

Figure Captions

Fig. S1. Particle size distribution of BHP-char and $\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$.

Fig. S2. TG and DTG profiles of BHP-char and $\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$.

Fig.S3. SEM micrographs of (a) and (d) BHP-char, (b) and (e) $\text{NH}_4\text{Cl-BHP-char}$, and (c) and (f) $\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$.

Fig.S4. FTIR spectra of $\text{NH}_4\text{Cl-BHP/Fe}_3\text{O}_4$ before and after co-adsorption of Zn^{2+} and TC.

Table Captions

Table S1. Structure and properties of TC.

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Table S4. Parameters of isotherms for the adsorption of TC and Zn(II) on BHP-char and $\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$. Conditions: pH of single-component adsorption of TC was 4.0, pH of single-component adsorption of Zn(II) was 6.5, pH of co-adsorption of TC/Zn(II) was 6.0, adsorbent concentrations 0.5 g L^{-1} , temperature $25 \text{ }^\circ\text{C}$, contact time 120 min.

Table S5. Parameters of thermodynamic for the adsorption of TC and Zn(II) on BHP-char and $\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$. Conditions: pH of single-component adsorption of TC was 4.0, pH of single-component adsorption of Zn(II) was 6.5, pH of co-adsorption of TC/Zn(II) was 6.0, adsorbent concentrations 0.5 g L^{-1} , initial TC/Zn(II) concentrations 25 mg L^{-1} , contact time 120 min.

Table S6. Constants of film diffusion model for TC and Zn(II) on BHP and $\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$.

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Table S1. Structure and properties of TC.

Compound	Chemical formula	Molecular weight	Density (g cm ⁻³)	Refractive index	Melting point (°C)	flash point (°C)	Molecular structure
Tetracycline	C ₂₂ H ₂₄ N ₂ O ₈	444.43	1.644	1.650	172-174	431.9	

Table S2. Particle size distribution of BHP-char and NH₄Cl-BHP-char/Fe₃O₄.

Adsorbent	D10 ^a (μm)	D50 ^b (μm)	D90 ^c (μm)
BHP-char	34.73	101.1	211.3
NH ₄ Cl-BHP-char/Fe ₃ O ₄	0.969	3.889	8.984

^a Particle diameter corresponding to 10% cumulative (from 0 to 100%) undersize particle size distribution;

^b Particle diameter corresponding to 50% cumulative (from 0 to 100%) undersize particle size distribution;

^c Particle diameter corresponding to 90% cumulative (from 0 to 100%) undersize particle size distribution.

Table S3. Parameters of pseudo-first-order and pseudo-second-order models for the adsorption of TC and Zn(II) on BHP-char and NH₄Cl-BHP-char/Fe₃O₄.

Single-component adsorption	Adsorbent	Q _{e,exp} (mg g ⁻¹)	Pseudo-first-order model			Pseudo-second-order model		
			k ₁	R ²	Q _{e,cal}	k ₂	R ²	Q _{e,cal}
			(1 min ⁻¹)		(mg g ⁻¹)	(g mg ⁻¹ min ⁻¹)		(mg g ⁻¹)
TC	BHP-char	28.80	0.0328	0.9759	21.53	0.0050	0.9929	28.99
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	47.55	0.0307	0.9921	38.02	0.0022	0.9959	48.78
Zn ²⁺	BHP-char	38.26	0.0734	0.9798	25.33	0.0074	0.9977	39.53
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	49.23	0.0691	0.9791	28.51	0.0094	0.9931	48.08
Co-adsorption	Adsorbent	Q _{e,exp} (mg g ⁻¹)	Pseudo-first-order model			Pseudo-second-order model		
			k ₁	R ²	Q _{e,cal}	k ₂	R ²	Q _{e,cal}
			(1 min ⁻¹)		(mg g ⁻¹)	(g mg ⁻¹ min ⁻¹)		(mg g ⁻¹)
TC	BHP-char	36.16	0.0799	0.9852	28.59	0.0064	0.9919	37.88
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	48.55	0.0871	0.9798	29.67	0.0057	0.9990	51.55
Zn ²⁺	BHP-char	39.51	0.0928	0.9806	18.48	0.0226	0.9970	39.06
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	49.66	0.0965	0.9934	29.92	0.0109	0.9959	50.25

Table S4. Parameters of isotherms for the adsorption of TC and Zn(II) on BHP-char and NH₄Cl-BHP-char/Fe₃O₄.

