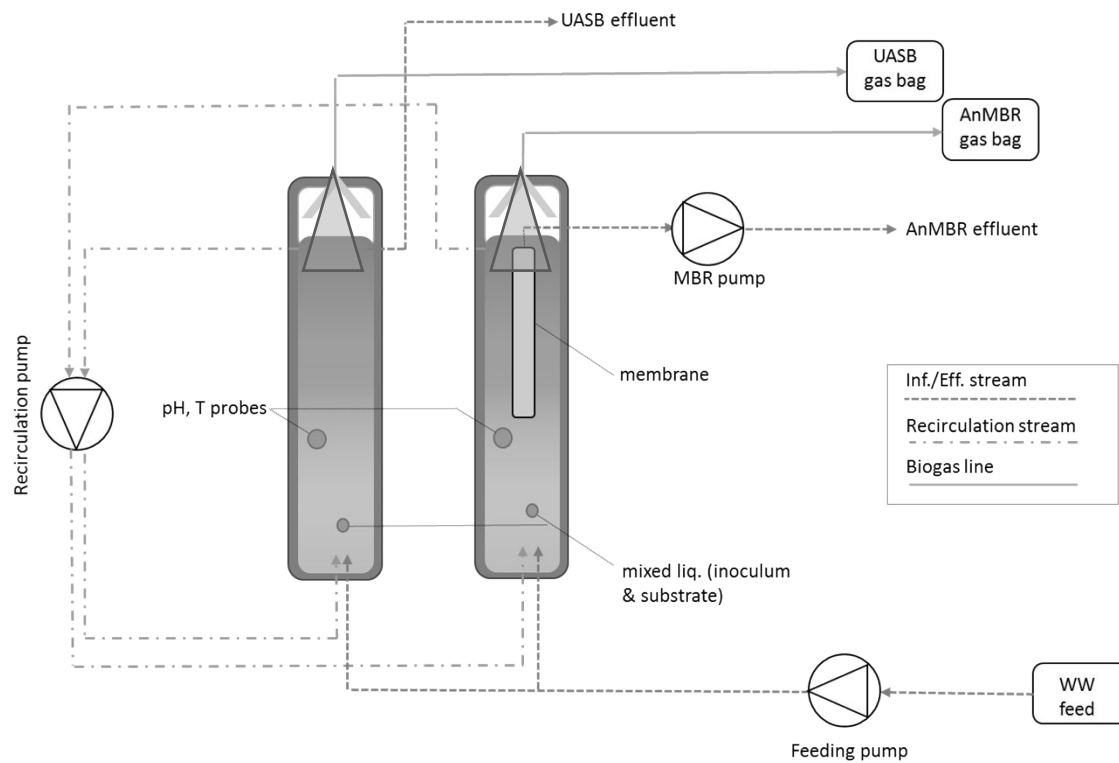


Figure S1 – Process scheme, as described by Petropoulos et al. (2019).

