

Supporting Information

Hydrodeoxygenation of Vegetable Oils over Biochar Supported Bimetallic Carbides for Producing Renewable Diesel under Mild Conditions

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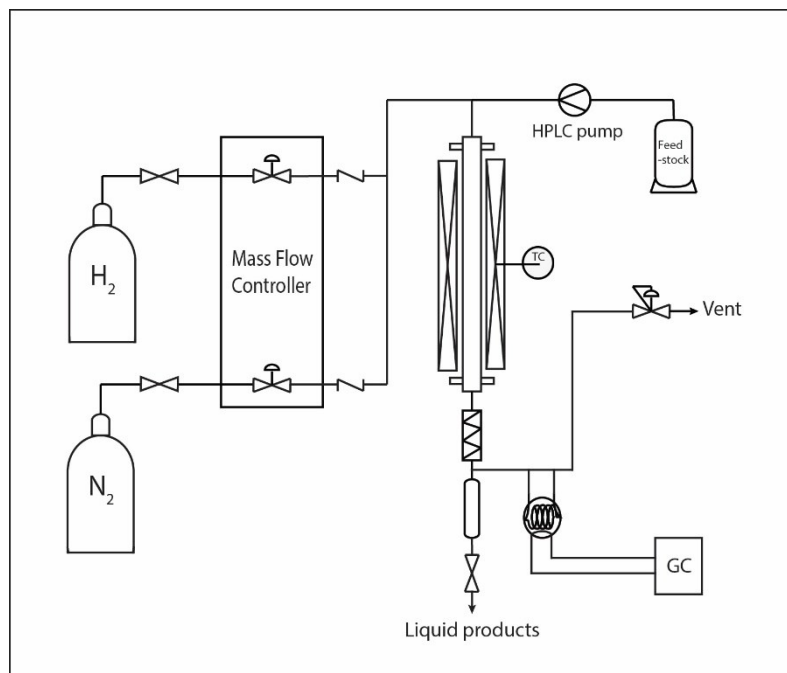


Figure S1. Continuous flow process diagram of HDO system

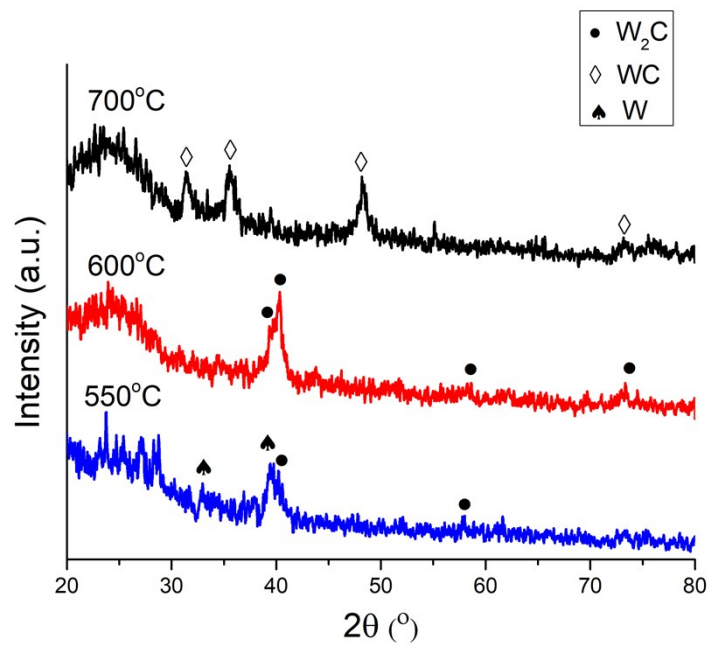


Figure S2. XRD diffractograms of biochar supported monometallic tungsten carbides WC/C prepared at different temperatures (550, 600, 700°C)