Single-component adsorption	Adsorbent	Langmuir			Freundlich		
		q _L	K _L	R ²	K _F	n	R ²
		(mg g ⁻¹)	(L mg ⁻¹)				
TC	BHP-char	39.68	0.3007	0.9913	6.68	1.7265	0.9746
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	106.38	0.8174	0.9951	35.59	1.3841	0.9777
Zn ²⁺	BHP-char	109.89	0.1033	0.9966	8.06	1.3972	0.9771
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	151.52	0.4342	0.9977	27.04	1.5230	0.9540
Single-component adsorption	Adsorbent	Temkin			D-R		
		K _T	β _T	R ²	q _D	E	R ²
		(L g ⁻¹)	(kJ mol ⁻¹)		(mg g ⁻¹)	(kJ mol ⁻¹)	
TC	BHP-char	10.03	0.4385	0.9169	16.92	2.9090	0.8413
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	38.47	0.1839	0.8710	41.16	3.9724	0.9148
Zn ²⁺	BHP-char	5.03	0.1670	0.9032	35.38	2.2854	0.7770
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	24.48	0.1266	0.9197	64.94	3.4598	0.8874

Co-adsorption	Adsorbent	Langmuir			Freundlich		
		q_L (mg g^{-1})	K_L (L mg^{-1})	R^2	K_F	n	R^2
TC	BHP-char	76.92	0.1783	0.8938	9.38	1.5202	0.9989
	$\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$	126.58	1.1791	0.9448	61.14	1.3307	0.9948
Zn^{2+}	BHP-char	192.31	0.081	0.7871	12.62	1.347	0.9986
	$\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$	357.14	1.077	0.8957	216.35	1.157	0.9943
Co-adsorption	Adsorbent	Temkin			D-R		
		K_T (L g^{-1})	β_T (kJ mol^{-1})	R^2	q_D (mg g^{-1})	E (kJ mol^{-1})	R^2
TC	BHP-char	10.68	0.2858	0.7772	19.17	5.9133	0.7445
	$\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$	70.99	0.1745	0.8038	45.92	4.703	0.9231
Zn^{2+}	BHP-char	7.99	0.1288	0.7459	38.83	3.902	0.7035
	$\text{NH}_4\text{Cl-BHP-char/Fe}_3\text{O}_4$	128.59	0.08468	0.7880	108.20	3.841	0.9341

Table S5. Parameters of thermodynamic for the adsorption of TC and Zn(II) on BHP-char and NH₄Cl-BHP-char/Fe₃O₄.

Single-component adsorption	Adsorbent	ΔG° (KJ mol ⁻¹)					ΔH° (KJ mol ⁻¹)	ΔS° (KJ mol ⁻¹)	R ²
		293K	298K	303K	308K	313K			
		TC	BHP-char	-1.346	-2.588	-3.830			
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	-6.519	-8.773	-11.027	-13.281	-15.535	125.633	0.4508	0.9902
Zn ²⁺	BHP-char	-2.948	-4.748	-6.548	8.348	-10.148	102.586	0.3600	0.9991
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	-10.049	-12.075	-14.100	-16.126	-18.151	108.706	0.4051	0.9936
Co-adsorption	Adsorbent	ΔG° (KJ mol ⁻¹)					ΔH° (KJ mol ⁻¹)	ΔS° (KJ mol ⁻¹)	R ²
		293K	298K	303K	308K	313K			
		TC	BHP-char	-2.344	-4.199	-6.055			
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	-8.167	-10.301	-12.434	-14.568	-16.701	116.920	0.4267	0.9989
Zn ²⁺	BHP-char	-3.209	-5.191	-7.173	-9.155	-11.137	112.996	0.3964	0.9947
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	-12.299	-13.858	-15.417	-16.976	-18.535	79.105	0.3118	0.9961

Table S6. Constants of film diffusion model for TC and Zn(II) on BHP and NH₄Cl-BHP-char/Fe₃O₄.

Adsorbate	Adsorbent	Film diffusion model		
		k_F (min ⁻¹)	A	R ²
TC (Single-component adsorption)	BHP-char	0.0328	-0.2908	0.9725
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	0.0298	-0.1342	0.9824
Zn ²⁺ (Single-component adsorption)	BHP-char	0.0734	-0.4123	0.9769
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	0.0691	-0.5462	0.9761
TC (Co-adsorption)	BHP-char	0.0779	-0.2350	0.9831
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	0.0644	-0.0257	0.9692
Zn ²⁺ (Co-adsorption)	BHP-char	0.0928	-0.7599	0.9778
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	0.0965	-0.5068	0.9925

Table S7. Constants of Intra-particle diffusion model for TC and Zn(II) on BHP and NH₄Cl-BHP-char/Fe₃O₄.

