# Bayberry tannin directed assembly of bifunctional graphene aerogel

## for simultaneously solar steam generation and uranium adsorption

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### 1. Property of bayberry tannin



**Figure S1**. (a) Photo images of BT powder (b)BT dispersion in water (c) Tyndall effect of BT dispersion.

### 2. Photo images and dynamic shear rheology behavior of the BGA gel precursor

#### and GO



**Figure S2.** Photo images of the BGA gel precursors fabricated with BT to GO feeding mass ratio of 1/8, 1/4, 1/2, 1, 2, 3, and 4 (the concentration of GO is fixed at 8 mg/ml).



**Figure S3.** The curves of storage modulus (G') and loss modulus (G'') with frequency. (a) BGA gel precursor prepared with different BT to GO feeding mass ratio and pure GO. (b) BGA gel precursor prepared with BT to GO feeding mass ratio of 1/8, 1/4, and pure GO.



**Figure S4.** Photo images of the BGA fabricated with BT to GO feeding mass ratio of 1/4, 1/2, 1, 2, 3 and 4.



**Figure S5.** (a) Photo images of the BGA gel precursors fabricated with different GO concentration when the concentration of BT is fixed at 40 mg/ml. (b) The curves of storage modulus (G') and loss modulus (G'') with frequency for BGA gel precursors fabricated with different GO concentration.

#### **3.** Effect of pH on the sol-gel process



**Figure S6.** (a) Photo images of BGA gel precursor prepared at different pH. (b) The curves of storage modulus (G') and loss modulus (G'') with frequency for BGA gel precursor prepared at different pH.

# 4. Microstructure of the BGA



Figure S7. SEM image of BGA(a, b) and U-BGA(c, d).



Figure S8. SEM images of BGA fabricated with different ratios.

### 5. Surface area and pore size distribution of BGA

Table S1. Statistics of BET surface area and pore volume of graphene aerogel reported

Materials	Drying Method	BET Surface Area (m²/g)	Pore Volume (cm <sup>3</sup> /g)	Ref.
GA (ascorbic acid)	SC-CO <sub>2</sub> drying	512	2.48	[1]
GA (hydrothermal method)	SC-CO <sub>2</sub> drying	394	1.46	[2]
GA (H <sub>2</sub> )	SC-CO <sub>2</sub> drying	867	1.90	[3]
AN-GA (HI)	SC-CO <sub>2</sub> drying	379.1	1.065	[4]
GA (organic cross-linker)	SC-CO <sub>2</sub> drying	584	2.96	[5]
GA (L-phenylalanine)	Freeze drying	117	0.991	[6]
NDGA (ethylenediamine)	Natural drying	190	0.6	[7]

over five years.

This work $(3:1)$	SC-CO <sub>2</sub> drying	310.27	0.72	
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**Table S2.** The analysis of the porous structure in BGA fabricated with BT to GO feeding mass ratio of 1/4, 1/2, 1, 2, 3 and 4.

food notio	BET Surface Area	Pore Volume	Average Pore Size
	$(m^{2}/g)$	$(cm^3/g)$	(nm)
1/4	443.05	1.25	10.22
1/2	323.02	0.85	11.53
1	399.08	1.33	11.40
2	379.26	1.15	12.16
3	310.27	0.72	10.20
4	282.98	0.60	10.47
Freeze drying	236.85	0.89	15.45

# 6. The reduction mechanism of GO by BT



Figure S9. Raman spectra of GO (a) and BGA (b).



Figure S10. Possible mechanism for reduction of GO by BT.

### 7. IR spectra of BGA



Figure S11. IR spectra of GO, BT and the BGA fabricated with BT to GO feeding mass

ratio of 1/4, 1/2, 1, 2, 3 and 4.

#### 8. Prussian blue method to confirm the BT in BGA



**Figure S12.** Photo images of the solution containing  $\text{Fe}^{3+}$  and  $\text{Fe}(\text{CN})_6^{3-}$  after adding the BGA.



### 9. Comparison of water transport rate

**Figure S13.** water transport rate of graphene aerogels reduced by bayberry tannin, vitamin C, hydrothermal method, hydrazine hydrate and hydroiodic acid, respectively.

# 10. Solar-thermal property of BGA



Figure S14. Temperature–time curves of top and bottom of the BGA under 1 sun illumination.