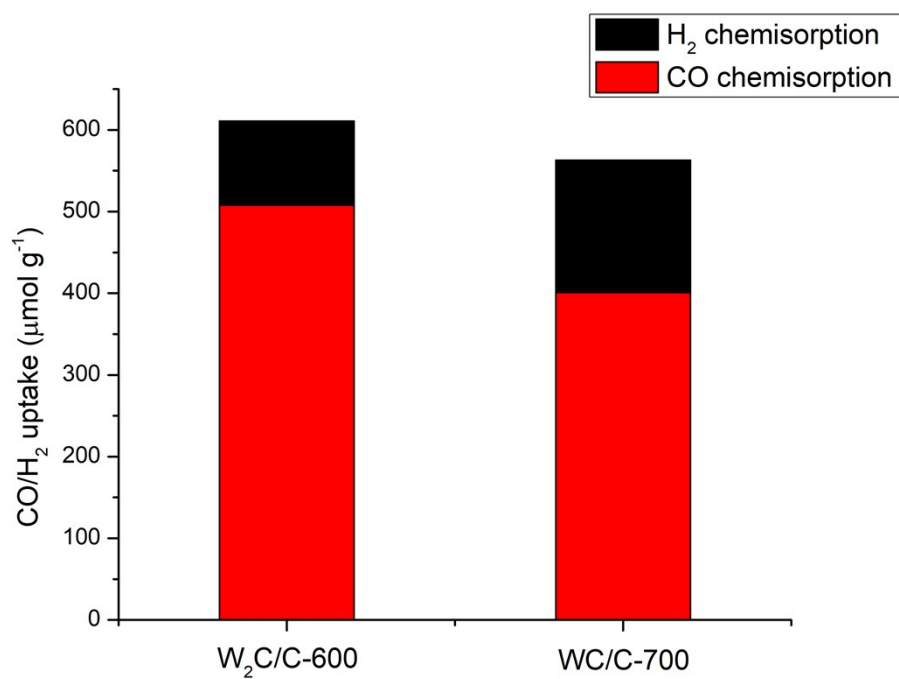


Figure S3. CO and H₂ uptake ($\mu\text{mol g}^{-1}$) of monometallic W carbides supported on biochar prepared at 600 and 700°C.

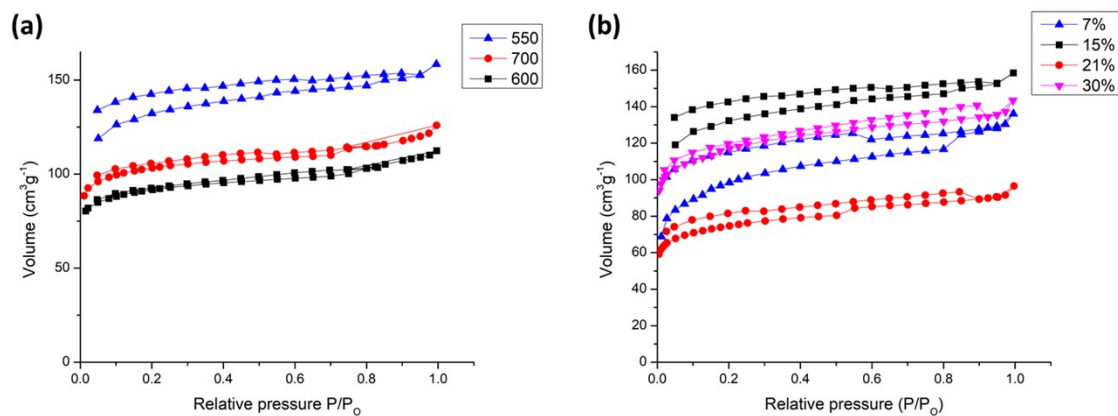


Figure S4. Physisorption isotherms of biochar supported bimetallic carbides synthesized at (a) different temperatures: 550, 600, and 700 °C; (b) different metal contents: 7, 15, 21, and 30 wt%.

