

## Supplementary Information

Stefan Wild,<sup>a</sup> Sabrina Polierer,<sup>a</sup> Thomas Zevaco,<sup>a</sup> David Guse,<sup>b</sup> Matthias Kind,<sup>b</sup> Jörg Sauer,<sup>a</sup> Stephan Pitter,<sup>a</sup> and Karla Herrera Delgado<sup>\*a</sup>

<sup>a</sup>IKFT - Institute of Catalysis Research and Technology, Karlsruhe Institute of Technology, Hermann-von-Helmholtz-Platz 1, D-76344 Eggenstein-Leopoldshafen, Germany. E-mail: karla.herrera@kit.edu

<sup>b</sup>TVT - Institute of Thermal Process Engineering, Karlsruhe Institute of Technology, Kaiserstraße 12, D-76131 Karlsruhe, Germany.

The carbon balance was calculated according to equation S1†.

$$C - balance = \frac{\dot{n}_{CO,in} + \dot{n}_{CO_2,in} - (\dot{n}_{MeOH,out} + 2 * \dot{n}_{DME,out} + \dot{n}_{CO,out} + \dot{n}_{CO_2,out} + \nu_x \dot{n}_{C_xH_y})}{\dot{n}_{CO,in} + \dot{n}_{CO_2,in}} \quad (S1)$$

The measuring procedure with purging and reference point repetition is shown in Fig. S1†.

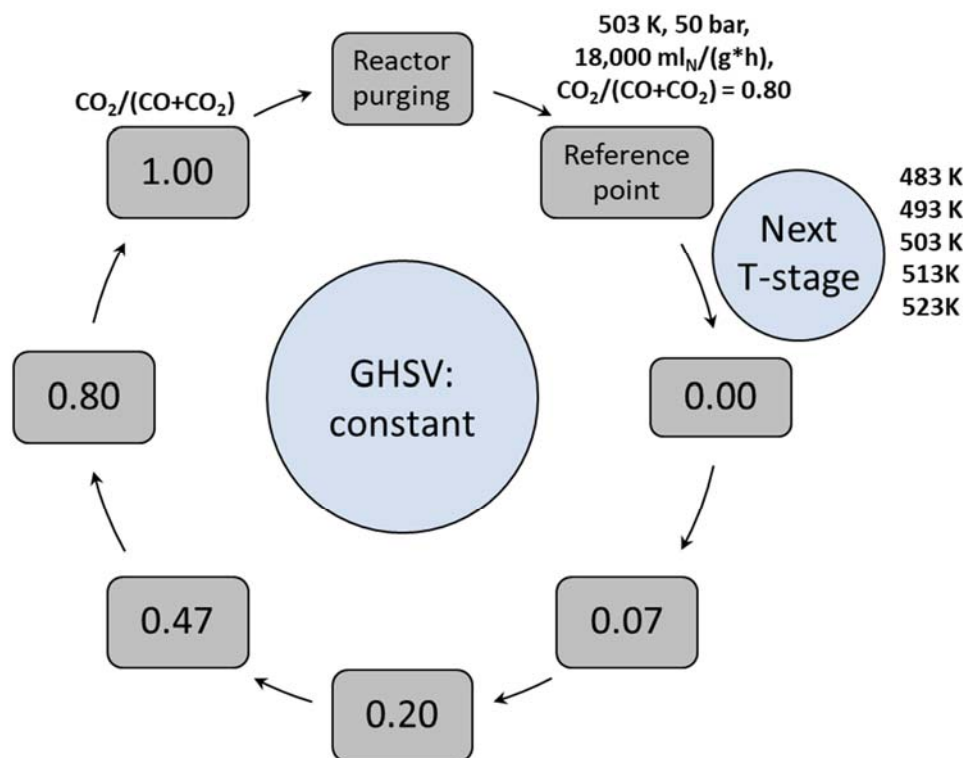


Fig. S1: Schematic illustration of the procedure of varying reaction conditions at a constant GHSV with recurring reference point at 50 bar.

