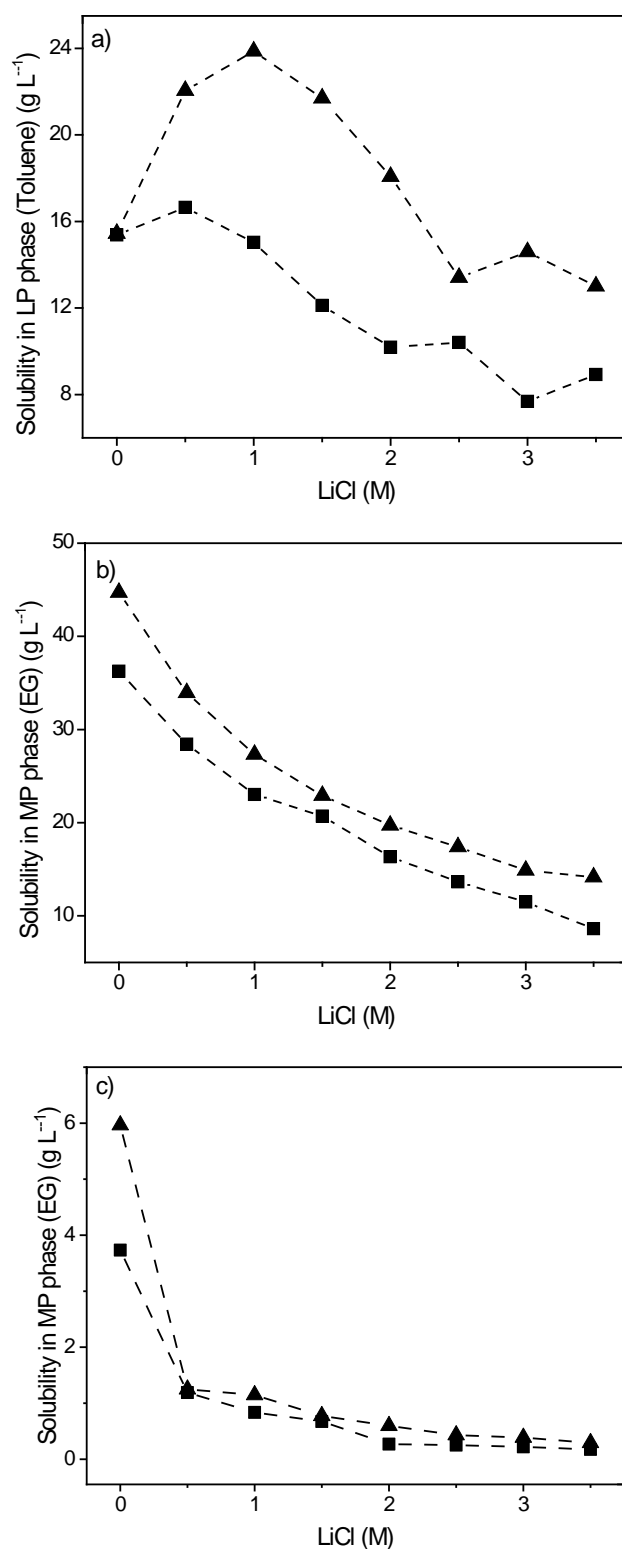


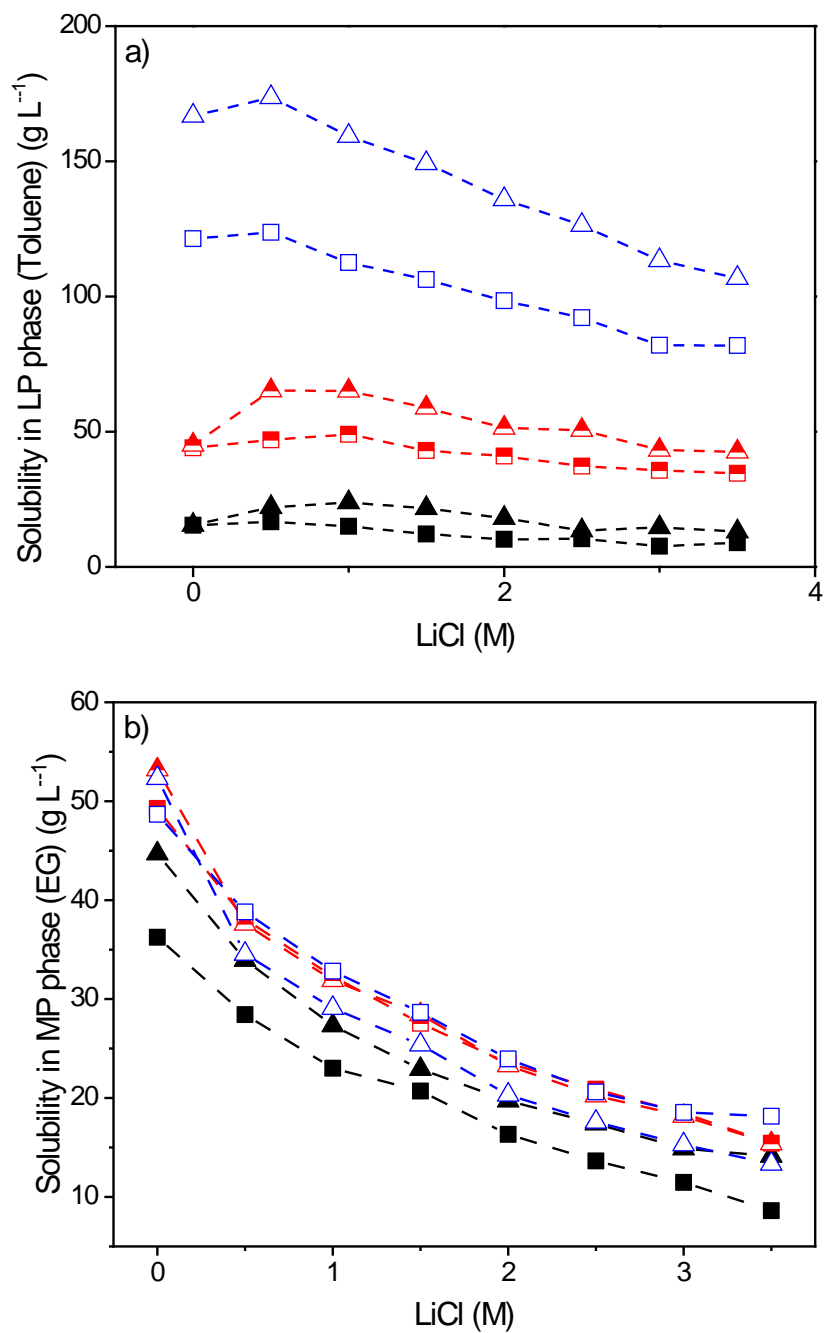
**Non-aqueous solvent extraction of indium from an ethylene glycol  
feed solution by the ionic liquid Cyphos IL 101: speciation study  
and continuous counter-current process in mixer-settlers**