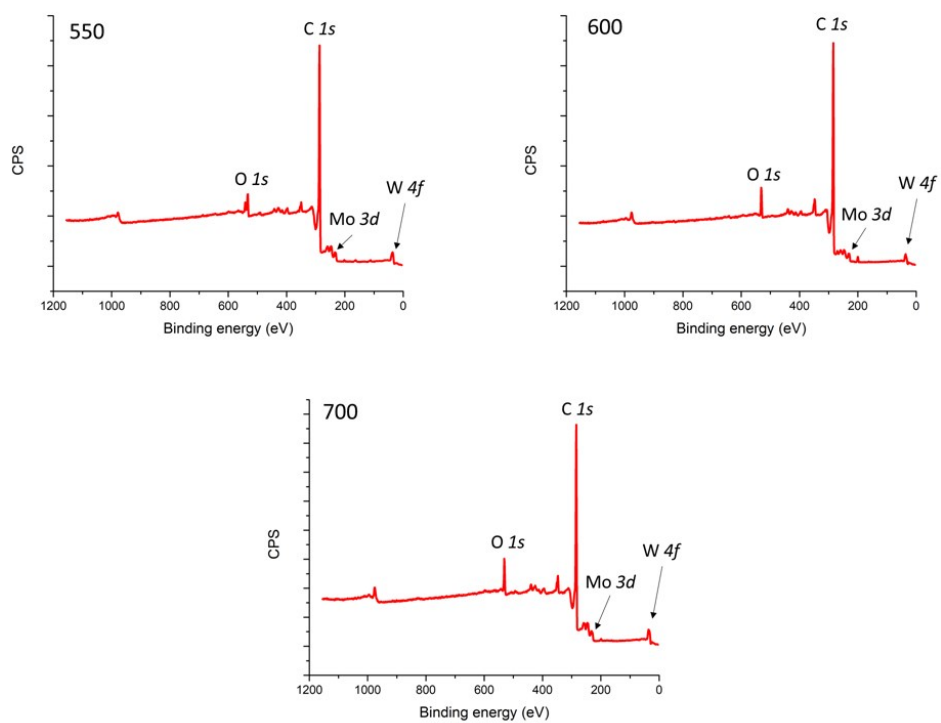


Figure S5. XPS survey spectra of MoWC/C carbides synthesized at 550, 600, and 700°C.

Table S1. Comparison of deoxygenation activity of vegetable oils and model compounds over various types of catalyst.

Catalysts	Reactant	Reaction conditions				Conversion [%]	Selectivity to hydrocarbons [%]	Ref
		T [°C]	P [psig]	LHSV ^a [h ⁻¹]	Time ^b [h]			
Mo ₂ C/NMC	Oleic acid	350	435	-	3	91.0	83.4	1
α-MoC _{1-x} /CNF	Stearic acid	350	580	-	6	92.0	-	2
β-Mo ₂ C/CNF	Stearic acid	350	580	-	6	85.0	-	2
Mo ₂ C/AC	Fatty acids	360	435	-	3	96	□85	3
Mo ₂ C/AC	Soybean oil	380	290	-	3	100	□100	4
β-Mo ₂ C/Al ₂ O ₃	Sunflower	360	725	5.0	-	100	90	5
W ₂ C/AC	Fatty acids	360	435	-	3	55	□53	3
NiMoC/ZSM5	Soybean	360-450	650	1.5	-	100	□50	6
NiMoC/Al-SBA-15	Soybean	400	600	1.0	-	96	97	7
MoC _x /Al ₂ O ₃	Rapeseed oil	350-390	797	1,2,4	-	-	□73-80	8
MoS ₂ /Al ₂ O ₃	Soybean oil	380	290	-	3	83.5	-	4
NiMoS/Al ₂ O ₃	Canola	350	450	1.0	-	100	77	9
CoMoS/Al ₂ O ₃	Canola	375	450	1.0	-	100	79	9
NiP/Al ₂ O ₃	Soybean oil	380	290	-	3	48.7	-	4
MoPx/Al ₂ O ₃	Rapeseed oil	350-390	797	1,2,4	-	-	-	8
Nitride NiMo/ZSM5	Soybean	360-450	650	1.5	-	100	□50	6
MoNx/Al ₂ O ₃	Rapeseed oil	350-390	797	1,2,4	-	-	-	8
MoO/Al ₂ O ₃	Soybean oil	380	290	-	3	85.6	-	4
Mo/Al ₂ O ₃	Soybean oil	380	290	-	3	68	-	4
Ni/Al ₂ O ₃	Canola	400	500	0.5	-	□80	92	10
Ni/Al ₂ O ₃	Soybean oil	380	290	-	3	18.1	-	4
Pd/C-biphasic	Stearic acid	260	400	-	6	100	□99	11
Pt/C	Oleic acid	350	435	-	3	79.8	69.1	1
MoWC/C	Canola oil	250	450	5.0	-	100	□ 87	Present work

^a liquid hourly space velocity (h⁻¹) for continuous reactor.

^b time of reaction (h) for batch reactor.

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