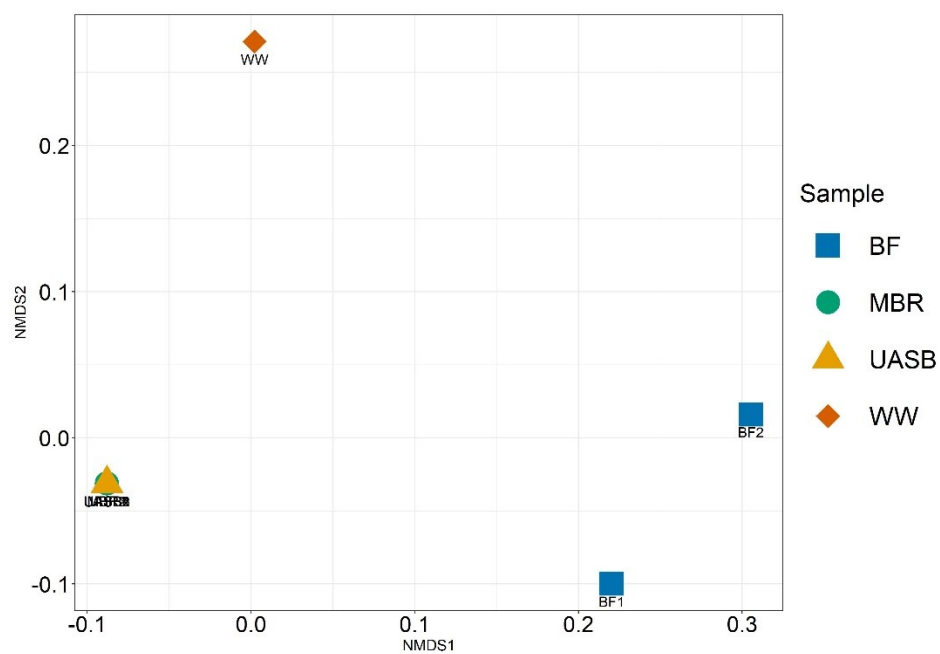
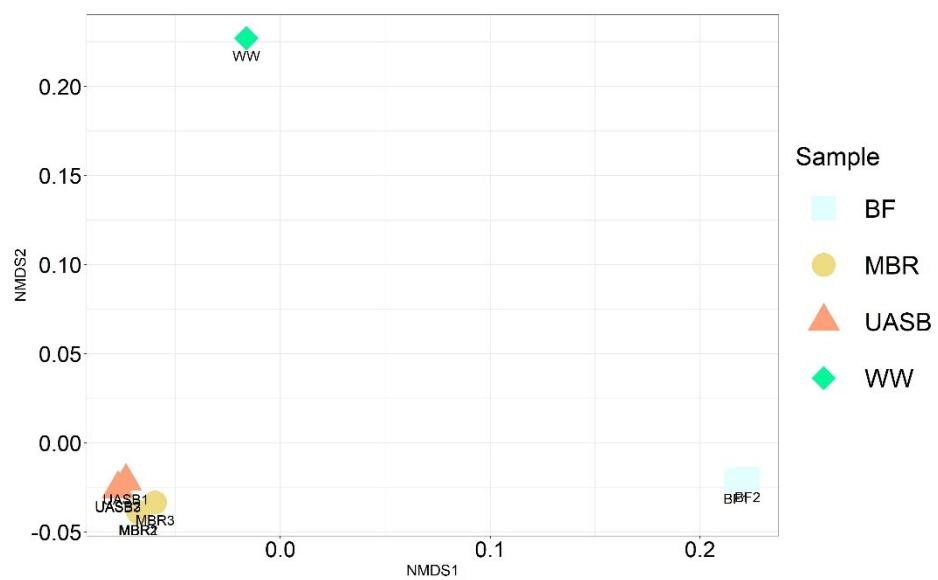


Figure S2 – NMDS plots for total bacteria (up) and archaea (bottom)

