## **Supplementary Information**

# Tuning selectivity of CO<sub>2</sub> hydrogenation by modulating the strong metal–support interaction over Ir/TiO<sub>2</sub> catalysts

Yaru Zhang,<sup>a,b</sup> Zhen Zhang,<sup>c</sup> Xiaofeng Yang,<sup>a</sup> Ruifeng Wang,<sup>a</sup> Hongmin Duan,<sup>a</sup> Zheng Shen,<sup>a</sup> Lin Li,<sup>a</sup> Yang Su,<sup>a</sup> Runze Yang,<sup>c</sup> Yongping Zhang,<sup>c</sup> Xiong Su,<sup>\*a</sup> Yanqiang Huang,<sup>\*a</sup> and Tao Zhang<sup>d</sup>

<sup>a</sup> CAS Key Laboratory of Science and Technology on Applied Catalysis, Dalian Institute of Chemical Physics, Chinese Academy of Sciences, Dalian 116023, China
<sup>b</sup> University of Chinese Academy of Sciences, Beijing 100049, China
<sup>c</sup> China Astronaut Research and Training Center, Beijing 100094, China
<sup>d</sup> State Key Laboratory of Catalysis, Dalian Institute of Chemical Physics, Chinese Academy of Sciences, Dalian 116023, China

\*To whom correspondence should be addressed. E-mail: <u>yqhuang@dicp.ac.cn</u> (Y. Huang) and <u>suxiong@dicp.ac.cn</u> (X. Su).

### **Supplementary Figures**



**Fig. S1.** Evolution of catalytic performance versus time and reaction temperature, over the (a)  $Ir/TiO_2$ -200 and (b)  $Ir/TiO_2$ -700 catalysts. Reaction conditions: atmospheric pressure, space velocity = 9000 mL h<sup>-1</sup> gcat<sup>-1</sup>, H<sub>2</sub>/CO<sub>2</sub>/N<sub>2</sub> = 70/20/10.



Fig. S2. Arrhenius plots for CO production over the  $Ir/TiO_2$ -x catalysts.



Fig. S3.  $N_2$  adsorption-desorption isotherms for the series Ir/TiO<sub>2</sub>-x catalysts.



**Fig. S4.** XRD patterns of the series Ir/TiO<sub>2</sub>-*x* catalysts.

#### **Supplementary Tables**

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Entry	Catalyst	H <sub>2</sub> /	Р	Т	Reaction rate	S <sub>CH4</sub>	S <sub>CO</sub>	Def
		$CO_2$	(MPa)	(°C)	$(mol_{CO2} g_{metal}{}^{-1} h^{-1})$	(%)	(%)	Kel.
1	2.45 wt% Ir/TiO <sub>2</sub> -200	3.5	0.1	280	0.159	100	0	This
2	2.45 wt% Ir/TiO <sub>2</sub> -700	3.5	0.1	280	0.146	0	100	I IIIS
3	2.45 wt% Ir/TiO <sub>2</sub> -200	3.5	0.1	400	0.769	87.4	12.6	WOLK
4	0.1 wt% Ir <sub>1</sub> /TiO <sub>2</sub>	1	0.1	350	0.043	0	~100	1
5	0.7 wt% Ir/Ce	4	1.0	300	0.422	trace	> 99	2
6	20 wt% Ir/Ce	4	1.0	300	0.045	88	12	2
7	6 wt% Rh/TiO <sub>2</sub>	1	0.1	200	0.028	98	2	3
8	2.56 wt% Ru(NC)/CeO <sub>2</sub>	4	0.1	190	0.264	> 98	< 2	4
9	5 wt% Ru/r-TiO <sub>2</sub>	4	0.1	200	0.73	100	0	5
10	0.5 wt% Pd/Al <sub>2</sub> O <sub>3</sub>	3	0.1	300	0.128	~10	~90	6
11	0.1 wt% Pt/TiO <sub>2</sub>	1	0.1	250	0.024	< 2	> 98	7
12	4 wt% AuMo/SiO <sub>2</sub>	2	0.81	300	0.525	0	100	8
13	10 wt% Co/r-TiO <sub>2</sub>	4	3.0	400	0.549	99.8	0.2	0
14	10 wt% Co/a-TiO <sub>2</sub>	4	3.0	400	0.091	10.5	89.5	9
15	5 wt% Ni/a-TiO <sub>2</sub>	4	0.1	360	0.127	0	100	10
16	5 wt% Ni/a-TiO <sub>2</sub> -NH <sub>3</sub>	4	0.1	360	1.481	96.9	3.1	10

**Table S1.** Comparison of the catalytic performance for  $CO_2$  hydrogenation over different catalysts.

A comparison of the catalytic performance for  $CO_2$  hydrogenation in this work with that of state-of-the-art catalysts as well as catalysts without precious metals is shown in Table S1.

