

## **Melamine-based Functionalized Graphene Oxide and Zirconium Phosphate for High Performance Removal of Mercury and Lead Ions from Water**

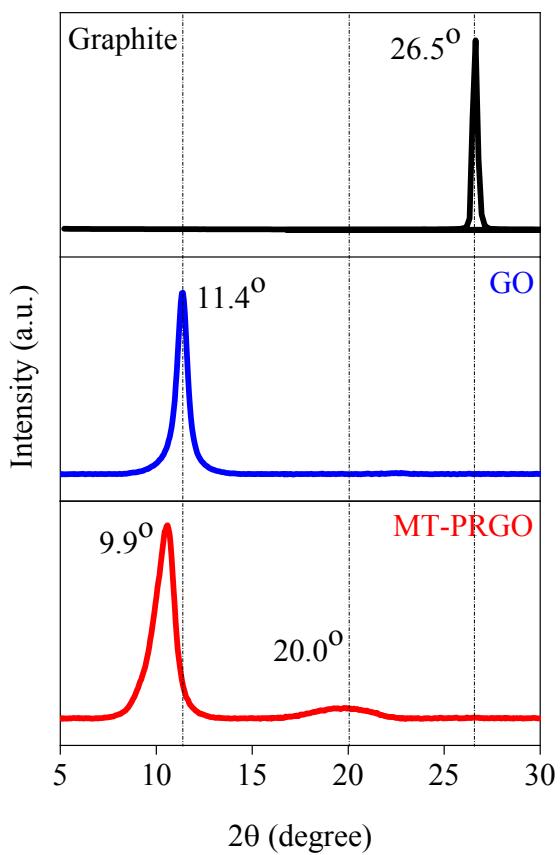
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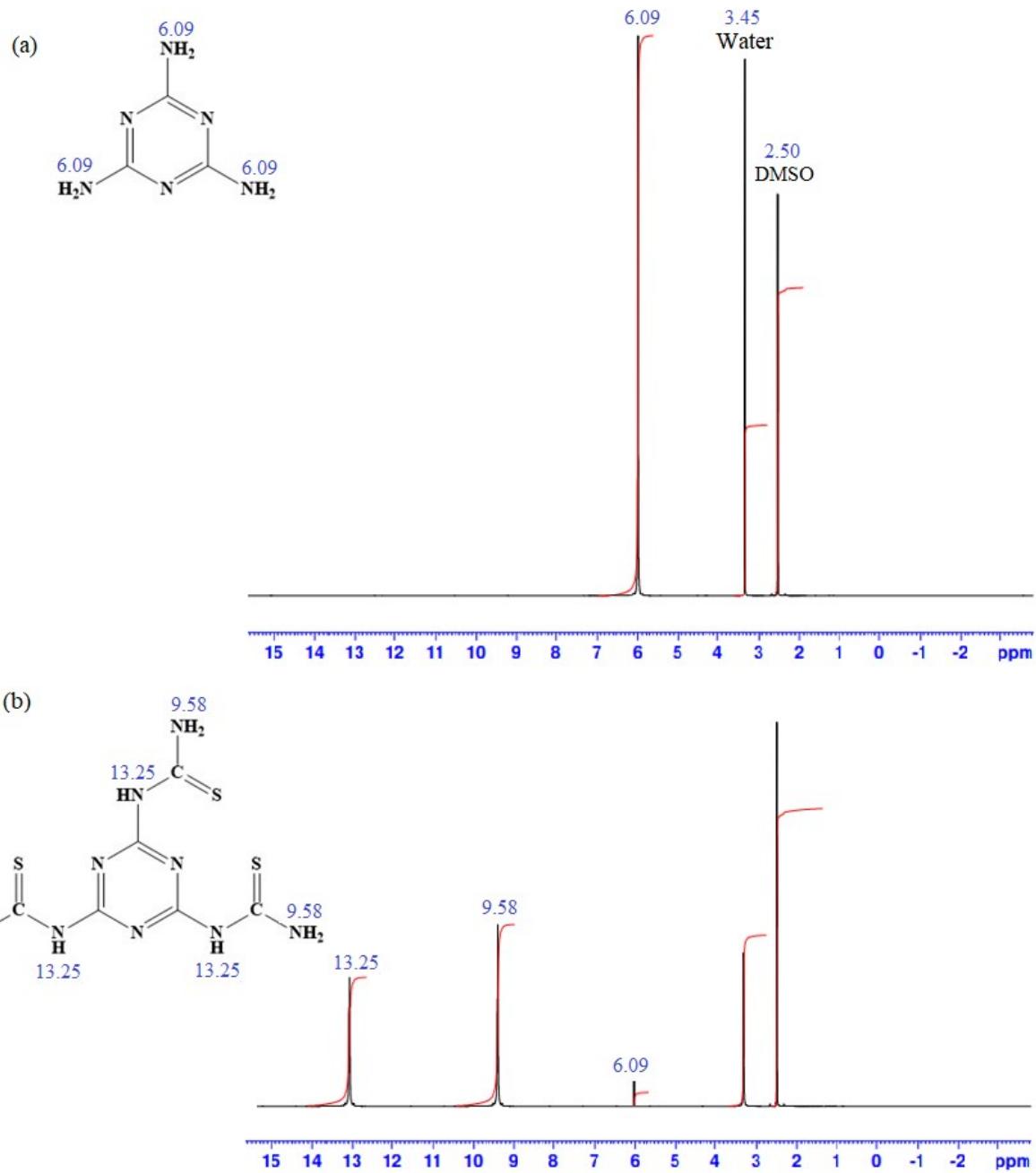
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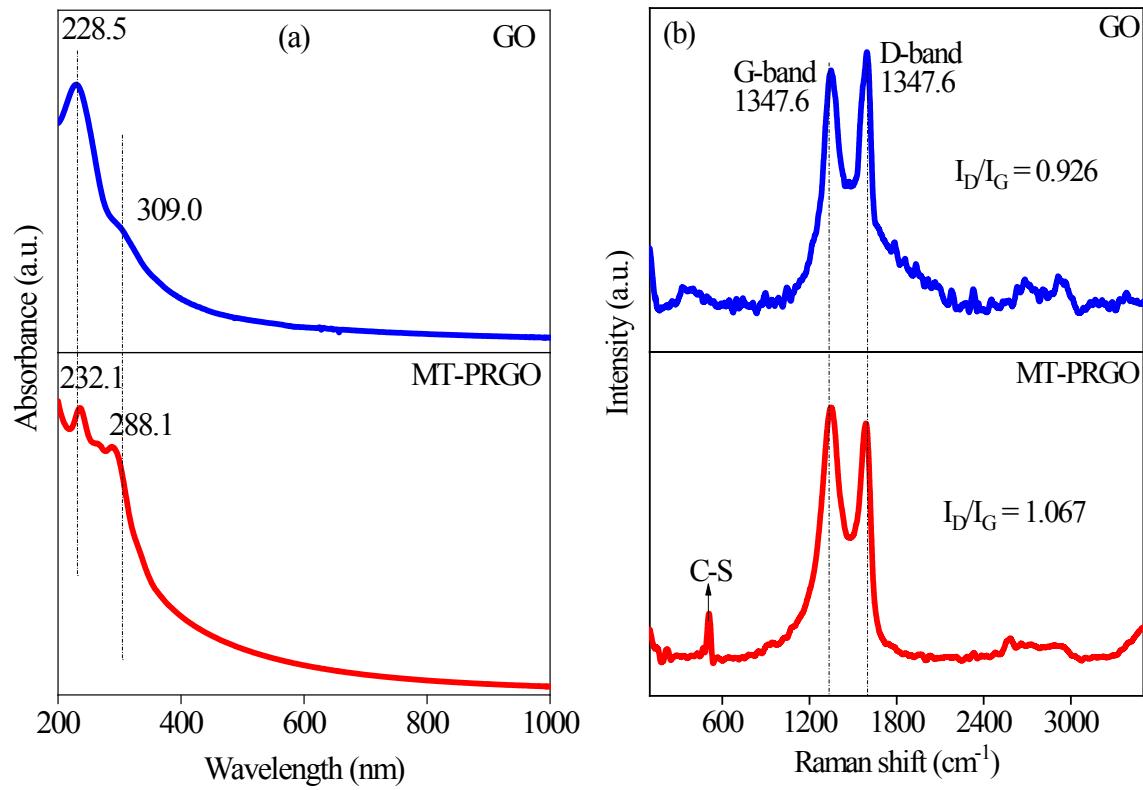
## **Supporting Information**



