

1 Supplementary Information

3 Greener production of dimethyl carbonate by Power-to-Fuel 4 concept: A comparative techno-economic analysis

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Table S1 Specific energy consumption of each process.

| | Oxidative carbonylation | Direct urea methanolysis | Indirect urea methanolysis via EC | Indirect urea methanolysis via PC |
|-----------------------------|-------------------------|--------------------------|-----------------------------------|-----------------------------------|
| Electrolysis | 65.11 | 56.07 | 56.25 | 57.57 |
| CO ₂ capture | 4.61 | 4.21 | 4.23 | 4.32 |
| LP steam | 1.88 | 3.17 | -0.08 | 3.30 |
| MP steam | 3.61 | 9.72 | 12.85 | 9.22 |
| HP steam | 0.00 | 0.00 | 3.02 | 4.44 |
| Operating electricity | 1.98 | 0.91 | 0.92 | 0.94 |
| Total (MJ/l _{DE}) | 77.18 | 74.09 | 77.18 | 79.79 |

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Table S2 Utility consumption of each section.

| | Oxidative carbonylation | Direct urea methanolysis | Indirect urea methanolysis via EC | Indirect urea methanolysis via PC |
|------------------------------------|---|---|---|---|
| MS | H ₂ and CO ₂ compression: 6796 kW | H ₂ and CO ₂ compression: 6796 kW | H ₂ and CO ₂ compression: 6796 kW | H ₂ and CO ₂ compression: 6796 kW |
| | LP steam: 22809 kW |
| | Operating electricity: 13735 kW | 0 | 0 | 0 |
| | CO ₂ compression: 1137 kW |
| RWGS and CO ₂ scrubbing | LP steam: -19726 kW |
| | MP steam: 44678 kW |
| | Pump: 62 kW | | Pump: 37 kW | |
| | LP steam: -88639 kW | Pump: 56 kW | LP steam: -17913 kW | Pump: 45 kW |
| Urea synthesis | 0 | MP steam: 40157 kW | MP steam: 24846 kW | MP steam: 12066 kW |
| | MP steam: 31344 kW | | LP steam: 26297 kW | LP steam: 24935 kW |
| | | | HP steam: 37749 kW | |
| | | | MP steam: 42229 kW | |
| DMC synthesis | | | | |
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| DMC separation | | | | |
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| EC/PC synthesis | | | | |
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Table S3 Fixed capital investment of each section.

| | Oxidative carbonylation | Direct urea methanolysis | Indirect urea methanolysis via EC | Indirect urea methanolysis via PC |
|---------------------------|-------------------------|--------------------------|-----------------------------------|-----------------------------------|
| MS | 46,859,504 | 46,859,504 | 46,859,504 | 46,859,504 |
| RWGS | 11,186,529 | 0 | 0 | 0 |
| CO ₂ scrubbing | 3,404,959 | 0 | 0 | 0 |
| Urea synthesis | 0 | 33,017,603 | 33,017,603 | 33,017,603 |
| DMC synthesis | 7,644,800 | 3,289,256 | 2,388,429.8 | 2,636,363.6 |
| DMC separation | 18,105,500 | 6,307,603 | 8,621,818.2 | 8,630,578.5 |
| EC/PC synthesis | 0 | 0 | 1,368,264.5 | 1,370,743.8 |
| WC | 15,388,463.2 | 15,789,524 | 16280404 | 16,326,140 |
| Total (€) | 102,589,754.9 | 105,263,490.5 | 108,536,023 | 108,840,933 |

Table S4 Cost of manufacturing of each process.

| | Oxidative carbonylation | Direct urea methanolysis | Indirect urea methanolysis via EC | Indirect urea methanolysis via PC |
|----------------------------|-------------------------|--------------------------|-----------------------------------|-----------------------------------|
| H ₂ | 1.748 | 1.504 | 1.511 | 1.468 |
| O ₂ | 0.033 | 0 | 0 | 0 |
| CO ₂ | 0.246 | 0.245 | 0.246 | 0.240 |
| Steam | 0.084 | 0.185 | 0.260 | 0.396 |
| Electricity | 0.054 | 0.0248 | 0.025 | 0 |
| Cooling water | 0.085 | 0.0815 | 0.091 | 0.135 |
| Labor | 0.006 | 0.0058 | 0.006 | 0.006 |
| Depreciation | 0.029 | 0.0307 | 0.032 | 0.038 |
| OPEX | 0.120 | 0.118 | 0.123 | 0.135 |
| Total (€/l _{DE}) | 2.41 | 2.19 | 2.29 | 2.42 |