**Clio Deferm, Bieke Onghena, Viet Tu Nguyen, Dipanjan Banerjee, Jan Fransaer and  
Koen Binnemans\***

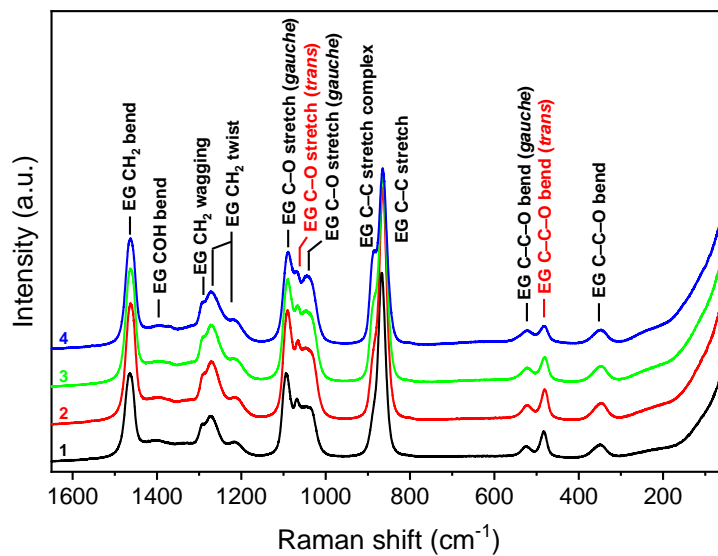
**Electronic Supplementary Information (ESI)**



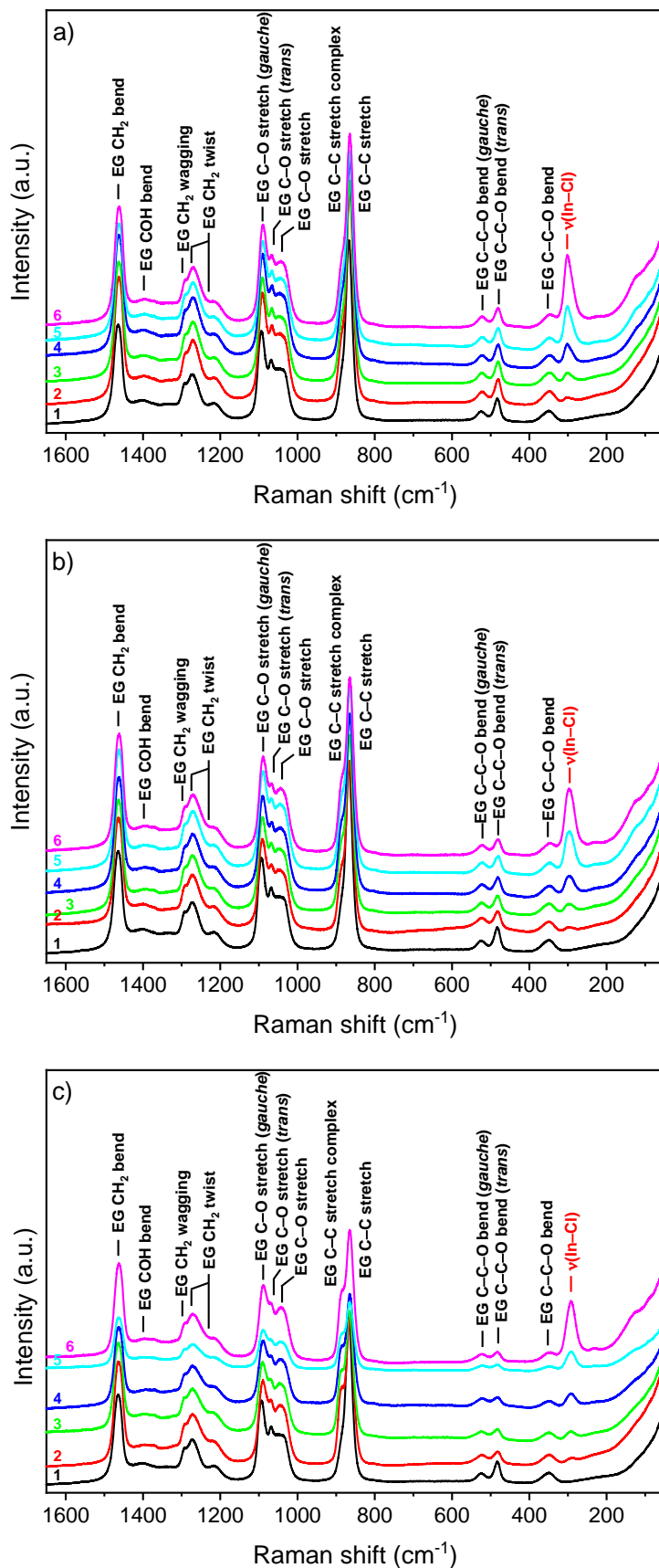
**Fig. S1** Effect of the LiCl concentration on the mutual solubility for the EG+(5 vol% Cyphos IL 101 in toluene) system (■) and the EG+(5 vol% Aliquat 336 in toluene) system (▲): (a) solubility of EG in the toluene phase; (b) solubility of toluene in the EG phase; (c) solubility of Aliquat 336 and Cyphos IL 101 in the EG phase.