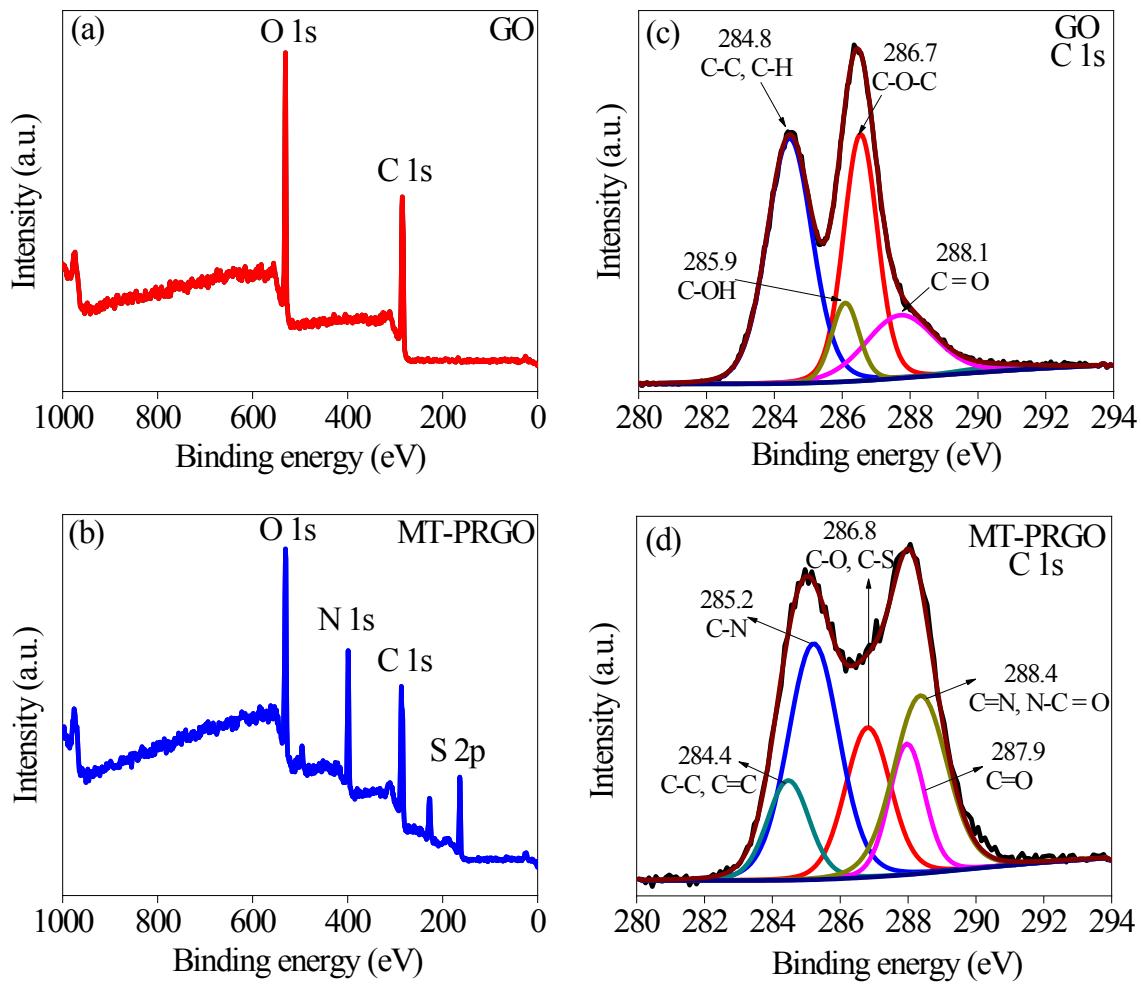
**Figure S1.** XRD patterns of Graphite, GO, and MT-PRGO.



