Selective production of bio-based para-xylene over FeOx-modified

Pd/Al₂O₃ catalyst

Yuxue Xiao, ^{a, b †} Qingwei Meng, ^{b †} Xiaoli Pan, ^b Chao Zhang, ^{*a} Zaihui Fu, ^a Changzhi Li^{*b, c}

^{a.} National & Local Joint Engineering Laboratory for New Petro-chemical Materials and Fine Utilization of Resources and Key Laboratory of Chemical Biology and Traditional Chinese Medicine Research (Ministry of Education), College of Chemistry and Chemical Engineering, Hunan Normal University, Chang sha 410081, Hunan

E-mail: chaozhang2006@126.com

^{b.} CAS Key Laboratory of Science and Technology on Applied Catalysis, Dalian Institute of Chemical Physics, Chinese Academy of Sciences, Dalian 116023, China

Email: licz@dicp.ac.cn

^c Dalian National Laboratory for Clean Energy, 457 Zhongshan Road, Dalian, 116023, China

+ These authors contributed equally to this work.

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Structure	Nomenclature	Abbreviation
Í)	Para-xylene	РХ
\bigcirc	Methyl cyclohexane	MCA
\bigcirc	4-Methyl-cyclohexene	MCE
\square	1,4-Dimethyl-cyclohexene	DMCE

2. Catalyst preparation

All the catalysts were prepared by incipient wetness impregnation method. For $1PdnFeOx/Al_2O_3$ (n=1, 3, 5, 7, 10, 15) catalysts, the support Al_2O_3 was impregnated in PdCl₂ aqueous solution for 5 h, followed by drying at 80 °C for 12 h. Then the obtained sample was impregnated in Fe(NO₃)₃ aqueous solution with calculated concentration. At last, the $1PdnFeOx/Al_2O_3$ catalyst was obtained by drying at 80 °C for 12 h and calcination at 500 °C for 4 h. $1Pd/Al_2O_3$ or $10FeOx/Al_2O_3$ catalyst was prepared with the similar procedure only without impregnation of PdCl₂ or Fe(NO₃)₃ aqueous solution. The nominal Pd loading of all the Pd-based catalysts is 1 wt%, and n indicates n% weight loading of Fe in $1PdnFeOx/Al_2O_3$ catalyst.

3. Catalyst characterization

 N_2 adsorption-desorption isotherms were performed at -196 °C with an ASAP-2010. Before N_2 adsorption, the samples were pretreated in a vacuum at 100 °C for 1 h and 300 °C for 4 h and then switched to the analysis station for adsorptiondesorption analysis.

X-ray powder diffraction (XRD) was recorded in the 2 θ range of 10–90° (scan rate = 5°/min) on an X'pert Pro PAN analytical X-ray diffractometer with a Ni-filtered Cu Ka radiation (40 kV, 30 mA). Prior to XRD experiments, the catalysts were reduced at 350 °C for 2 h.

TEM and HRSTEM of the reduced catalysts at 350 °C for 2 h were performed on a JEM-2100F high-resolution transmission electron microscope equipped with an energy-dispersive X-ray (EDX) detector operating at 200 kV.

 H_2 -TPR was carried out with a Micromeritics AutoChem 2920 apparatus. Prior to the measurement, the catalyst sample was pretreated in Ar flow at 120 °C for 2 h. After cooling to room temperature in Ar, the gas flow was switched to 10% H_2 /Ar and the sample was heated from room temperature to 800 °C with a temperature ramp of 5 °C/min. The results were recorded by Mass spectrum and TCD detector.

The in situ CO-FTIR and Propanal-FTIR was performed on an infrared spectrometer (VEREX70, Bruker, Germany). Prior to the adsorption of CO/propanal, the catalysts were reduced in H_2 flow (20 ml min⁻¹) at 350 °C for 2 h, purged with He for 0.5 h and cooled down to 20 °C. Then the samples were purged with helium and the CO-FTIR spectra were recorded.

