

Experimental section

Synthesis of iron-containing complex nanoflakes. Iron-containing complex nanoflakes were synthesized via a facile hydrothermal method. Both 0.5927 g of $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ and 1.5916 g of urea were dissolved in 70 mL of ethylene glycol under magnetic stirring at room temperature for 30 min to form a solution, which was then transferred into a 100 mL Teflon-lined stainless steel autoclave and heated at 180 °C for 8 h. After cooling at room temperature, the precipitates were collected by centrifugation, washed several times with ethanol, and dried at 60 °C for 24 h in an oven.

Synthesis of 2D- $\text{Fe}_3\text{O}_4/\text{C}$ nanoflakes. Iron-containing complex nanoflakes were annealed in a nitrogen atmosphere at 400, 450, and 500 °C for 2 h with a heating rate of 5 °C min^{-1} , and denoted as 2D- $\text{Fe}_3\text{O}_4/\text{C}$ -400, 2D- $\text{Fe}_3\text{O}_4/\text{C}$ -450, and 2D- $\text{Fe}_3\text{O}_4/\text{C}$ -500, respectively.

Synthesis of NiCo-LDHs. First, ZIF-67 nanoparticles were synthesized as the precursor of NiCo-LDHs. After that, the as-prepared ZIF-67 nanoparticles were transformed to NiCo-LDH nanosheets in accordance with the precedent of the previous report.^{S1} Briefly, 120 mg of ZIF-67 and 480 mg of $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ were dissolved in a mixed solvent comprised of 120 mL of ethanol and 30 mL of deionized water under magnetic stirring for 30 min; the solution was then sealed in a Teflon-lined autoclave and heated at 90 °C for 1 h. NiCo-LDHs were obtained by centrifugation, washed several times with absolute ethanol, and then dried in an oven at 60 °C for 24 h.

Characterization. The morphologies and structural details of the samples were examined by field-emission scanning electron microscopy (FESEM, Hitachi S-4800) and transmission electron microscopy (TEM, JEOL-2010). The phase and crystallographic structures of the samples were investigated by X-ray diffraction (XRD, Rigaku, Ultima IV with D/teX Ultra) using Cu K α radiation in a range of 10° to 90° with a scan speed of 5° min^{-1} . The chemical elemental compositions of the materials were measured by X-ray photoelectron spectrometer (XPS, Axis Ultra, Kratos Analytical Ltd.). Thermogravimetric analysis (TGA) was performed using a Shimadzu-50 thermoanalyzer from room temperature to 900 °C at a ramp rate of 10 °C min^{-1} in air. The Brunauer-Emmett-Teller (BET) specific surface areas and Barrett–Joyner–Halenda (BJH) pore-size distributions were obtained from the nitrogen physical adsorption-desorption isotherms at 77 K using an Autosorb iQ2 analyzer (Quantachrome Instruments).

Electrochemical measurements. Working electrodes were fabricated by mixing 80 wt.% of active material, 10 wt.% of carbon black, and 10 wt.% of polyvinylidene fluoride in N-methyl-2-pyrrolidone solution. The slurries were coated onto graphite substrates, which were then dried at 120 °C for 12 h under vacuum conditions.

The electrochemical measurements were carried out in a three-electrode system in 2 M KOH aqueous solution for supercapacitors and 1 M NaCl aqueous solution for CDI. The as-prepared electrode materials, an Ag/AgCl electrode, and platinum foil were used as the working electrode, reference electrode, and counter electrode, respectively. The electrochemical performance of the as-synthesized material electrodes was

studied using cyclic voltammetry (CV), electrochemical impedance spectroscopy (EIS) at 0.1 Hz - 100 kHz and 5 mV AC amplitude, and galvanostatic charge-discharge (GCD) on an AUTO-LAB PGSTAT 204N electrochemical workstation.

The specific capacitance (C_s , F g⁻¹) was calculated from the GCD process with the following equation:

$$C_s = I \times \Delta t / (m \times \Delta V), \quad (S1)$$

where I and Δt represent the discharge current (A) and discharge time (s), respectively; and, m and ΔV are the mass of active material (g) and the potential window during the discharge process, respectively.

Supercapacitor measurements. For the preparation of gel electrolytes, 2 g of polyvinyl alcohol (PVA) was first dissolved in 20 mL of deionized water under stirring at 85 °C for 4 h to form solution A. Second, 3.366 g of KOH was added to 10 mL of deionized water to form solution B. Then, solution B was added into solution A drop by drop. Afterward, the electrolyte was placed under low temperature conditions until the gel solidified.^{S2} Finally, the hybrid supercapacitor was assembled by using the 2D-Fe₃O₄/C-450 electrode as the negative electrode and NiCo-LDHs as the positive electrode using a PVA-KOH gel as a solid-state electrolyte.