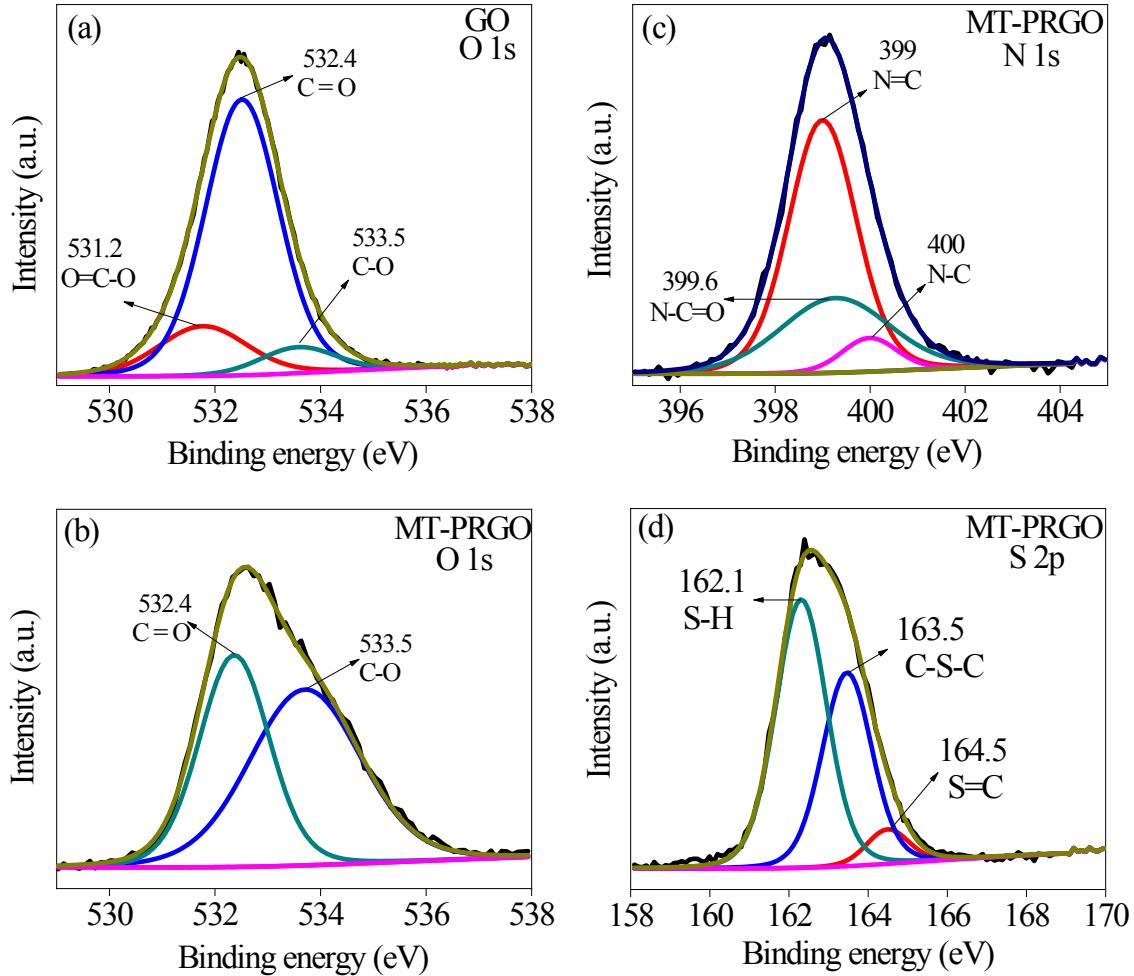
**Figure S2.**  $^1\text{H}$  NMR spectra of (a) melamine and (b) melamine thiourea (MT).