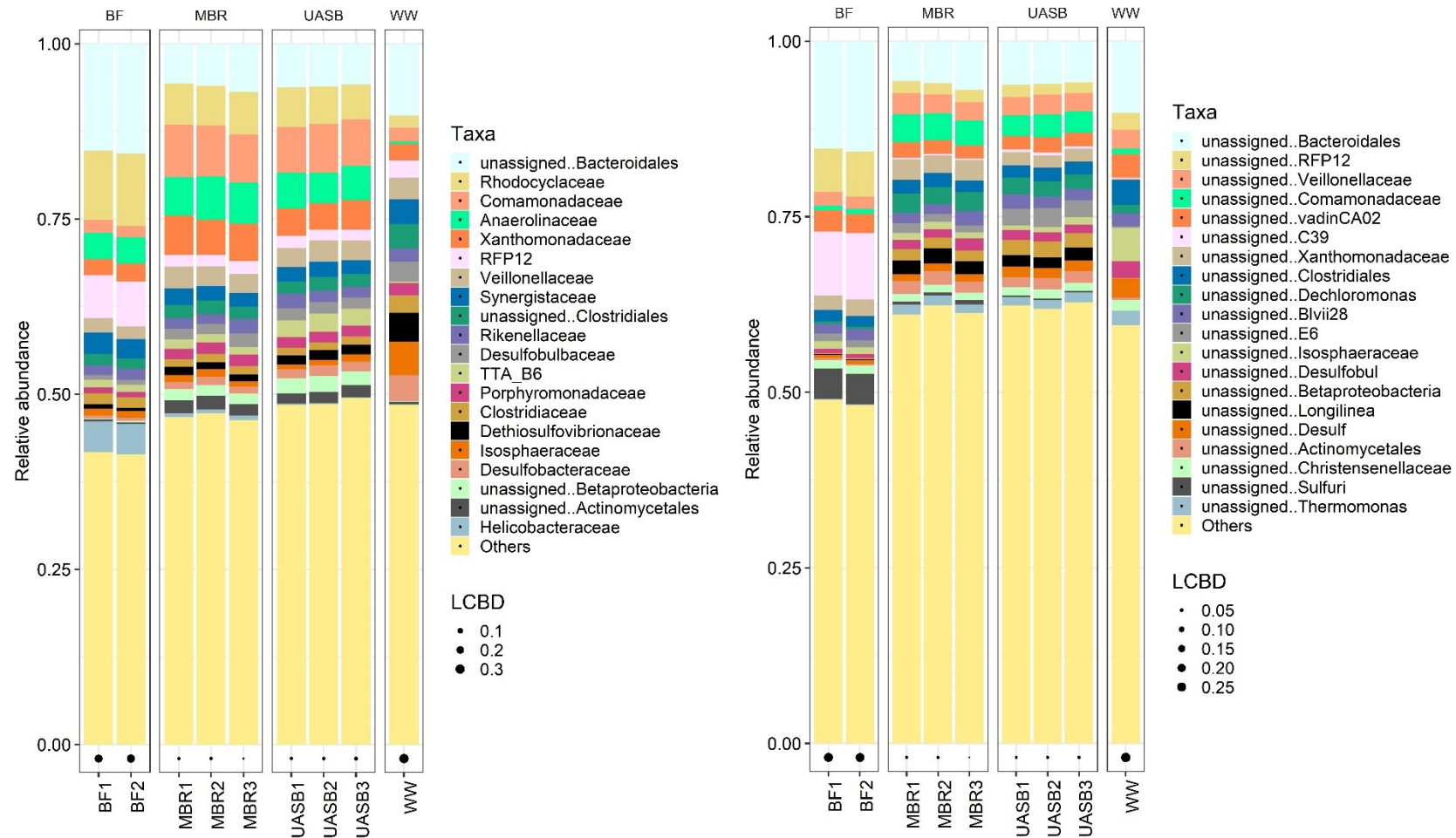


Figure S3 - Bar plot for total bacteria at a family (left) and species level (right); the plot shows the top 20 most abundant taxa whilst the rest are displayed as a group of 'others'; dots stand for the LCBD rate of the community; (WW stands for wastewater; BF stands for biofilm; UASB stands for the Upflow Anaerobic Sludge Blanket reactor; MBR stands for the Anaerobic Membrane Bio-Reactor).