The energy density (E , W h kg⁻¹) and power density (P , W kg⁻¹) were obtained as follows:

$$E = C_s \times \Delta V^2 / 7.2, \quad (S2)$$

$$P = 3600 \times E / \Delta t, \quad (S3)$$

where C_s , ΔV , and Δt are the specific capacitance (F g⁻¹), potential window (V), and discharge time (s), respectively.

CDI measurements. Desalination experiments were carried out using a batch-mode CDI unit under constant recycling in 500 mg L⁻¹ NaCl solution. The mass of the active material, Fe₃O₄/C-450 was 0.046 g. Ion exchange membranes were used to suppress the co-ion expulsion. During the desalination process, the flow rate, temperature, and volume were kept at 100 mL min⁻¹, 298 K, and 80 mL, respectively. Furthermore, the conductivity of the NaCl solution was monitored by using a conductivity meter (DDS-308, Precision and Scientific Instrument). The desalination capacity (Γ , mg g⁻¹) was calculated according to previous reports:^{S3,S4}

$$\Gamma = \frac{(C_0 - C_t) \times V}{m}, \quad (S4)$$

where C_0 and C_t are the NaCl concentrations (*i.e.*, half of the NaCl solution's conductivity) at the initial stage and t time (mg L⁻¹), respectively, V is the volume of the NaCl solution (L), and m is the mass of active materials (g).

Supplementary Figures and Tables

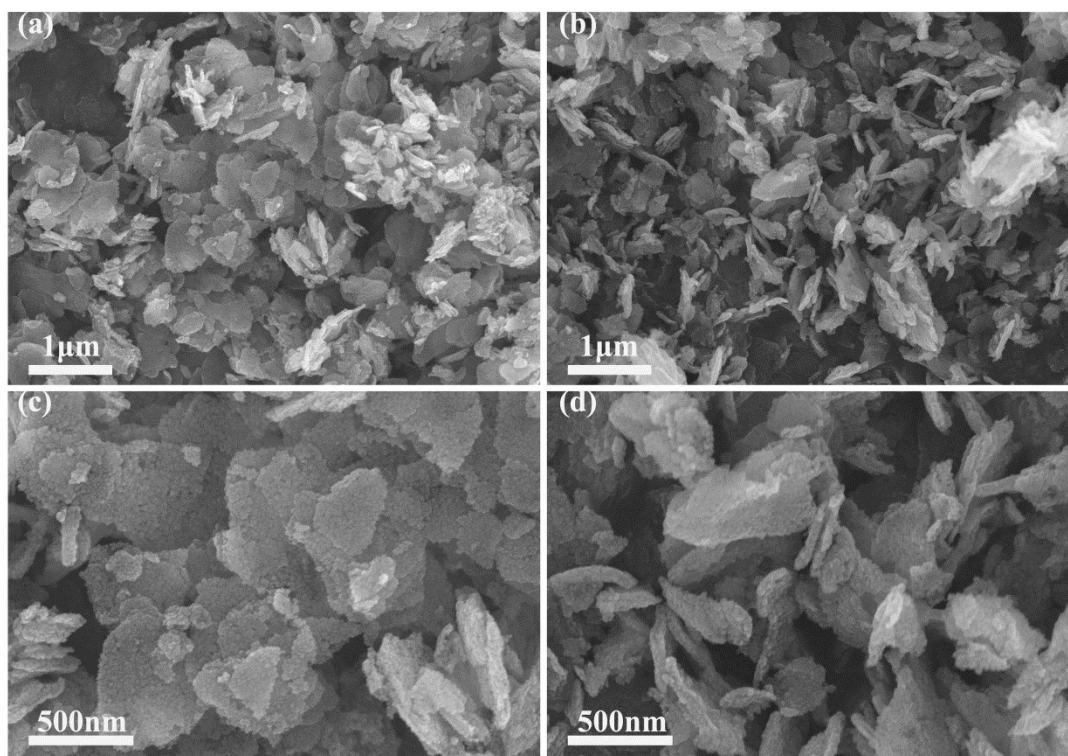


Fig. S1 (a, b) Low- and (c, d) high-resolution FESEM images of (a, c) 2D-Fe₃O₄/C-400 and (b, d) 2D-Fe₃O₄/C-500 at different magnifications.