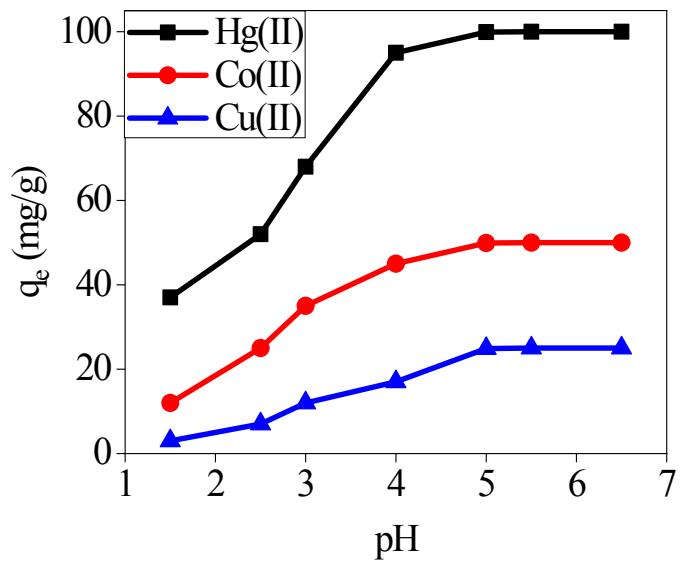
**Figure S3** (a) UV-Vis and (b) Raman spectra of GO and MT-PRGO.



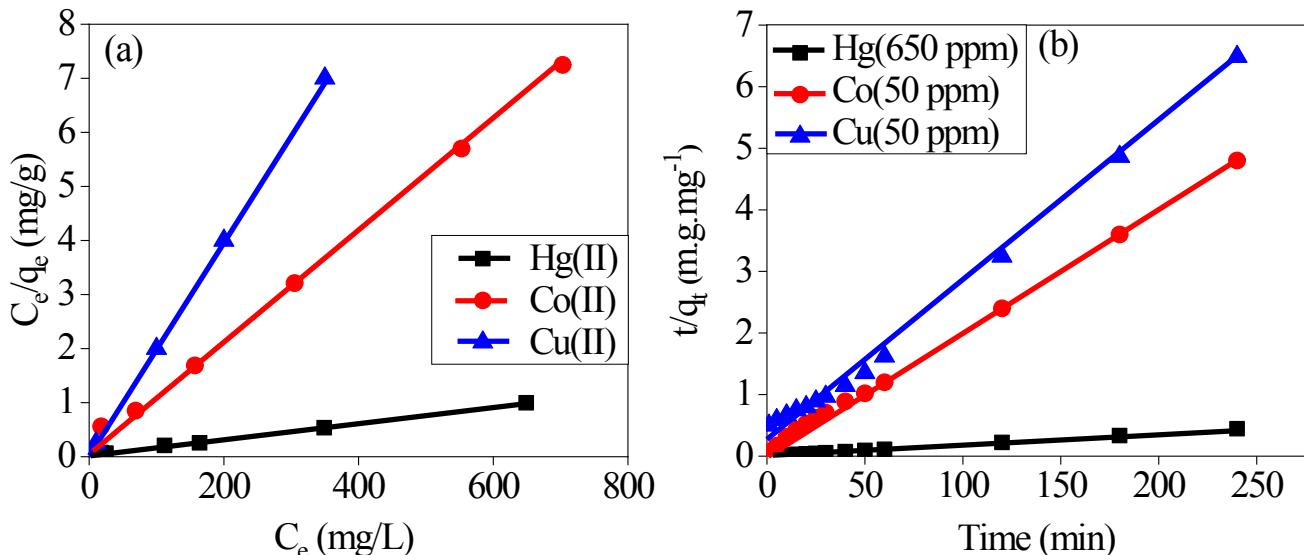
**Figure S4.** (a & b) XPS survey spectra, (c & d) C 1s of GO and MT-PRGO.



