

**THE EFFECT OF CONTINUOUS TUBULAR REACTOR TECHNOLOGIES
ON THE PRETREATMENT OF LIGNOCELLULOSIC BIOMASS AT
PILOT-SCALE FOR BIOETHANOL PRODUCTION**

ELECTRONIC SUPPLEMENTARY INFORMATION (ESI)

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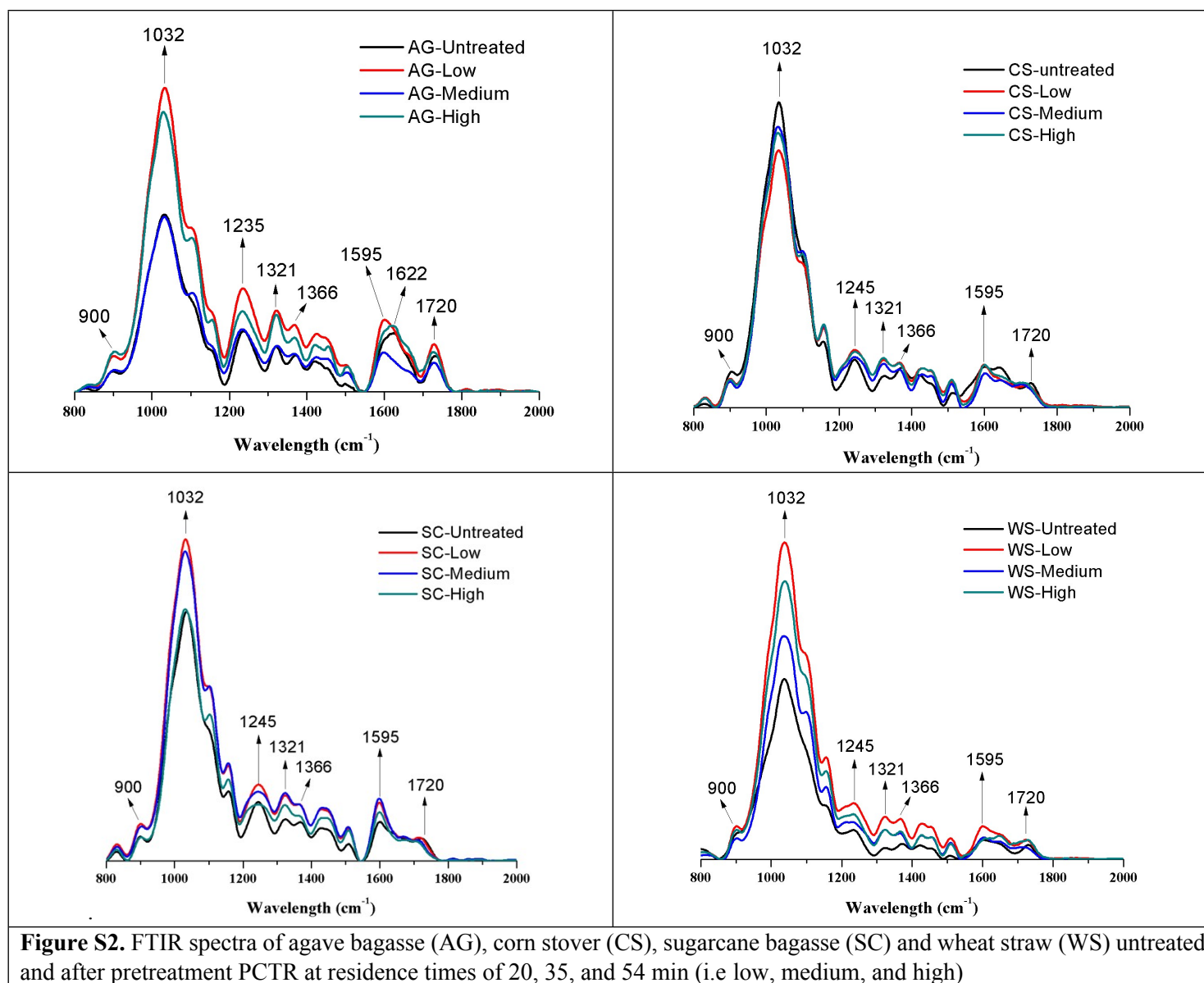
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Feedstock	Untreated	Pretreatment		
		Low (L)	Medium (M)	High (H)
Agave bagasse				
Corn stover				
Sugarcane bagasse				
Wheat straw				

Figure S1. Macroscopic effect on different feedstocks pretreated using PCTR at residence times of 20, 35, and 54 min [low (L), medium (M) and high (H) respectively].