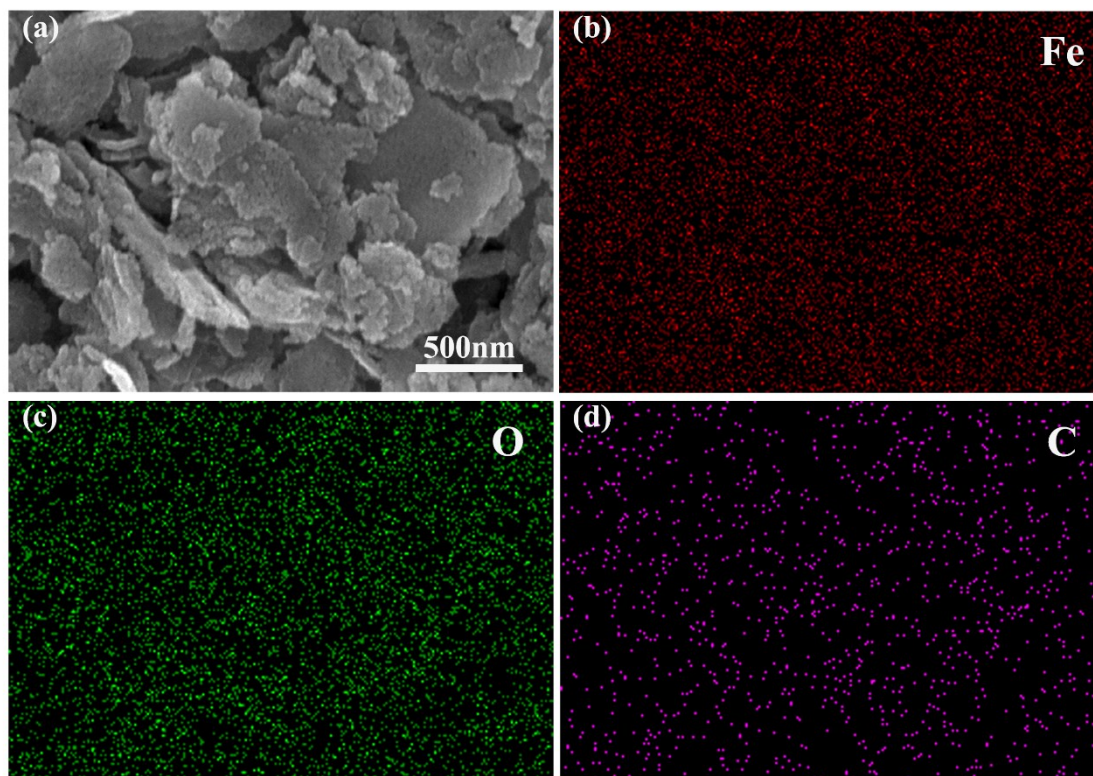


Fig. S2 (a) FESEM and (b–d) corresponding elemental mapping images of 2D-Fe₃O₄/C-450.

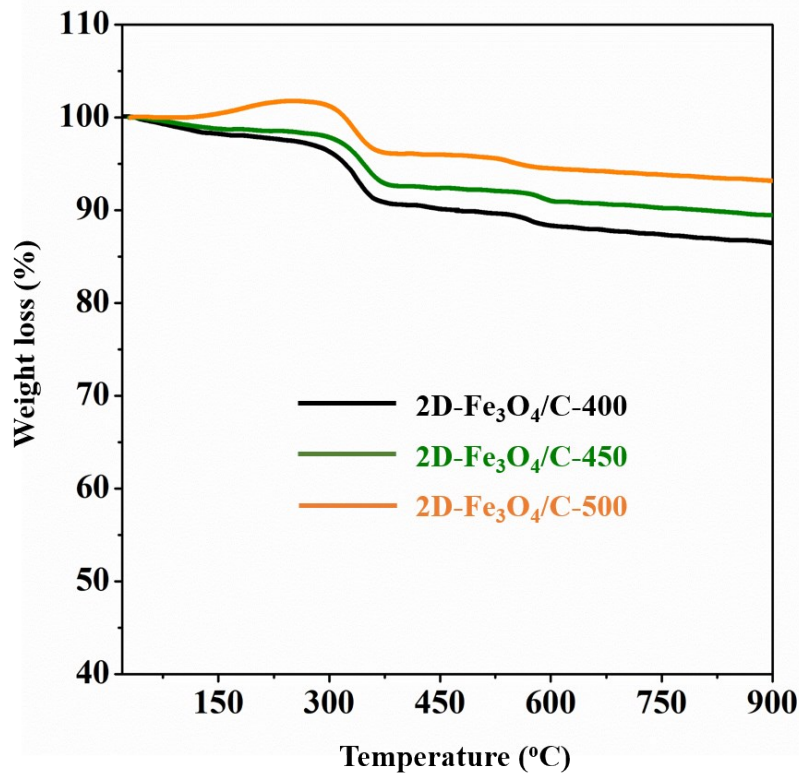


Fig. S3 TGA curves of all 2D-Fe₃O₄/C samples.

