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## **Supporting information**

Direct synthesis of imines from nitro compounds and biomass-

## derived carbonyl compounds over nitrogen-doped carbon materials

## supported Ni nanoparticles

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Fig. S1 Particle size distributions for the Ni/CN-MgO-T









Fig. S2 TEM(a,b,c) and Particle size distributions for the Ni/ MgO-600



Fig. S3 XPS survey scan of the Ni/CN-MgO-600 catalyst





Fig. S5 XPS spectra of C 1s in the Ni/NC-MgO-500 and Ni/CN-MgO-700 catalysts

Table S1. The percentage of different carbon in the Ni/CN-MgO-T catalysts.

Entry	Samples	O-C=O	C-N	C-O/C=N	C=C
1	Ni/CN-MgO-500	12.7%	16.7%	36.0%	34.6%
2	Ni/CN-MgO-600	11.1%	19.2%	29.0%	40.7%
3	Ni/CN-MgO-700	10.7%	22.8%	16.4%	50.1%



Fig. S6 XPS spectra of N 1s in the Ni/NC-MgO-500 and Ni/CN-MgO-700 catalysts

Table S2. The percentage of different nitrogen in the Ni/CN-MgO-T catalysts

Entry	Samples	Pyridinic N	Pyrrolic N	Graphitic N	Oxidized N
1	Ni/CN-MgO-500	50.4%	25.7%	8.2%	15.7%
2	Ni/CN-MgO-600	49.6%	32.4%	18.0%	-
3	Ni/CN-MgO-700	32.2%	37.6%	30.2%	-



Fig. S7 XPS spectra of O 1s in the Ni/NC-MgO-500 and Ni/CN-MgO-700 catalysts

Table S3. The percentage of different oxygen in the Ni/CN-MgO-T catalysts

Entry	Samples	Ni-O	Mg-O	CO(OH)	C-C=O
1	Ni/CN-MgO-500	20.1%	21.1%	31.8%	27.0%
2	Ni/CN-MgO-600	16.6%	22.8%	35%	25.6%
3	Ni/CN-MgO-700	12.3%	26.9%	38.7%	22.1%



Fig. S8 pore size distributions of the Ni/CN-MgO-T catalysts

Table S4. The texture properties of the as-prepared catalysts.

Entry	Samples	$S_{BET}$ (m <sup>2</sup> g <sup>-1</sup> )	Pore Volume <sup>a</sup> (cm <sup>3</sup> g <sup>-1</sup> )	Pore Size <sup>b</sup> (nm)
1	Ni/CN-MgO-500	35.5	0.039	14.0
2	Ni/CN-MgO-600	181.0	0.107	7.67
3	Ni/CN-MgO-700	171.2	0.214	10.4

Table S5. The comparison between other catalysts and our Ni/CN-MgO catalyst.

Entry	Catalyst	Condition	Compared
1	Au/TiO <sub>2</sub> <sup>[1]</sup>	25 °C, 1 mmol	The use of precious metals as precursors
		$H_2O$ , 5 atm CO	makes the catalyst expensive.
2	Au-Pd/Al <sub>2</sub> O <sub>3</sub> <sup>[2]</sup>	140 °C, 2 MPa Ar,	The use of precious metals to prepare the
		40 mL methanol,	catalyst increases the cost of the catalyst. It is
		10 mL H <sub>2</sub> O, 0.5 g	also a bimetallic catalyst. At the same time,
		cat	the temperature condition of the reaction is
			also harsh.
3	CoOx@NC-	110 °C, 5.0 MPa	The reaction conditions are harsh such as
	800 <sup>[3]</sup>	H <sub>2</sub> , THF (3.2 mL),	temperature and pressure.
		H <sub>2</sub> O (0.8 mL), 24	
		h	
4	CoS2@MoS2 <sup>[4]</sup>	60 °C, 1.5 MPa H <sub>2</sub>	This reaction condition is indeed in
			compliance with environmental protection
			regulations, but its poor selectivity makes the

			separation work cost much.
5	PtCo/CoBO <sub>x</sub> <sup>[5]</sup>	60 °C and 1 MPa	The catalyst is prepared by using precious
		H <sub>2</sub> , 5mg Cat	metals, and it is also a bimetallic catalyst,
			which is more complicated to prepare.
6	Ni <sub>2</sub> Si/SiCN-	170 °C, 5 MPa H₂,	The reaction conditions are very harsh such as
	1000 <sup>[6]</sup>	100 mg cat	reaction temperature and pressure.
7	Ni/SiO <sub>2</sub> <sup>[7]</sup>	378 K, 1.4 MPa	The preparation method of the catalyst is
		$H_2$ , 15 mg cat	complicated.
8	Ni/SiO <sub>2</sub> <sup>[8]</sup>	80 °C, 1.4 MPa H <sub>2</sub> ,	The preparation method of the catalyst is
		5 mg cat	complicated.
9	Ni/CN-MgO-	80 °C, 1.0 MPa H <sub>2</sub> ,	Simple preparation method, economical source
	600	20 mg cat.	of materials.

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