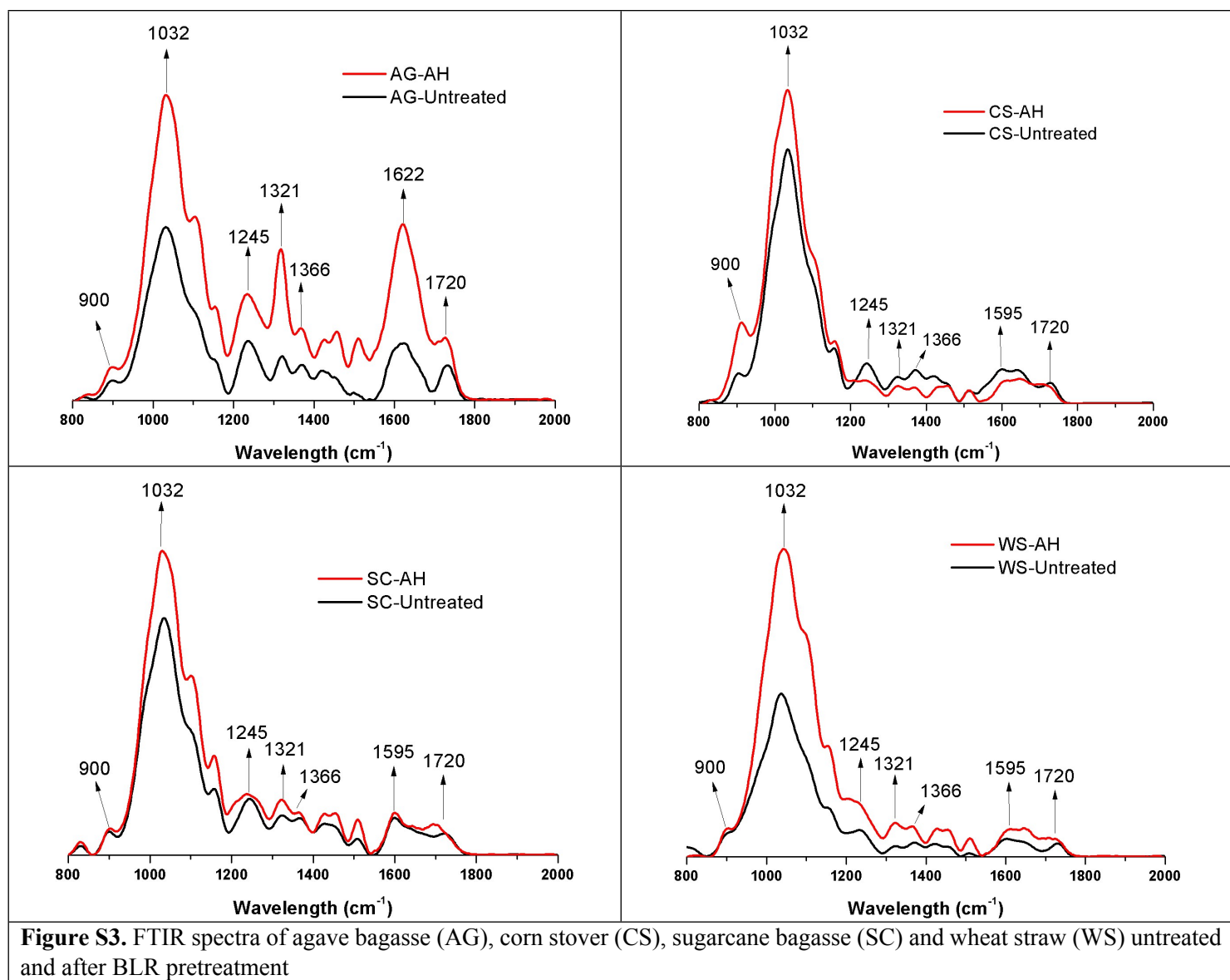


Table S1. FTIR band assignment.

Band position	Assignment
900	Anti-symmetric out of plane ring stretch of amorphous cellulose
1032	C-O stretching in cellulose & hemicellulose
1235	C=O deformation in cellulose & hemicellulose
1245	C-O adsorption (resulting from acetyl groups cleavage)
1321*	C=O stretching of calcium oxalate
1366	C-H deformation in cellulose & hemicellulose
1595	Aromatic ring stretch
1622*	C-O stretching of calcium oxalate
1720	Carbonyl (C=O) stretching

*Only for agave bagasse.

Table S2. Comparison of sugar and ethanol yields of PCTR-pretreated biomass using SSF with a total process time of 96 h.

Feedstock	Glucose ^a	Xylose ^a	Ethanol ^b	Y _E (%)	Q _{EtOH 24 h} (g _{EtOH} /L h)
	g/L				
AG	77.2±5.1	22.5±1.3	37.6±0.6	60.7±0.9	1.38±0.02
CS	87.5±1.9	29.8±0.9	40.4±0.5	60.0±0.7	1.51±0.03
SC	73.6±2.7	18.0±0.7	36.3±2.1	46.0±2.7	1.30±0.03
WS	92.9±1.0	25.1±0.5	41.6±0.5	60.6±0.7	1.59±0.03

^a 1st stage: saccharification (24 h)

^b 2nd stage: fermentation (72 h)

Ethanol yield based on the glucan content in the pretreated material as % of the theoretical.

Q_{EtOH 24 h} = volumetric productivity of ethanol at 24 h elapsed fermentation time.

Error bars show standard deviation of triplicate measurements.