Supplementary Note for Fig. S3: We assume that the weight ratio of carbon is x , so the weight ratio of Fe₃O₄ (molar mass: 231.54 g/mol) in the composite is $1-x$. As we all know, after annealing 2D-Fe₃O₄/C samples in air, the final product will be Fe₂O₃ (molar mass: 159.69 g/mol), which will refer to a weight ratio of $239.54 \times (1-x)/231.54$. Based on the results of TGA curves (**Fig. S3**), the remaining weight ratios of all 2D-Fe₃O₄/C samples are 89.49, 92.59, and 96.40 wt.% for 2D-Fe₃O₄/C-400, 2D-Fe₃O₄/C-450, and 2D-Fe₃O₄/C-500, respectively. Therefore, the corresponding mass ratios of carbon in 2D-Fe₃O₄/C-400, 2D-Fe₃O₄/C-450, and 2D-Fe₃O₄/C-500 are 13.5, 10.5, and 6.82 wt.%, respectively.

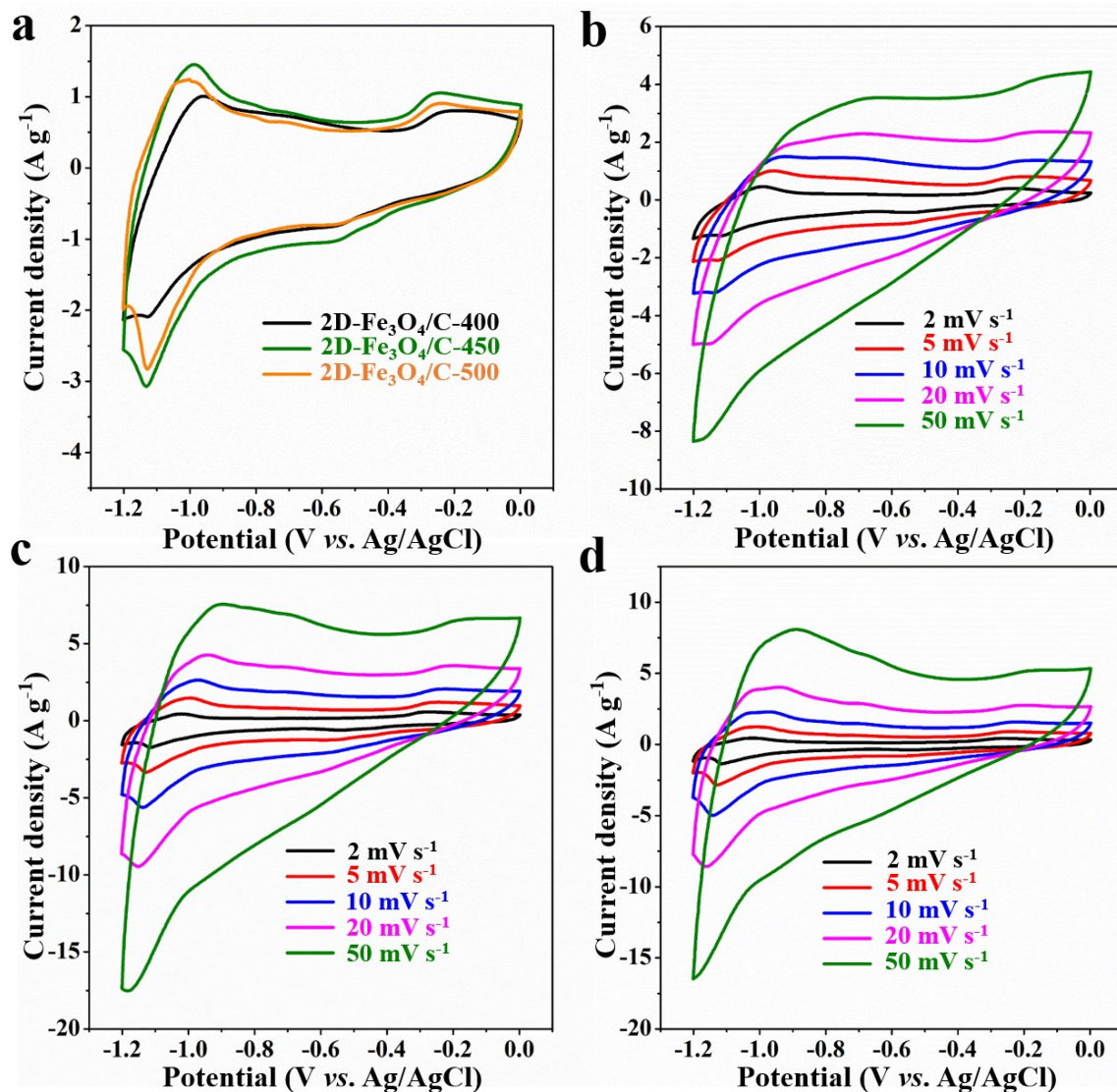


Fig. S4 (a) CV curves for 2D-Fe₃O₄/C-400, 2D-Fe₃O₄/C-450, and 2D-Fe₃O₄/C-500 electrodes at 5 mV s⁻¹; CV curves of (b) 2D-Fe₃O₄/C-400, (c) 2D-Fe₃O₄/C-450, and (d) 2D-Fe₃O₄/C-500 at various scan rates.