All reaction conditions in this work were strongly, kinetically controlled due to the large distance to equilibrium (Fig S2†), exemplified by the CO<sub>x</sub> conversion at the reaction conditions shown in main manuscript (Figure 2 a).

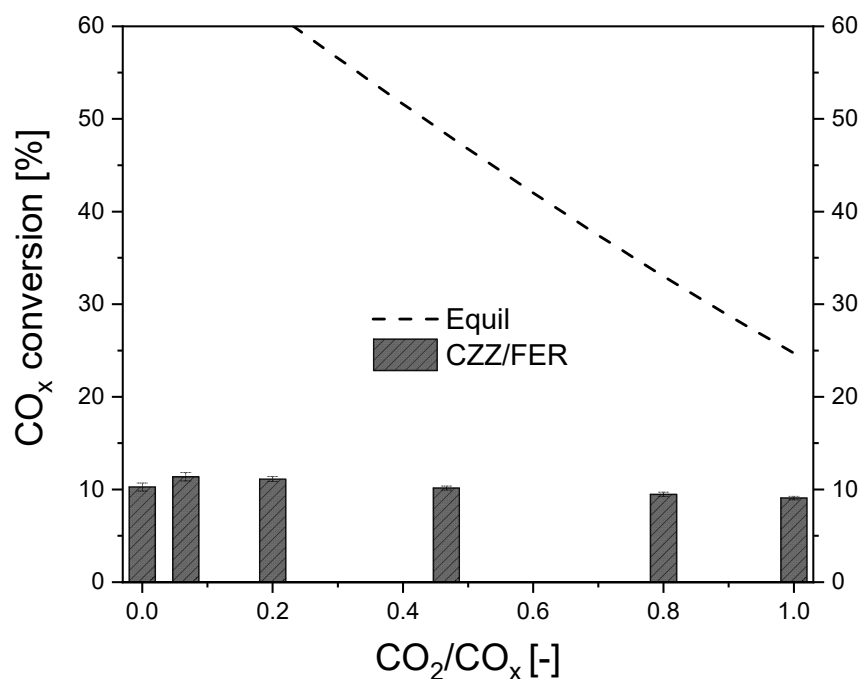


Fig. S2: CO<sub>x</sub> conversion with CZZ/FER (1:1 wt%) (black bars) under variation of the CO<sub>2</sub>/CO<sub>x</sub> inlet ratio at 50 bar, 523 K and 36 000 mlN/(g·h) and the respective equilibrium curve calculated via ASPEN PLUS.

An overview of the influence of the CO<sub>2</sub>/CO<sub>x</sub> inlet-ratio on selectivity, CO/CO<sub>2</sub> conversion and MeOH/DME productivity can be found in Table S1<sup>†</sup>.

Table S1: Effect of CO<sub>2</sub>/CO<sub>x</sub> inlet-ratio with the use of CZZ/FER 1:1 wt% on the CO<sub>2</sub> and CO conversion, the DME, MeOH, CO<sub>2</sub> and CO selectivity, and the DME and MeOH productivity. Measurement conditions: GHSV: 18 000 ml<sub>N</sub>/(g·h), 50 bar and 523 K.

Inlet-ratio/ - CO <sub>2</sub> /CO <sub>x</sub>	Conversion/ %		Selectivity/ %				Productivity/ g <sub>i</sub> /(kg <sub>Cu</sub> *h)	
	CO <sub>2</sub>	CO	DME	MeOH	CO <sub>2</sub>	CO	DME	MeOH
0.00	<0	25.2	58.6 <sup>b</sup>	1.4	32.9	<0	643.1	21.3
0.07	<0	26.9	64.3 <sup>b</sup>	1.9	28.6	<0	684.1	28.1
0.20	<0	27.9	69.8 <sup>b</sup>	3.4	23.3	<0	659.7	44.5
0.47	<0	30.0	88.3 <sup>b</sup>	7.6	2.3	<0	586.2	69.8
0.80	13.2	15.4	85.8 <sup>a</sup>	13.6	<0	<0	468.1	103.6
1.00	20.9	<0	42.3 <sup>c</sup>	8.5	<0	49.1	364.0	101.3

a: Eq 5, b: Eq 6, c: Eq 7