

## **Supporting Information**

### **Demonstration of green hydrogen production using solar energy at 28% efficiency and evaluation of its economic viability**

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Additional details of the TEA for making hydrogen (50 tons/ day) from water using CPV-E for 9.1 hours per day and direct electrolysis (from the grid) for 14.9 hours per day.

### Capital and Working Parameters

plant lifetime (years)	20
H <sub>2</sub> Production (ton/day)	50
Sunshine (hours/day)	9.1
Night hours (hours/day)	14.9
H <sub>2</sub> Production Rate during day (ton/h)	2.08
H <sub>2</sub> produced by PV (ton/day)	18.96
H <sub>2</sub> produced by electricity (ton/day)	31.04
Annual Working Days (days/yr)	333
H <sub>2</sub> Production Rate from PV (ton/year)	6313.7
Total H <sub>2</sub> Production Rate (ton/year)	16150

### PV Energy & land

PV lifetime (years)	20
Land factor	4
Power needed for Solar Farm (kW)	97,202.38
Energy produced by solar farm (kWh)	884,541.67
Solar Irradiation in Tabuk KSA (kWh/m <sup>2</sup> )	7.37
PV module efficiency	41.00%
Power produced by PV module (kWh/m <sup>2</sup> )	3.022
Area needed by PV modules (m <sup>2</sup> )	2.93E+05
Total area required (m <sup>2</sup> ) including land factor	1.17E+06
module and tracker lifetime (years)	25.00
Module and tracker cost (\$/W)	\$ 0.720
Labor, Design, and installation (\$/W)	\$0.43
PV inverter (\$/W)	\$0.08
Total Module and tracker cost (\$)	\$69,985,714.29
Total cost of Labor, design, permitting and installation	\$41,991,428.57
PV inverter cost (\$)	\$7,776,190.48
PV Farm turnkey Capital	\$119,753,333.33
PV O&M cost (USD/kWh)	0.008
PV annual Opex	\$7,076.33

**Electrolyzer (Alkaline)**

Reference Operating current density (A/cm <sup>2</sup> )	0.40
Reference Operating voltage (V)	1.70
Actual operating current density	0.40
Pressure of H <sub>2</sub> (bar) before compression	10
electrical usage per kg of H <sub>2</sub> (KWh <sub>elec</sub> /kg(H <sub>2</sub> )) -LHV	32.66
Electrolysis efficiency (electrical efficiency) (1.23/1.7)	0.70
Fixed O&M (%) - of total uninstalled CAPEX	3.00%
Electrolyzer replacement cost (% of uninstalled capex)	15.00%
Stack Cost of reference electrolyzer (USD/kW)	\$272.00
Balance of plant capital cost includes power electronics (USD/kW)	\$272.00
Electrolyzer installation factor	12.0%
Reference Stack cost (\$/m <sup>2</sup> )	1849.60
H <sub>2</sub> production (mol/day)	2.50E+07
electrons to make 1 H <sub>2</sub> molecule	2.00
electrons to make 1 mole of H <sub>2</sub>	1.20E+24
total electrons needed per day (electrons/day)	3.01E+31
total charge (C /day)	4.82E+12
Amps (C / second)	5.58E+07
Area of electrolyzer (cm <sup>2</sup> )	1.39E+08
Area of electrolyser (m <sup>2</sup> )	13942.13
stack cost of electrolyser based on m <sup>2</sup> (USD)	\$25,787,362.96
BOP cost (USD)	\$25,787,362.96
installation cost of electrolyser (USD)	\$6,188,967.11
Capex of electrolyzer stack, BOS & installation (USD)	\$57,763,693.04
Yearly Opex of electrolyzer (\$/year)	\$1,547,241.78
Yearly electricity cost of (\$/year)	\$9,645,781.07
Electrode replacement time (years)	7.00
number of times electrodes will be replaced in plant lifetime	2.00
Electrolyzer replacement factor	1.5%
annual electrolyzer replacement cost (USD/yr)	\$866,455.40
Electrolyzer annual Opex (USD/yr)	\$2,413,697.17

**Water pump, Compressor gas processing (to 20 bar)**

Duty(kW)	51.94
Capex of pump	\$29,306.58
Opex (USD/yr) of pump	\$8,302.09
Duty (kW)	984.68
Opex (USD/hr)	\$19.69
Capex (USD)	\$4,143,572.97
Opex (USD/yr)	\$157,391.09