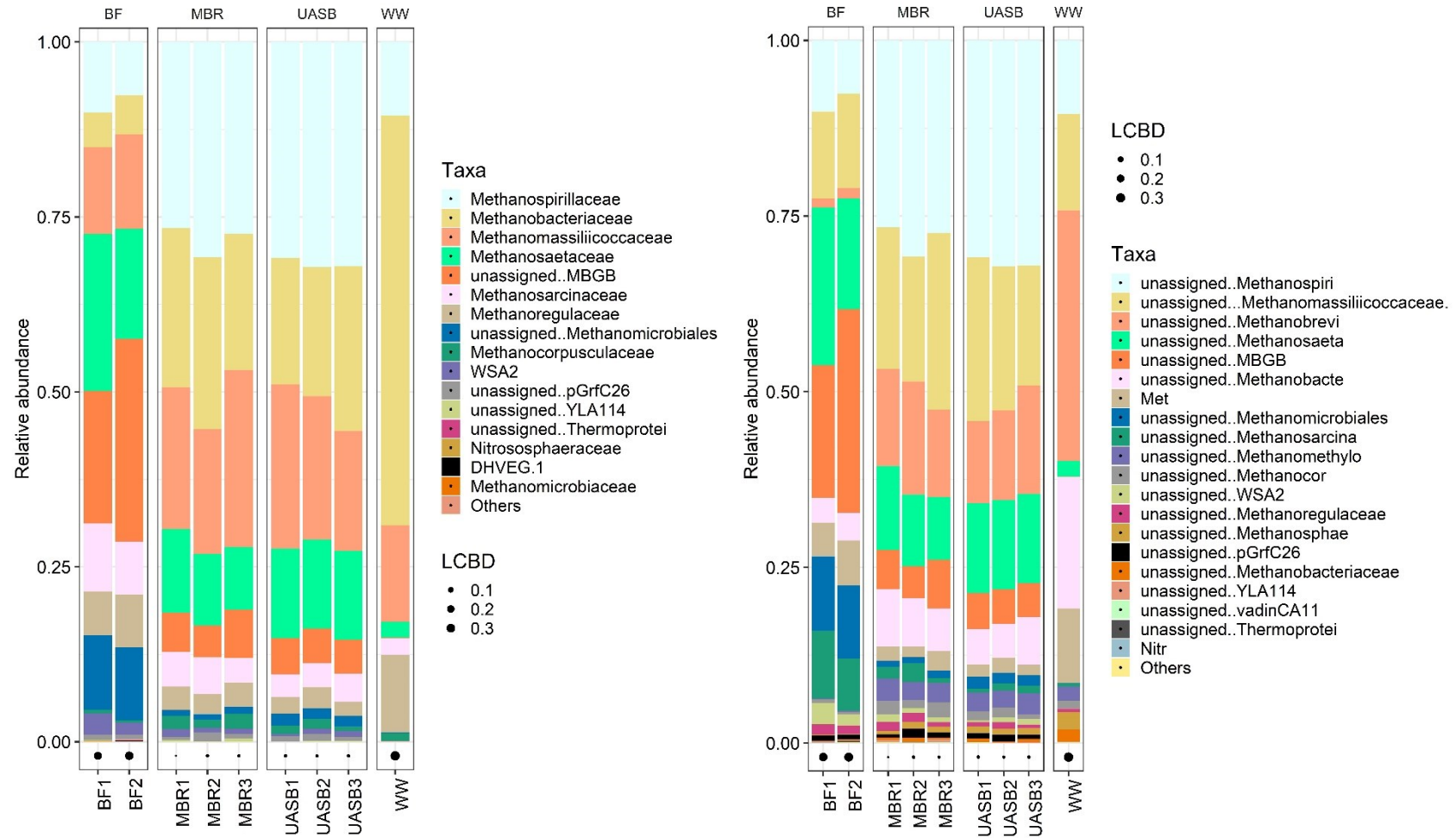


Figure S4 - Bar plot for total Archea at a family (left) and species (right) level; the plot shows the top 20 most abundant taxa whilst the rest are displayed as a group of 'others'; dots stand for the LCB rate of the community; (WW stands for wastewater; BF stands for biofilm; UASB stands for the Upflow Anaerobic Sludge Blanket reactor; MBR stands for the Anaerobic Membrane Bio-Reactor).

Table S1 - Net energy consumption and production from the methane produced at the AnMBR and the UASB during the steady methane peak periods (85-181)

General				
Steady period (days):		85-181		
Days:		85, 96, 130, 167, 181		
Observations (n):		5		
Energy production				
Reactor ID:		MBR	UASB	
mmol CH <sub>4</sub> .HRT <sup>-1</sup> (or mmol.L <sub>wastewater</sub> <sup>-1</sup> )		0.66	0.68	
mmol CH <sub>4</sub> .m <sub>wastewater</sub> <sup>-3</sup>		662.60	680.00	
mol CH <sub>4</sub> .m <sub>wastewater</sub> <sup>-3</sup>		0.66	0.68	
m <sup>3</sup> CH <sub>4</sub> .m <sup>-3</sup> WW		0.02	0.02	at STP 25°C
KWh.m <sup>-3</sup>		0.16	0.16	1.0 m <sup>3</sup> CH <sub>4</sub> :10.0 kWh
Actual KW.m <sup>-3</sup>		0.099	0.101	61.8% CHP efficiency ( <i>Li et al.,2011</i> )
Energy use			Reference	
Minimum membrane operation (kWh.m <sup>-3</sup> )		0.30	0.00	<i>Judd, 2010</i>
Pumping wastewater (kWh.m <sup>-3</sup> )		0.02	0.02	<i>Bodik and Kubaska, 2013</i>
Mixing via pumping (kWh.m <sup>-3</sup> )		0.02	0.02	<i>Bodik and Kubaska, 2013</i>
Fouling mitigation via effluent pumping (kWh.m <sup>-3</sup> )		0.02	0.00	<i>Bodik and Kubaska, 2013</i>
Dissolved CH <sub>4</sub> strip (kWh.m <sup>-3</sup> )		0.05	0.05	<i>McCarty et al., 2011</i>
Total energy demand (kWh.m <sup>-3</sup> )		0.410	0.090	
Net energy				
Energy net (kWh.m <sup>-3</sup> )		-0.3113	0.0113	

\* Standard error for the gas production at normal operation regime (SO<sub>4</sub> reduction in) of 0.04 and 0.08 mmol CH<sub>4</sub>.HRT<sup>-1</sup> for AnMBR and UASB respectively

\*\* In the absence of SO<sub>4</sub> the methane rate was 0.82±0.16 and 1.06±0.17 mmol CH<sub>4</sub>.HRT<sup>-1</sup> corresponding to -0.288±0.024 and 0.0664±0.025 kW.m<sup>-3</sup> for the AnMBR and the UASB respectively

I. Bodik and M. Kubaska, Energy and sustainability of operation of a wastewater treatment plant, *Environment Protection Engineering*, 2013, **39**, 15-24.

P. L. McCarty, J. Bae and J. Kim, Domestic Wastewater Treatment as a Net Energy Producer—Can This be Achieved?, *Environmental Science and Technology*, 2011, **45**, 7100-7106

S. Judd, *The MBR book: principles and applications of membrane bioreactors for water and wastewater treatment*, Elsevier, 2010.

Y. Li, Q. Qi., He, X. and J. Li, Energy use project and conversion efficiency analysis on biogas produced in breweries, Proceedings in World Renewable Energy Congress, 2011, Linköping, Sweden