X-ray photoelectron spectroscopy (XPS) patterns of the samples (at 350 °C for 2 h) were conducted on a Kratos AXIS ULTRA DLA X-ray photoelectron spectrometer equipped with a AI Kα radiation source (1486.6 eV, 15 kV) after reduced in situ at 350 °C for 2h. All binding energies were calibrated with the C1s peak at 284.8 eV for the adventitious carb.

CO-Chemisorption was conducted using dynamic pulse technique on Auto Chem. II 2920 equipment (Micromeritics, USA) at 20 °C using a pulse of 5% CO in He. Prior to the measurement, the samples were reduced in situ by flowing H_2 at 350 °C for 2 h and then purged with He for 30 min to remove hydrogen species adsorbed on the surface. **4. General procedure for the Diels–Alder reaction:** In a typical reaction, isoprene (30 mmol) was added slowly to ionic liquid [Bmim] Zn_2Cl_5 (2.5 mmol) and acrolein (25 mmol) at 25 °C under vigorous stirring for 24 h. Then, two phases were formed and the upper clear liquid was pipetted off for gas chromatographic analysis [Agilent Technologies 6890N, flame ionization detector (FID), 30 m x 0.32 mm x 0.25 mm HP-5 column, N₂ as carrier gas] with external standard. The isolated products were further purified by distillation (125 °C, 2 KPa) to afford the two regioselective cycloadducts para- and meta-MCHCA. The ionic liquid phase (bottom) was washed with hexane, purified under vacuum, and directly reused in subsequent runs.

5. Supplemental results





Reaction Conditions: diene (0.30 mol), dienophile (0.24 mol), [Bmim] Zn_2Cl_5 (10 mmol), reacting at 25 °C for 24 h.

	Catalyst	Con. Temp. (%) (°C)	Temp.	Yield (%)				
Entry			•	\bigcirc		\bigcup	\square	\square
1	1Pd10FeOx/Al ₂ O ₃	100	275	17.0	8.5	15.7	44.5	5.8
2	1Pd10FeOx/Al ₂ O ₃	100	300	4.1	18.9	4.0	70.1	2.8
3	1Pd10FeOx/Al ₂ O ₃	100	325	0.9	16.1	1.0	81.1	0.9
4	1Pd10FeOx/Al ₂ O ₃	100	375	0.2	16.0	1.1	80.0	2.7

Table S1. Catalytic conversion of 4-MCHCA to p-xylene over 1Pd10Fe/Al₂O₃ at different temperature.

Reaction conditions: 4-MCHCA concentration: 20 mg/mL; solvent: hexane; Flow rate of feed solution: 2.5 mL/min; Catalyst: 0.25 g; Carrier gas: H₂ (10 ml·min⁻¹).

5.3

Table S2. CO-Chemisorption results of the catalysts.

Catalyst	Metal cont	ent (wt. %)	CO chemisorption	
	Pd	Fe	(µmol/g⁻¹)	
$1Pd/Al_2O_3$	1	0	17.49	
1Pd1FeOx/Al ₂ O ₃	1	1	18.89	
1Pd5FeOx/Al ₂ O ₃	1	5	4.89	
1Pd10FeOx/Al ₂ O ₃	1	10	4.64	
10FeOx/Al ₂ O ₃	0	10	0	

5.2





5.4



Figure S2. XRD patterns of freshly reduced and used $1Pd10FeOx/Al_2O_3$ catalysts.

5.6

 Table S3.
 BET results of the catalysts.

		Surface Area	Pore	Pore
Entry	Catalyst		volume (cm³	diameter
		(cm²/g)	/ g)	(nm)
1	Al ₂ O ₃	207.223	0.775	12.471
2	$1Pd/Al_2O_3$	206.042	0.753	12.435
3	$1Pd1FeO_X /Al_2O_3$	198.75	0.724	12.405
4	$1Pd3FeO_X /Al_2O_3$	197.322	0.704	12.320
5	$1Pd5FeO_X /Al_2O_3$	190.445	0.688	12.475
6	$1Pd7FeO_X/Al_2O_3$	189.345	0.647	12.337
7	$1Pd10FeO_X/Al_2O_3$	177.666	0.533	9.606