	Water evaporation	Conversion	
Materials	rate	efficiency	Ref.
	$[kg/(m^2 \cdot h)]$	(%)	
RGO-SA-CNT aerogel	1.622	83	[8]
NGCA-600	1.558	90	[9]
srGA	1.78	91	[10]
RGO/MoS <sub>2</sub> aerogel bead	0.90	62.1	[11]
PNGA	1.3542	93.8	[12]
RGO-SA-cellulose aerogel	2.25	88.9	[13]
h-G foam	1.4	93.4	[14]
3DG	2.6	87	[15]
PFS@rGO	1.375	88.8	[16]
BHMG	1.476	92.9	[17]
rGO foam	2.40	~100	[18]
rGO/PU	0.9	65	[19]
PAAm aerogel	2.0	85.7	[20]
Poly(vinyl alcohol) hydrogel	2.6	91%	[21]
Nanocellulose	1.13	78%	[22]
Aluminium nanoparticles	1.0	90%	[23]
Polymer foam	1.20	80%	[24]
Wood	1.08	74%	[25]
BGA	1.84	95.5	This work

 Table S3. Solar steam generation performance of different materials.



Figure S15. Water evaporation rate of the BGA and BGA gel precursor.



Figure S16. Water evaporation rate of the BGA fabricated with  $SC-CO_2$  and Freeze

drying.



**Figure S17.** (a) Nitrogen adsorption and desorption isotherms, and pore size distribution of the BGA fabricated by freeze drying. (b) SEM image of the BGA fabricated with freeze drying.



**Figure S18** (a) Water evaporation rate of the BGA in salty water with different salinity from 5% to 15% (weight ratio). (b) Photo images of upper surface of the BGA when the light duration is 0 h, 5 h, 10 h.

#### The Calculation of the actual efficiency

According to reported method, the actual efficiency of BGA is calculated as follows:

$$\eta = \frac{\dot{m}(h_v + c \int_{T_0}^T dT)}{P_0}$$
(1)

c is the specific heat capacity of the water  $[kJ/(kg \cdot {}^{0}C)]$ , T<sub>0</sub> and T is the initial and the final temperature of the system ( ${}^{0}C$ ).

It can be seen from Figure 3d that the starting temperature is  $25 \, {}^{0}$ C, and the ending temperatures of the upper and lower surfaces after 1 hour are 50 and 33  ${}^{0}$ C respectively. For the convenience of calculation, it is assumed that the temperature of BGA presents a trapezoidal distribution (the specific heat capacity of water is 4.2 kJ/(kg ${}^{.0}$ C)

Thus, η=0.994.

#### 11. Uranium extraction performance of BGA



Figure S19. IR spectra of the BGA before and after uranium adsorption.

Matariala	ъЦ	Temp.	Uranium adsorption	Dof
Materials	(K) (mg		(mg/g)	Kel.
GO-CS aerogel	8.3	RT	384.6	[26]
Fe-PANI-GA	5.5	298	350.47	[27]
FH/GOA	5.0	293	288.42	[28]
CA-PO4	5.5	298	150.3	[29]
phos-GOF	5~7	298	~483	[30]
GCZ8A	8.0	298.15	361.01	[31]
COF	6.0	298	408	[32]
PAF-NH(CH <sub>2</sub> ) <sub>2</sub> AO	6.0	298	385	[33]
MOF	9.0	298	118	[34]
Amidoxime-	6.0	208	200	[35]
functionalized PAF	0.0	298	500	[50]
Polyamidoxime/				
polyethyleneimine	6.0	298	200	[36]
magnetic graphene oxide				
Hybrid MS@PIDO/Alg	65	208	201.5	[37]
sponge	0.5	298	271.3	[- · ]
Porous aromatic	1.0	208	16	[38]
framework	1.0	270	10	[]
Amidoxime-	8.0	298	80	[39]
functionalized wool fiber	0.0	298	00	
Chimeric spidroin-based				
super uranyl-binding	7.0	298	12.3	[40]
protein				
BGA	5.0	298	279 10	This
BUA	5.0	5.0 270	217.10	work

Table S4. Uranium extraction performance of graphene-based and other typical materials.

