# **Supporting Information**

# Electrodeposited Cu-Pd Bimetallic Catalysts for the Selective Electroreduction of CO<sub>2</sub> to Ethylene

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## **Experimental Section**

## Materials

Palladium (II) sulfate (PdSO<sub>4</sub>), Copper (II) sulfate (CuSO<sub>4</sub>·5H<sub>2</sub>O), sulfuric acid (H<sub>2</sub>SO<sub>4</sub>), Toray Carbon Paper (CP, TGP-H-60, 19 cm  $\times$  19 cm), and Nafion N-117 membrane (0.180 mm thick,  $\geq$  0.90 meg/g exchange capacity) were purchased from Alfa Aesar China Co., Ltd. Both CO<sub>2</sub> and N<sub>2</sub> had a purity of 99.999%, and were provided by Shanghai Chemistry Industrial Zone Pujiang Special Type Gas Co., Ltd.

## Preparation of Cu-Pd bimetallic catalysts

Electrochemical deposition was carried out using a solution of 0.1 M CuSO<sub>4</sub>, 1 mM PdSO<sub>4</sub>, and 0.1 M H<sub>2</sub>SO<sub>4</sub> in a 50 mL electrolytic tank. Carbon paper and Pt gauze with 1 cm<sup>2</sup> area each acted as cathode and anode. The electrodeposition was conducted by high resolution DC power supply (HY3005B, Hangzhou Huayi Electronics Industry Co., Ltd.) which outputted a steady current for desired time.

Other electrocatalysts (Cu-Pd/CP-CV, Cu-Pd/CP-IT) were synthesized by electrochemical workstation (Voltammetry and Amperometric-i-t) in three electrode system for comparison. The number of electrons was controlled to 12 coulombs, cyclic voltammetry and Amperometry were performed at -0.2 V with scan rate 50 mv s<sup>-1</sup>, respectively.

#### Characterization

The morphology of the electrodes was characterized by Hitachi S4800 scanning electron microscope (SEM) at 3 kV and transmission electron microscopy (TEM, JEOL JEM-2100F) equipped with EDS. X-ray diffraction (XRD) analysis of the samples were performed on Rigaku and model with CuK $\alpha$  radiation (1.5418 Å). X-ray photoelectron spectroscopy (XPS) study was carried out on the AXIS Supra surface analysis instrument with an X-ray monochromatic source (combined Al/Ag anode, energy 1486.6/2984.2eV) and studies were performed in 10<sup>-9</sup> mbar vacuum.

#### **Electrochemical study**

All the electrochemical experiments were conducted on the electrochemical workstation (CHI 660E, Shanghai CH Instruments Co., China). Linear sweep voltammetry (LSV) measurement was carried out in a two-compartment H-cell separated by an ion exchange membrane (Nafion 117) with three electrodes on an electrochemical workstation (CHI 660E, Shanghai CH Instruments Co., China), which were a working electrode (Cu-Pd), a platinum gauze auxiliary electrode, and an Ag/AgCl (3M KCl). 0.1 M KCl solution and 0.1 M KHCO<sub>3</sub> solution were utilized as the cathode and anodic electrolytes, respectively.<sup>[1]</sup> In all measurements, we used Ag/AgCl as the reference electrode, and the potential (vs. Ag/AgCl) was converted to RHE using the following equation<sup>[2]</sup>:

#### $E(RHE) = E(Ag/AgCl) + 0.197 + 0.059 \times pH$

The electrolytes were bubbled with  $CO_2$  or  $N_2$  at least 30 min to ensure formation of  $N_2$ -saturated or  $CO_2$ -saturated solution before experiments. LSV measurements in gas-saturated electrolytes were carried out in the potential range of 0 V to -1.4 V versus RHE at a sweep rate of 50 mV s<sup>-1</sup>. Slight magnetic stirring was employed to acquire uniform electrolytes.

#### Electrochemical impedance spectroscopy (EIS) measurements

The experimental apparatus was the same as that used for the LSV measures. Measurements were carried out in CO<sub>2</sub>-saturated 0.1 M KCl solution at an open circuit potential (OCP) with a frequency range from  $10^{-2}$  Hz to  $10^{5}$  Hz and the amplitude was 5 mV. The data were fitted by View<sup>®</sup> software (Version 2.9c, Scribner Associates, USA).