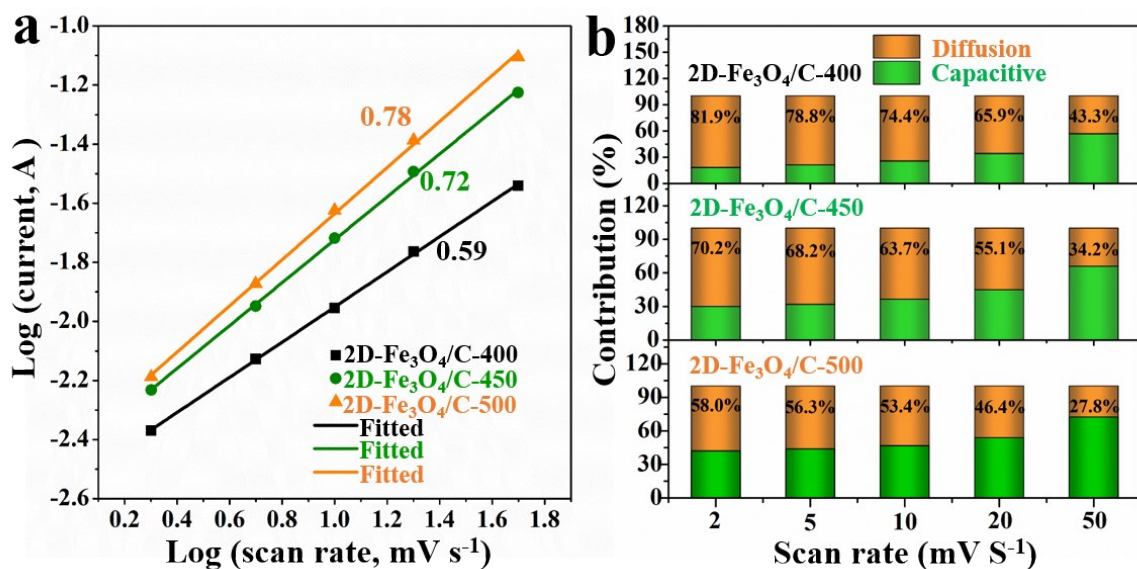


Fig. S5 (a) Linear relationship for $\log(i, \text{anodic peak current})$ versus $\log(v, \text{scan rate})$ of different samples; (b) ratios of capacitive and diffusion-controlled contributions at different scan rates.

Supplementary Notes for Figs S4–5:

To further explore the capacitive behavior of the composites, the CV curves of the 2D-Fe₃O₄/C electrodes at scan rates from 2 to 50 mV s⁻¹ in 2 M KOH electrolyte are shown in **Fig. S4b–d**. The proportion of diffusion-controlled contribution and surface-controlled capacitive contribution are calculated using the following equation:

$$i = av^b, \quad (\text{S5})$$

where i and v are the corresponding currents at a certain voltage (A) and scan rate in CV measurements (mV s⁻¹), respectively; a and b are adjustable values. When the b value equals 0.5, a diffusion-controlled process is indicated, whereas the b value is close to 1, which suggests a capacitive-controlled behavior.⁴⁰ **Fig. S5a** shows the profiles regarding $\log(i)$ versus $\log(v)$ of the 2D-Fe₃O₄/C composites, and the calculated b values are 0.59, 0.72, and 0.78, implying that the electrochemical behaviors of the 2D-Fe₃O₄/C composite are dominated by both surface-controlled capacitive effects and diffusion-controlled processes. The diffusion-controlled and capacitive contributions can be calculated by the following equation:

$$i = k_1v + k_2v^{1/2}, \quad (\text{S6})$$

where k_1v and $k_2v^{1/2}$ correspond to the currents at a certain voltage controlled by capacitive behavior and diffusion-controlled process, respectively. As shown in **Fig. S5b**, the diffusion-controlled process dominates the electrochemical behaviors at lower scan rates, especially in the 2D-Fe₃O₄/C-400 and 2D-Fe₃O₄/C-450 electrodes, and with the increase of scan rates, the surface-controlled capacitive contributions of 2D-Fe₃O₄/C samples increase. In addition, an interesting phenomenon has also been observed, that is, with the decrease of carbon content in the sample from 2D-Fe₃O₄/C-400 and 2D-Fe₃O₄/C-450 to 2D-Fe₃O₄/C-500, the surface-controlled capacitive contributions are enhanced

accordingly. This might be due to following reasons: as discussed in a previous paper titled “Definitions of pseudocapacitive materials: a brief review (*Energy & Environmental Materials*, 2 (2019): 30–37), it is hard to ascribe all of the surface-controlled capacitive contribution to the electrochemical double-layer capacitive effects, since the fast redox reactions and the ion intercalation/de-intercalation that happened at the surface can also contribute to the surface-controlled current response, especially in a system using ultrafine-sized nanomaterials. In other words, since our 2D-Fe₃O₄/C nanoflakes are composed of numerous Fe₃O₄ nanoparticles with sizes of 10–20 nm, we cannot ignore the presence of redox reactions or ion intercalation/de-intercalation behavior at the surface. Thus, although the carbon content decreases, the capacitive contribution still increases.