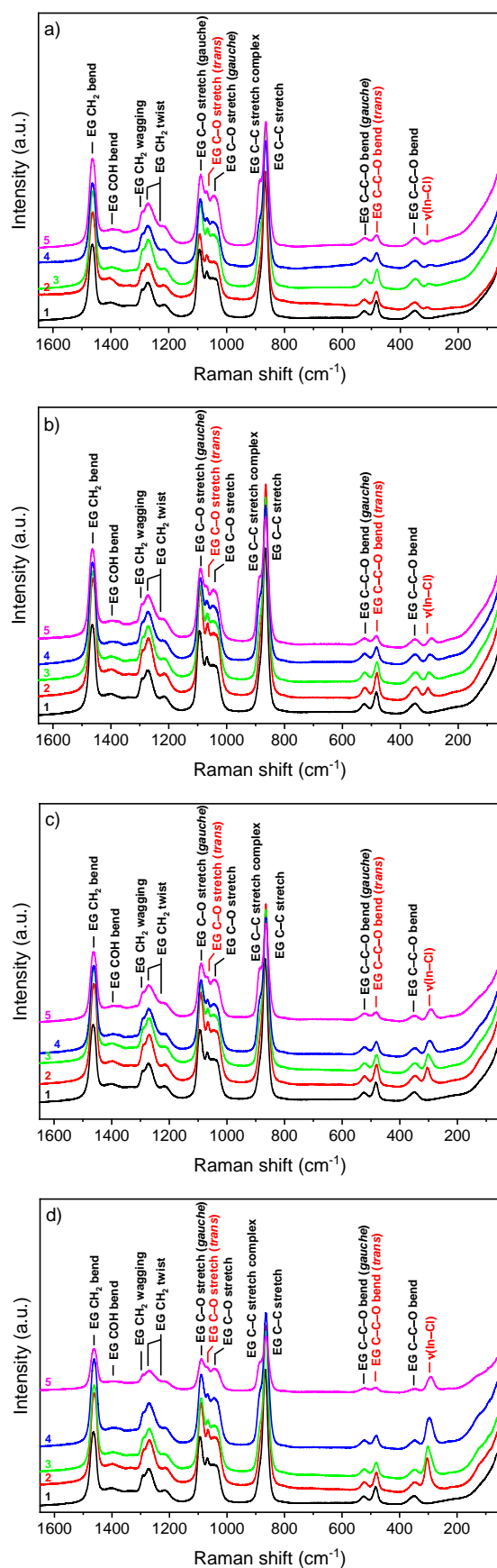
**Fig. S2** Effect of the extractant and LiCl concentration on the mutual solubility for the EG+(Cyphos IL 101 in toluene) system (■) and the EG+(Aliquat 336 in toluene) system (▲): (a) solubility of EG in the toluene phase, 5 vol% (filled), 10 vol% (half-filled), 20 vol% (unfilled) of extractant; (b) solubility of toluene in the EG phase, 5 vol% (filled), 10 vol% (half-filled), 20 vol% (unfilled) of extractant.



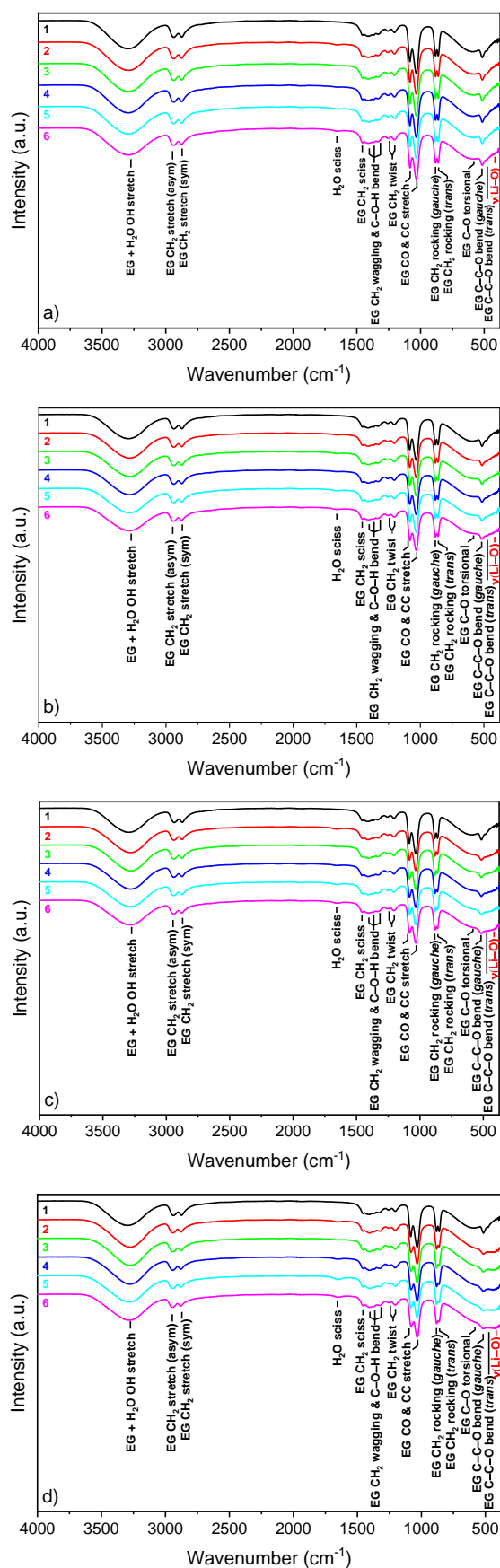
**Fig. S3** Raman spectra at of solutions containing 1 M LiCl (2), 2 M LiCl (3) and 3.5 M LiCl (4) in EG (1).  $\lambda_{\text{laser}} = 532.0 \text{ nm}$ .