#### CO<sub>2</sub> reduction electrolysis

The electroreduction of  $CO_2$  was performed at room temperature in a gas-tight H-type electrolysis cell separated by an ion exchange membrane (Nafion 117), which is equipped with a three-electrode system including a working electrode (Cu-Pd), a platinum gauze auxiliary electrode, and an Ag/AgCl (3 M KCl) reference electrode. In the experiments, 0.1 M KCl (30 mL) solution and 0.1 M KHCO<sub>3</sub> (30 mL) solution were utilized as catholyte and anolyte, respectively. Before the electrolysis,  $CO_2$  was bubbled through the cathodic electrolyte for 30 min to remove the air and form a  $CO_2$ -suturated solution. The reaction was performed with a steady flow of  $CO_2$  (10 sccm) at a constant potential. Before electrolysis, the cathode was electrochemically reduced using cyclic voltammetry (CV), which ranged from 0 to -1.4V (vs. RHE) at a scan rate of 100 mV s<sup>-1</sup> for 5 cycles to remove the possible oxidized species.

#### **Product analysis**

After the electrolysis reaction, the gas-phase products were analyzed by a gas chromatograph (GC; Agilent-8890A), which was equipped with TCD detector. The liquid product was quantified using a nuclear magnetic resonance (NMR) spectrometry (Bruker, Ascend 400-400 MHz) in [D<sub>6</sub>] DMSO with phenol as the internal standard. The Faradaic efficiency (FE) of the products was calculated using FE= $\alpha$ nF/Q, where  $\alpha$  is the number of electrons transferred in the electrochemical reaction, n is the number of moles for a given products, F is Faraday's constant (96485 C mol<sup>-1</sup>), and Q represents all the charge passed throughout the electrolysis process.

#### Double-layer capacitance (C<sub>dl</sub>) measurements.

The electrochemical active surface area is proportional to  $C_{dl}$  value.  $C_{dl}$  was determined in H-type electrolysis cell by measuring the capacitive current associated

with double-layer charging from the scan-rate dependence of cyclic voltammogram (CV). The CV ranged from -1.35 V -1.45 V vs. Ag/AgCl. The C<sub>dl</sub> was estimated by plotting the  $\Delta j$  ( $j_a$ - $j_c$ ) at -1.35 V vs Ag/AgCl against the scan rates, in which the  $j_a$  and  $j_c$  were the anodic and cathodic current density, respectively.

#### **Supplementary Figures**



Figure S1. LSV of Cu-Pd/CP in N<sub>2</sub>-and CO<sub>2</sub>-saturated 0.1 M KCl.



Figure S2. Charging current density against scan rates over different electrodes in  $CO_2$  saturated 0.1 M KCl electrolyte.



Figure S3. Nyquist plots over the four electrodes (CP, Cu/CP, Pd/CP and Cu-Pd/CP).



**Figure S4**. Equivalent circuit used for fitting the data of Nyquist plots. The components contain solution resistance (Rs), double layer capacitance ( $CPE_{dl}$ ), electron transfer resistance ( $R_{ct}$ ), film capacitance ( $C_f$ ), film resistance (Rf) and Warburg-type impedance ( $Z_w$ ).



**Figure S5.** The FE of  $C_2H_4$  over Cu-Pd/CP catalyst in various electrolytes at -1.2 V vs. RHE.



Figure S6. SEM images: A) Cu-Pd/CP-CV catalyst; B) Cu-Pd/CP-IT catalyst.



**Figure S7.** XPS spectra of: A) Cu 2p, B) Pd 3d XPS spectra of Cu-Pd/CP, Cu–Pd/CP-CV and Cu-Pd/CP-IT.



**Figure S8**. XPS spectras of Cu 2p of A) Cu-Pd/CP-CV and C) Cu-Pd/CP-IT catalysts, Pd3p of B) Cu-Pd/CP-CV and D) Cu-Pd/CP-IT. E) Cu/CP and F) Pd/CP.