### Production using electricity

H <sub>2</sub> Production Rate (ton/h)	2.08
working hours/day	14.9
Power needed from grid (kW)	97202.38
Energy provided by grid (kWh)	1,448,315.48
Total system electrical usage at night for a year (kWh)	4.82E+08

### Factors

KSA Location Markup Factor (1.0 for USA)	1.00
Land cost (USD/km <sup>2</sup> )	\$123,497.00
H <sub>2</sub> loss due to separation	3.0%

### Operation Parameters

DI Water amount (ton/tonH <sub>2</sub> )	10
DI Water price (USD/ton)	1.3
Annual water consumption (ton/yr)	166,500.00
Annual water cost (USD/yr)	\$216,450.00
Required electricity for utilities (kWh/tonH <sub>2</sub> )	161.00
Annual electricity requirement for utilities (kWh/yr)	2,680,650.00
Electricity price (USD/kWh)	0.02
Annual electricity cost (USD/yr)	\$53,613.00
Number Plant Staff	10
Staff salary cost (USD/h)	20.00
Annual cost of plant staff (USD/yr)	\$1,598,400.00

### Revenue

Levelized H <sub>2</sub> Price (USD/ton)	\$2,555
Annual H <sub>2</sub> revenue (USD/yr)	\$41,257,830.32
Oxygen Credit (USD/ton O <sub>2</sub> )	\$40.00
Oxygen Credit (USD/ton H <sub>2</sub> )	\$320.00
Annual Oxygen Credit (USD)	\$5,168,160.00
CO <sub>2</sub> Credit (USD/ton CO <sub>2</sub> ) based on stoichiometric ratio of the SMR reaction (CH <sub>4</sub> + 2H <sub>2</sub> O → 4H <sub>2</sub> + CO <sub>2</sub> ) – excluding process energy.	\$50.00
CO <sub>2</sub> Credit (USD/ton H <sub>2</sub> )	\$275.00
Annual CO <sub>2</sub> Credit (USD)	\$4,441,387.50

**Total Capex**

PV Farm turnkey Capital	\$119,753,333.33
Capex of electrolyzer stack, BOS & installation (USD)	\$57,763,693.04
Compressor & gas processing (USD)	\$4,143,572.97
Water pump	\$29,306.58
Fixed Capital Cost (USD)	\$181,689,905.92
Contingency	20.0%
Total Fixed Capital Cost in KSA + plus contingency (USD)	\$218,027,887.10
Land Cost (USD)	\$146,326.82
Working capital - (Installation Cost of whole plant) (USD)	\$48,180,395.68

**Annual Opex**

Annual PV Maintenance (USD/yr)	\$7,076.33
O&M of electrolyzer (USD/yr)	\$2,413,697.17
Electricity cost to run electrolyzer + utilities (\$/year)	\$9,699,394.07
Compressor	\$157,391.09
Water pump	\$8,302.09
Annual water cost (USD/yr)	\$216,450.00
Annual staff cost (USD/yr)	\$ 1,598,400.00
Total Annual Variable Cost (USD/yr) (OPEX)	\$14,100,710.76

**Revenue**

Annual H <sub>2</sub> Revenue	\$41,257,830.32
annual oxygen + CO <sub>2</sub> credit	\$9,609,547.50
Total Annual Revenue (USD/yr)	\$ 50,867,377.82

<b>Internal Rate of Return: IRR</b>	<b>12.0%</b>
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**Effect of operation time and electricity cost on the Levelized Cost of Hydrogen from water.**

50 tons H <sub>2</sub> /day	CPV (9.1 hour operation)	CPV + grid (24 hour operation) Electricity at 0.05 \$/kWh	CPV + grid (24 hour operation) Electricity at 0.02 \$/kWh
<b>Energy provided and power needed</b>			
<b>Power needed for the solar farm (kW)</b>	256,357.93	97,202.38	97,202.38
<b>Energy provided by the solar farm (kWh)</b>	2,332,857.14	884,541.67	884,541.67
<b>Energy provided by grid (kWh)</b>	0	1,448,315.48	1,448,315.48
<b>Capex</b>			
<b>Total solar farm cost (\$)</b>	\$315,832,967.03	\$119,753,333.33	\$119,753,333.33
<b>Total electrolysers capital (\$)</b>	\$156,193,758.24	\$57,763,693.04	\$57,763,693.04
<b>Opex</b>			
<b>Annual PV Maintenance (\$/yr)</b>	\$18,662.86	\$7,076.33	\$7,076.33
<b>Annual electricity cost (\$/yr)</b>	\$134,032.50	\$24,248,485.18	\$9,699,394.07
<b>Levelized H<sub>2</sub> Price (\$/ton)</b>	\$5,900	\$3,471	\$2,555

At 0.05 \$/kWh the LCH is found to be \$3.47 the kg (a drop of \$2.5 per kg when compared to a 9.1 hours/day operation). The effect of electricity, while important, seems to affect less the cost in the investigated range, a drop of \$0.9 per kg<sub>H2</sub> (ca. 25%) when the electricity dropped 2.5 times (from \$0.05 to \$0.02 the kWh; a 250% drop).