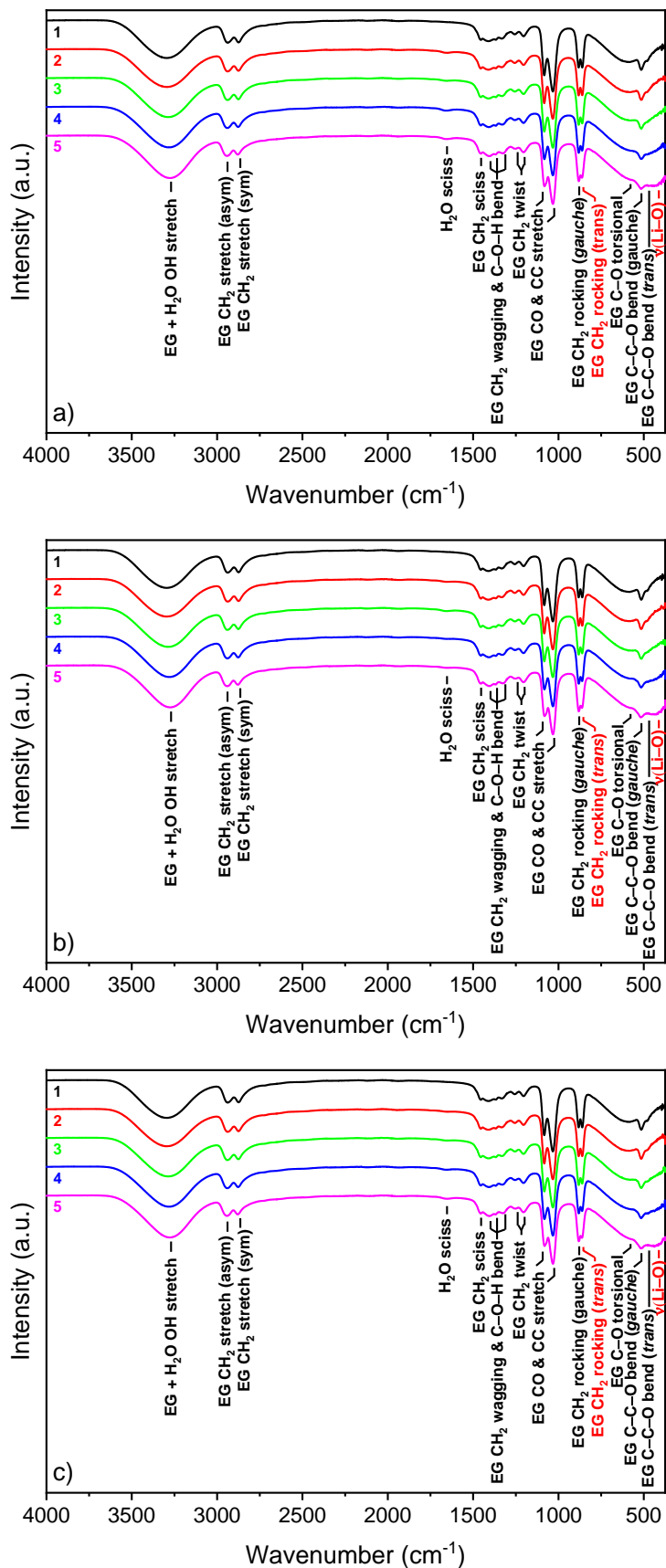
**Fig. S4** Raman spectra of solutions containing 1 M LiCl (a), 2 M LiCl (b) and 3.5 M LiCl (c) as a function of the indium concentration. EG (1), 5 gL<sup>-1</sup> indium (2), 10 gL<sup>-1</sup> indium (3), 20 gL<sup>-1</sup> indium (4), 40 gL<sup>-1</sup> indium (5), 60 gL<sup>-1</sup> indium (6).  $\lambda_{\text{laser}} = 532.0$  nm.



**Fig. S5** Raman spectra of solutions containing 5 gL<sup>-1</sup> indium (a), 10 gL<sup>-1</sup> indium (b), 20 gL<sup>-1</sup> indium (c) and 40 gL<sup>-1</sup> indium (d) as a function of the LiCl concentration. EG (1), 0 M LiCl (2), 1 M LiCl (3), 2 M LiCl (4), 3.5 M LiCl (5).  $\lambda_{laser} = 532.0$  nm.