**Figure S5.** XPS spectra of (a & b) O 1s for GO and MT-PRGO, (c) N 1s, and (d) S 2p of MT-PRGO.



**Figure S6.** The effect of pH on the removal of Hg(II), Co(II), and Cu(II) ions by the MT-PRGO adsorbent [conditions:  $C_0 = (100, 50, 25 \text{ mg/g})$ , respectively,  $T = 298 \text{ K}$ ; adsorbent dose = 0.005 g/5 mL,  $t = 6 \text{ h}$ ].



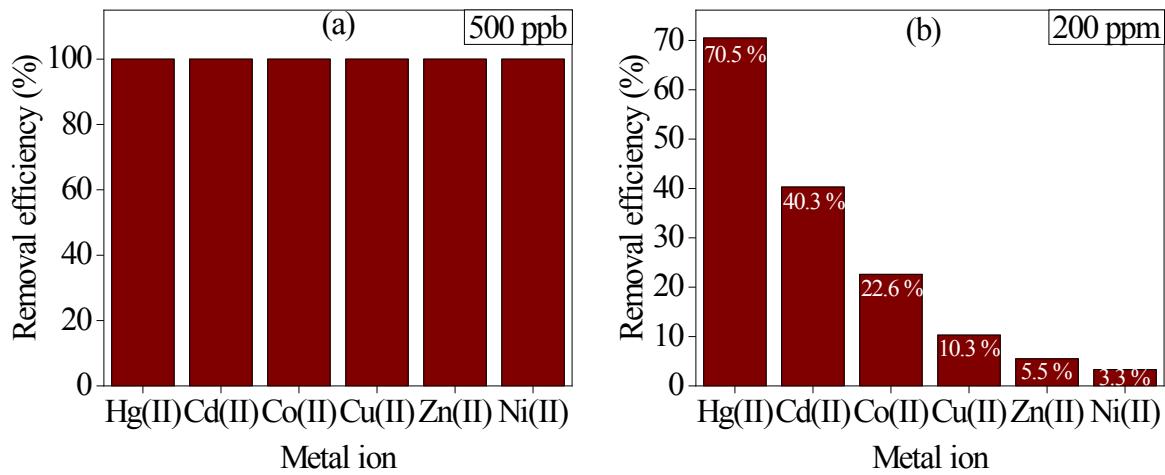
**Figure S7.** Langmuir isotherm model for the adsorption of Hg(II), Co(II), and Cu(II) ions on MT-PRGO. (B) Pseudo-second-order kinetic model for the adsorption Hg(II), Co(II), and Cu(II) ions on MT-PRGO.

**Table S1.** Parameters of the Langmuir isotherms model for the adsorption of Hg(II), Co(II), and Cu(II) ions on MT-PRGO.

Metal ion	R <sup>2</sup>	b (L/mg)	Q <sub>max, fitted</sub>	Q <sub>exp</sub>	R <sub>L</sub>
Hg(II)	0.997	0.096	661.0	651.0	0.0079
Co(II)	0.995	0.080	98.8	98.0	0.0153
Cu(II)	0.994	0.044	50.1	50.0	0.0537

**Table S2.** Kinetic parameters for the adsorption of Hg(II), Co(II) and Cu(II) ions on MT-PRGO.

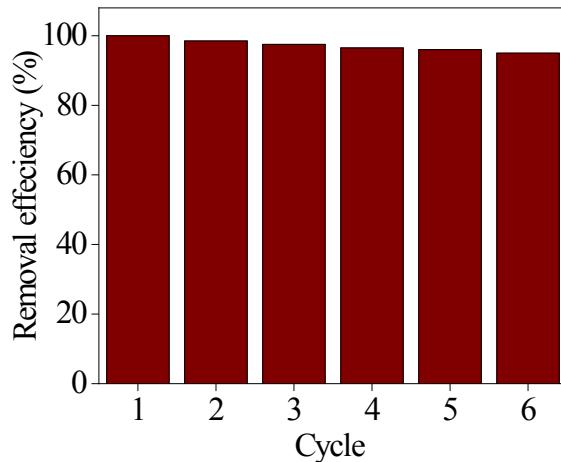
Metal ion	q <sub>e, exp</sub> (mg g <sup>-1</sup> )	q <sub>e, calc</sub> (mg g <sup>-1</sup> )	k <sub>2</sub> (g mol <sup>-1</sup> min <sup>-1</sup> )	R <sup>2</sup>
Hg(II)	538.0	543.2	0.001218	0.997
Co(II)	48.8	51.3	0.004029	0.998
Cu(II)	40.1	39.5	0.002211	0.993



**Figure S8.** The effect of competitive ions on the removal of a mixture of toxic metals by MT-PRGO (a)  $C_0 = 500 \mu\text{g/L}$ , (b)  $C_0 = 200 \text{ mg/L}$  [conditions: adsorbent dose = 0.05 g/ 5 mL, pH = 5.5, T = 298 K].