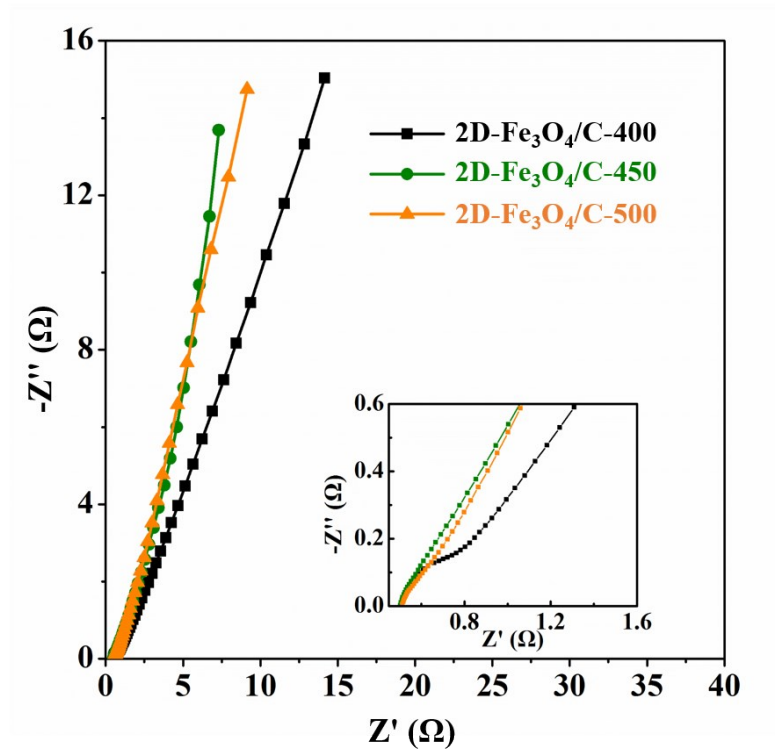


Fig. S6 Nyquist plots of 2D-Fe₃O₄/C samples. Insets show the corresponding magnified spectra in the high-frequency region and the equivalent circuit model.

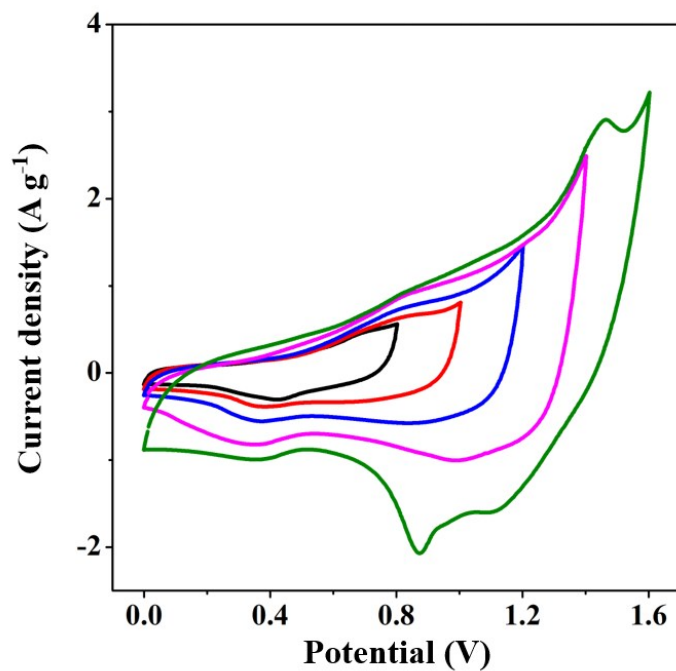


Fig. S7 CV curves for the $\text{Fe}_3\text{O}_4/\text{C-450}/\text{NiCo-LDHs}$ asymmetrical system with varying operation windows in 2 M KOH at 10 mV s^{-1} .