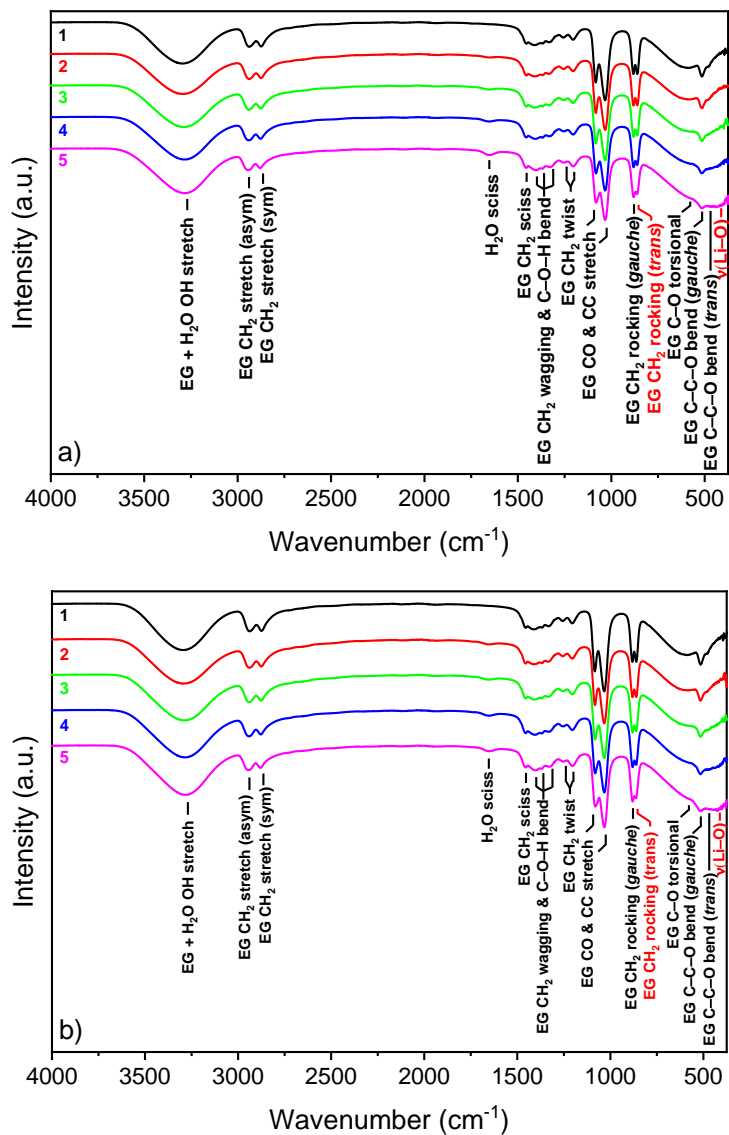


**Fig. S6** Infrared spectra of solutions containing 0 M LiCl (a), 1 M LiCl (b), 2 M LiCl (c) and 3.5 M LiCl (d) as a function of the indium concentration. EG (1), 5 gL<sup>-1</sup> indium (2), 10 gL<sup>-1</sup> indium (3), 20 gL<sup>-1</sup> indium (4), 40 gL<sup>-1</sup> indium (5), 60 gL<sup>-1</sup> indium (6).

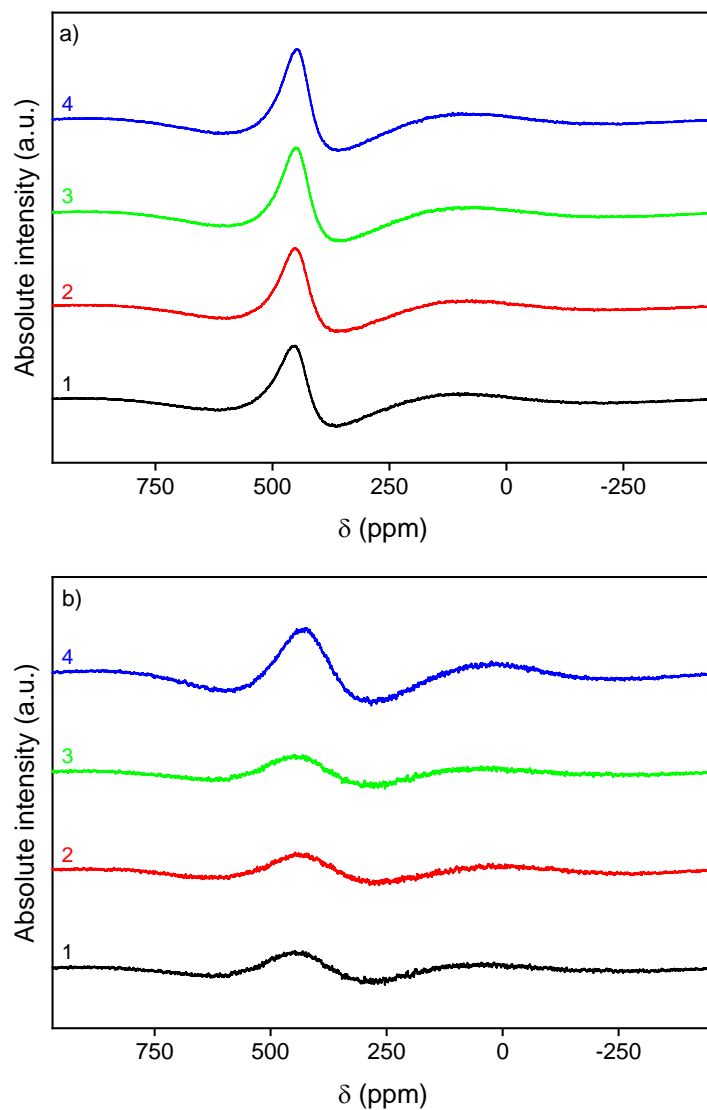


**Fig. S7** Infrared spectra of solutions containing 5  $\text{g L}^{-1}$  indium (a), 10  $\text{g L}^{-1}$  indium (b) and 20  $\text{g L}^{-1}$  indium (c) as a function of the LiCl concentration. EG (1 0 M LiCl (2), 1 M LiCl (3), 2 M LiCl (4), 3.5 M LiCl (5).