**Table S3.** Adsorption capacities of MT-PRGO in mixed metal ions system 500 ppb and 200 ppm at pH 5.5.

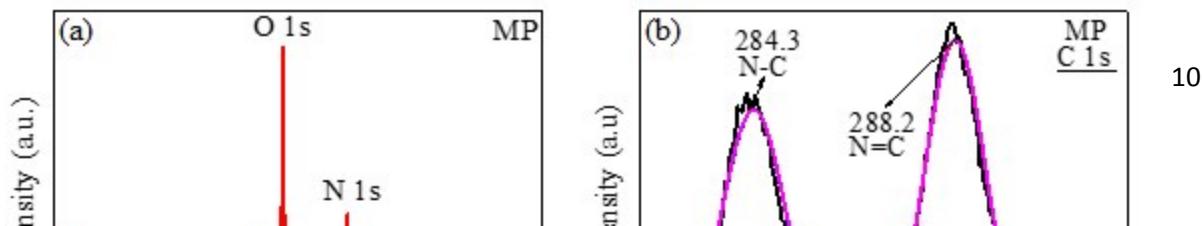
Concentration	Metal ion	Hg(II)	Cd(II)	Co(II)	Cu(II)	Zn(II)	Ni(II)
500 $\mu\text{g/L}$	$C_e (\text{mg/L})$	0	0	0	0	0	0
	$q_e (\mu\text{g/g})$	500.0	500.0	500.0	500.0	500.0	500.0
200 mg/L	$C_e (\text{mg/L})$	59.0	120.0	155.0	179.0	189.0	193.3
	$q_e (\text{mg/g})$	141.0	80.0	40.0	21.0	11.0	6.7



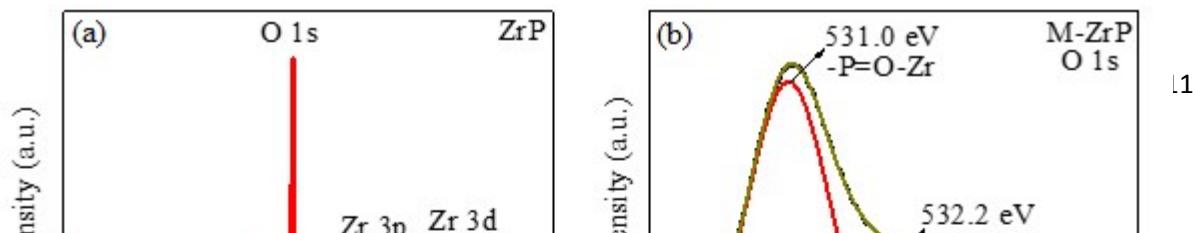
**Figure S9.** Recycling of MT-PRGO for the removal of Hg(II) [desorption condition: 1.0 M HNO<sub>3</sub>, adsorption conditions: pH 5.5, dose: 1 g/L, initial concentration of Hg (II) = 250 mg/L].

**Table S4.** Desorption studies of Hg(II) from MT-PRGO using HNO<sub>3</sub>.

Metal	Eluent	q <sub>e</sub> Adsorbed (mg/g)	q <sub>e</sub> Desorbed (mg/g)	De (%)
250 mg/L Hg(II)	HNO <sub>3</sub> (0.5 M)	232.0	135.5	58.40
	HNO <sub>3</sub> (1.0 M)	232.0	155.2	66.89
	HNO <sub>3</sub> (1.5 M)	232.0	221.2	95.34
	HNO <sub>3</sub> (2.0 M)	232.0	232.0	100.00



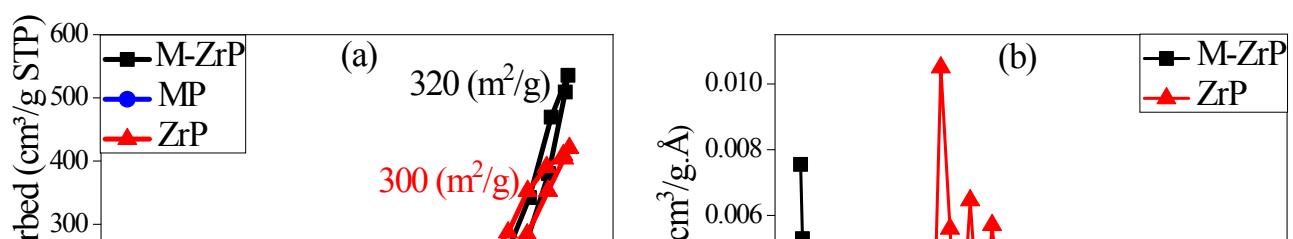
**Figure S10.** XPS spectra of MP (a) Survey scan, (b) C 1s, (c) N 1s, (d) P 2p, and (e) O 1s.



