

Supplementary Information

Unraveling Driving Regimes for Destabilizing Concentrated Emulsions within Microchannels

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A: Resistance and flow rate calculations

A schematic of the microchamber is shown in Fig. 1. This microchamber houses the packed emulsion droplets. Pressure-induced stress occurs by injecting fluid (deionized water/saline solution) from the input. The fluid interacts with the emulsion packing and then exits at the output.

The resistance, R , of microchannels is calculated from the following equations.^{1,2}

$$R = \frac{12\mu L}{WH^3} \left\{ 1 - \left[\left(\frac{192W}{W\pi^5} \right) \tan \left(\frac{\pi W}{2H} \right) \right] \right\}^{-1} \quad (1)$$

where $\mu = 10^{-3}$ Pa·s, L is the length, W is the width and H is the height of the microchannel chamber. The parameters L , H , and W refer to different parts of the location in the chamber as explained below.

For the triangular part of the chamber:

$$L_{tri} = 2800\mu\text{m}; W_{tri} = 1650\mu\text{m}; H_{tri} = 55\mu\text{m}$$

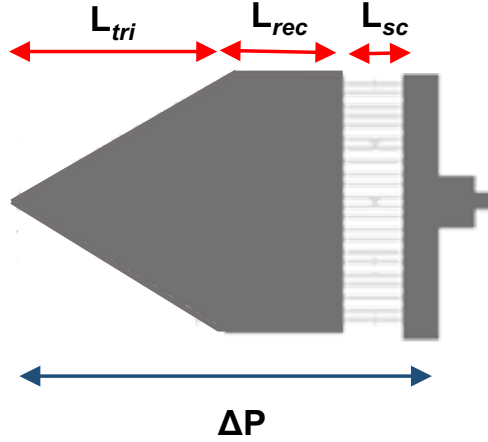


Figure 1: Sketch of the principal microchamber with its component parts. The entire microchamber can be subdivided into a triangular section (where L_{tri} is the length of this subsection), a rectangular section (where L_{rec} is the length of this subsection), and the section with the small channels at the outlet (where L_{sc} is the length of the small outlet channels). The pressure difference, ΔP , is calculated across the entire total length of the microchamber.

Using Eq.1, we can calculate the resistance of the triangular chamber, R_{tri} .

For the rectangular part of the chamber:

$$L_{rec} = 1400\mu\text{m}; W_{rec} = 3300\mu\text{m}; H_{rec} = 55\mu\text{m}$$

Using Eq.1, we can calculate the resistance of the rectangular chamber, R_{rec} .

For the small channels in the outlet:

$L_{sc} = 1020\mu\text{m}; W_{sc} = 20\mu\text{m}; H_{sc} = 55\mu\text{m}$ or $H_{sc} = 20\mu\text{m}$ (for $P=20\text{mbar}$ and $P=200\text{mbar}$ respectively).

Because the small channels are in parallel:

$$\frac{1}{R_{sc-total}} = \frac{1}{R_1} + \frac{1}{R_2} + \frac{1}{R_3} + \dots \frac{1}{R_N} \quad (2)$$

where N is the number of channels in the outlet, $N = 22$.

Since all resistances are equal ($R_1 = R_2 = \dots = R_{sc}$), we can calculate the resistance of each individual outlet channel using the general Eq.1. The total resistance of all the small outlet channels combined is then:

$$R_{sc-total} = \frac{R_{sc}}{N} \quad (3)$$

Total resistance of the entire microfluidic chip:

From the aforementioned parameters, the total resistance of the entire chip is a series of its individual components:

$$R_T = R_{tri} + R_{rec} + R_{sc-total} \quad (4)$$

And the flow rate can be calculated from:

$$Q = \frac{\Delta P}{R_T} \quad (5)$$

where ΔP is either 20 or 200 mbar (converted to Pa) and R_T is the total resistance from Eq.4.

B: Permeability and flow rate calculations

When the interior of the microchannel chamber is packed with emulsion droplets, the system can be considered as a porous medium. Since we are injecting an external phase (saline solution/water) into the chamber, then the permeability of both emulsion droplet packing as well as the small channels should also be considered.

Permeability of the small channels (k_{sc}):

$$\frac{dP_{sc}}{dL} = \frac{\Delta P}{L_{sc}} \quad (6)$$

where $\frac{dP_{sc}}{dL}$ is the change in pressure per unit length of the small channels, L_{sc} is the length of the small channels and ΔP is the pressure difference applied in the system. Thus, the permeability of the small channels, k_{sc} , can be calculated according to Eq.7.

$$k_{sc} = \frac{\mu Q}{WHN} \frac{dL}{dP_{sc}} \quad (7)$$

where W , H and N are the width, height and number of the small channels, respectively: $H = 55\mu\text{m}$ or $20\mu\text{m}$ and $N = 22$; Q is the flow rate obtained from Eq.5 and $\mu = 10^{-3}$ Pa.s.

Permeability of the the emulsion droplet packing (k_{drop}):

$$\frac{dP_{total}}{dL} = \frac{\Delta P}{L_{tri} + L_{rec} + L_{sc}} \quad (8)$$

where $\frac{dP_{total}}{dL}$ is the change in pressure per unit length of the entire system, L_{sc} , L_{tri} , and L_{rec} are the length of the small channels, the triangle chamber, and the rectangle chamber respectively. ΔP is the pressure applied in the system.

$$\frac{\sigma}{\sigma_0} = \left[\frac{\varphi - \varphi_c}{1 - \varphi_c} \right]^u \quad (9)$$

where $\frac{\sigma}{\sigma_0}$ is the conductivity of the fluid phase within the porous material with respect to the fluid's bulk conductivity.³ $\varphi = 0.64$ is the porosity of the emulsion packing in quasi-2D cases assuming random close packing, $\varphi_c = 0.32$ is the percolation threshold of overlapping droplets in quasi-2D

and $u = 1.3$ is the critical exponent.

The permeability of the porous medium (emulsion droplet packing), k_{drop} , is:

$$k_{drop} = C(l_c)^2 \frac{\sigma}{\sigma_0} \quad (10)$$

where $C=1/12$ is a constant for 2D systems; $l_c = 40\mu\text{m}$ is the local pore geometry (usually the same order of magnitude of droplet size).

Therefore, total permeability is:

$$k_{total} = k_{sc} + k_{drop} \quad (11)$$

And the actual flow rate is:

$$Q_{final} = \left(\frac{k_{total}}{\mu} \right) \cdot P_{total} \cdot W \cdot H \cdot N \quad (12)$$

where W , H , and N are the width, height, and number of small channels respectively. In Eq.12, the area considered is $W \cdot H \cdot N$ and $\mu = 10^{-3}\text{Pa}\cdot\text{s}$.

References

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