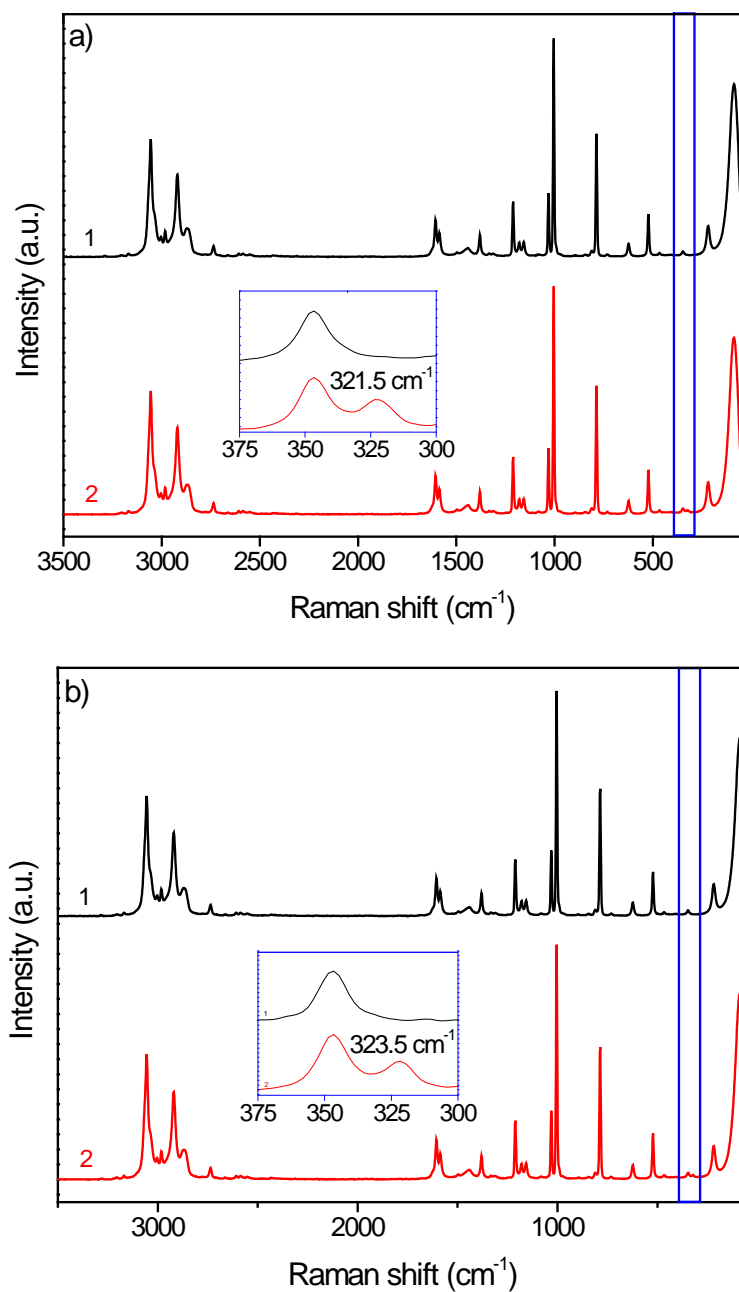




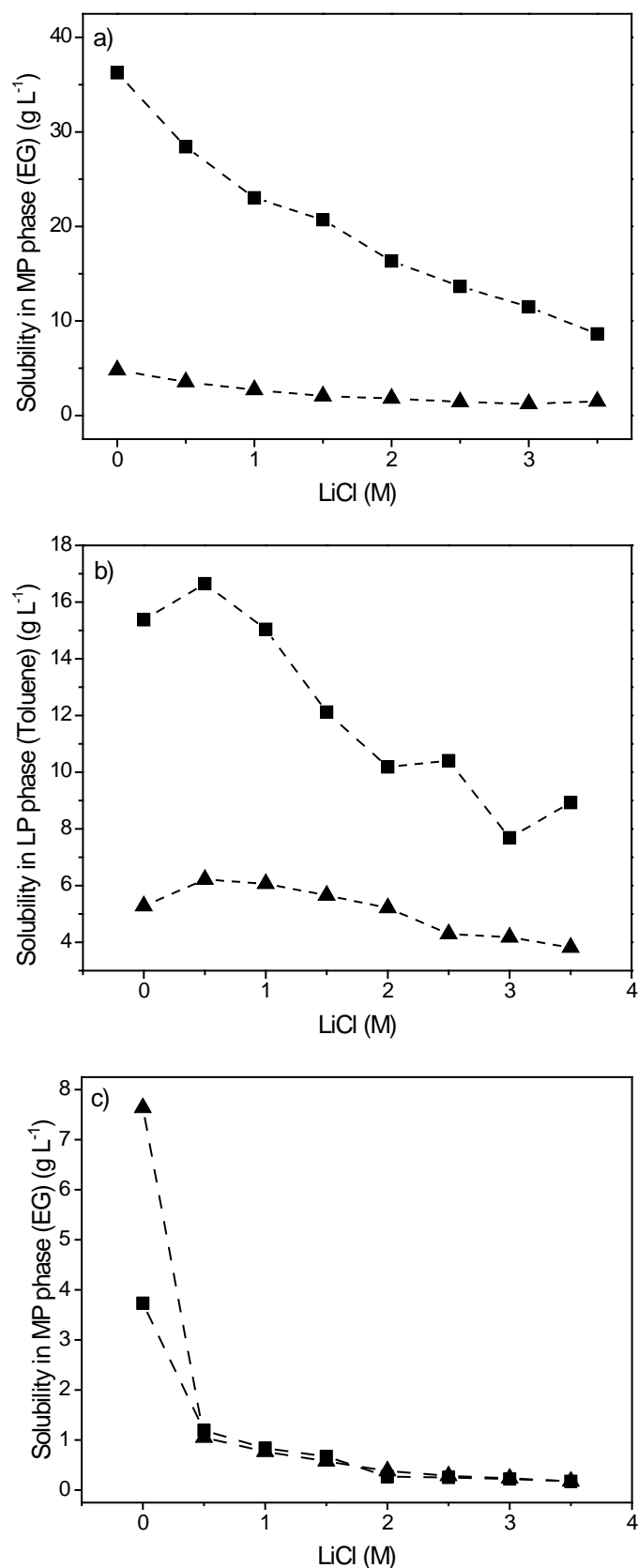
**Fig. S8** Infrared spectra of solutions containing 40  $\text{gL}^{-1}$  indium (a) and 60  $\text{gL}^{-1}$  indium (b) as a function of the LiCl concentration. EG (1), 0 M LiCl (2), 1 M LiCl (3), 2 M LiCl (4), 3.5 M LiCl (5).



**Fig. S9**  $^{115}\text{In}$  NMR spectra of the LP phase 5 vol% of Cyphos IL 101 in toluene (a) and the LP phase 5 vol% of Aliquat 336 in toluene (b) obtained after extraction with  $5 \text{ g L}^{-1}$  indium(III) and varying LiCl concentration: 0 M LiCl (1), 1 M LiCl (2), 2 M LiCl (3), 3.5 M LiCl (4).