**Figure S11.** XPS spectra of ZrP (a) Survey scan, (b) O 1s, (c) P 2p, and (d) Zr 3d.

**Table S5.** Surface elemental composition of MP and M-ZrP from XPS analysis.

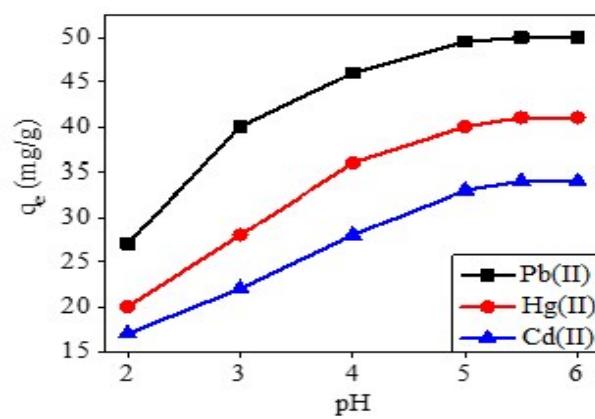
Adsorbent	Elemental Content (%)				
	C <sub>1s</sub>	N <sub>1s</sub>	O <sub>1s</sub>	P <sub>2p</sub>	Zr <sub>3d</sub>
MP	10.8	24.1	49.3	15.8	0.0
ZrP	0.0	0.0	57.2	20.3	22.5
M-ZrP	8.8	22.9	40.9	15.6	11.9



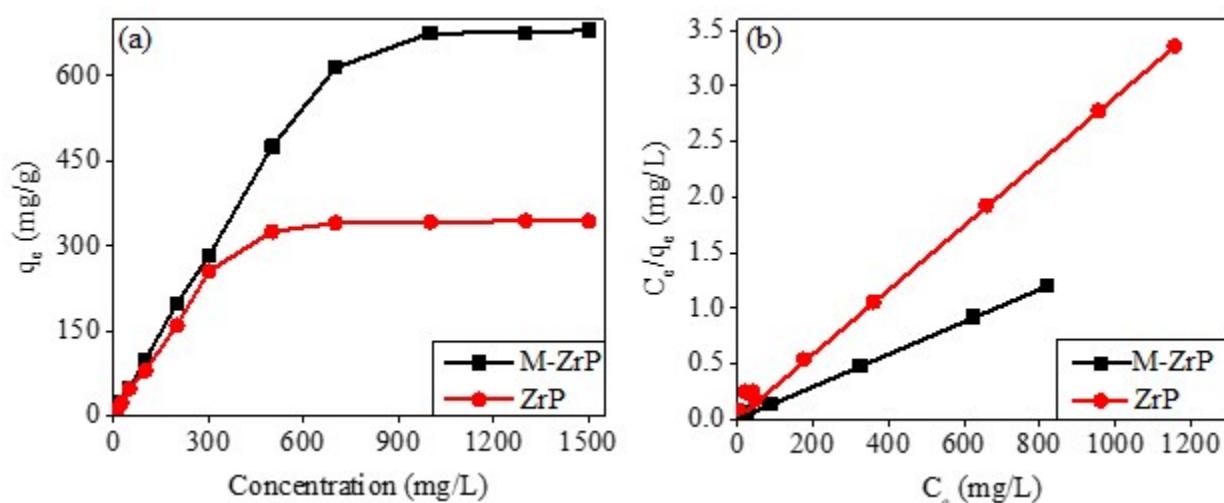
**Figure S12.** (a) N<sub>2</sub> adsorption-desorption isotherms of MP, ZrP, and M-ZrP. (b) Estimated pore size distributions of ZrP and M-ZrP.

**Table S6.** BET surface area and estimated pore volume of MP, ZrP and M-ZrP.

Sample	Surface area (m <sup>2</sup> /g)	Pore volume (cm <sup>3</sup> /g.Å)
MP	9	-
ZrP	300	0.010
M-ZrP	320	0.008

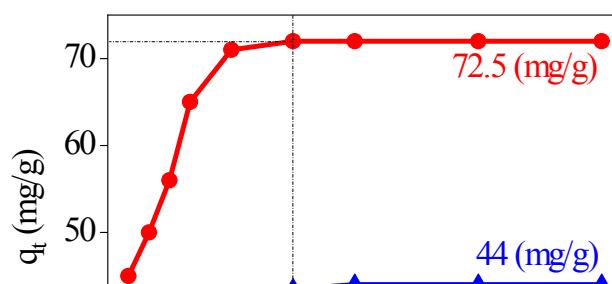


**Figure S13.** Dependence of the M-ZrP adsorption capacity of Pb(II), Hg(II), and Cd(II) ions on the pH of the solution [conditions:  $C_0 = 50$  mg/L T = 298 K; adsorbent dose = 0.005 g/5 mL].



**Figure S14.** (a) Comparison of the removal of Pb(II) by the ZrP and M-ZrP adsorbents [Conditions:  $C_0 = 10 - 1500$  mg/L Pb(II), pH 5.5, T = 298 K, adsorbent dose = 0.005 g/5 mL]. (b) Langmuir isotherm model for the adsorption of Pb(II) on ZrP and M-ZrP. The parameters of the Langmuir-isotherms for the adsorption of Pb(II) on ZrP and M-ZrP are shown below.