Rate of uranium absorption (mg.g <sup>-1</sup> .h <sup>-1</sup> )	Materials	Reference
4.0	Cross-linked chitosan	[41]
0.4	MOF	[42]
16.7	MOF	[43]
13.3	PAF-1-NH(CH <sub>2</sub> ) <sub>2</sub> AO	[33]
15	MOF	[34]
25	amidoxime-functionalized PAF-1	[35]
20	polyamidoxime/	[36]
	polyethyleneimine magnetic graphene	
	oxide	
12.6	hybrid MS@PIDO/Alg sponge	[37]
3	porous aromatic framework	[44]
0.8	porous aromatic framework	[38]
20.8	BP-PAO fiber	[45]
5.4	nano-ZnO loaded amidoxime-	[39]
	functionalized wool fiber	
27.2	porous	[46]
	amidoxime-based nanofiber	
40.8	amidoximated	[47]
	poly(imide dioxime) nanofiber	
21.3	chimeric spidroin-based super uranyl-	[48]
	binding protein	
31.25	BGA	This work

Table **S5.** The rates of uranium absorption of different materials.

### The Fitting of adsorption kinetics of BGA

According to adsorption kinetics, there are two kinds of kinetic models used to describe the adsorption behavior of  $UO_2^{2+}$ , which are pseudo-first-order (2) and pseudo-second-order (3) kinetic models, respectively. The corresponding equations are listed as follows:

$$\ln\left(q_e - q_t\right) = \ln q_e - k_I t \tag{2}$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \tag{3}$$

where  $q_e$  and  $q_t$  (mg/g) refer to the adsorption capacity at equilibrium and t time, respectively;  $k_1$  (1/min) and  $k_2$  [g/(mg·min)] are the rate constants of pseudo-first-order and pseudo-second-order kinetic models, respectively.



**Figure S20.** Uranium adsorption kinetics of BGA at 298 K (initial uranium concentration: 0.25 mg/mL, pH 5.0, V/m ratio: 2000 mL/g).



**Figure S21.** Uranium adsorption kinetics of BGA at different temperatures (initial uranium concentration: 0.025-0.25 mg/mL, pH 5.0, V/m ratio: 2000 mL/g). Regression by the pseudo-second-order equation.

Table S6. Fitting parameters of the pseudo-first-order and pseudo-second-order models

Temperature	pseudo-first-order	pseudo-second-order	
(K)	R <sup>2</sup>	R <sup>2</sup>	
298	0.91667	0.95961	
308	0.94521	0.9755	

#### The Fitting of adsorption isotherms of BGA

Both Langmuir and Freundlich models are used to fitting the experimental data. The equations are listed as follows:

$$\frac{c_e}{q_e} = \frac{c_e}{q_m} + \frac{1}{bq_m}$$
(1) Langmuir linear model  

$$\ln q_e = \ln k_F - \frac{1}{n}c_e$$
(2) Freundlich linear model

where  $q_e$  and  $q_m$  (mg/g) are the equilibrium and maximum adsorption capacity, respectively;  $c_e$  (mg/mL) is the equilibrium concentration; b (mL/mg) is the Langmuir constant;  $k_F$  [(mg/g)×(mg/mL)<sup>-1/n</sup>] is the Freundlich constant; n is an empirical parameter related to adsorption intensity.



**Figure S22.** Uranium adsorption isotherms of BGA at different temperatures (initial uranium concentration: 0.25 mg/mL, pH 5.0, V/m ratio: 2000 mL/g). Regression by the Langmuir model (a) and Freundlich model (b).

Tomporatura		Langmuir		
(K)	R <sup>2</sup>	$q_{m,cal}$ (mg/g)	$q_{m,exp}$ (mg/g)	R <sup>2</sup>
298	0.99636	210.08	211.07	0.37646
308	0.99856	284.09	-	0.53865
318	0.99598	330.03	-	0.51788

Table S7. Fitting parameters of the Langmuir and Freundlich models

Element	Concer (µg	ntration (/L)
(K)	Before	After
U	18.6	8.6
Fe	50760	47460
Ni	1455.4	1334.8
Cu	1149.2	882.4
Zn	2830	2268
Pb	201.4	167.4
Na	11.44×10 <sup>6</sup>	11.38×10 <sup>6</sup>
Mg	$1.37 \times 10^{6}$	$1.32 \times 10^{6}$
Са	0.49×10 <sup>6</sup>	$0.46 \times 10^{6}$

**Table S8.** Uranyl ion and coexisting ion concentration before and after adsorption

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