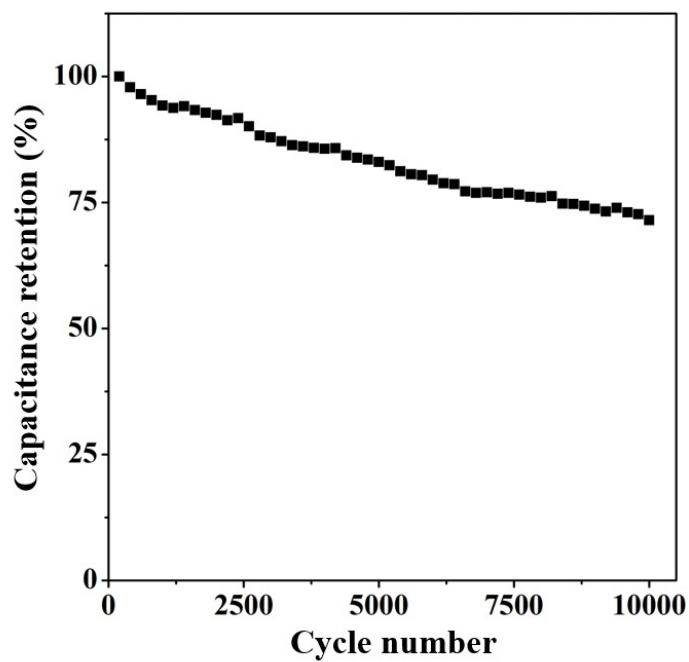


Fig. S8 Cycling capacitance retention of a hybrid supercapacitor.

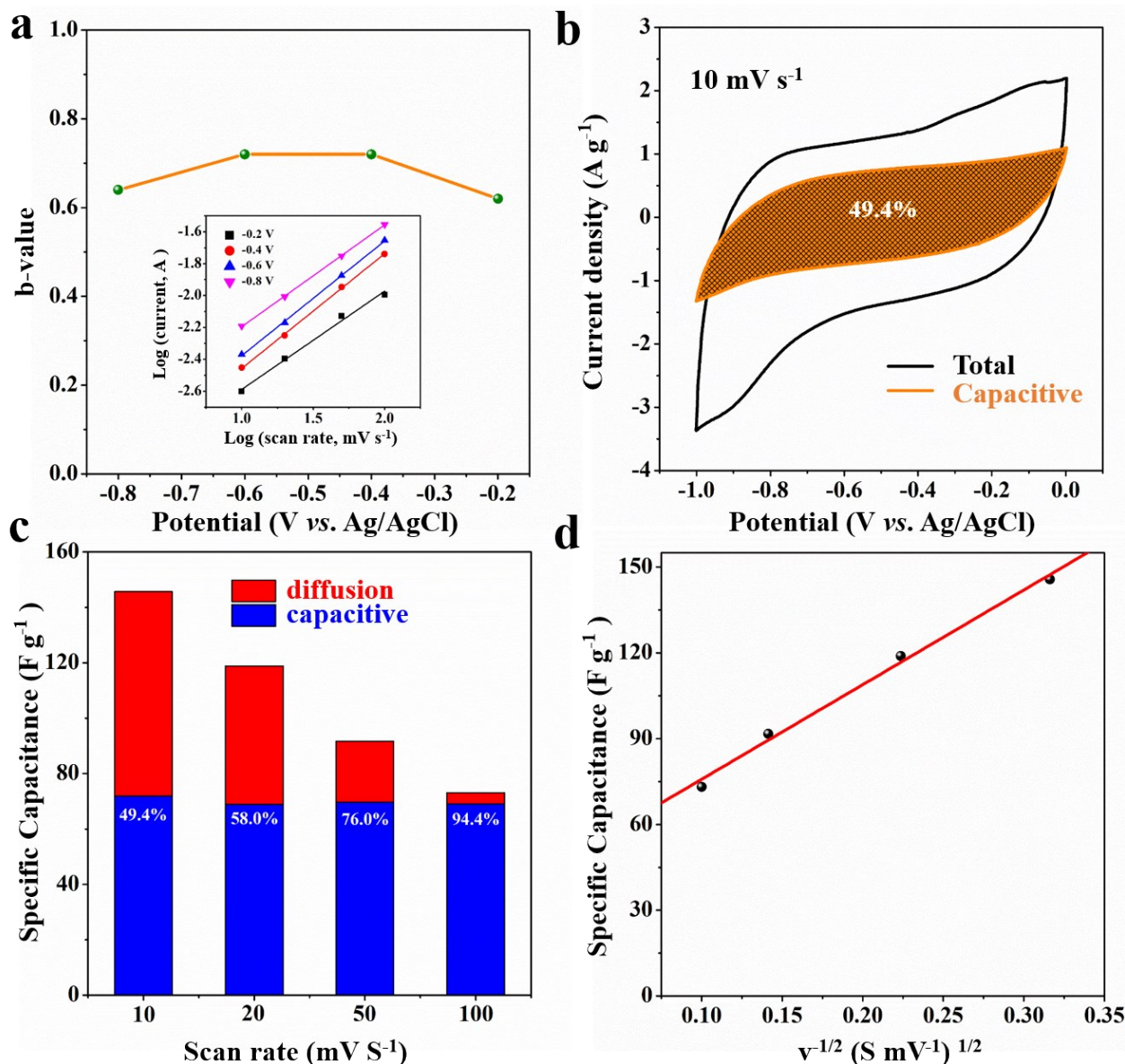


Fig. S9 (a) Curve of b-values versus potential; (b) illustration of capacitive and total contributions at 10 mV s⁻¹; (c) separate capacitances at varying scan rates; (d) relationships of specific capacitances *versus* the square root of the scan rate; Inset of (a) Linear relationship for log(*i*, current) *versus* log(*v*, scan rate) at different potentials.