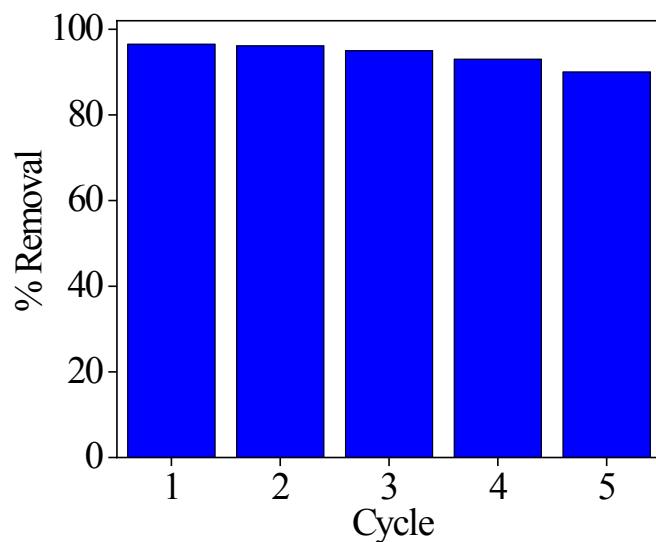
Langmuir parameters					
Adsorbent	$R^2$	b (L/mg)	$Q_{\max, \text{fitted}}$	$Q_{\exp}$	$R_L$
M-ZrP	0.993	0.164	682.6	680.4	0.0041
ZrP	0.997	0.024	348.3	344.2	0.0400



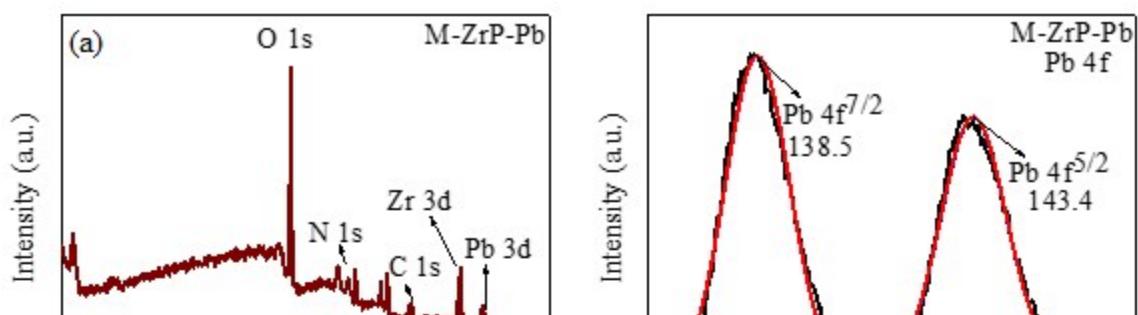
**Figure S15.** Effect of contact time on the removal of Hg(II) and Cd(II) ions by M-ZrP [Conditions:  $C_0 = 100 \text{ mg/L}$ , pH = 5.5; T = 298 K; adsorbent dose = 0.005 g/5 mL].

**Table S7.** Desorption studies of Pb(II), Hg(II) and Cd(II) from M-ZrP using different concentrations of nitric acid.

Metal	Eluent	$q_e$ Adsorbed (mg/g)	$q_e$ Desorbed (mg/g)	$D_e$ (%)
1000 mg/L Pb(II)	HNO <sub>3</sub> (0.1 M)	672.0	564.0	83.92
	HNO <sub>3</sub> (0.5 M)	672.0	584.0	86.90
	HNO <sub>3</sub> (1.0 M)	672.0	646.0	96.13
	HNO <sub>3</sub> (1.5 M)	642.0	642.0	100.0
300 mg/L Hg(II)	HNO <sub>3</sub> (0.1 M)	108.0	78.0	72.22
	HNO <sub>3</sub> (0.5 M)	108.0	90.0	83.33
	HNO <sub>3</sub> (1.0 M)	108.0	98.0	90.74
	HNO <sub>3</sub> (1.5 M)	108.0	108.0	100
300 mg/L Cd(II)	HNO <sub>3</sub> (0.1 M)	56.0	37.5	66.96
	HNO <sub>3</sub> (0.5 M)	56.0	44.7	79.82
	HNO <sub>3</sub> (1.0 M)	56.0	53.0	94.64
	HNO <sub>3</sub> (1.5 M)	56.0	56.0	100



**Figure S16.** Recycling of M-ZrP adsorbent for the removal of Pb(II) (desorption condition: 1.5 M HNO<sub>3</sub>) [adsorption conditions: pH 5.5, dose = 1 g/L, initial concentration of Pb (II) = 1000 mg/L].



**Figure S17.** XPS spectra of M-ZrP after the adsorption of Pb(II) ions. (a) Survey scan and high resolution spectra of (b) Pb 4f, (c) C 1s, (d) Zr 3d (e) N 1s, and (f) O 1s electrons.