Adsorbate	Adsorbent	Intra-particle diffusion model					
		k_{s1} (mg g min ⁻¹)	C_1 (mg g ⁻¹)	R^2	k_{s2} (mg g min ⁻¹)	C_2 (mg g ⁻¹)	R^2
TC (Single-component adsorption)	BHP-char	4.743	0.209	0.9971	1.388	14.514	0.9998
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	8.977	-5.610	0.9566	3.745	9.867	0.9987
Zn ²⁺ (Single-component adsorption)	BHP-char	8.768	1.919	0.9785	2.141	23.114	0.9525
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	7.959	12.063	0.9960	3.080	28.392	0.9604
TC (Co-adsorption)	BHP-char	7.678	0.042	0.9977	1.844	22.965	0.9301
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	8.519	-2.061	0.9815	5.656	7.927	0.9724
Zn ²⁺ (Co-adsorption)	BHP-char	5.802	15.536	0.9796	1.558	29.681	0.9407
	NH ₄ Cl-BHP-char/Fe ₃ O ₄	7.892	13.812	0.9846	4.288	24.733	0.9670

Text 1

Determination of Zn(II)

FAAS determination conditions: Wavelength of 213.86 nm, hollow cathode lamp current of 15 mA, slit of 2.7/1.8 mm, airflow rate of 10 L min⁻¹, and acetylene flow rate of 2.5 L min⁻¹.

Preparation of 50 mg L⁻¹ standard solution of Zn(II): Transfer 5 mL of 1,000 mg L⁻¹ stock solutions of Zn(II) to a 100 mL volumetric flask, and dilute with ultrapure water to a specific volume.

Preparation of Zn(II) working standard solution: Transfer 0, 1.0, 2.0, 4.0, 6.0, 8.0 and 10.0 mL of 50 mg L⁻¹ standard solution of Zn(II) to a 50 mL volumetric flask, respectively, and dilute with 1% nitric acid to volume. Zn(II) working standard solution concentrations were 0, 1.0, 2.0, 4.0, 6.0, 8.0 and 10.0 mg L⁻¹, respectively.

The linear relationship between absorbance and concentration is

$$y = 0.0567x + 0.438 \quad (R^2=0.9995)$$

Determination of TC

Preparation of TC working standard solution: Transfer 0, 0.05, 0.1, 0.25, 0.5, 1.0, 1.5 and 2.0 mL of 1,000 mg L⁻¹ stock solutions of TC to a 100 mL volumetric flask, respectively, and dilute with ultrapure water to a specific volume. TC working standard solution concentrations were 0, 0.5, 1.0, 2.5, 5.0, 10.0, 15.0 and 20.0 mg L⁻¹, respectively.

The linear relationship between absorbance and concentration is

$$y = 0.0354x + 0.2814 \quad (R^2=0.9992)$$

Text 2

Pseudo-first order model $\ln(q_e - q_t) = \ln q_e - k_1 t$

Pseudo-second order model $\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$

Film diffusion model $\ln\left(1 - \frac{q_t}{q_e}\right) = -k_F t + A$

Intra-particle diffusion model $q_t = k_s t^{1/2} + I$

where q_e (mg g^{-1}) and q_t (mg g^{-1}) are the amounts of TC or Zn(II) adsorbed on the biochar at equilibrium and at time t (min), respectively, k_1 (1 min^{-1}) is the rate constant of pseudo-first order adsorption. k_2 ($\text{g mg}^{-1} \text{ min}^{-1}$) is the rate constant of pseudo-second order adsorption. k_f (1 min^{-1}) and A are liquid film diffusion constants, where k_s ($\text{mg g}^{-1} \text{ min}^{-0.5}$) is the rate constant of intra-particle diffusion model, and I (mg g^{-1}) is a constant describing the thickness of boundary layer.

Text 3

Langmuir isotherm
$$\frac{C_e}{q_e} = \frac{1}{q_L K_L} + \frac{C_e}{q_L}$$

Freundlich isotherm
$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e$$

Temkin isotherm
$$q_e = \frac{RT}{\beta_T} \ln(K_T C_e)$$

D-R isotherm
$$\ln q_e = \ln q_D - \left(\frac{RT}{\sqrt{2E}}\right)^2 \times \left(\ln\left(1 + \frac{1}{C_e}\right)\right)^2$$

where q_L (mg g^{-1}) is the Langmuir maximum adsorption capacity of TC or Zn(II), K_L (L mg^{-1}) is the Langmuir constant termed as apparent energy of adsorption, K_F ($(\text{mg g}^{-1}) (\text{L mg}^{-1})^{1/n}$) is the Freundlich constants related to adsorption capacity, n is a measure of adsorption linearity, β_T (J mol^{-1}) is the Temkin constant related to heat of adsorption, K_T (L g^{-1}) is the Temkin isotherm constant, R ($8.314 \text{ J mol}^{-1} \text{ K}^{-1}$) is the gas constant, T (K) is the absolute temperature, q_D (mg g^{-1}) is the D-R maximum adsorption capacity of TC or Zn(II), and E (J mol^{-1}) is mean free energy of adsorption per molecule of the adsorbate.

Text 4

$$K_C = q_e / C_e$$

$$\Delta G^\circ = -RT \ln K_C$$

$$\Delta G^{\circ} = \Delta H^{\circ} - T\Delta S^{\circ}$$

$$\ln K_c = \frac{\Delta S^{\circ}}{R} - \frac{\Delta H^{\circ}}{RT}$$

where K_c (ml g^{-1}) is the thermodynamic equilibrium constant.