**Figure S9.** A) Nyquist plots B) and C) Bode plots obtained for three electrodes (Cu-Pd/CP, Cu-Pd/CP-CV, Cu-Pd/CP-IT) in CO<sub>2</sub>-saturated 0.1 M KCl solution.



**Figure S10.** SEM images of Cu-Pd/CP catalysts under the deposition current of A) 8.7mA (-0.1 V), B) 25.4 mA (-0.4 V), C) 26 mA (-0.6 V), D) 32.5 mA (-0.8 V) vs. Ag/AgCl.



Figure S11. Cyclic voltammetry curves of bulk carbon paper in three electroplating baths.



Figure S12. SEM images of A) 5 min, B) 10 min, C) 15 min, D) 20 min deposition time at 20 mA cm<sup>-2</sup>.

# **Supplementary Tables**

Electrocatalyst	Potential / V	Electrolyte	FE/%	Current density / mA cm <sup>-2</sup>	Ref.
H-type cell					
Bimetallic Cu-Pd catalysts	-1.2 V vs. RHE	0.1 M KCl	45.2	17.4	This work
$Cu_{10}$ -Sb <sub>1</sub>	-1.19 V vs. RHE	0.1 M KCl	49.5	28.5	[2]
Ag/Cu nanocrystals	–1.1 V vs. RHE	0.1 M KHCO3	40	1.0	[3]
Carbon–supported Cu catalyst	–2.2 V vs. Ag/AgCl	0.1 M KHCO <sub>3</sub>	45	22.5	[4]
Ag-Cu arrays	-1.2 V vs. RHE	0.5 M KHCO <sub>3</sub>	41.3	8.45	[5]
Cu <sub>2</sub> O/rGO	-1.4 V vs. RHE	0.1 M KHCO <sub>3</sub>	19.7	12	[6]
Cu-C <sub>3</sub> N <sub>4</sub>	1.6 V vs Ag/AgCl	0.1 M KHCO <sub>3</sub>	10	~7.5	[7]
Cu-Zn bimetallic catalyst	–1.1 V vs. RHE	0.1 M KHCO3	33.3	6.1	[8]
Cu/ICTF <sub>50</sub>	-1.3 V vs. RHE	0.1 M KCl+ 0.1 M KHCO <sub>3</sub>	34	11.8	[9]
4H Au@Cu nanoribbon	-1.11 V vs RHE	0.1 M KHCO <sub>3</sub>	44.9	30.2	[10]
GMC-[Cu <sub>2</sub> (NTB) <sub>2</sub> ]	-1.27 V vs RHE	0.1 M KCl	40	13	[11]
Flow cell					
Cu/N-CNF	-0.57 V vs. RHE	5 M KOH	62	600	[12]
Cu@Cu <sub>x</sub> O	-1.58 V vs. RHE	0.1 M KHCO <sub>3</sub>	45.8	150	[13]
Electrodeposited CuAg alloy	-0.7 V vs. RHE	1M KOH	60	300	[14]

**Table S1.** Comparison of the results of  $CO_2$  electroreduction to ethylene over variousCu-based composite electrocatalysts.

Electrodes	Cu/Pd ratio (by XPS)	Atomic ratio of $(Cu^0+Cu^{T})/Cu^{II}$	Atomic ratio of Pd <sup>0</sup> /Pd <sup>II</sup>
Cu-Pd/CP	6.83	2.48	0.405
Cu-Pd/CP-CV	32.20	3.20	0.625
Cu-Pd/CP-IT	61.20	3.00	0.617

**Table S2.** Ratio of Cu/Pd,  $(Cu^0+Cu^I)/Cu^I$  and  $Pd^I/Pd^0$  calculated from Cu2p and Pd3p signals of three electrodes.

Electrodes	$R_s (\Omega cm^{-2})$	$R_{ct} \left(\Omega \text{ cm}^{-2}\right)$	$R_{f}(\Omega \text{ cm}^{-2})$
Cu-Pd/CP	8.756	13.35	2.50
Cu-Pd/CP-CV	9.449	15.42	10.50
Cu-Pd/CP-IT	10.540	15.90	2.51

 Table S3. Parameter values of the equivalent circuit model.

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