## **Supplementary Information**

### Effect of Fe, Co and Ni promoters on MoS<sub>2</sub> based catalysts for

#### chemoselective hydrogenation of nitroarenes

Wenpeng Han<sup>a, b</sup>, Shanmin Wang <sup>c</sup>, Xuekuan Li <sup>a</sup>, Ben Ma <sup>a</sup>, Mingxian Du <sup>a</sup>, Ligong Zhou <sup>a</sup>, Ying Yang <sup>a</sup>, Ye Zhang, <sup>a\*</sup> Hui Ge <sup>a\*</sup>

<sup>a</sup> Institute of Coal Chemistry, Chinese Academy of Sciences, Taiyuan 030001, China

<sup>b</sup> University of Chinese Academy of Science, Beijing 100049, China

<sup>c</sup> Department of Physics, Southern University of Science & Technology, Shenzhen, Guangdong, 518055, China

\* Corresponding author. Tel: +86-351-4046547; 18135105377

E-mail address: <u>gehui@sxicc.ac.cn</u> (H. Ge); <u>yzhang@sxicc.ac.cn</u> (Y. Zhang)

# 1. The evaluation on compatibility and stability over $Ni\text{-}MoS_2/\gamma\text{-}$

## Al<sub>2</sub>O<sub>3</sub> catalyst

**Table S1.** Summary on the hydrogenation of various nitroarenes over Ni-MoS $_2/\gamma$ -Al $_2O_3$  catalyst.

		Ni-MoS <sub>2</sub> /Al <sub>2</sub> O <sub>3</sub>	R NH2	
Entry	Substrate	N <sub>2</sub> H <sub>4</sub> ·H <sub>2</sub> O (equiv.)	Time/ h	Sel./ yield <sup>a</sup> (%)
1	NO <sub>2</sub>	3	2	99/99
2	CINO2	3	6	99/99
3	CI NO2	3	4	99/99
4	F NO <sub>2</sub>	3	4	98/97
5	Br NO <sub>2</sub>	3	4	99/99
6	NO <sub>2</sub>	5	8	98/97
7	CI NO <sub>2</sub>	5	8	99/99
8	H <sub>3</sub> C NO <sub>2</sub>	5	12	100/99

9	H <sub>2</sub> N NO <sub>2</sub>	8	4	100/99
10	NO <sub>2</sub> NH <sub>2</sub>	8	10	99/98
11	H <sub>2</sub> N NO <sub>2</sub>	8	6	100/99
12	HO NO <sub>2</sub>	6	16	99/99
13	H <sub>3</sub> CO NO <sub>2</sub>	5	8	99/98
14	HOOC NO2	5	8	99/99
15	H <sub>3</sub> COOC	5	8	99/99
16	NC NO <sub>2</sub>	3	4	99/99
17	O NO2	5	8	99/98
18	NO <sub>2</sub>	3	2	98/98
19	NO <sub>2</sub>	5	4	99/99
20	HS NO <sub>2</sub>	5	8	99/99

Reaction conditions: 0.1 g catalyst, 1 mmol substrate, 100 °C, 15 mL isopropyl alcohol, 1 MPa N<sub>2</sub>, n equiv. N<sub>2</sub>H<sub>4</sub>·H<sub>2</sub>O, calibration concentration of N<sub>2</sub>H<sub>4</sub>·H<sub>2</sub>O is 79.2%.



**Fig. S1.** (a) Recyclability test; (b) Hot filtration test. After reaction for 0.5 h, the catalyst was separated under the reaction conditions. Inset of (b): The photographs showing before and after the facile separation via the centrifugation. Reaction conditions: 0.1 g catalyst, 1 mmol nitrobenzene, 100 °C, 15 mL isopropyl alcohol, 1 MPa N<sub>2</sub>, 2 equiv.  $N_2H_4$ ·H<sub>2</sub>O, 1 h.

#### 2. Catalysts characterization

#### **ICP-AES**

Table S2. The ICP-AES analysis of the metal loading.				
Catalysts	Content of metals			
NiO <sub>x</sub> /γ-Al <sub>2</sub> O <sub>3</sub>	Ni 2.32wt%			
$MoO_3/\gamma$ - $Al_2O_3$	Mo 9.67wt%			
Fe-MoO <sub>3</sub> /γ-Al <sub>2</sub> O <sub>3</sub>	Fe 2.30wt%; Mo 9.71wt%			
Co-MoO <sub>3</sub> /γ-Al <sub>2</sub> O <sub>3</sub>	Co 2.26wt%; Mo 9.75wt%			
Ni-MoO <sub>3</sub> /γ-Al <sub>2</sub> O <sub>3</sub>	Ni 2.34wt%; Mo 9.77wt%			



Fig. S2. XRD patterns of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (a), MoS<sub>2</sub>/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (b), Co-MoS<sub>2</sub>/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (c), Ni-MoS<sub>2</sub>/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (d) and Fe-MoS<sub>2</sub>/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (e) catalysts.

XPS



Fig. S3 XPS spectra showing the binding energies of Ni  $2p_{3/2}$  (a), Co  $2p_{3/2}$  (b) and Fe  $2p_{3/2}$  (c) in various catalysts.

**Table S3.** Synthesis of aniline using different intermediates as substrates over theNi-MoS $_2/\gamma$ -Al $_2O_3$  catalyst <sup>a</sup>

Entry	Reactant	Conv. (%)	Select. (%)
1	NO <sub>2</sub>	67	99
2	NO	95	98
3	NHOH	99	99
4		7	92
5		10	98

<sup>*a*</sup> Reaction conditions: 0.1 g catalyst, 1 mmol substrate, 100 °C, 0.5 h, 15 mL isopropyl alcohol, 1 MPa  $N_2$ , 2 equiv.  $N_2H_4$ · $H_2O$ .

Table S4. The NO adsorption on Mo edge by DFT calculation				
	Adsorption (eV)	kJ/mol		
Мо	-0.356	-34.346		
Fe	-0.365	-35.260		
Со	-0.446	-43.062		
Ni	-0.348	-33.560		