As compared with other reported Ir-based catalysts (Entry 4–6), Ir/TiO<sub>2</sub>-200 in this work exhibits a much higher activity for CO<sub>2</sub> methanation, and Ir/TiO<sub>2</sub>-700 catalyst exhibits at least comparable activity for reverse water-gas shift reaction.

For Sabatier reaction (Entry 7–9), the activity of  $Ir/TiO_2$ -200 in this work is inferior to that of Ru-based catalysts, but at least a comparable value with that of Rh-based catalysts. As for reverse water-gas shift reaction (Entry 10–12),  $Ir/TiO_2$ -700 exhibits comparable or higher activity with the reported catalysts.

When it comes to Co-based (Entry 13, 14) or Ni-based (15, 16) catalysts for  $CO_2$  hydrogenation, a higher reaction temperature or pressure is usually employed to initiate  $CO_2$  activation. For  $CO_2$  methanation, the Ir/TiO<sub>2</sub>-200 catalyst shows a higher activity than Co-based catalysts, but lower than that of Ni-based catalysts. For reverse water-gas shift reaction, the Ir/TiO<sub>2</sub>-700 catalyst shows a higher activity than both Co-based catalysts.

Catalvat	$E_a$ (CO <sub>2</sub> )	$E_a$ (CO)	$E_a$ (CH <sub>4</sub> )
Catalyst	(kJ mol <sup>-1</sup> )	(kJ mol <sup>-1</sup> )	(kJ mol <sup>-1</sup> )
Ir/TiO <sub>2</sub> -200	42.5	_	39.6
Ir/TiO <sub>2</sub> -300	40.5	_	42.0
Ir/TiO <sub>2</sub> -400	45.4	50.7	44.1
Ir/TiO <sub>2</sub> -500	40.5	41.9	58.4
Ir/TiO <sub>2</sub> -600	44.1	41.1	110.6
Ir/TiO <sub>2</sub> -700	47.1	41.1	233.9

**Table S2.** Apparent activation energies obtained from Arrhenius plots for the series  $Ir/TiO_2$ -*x* catalysts.

**Table S3.** BET surface areas and pore volumes of the series  $Ir/TiO_2$  catalysts pretreated at different temperatures ( $Ir/TiO_2$ -*x* samples).

Catalyst	$S_{BET}\left(m^2 \ g^{-1}\right)$	$V_{pore} (cm^3 g^{-1})$
Ir/TiO <sub>2</sub> -200	26	0.038
Ir/TiO <sub>2</sub> -300	27	0.041
Ir/TiO <sub>2</sub> -400	26	0.038
Ir/TiO <sub>2</sub> -500	25	0.036
Ir/TiO <sub>2</sub> -600	25	0.037
Ir/TiO <sub>2</sub> -700	25	0.033

Oxide	Crystal form	M–O bond distance	Lattice spacing (nm)		
		(nm)	a, b axis	c axis	
IrO <sub>2</sub>	rutile	0.1958	0.4505	0.3158	
TiO <sub>2</sub>	rutile	0.1980	0.4594	0.2958	

**Table S4.** The crystal parameters of rutile-type  $IrO_2$  and  $TiO_2$ .

**Table S5.**  $H_2$  consumption results of the Ir/TiO<sub>2</sub> catalyst.

Sample	$H_{T}$ , theoretical	H <sub>M</sub> , measured	- U /U		
	value <sup>[a]</sup> ( $\mu$ mol g <sup>-1</sup> )	50–285 °C	285–800 °C	50–800 °C	$\Pi_{M}/\Pi_{T}$
Ir/TiO <sub>2</sub>	254.9	253.7	149.0	402.7	1.6

[a] The theoretical  $H_2$  consumption ( $H_T$ ) was estimated by the assumption of complete IrO<sub>2</sub> reduction with 2.45 wt% Ir loading.

	Ti <sup>4+</sup>			Ti <sup>3+</sup>		
Sample	Bind energy (eV)		Contont	Bind energy (eV)		Contont
	2p <sub>1/2</sub>	2p <sub>3/2</sub>	- Content -	2p <sub>1/2</sub>	2p <sub>3/2</sub>	Content
Ir/TiO <sub>2</sub> -200	464.1	458.5	98.9%	463.3	457.8	1.1%
Ir/TiO <sub>2</sub> -400	464.1	458.5	92.7%	463.2	457.7	7.3%
Ir/TiO <sub>2</sub> -600	464.1	458.4	91.4%	463.2	457.7	8.6%
Ir/TiO <sub>2</sub> -700	464.1	458.4	90.3%	463.2	457.7	9.7%

**Table S6.** Quantified XPS data for surface Ti on the series Ir/TiO<sub>2</sub>-*x* catalysts.

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