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Supplementary Information

Probing the charged nature and ion-exclusion mechanism of fluorine-

enriched non-ionogenic polyamide derived thin film composite

nanofiltration membranes

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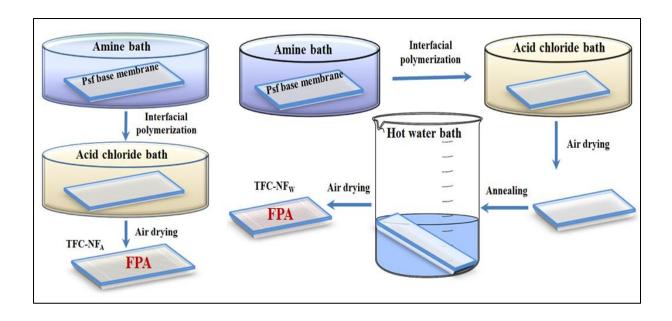


Figure S1. Schematic of FPA-based TFC-NF membrane fabrication process following *in-situ* interfacial polymerization technique, by using PIP as diamine monomer and TFSC as fluorine-bearing diacyl chloride monomer; in one route of preparation (depicted on left side), the membrane (TFC-NF_A) is dried in air, and in another route of preparation (depicted on right side), the membrane (TFC-NF_W) is annealed in hot water-bath and then dried in air.

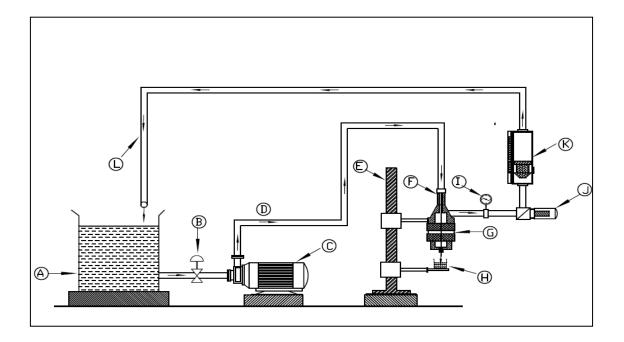


Figure S2. Schematic description of cross-flow filtration equipment for evaluation of nanofiltration performance; (A) feed tank, (B) valve, (C) diaphragm pump, (D) feed line, (E) stand with clamps, (F) test cell, (G) membrane, (H) permeate collector, (I) pressure gauge, (J) pressure relief valve, (K) rota meter, and (L) reject line.

 $\label{eq:Table S1} \textbf{Surface hydrophilicity and electrokinetic features of TFC-NF}_A \ \text{type membranes}.$

Membrane Code	θ_{W} (°)	ζ (mV)	$\sigma_{\rm s}$ (C/m ²)× 10^{-3}
TFC-NF _A /60s	42.1(±0.3)	- 4.4	- 3.1
$TFC-NF_A/90s$	$35.8(\pm0.1)$	- 5.6	- 4.0

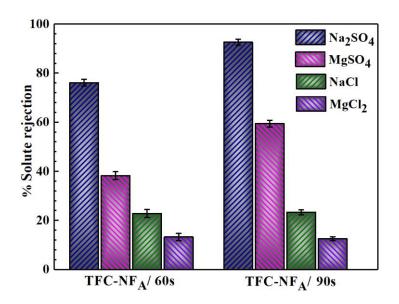


Figure S3. Nanofiltration performances of TFC-NF_A type membranes, prepared undergoing 60 and 90 s of reaction time during *in-situ* interfacial polymerization; solute rejection against isosmotic solutions of Na₂SO₄, MgSO₄, NaCl, and MgCl₂ at 15 bar transmembrane pressure.

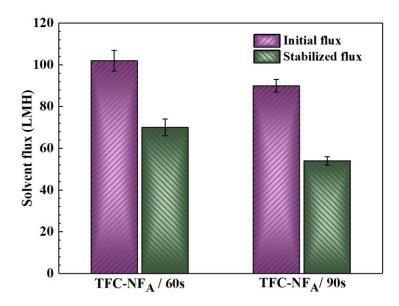


Figure S4. Solvent fluxes of TFC-NF_A type membranes, prepared undergoing 60 and 90 s of reaction time during *in-situ* interfacial polymerization, at 15 bar transmembrane pressure.