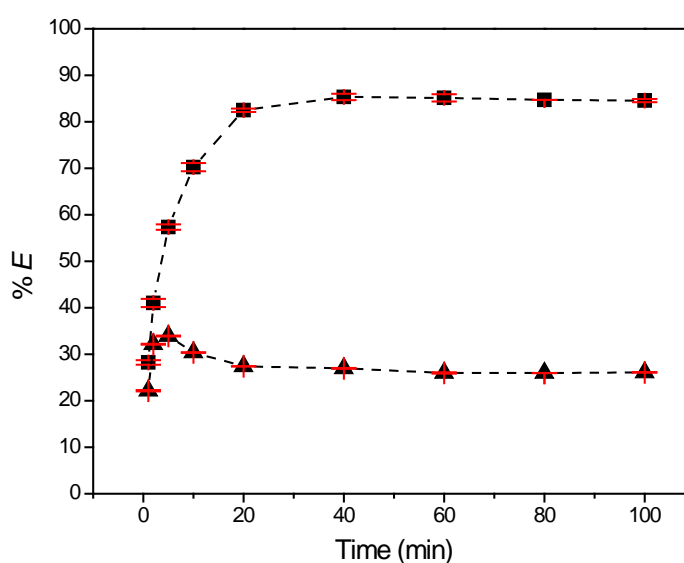
**Fig. S10** Raman spectra of the less polar phase: 5 vol% Cyphos IL 101 in toluene (a) and 5 vol% Aliquat 336 in toluene (b) obtained before (1) and after extraction (2) with 5 g L<sup>-1</sup> indium(III) and 3.5 M LiCl in EG.



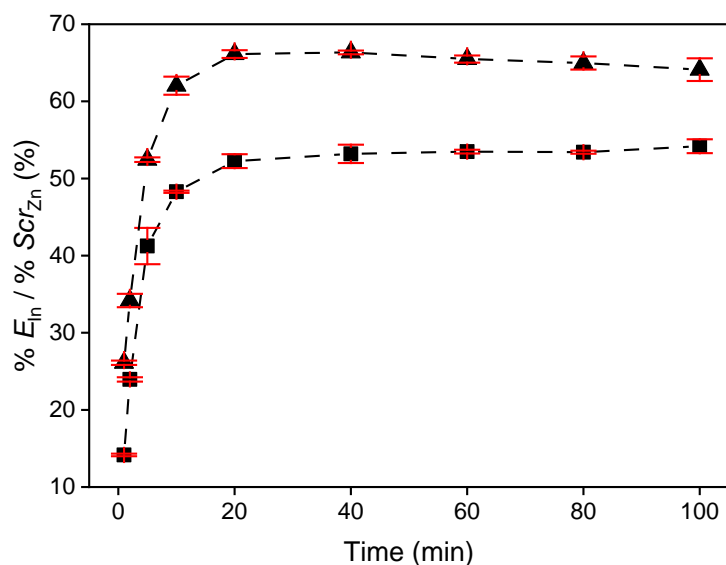
**Fig. S11** Effect of the LiCl concentration on the mutual solubility for EG+(2.56 vol% Cyphos IL 101 in toluene) system (■) and the EG+(2.56 vol% Cyphos IL 101 in *p*-cymene) system (▲): (a) solubility of EG in the toluene/*p*-cymene phase; (b) solubility of toluene/*p*-cymene in the EG phase; (c) solubility of Cyphos IL 101 in the EG phase.

**Table S1** % $E_{Zn}$  and % $S_{Zn}$  at different MP:LP phase ratio. Conditions: room temperature, 600–1000 rpm, 3 h, [Cyphos IL 101] = 2.56 vol%, [LiCl] = 3.5 M, [1-decanol] = 1 vol%. Initial metal concentrations extraction: [In(III)] = 5 g L<sup>-1</sup>, [Zn(II)] = 5 g L<sup>-1</sup>. Metal concentration scrubbing solution: [In(III)] = 5 g L<sup>-1</sup>.

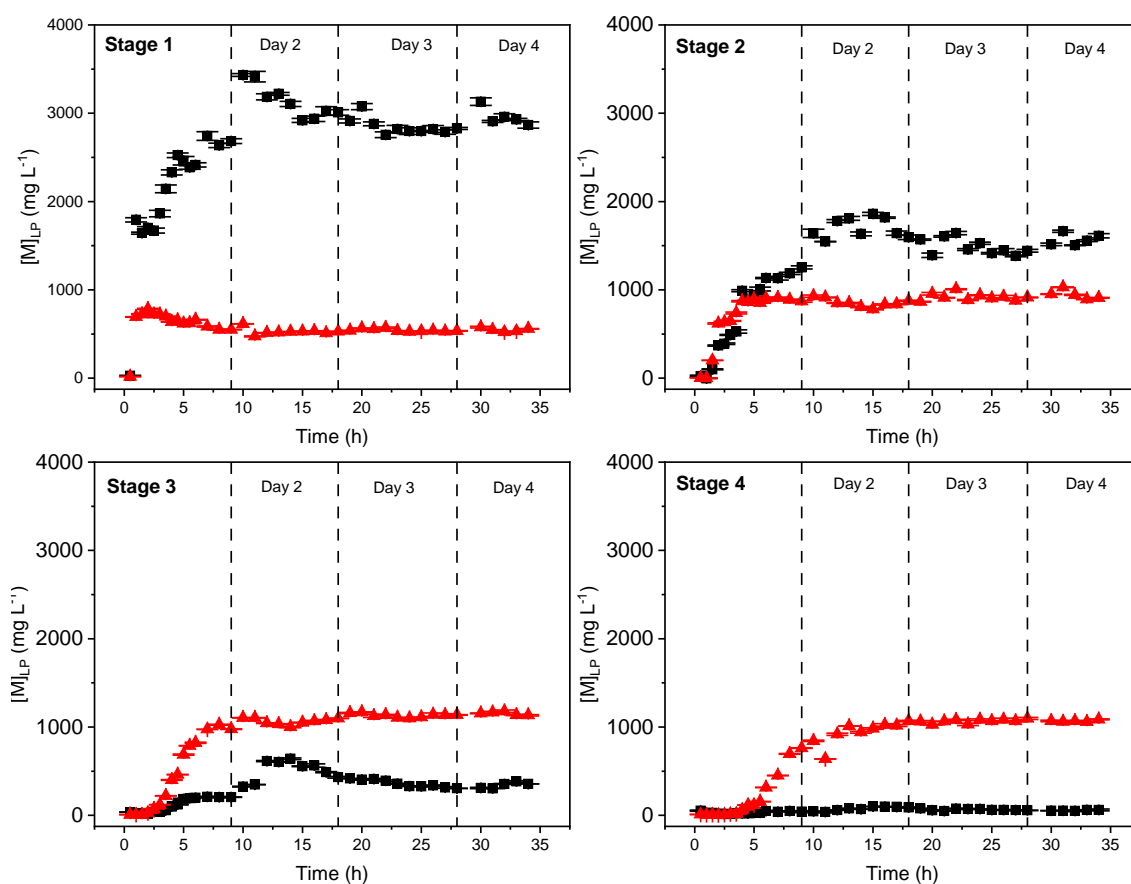
	McCabe–Thiele diagram extraction	McCabe–Thiele diagram scrubbing
MP:LP phase ratio	% $E_{Zn}$	% $S_{Zn}$
1:11	98	20
1:7	91	33
1:5	80	42
1:3	47	55
1:2	27	68
1:1	9	80
2:1	4	87
3:1	2	92
5:1	1	97
7:1	0.8	98
11:1	0.4	98