Supplementary Note for Fig. S9d: The current response at a fixed potential could be expressed as following equation:

$$i(V) = k_1 v + k_2 v^{1/2}, \quad (\text{S7})$$

wherein $k_1 v$ and $k_2 v^{1/2}$ correspond to the current contributions from surface-controlled charging and diffusion-controlled Na ion-insertion processes, respectively.

According to the relationship between the total capacitance (C , F g⁻¹) and the current $i(V)$:

$$C = \int i(V) dV / 2mv\Delta V, \quad (\text{S8})$$

where m is the mass of the electrode (g), and v is the scan rate, C could be further expressed as the total of the capacitances from the surface-controlled charging contribution (C_1 , F g⁻¹), *i.e.*, $\int(k_1v)dV/2mv\Delta V$, and the diffusion-controlled Na ion-insertion process (C_2 , F g⁻¹), referring to $\int(k_2v^{1/2})dV/2mv\Delta V$, which is displayed in the following formula:

$$C = \int (k_1v)dV/2mv\Delta V + \int (k_2v^{1/2})dV/2mv\Delta V. \quad (\text{S9})$$

This formula can be further simplified as:

$$C = \int k_1dV/2m\Delta V + \int k_2dV/2mv^{1/2}\Delta V. \quad (\text{S10})$$

We therefore analyzed the correlation between C and $v^{1/2}$ and fitted the plots as shown in **Fig. S9d**. The intercept of the y -axis corresponds to the separate capacitance C_1 of the surface-controlled charging process. As calculated, the value is 67.5 F g⁻¹.

Table S1 Comparison of 2D-Fe₃O₄/C with other TMOs materials in CDI

| Material | Voltage (V) | Desalination capacity (mg g⁻¹) | Desalination time (min) | Mean desalination rate (mg g⁻¹ min⁻¹) | Reference |
|--|--------------------|--|--------------------------------|--|------------------|
| Ti-ACC | 1.0 | 2.05 | >180 | <0.0115 | S5 |
| AC-TiO ₂ | 1.2 | ~12.7 | >200 | <0.0635 | S6 |
| TiO ₂ /AC | 1.2 | 8.05 | >25 | <0.322 | S7 |
| GA/TiO ₂ | 1.2 | 15.1 | >6.7 | <2.265 | S8 |
| ACTNF | 1.2 | 17.7 | 5 | 3.54 | S9 |
| TiO ₂ -coated AC | 1.2 | 17 | 10 | 1.7 | S10 |
| RGO/TiO ₂ nanorod | 1.2 | 16.4 | 5 | 3.28 | S11 |
| TiO ₂ /CNTs | 1.2 | 4.3 | 20 | 0.215 | S12 |
| THC-A | 1.2 | 13.11 | >40 | <0.328 | S13 |
| MnO ₂ /NCs | 1.2 | 0.99 | 50 | 0.0198 | S14 |
| MnO ₂ /PSS/CNTs | 1.2 | 4.7 | ~25 | ~0.188 | S15 |
| CAGDMnAct | 1.5 | 6.4 | 150 | 0.0427 | S16 |
| RGO-PPy-Mn | 2.0 | 18.4 | 120 | 0.153 | S17 |
| MnO ₂ /MWCNTs | 1.8 | 6.65 | 24 | 0.277 | S18 |
| MnO ₂ /AC | 1.0 | 9.26 | 30 | 0.309 | S19 |
| MnO ₂ /CNT-CS | 1.6 | 10.07 | 30 | 0.336 | S20 |
| ZnO-ACC | 1.2 | 8.5 | 7.08 | 1.2 | S21 |
| ZnO/AC | 1.2 | 9.4 | 40 | 0.235 | S22 |
| ZnO-coated ACC | 1.5 | 5.72 | 6.8 | 0.841 | S23 |
| RGO@Fe ₃ O ₄ | 1.2 | ~8.33 | 30 | 0.278 | S24 |
| Graphene/SnO ₂ | 1.4 | 1.49 | 90 | 0.0166 | S25 |
| N-AC/SnO ₂ | 1.2 | 3.42 | 1.83 | 2.052 | S26 |
| RGO-SnO ₂ | 1.2 | 17.62 | 30 | 0.587 | S27 |
| ZrO ₂ fibers/AC | 1.2 | 16.35 | 30 | 0.545 | S28 |
| RuO ₂ (20)-AC | 1.2 | 11.3 | 60 | 0.188 | S29 |
| rGO/Co ₃ O ₄ | 1.6 | 20.21 | 30 | 0.674 | S30 |
| 2D-Fe ₃ O ₄ /C-450 | 1.2 | 28.5 | 7.5 | 3.8 | This work |

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