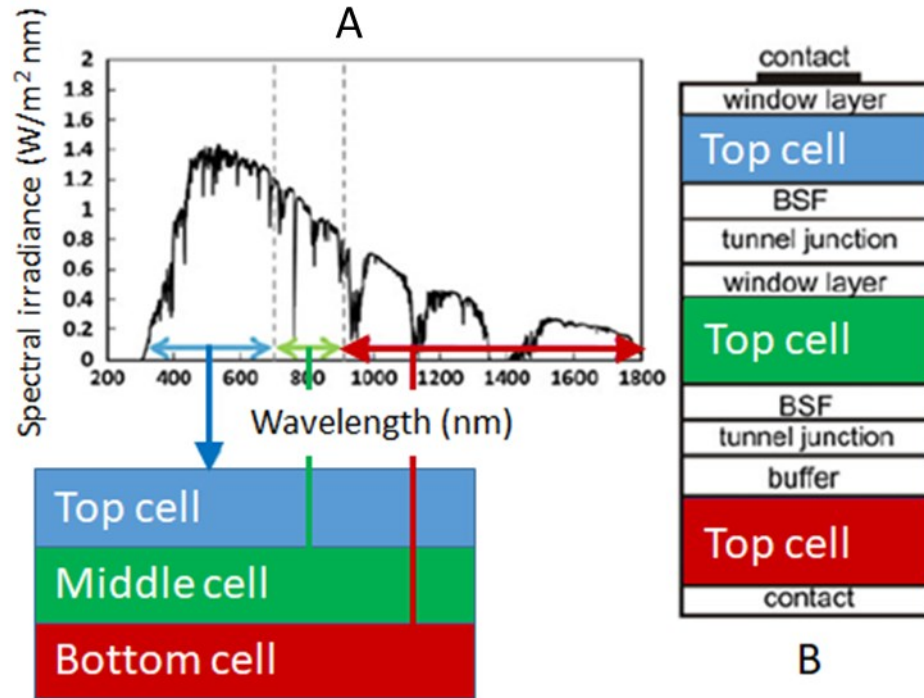


Figure S1. Part of the solar spectrum absorbed in a triple junction solar cell (A) and a schematic representation of a typical triple-junction solar cell (B) (adapted from ref. 1)

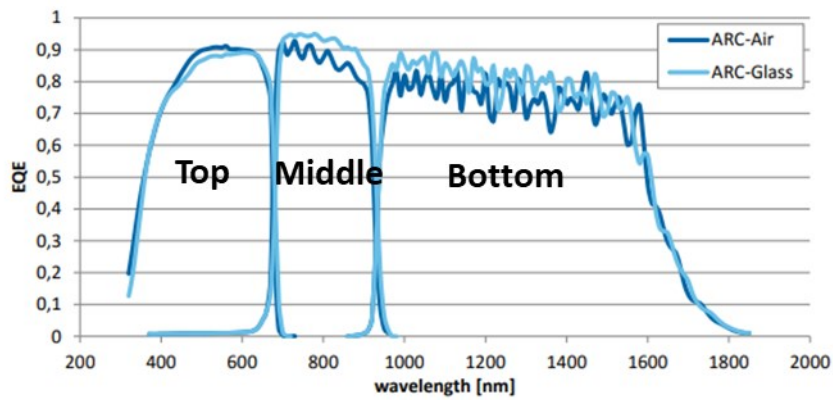


Figure S2. External quantum efficiency (EQE) of a GaInP/GaInAs/Ge AzurSpace solar cell (adapted from ref. 2).

### **References**

- 1) Fernández, Eduardo F., Antonio J. García-Loureiro, and Greg P. Smestad. "Multijunction concentrator solar cells: analysis and fundamentals." High Concentrator Photovoltaics. Springer, Cham, 2015. 9-37.
- 2) [http://www.azurspace.com/images/products/0004357-00-01\\_3C44\\_AzurDesign\\_3x3.pdf](http://www.azurspace.com/images/products/0004357-00-01_3C44_AzurDesign_3x3.pdf)