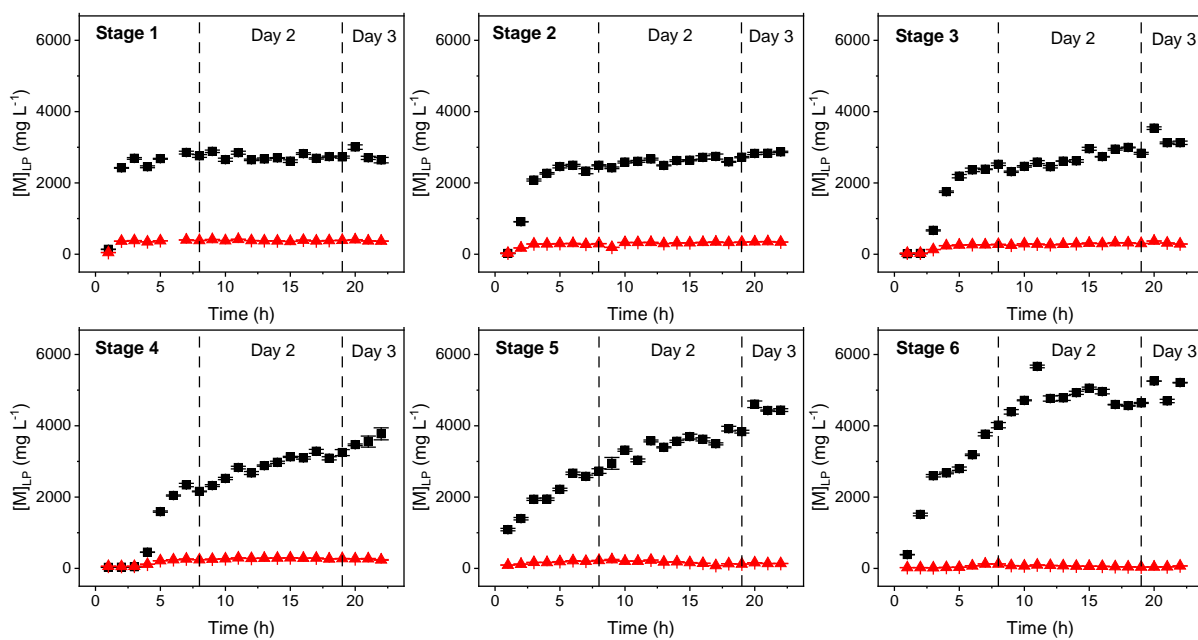
**Fig.S12** Percentage extraction (%E) of indium(III) (■) and zinc(II) (▲) as a function of the reaction time for the EG+(2.56 vol% Cyphos IL 101 in *p*-cymene) system. Conditions: volume MP:LP = 1:2, room temperature, 600 rpm, [LiCl] = 3.5 M, [1-decanol] = 1 vol%. Initial metal concentrations: [In(III)] = 5 g L<sup>-1</sup>, [Zn(II)] = 5 g L<sup>-1</sup>.



**Fig. S13** Percentage extraction of indium(III) (% $E_{In}$ ) (■) and percentage scrubbing of zinc(II) (% $S_{Zn}$ ) (▲) as a function of the reaction time for the loaded MP phase. Conditions: volume MP:LP = 1:1, room temperature, 600 rpm, [LiCl] = 3.5 M. Metal concentration scrubbing solution: [In(III)] = 5 g L<sup>-1</sup>.



**Fig. S14** Concentration profile of In(III) (black) and Zn(II) (red) in the extraction stages of the mixer-settler units. Conditions: volume MP:LP = 1:2, room temperature, 1000 rpm. Initial metal concentrations: [In(III)]<sub>MP</sub> = 5 g L<sup>-1</sup>, [Zn(II)]<sub>MP</sub> = 5 g L<sup>-1</sup> in EG. LP phase: 2.56 vol% Cyphos IL 101, 1 vol% 1-decanol in *p*-cymene.



**Fig. S15** Concentration profile of In(III) (black) and Zn(II) (red) in the scrub stages of the mixer-settler units. Conditions: volume MP:LP = 1:2, room temperature, 1000 rpm. Initial scrub feed concentration:  $[\text{In(III)}]_{\text{MP}} = 5 \text{ g L}^{-1}$  in EG. Loaded LP phase:  $2.85 \text{ g L}^{-1}$  indium(III),  $0.55 \text{ g L}^{-1}$  zinc (III), 2.56 vol% Cyphos IL 101, 1 vol% 1-decanol in *p*-cymene.