

## Supporting Information

# Amorphous Molybdenum Selenide Intercalated Magnetite as Recyclable Trap for Effective Sequestration of Elemental Mercury

*Zequn Yang<sup>a</sup>, Hailong Li<sup>b\*</sup>, Qin Yang<sup>b</sup>, Jiexia Zhao<sup>b</sup>, Fanyue Meng<sup>b</sup>, Yong Feng<sup>c</sup>, Wenqi Qu<sup>b</sup>,  
Jianping Yang<sup>b</sup>, Kaimin Shih<sup>a\*\*</sup>*

- a. Department of Civil Engineering, The University of Hong Kong, Hong Kong, Hong Kong SAR,  
China
- b. School of Energy Science and Engineering, Central South University, Changsha, 410083, China
- c. Environmental Research Institute, South China Normal University, Guangzhou, 510631, China

Revision submitted to  
**Journal of Materials Chemistry A**

\*To whom correspondence should be addressed:

TEL: +86-18670016725

E-mail: [hailongli18@gmail.com](mailto:hailongli18@gmail.com)

\*\*To whom correspondence should be addressed:

TEL: +852-2859-2973

Email: [kshih@hku.hk](mailto:kshih@hku.hk)

**Sorbent characterizations.** The crystallinity of the sorbents was analyzed using X-ray diffraction (XRD, D8 Bruker AXS) with  $2\theta$  from  $10^\circ$  to  $80^\circ$  in Cu  $\alpha$  ( $\lambda = 0.15406$  nm) radiation. A vibrating sample magnetometer (VSM, SQUID) was employed to characterize the magnetization of the sorbents. A scanning electron microscopy (SEM, FEI-50, USA) was adopted to characterize the morphologies of the sorbents. The amorphism of the  $\text{MoSe}_x$  was further evidenced by a transmission electron microscopy (TEM, JEOL 2100F) at 200 kV. The Brunauer-Emmett-Teller (BET) surface area of the sorbents was determined by the  $\text{N}_2$  adsorption and desorption method with a BET analyzer (ASAP 2020, Micromeritics, USA). The Raman spectroscopy (LabRAM HR800, HORIBA JOBIN YVON S.A.S) was recorded to further analyze the bond vibrations in the sorbents. With a reference of the C 1s binding energy value of 284.8 eV, X-ray photoelectron spectroscopy (XPS) spectra (Thermo ESCALAB 250Xi) were recorded for fresh and spent  $\text{MoSe}_x(\text{inter})\text{Fe}_3\text{O}_4$  [the spent  $\text{MoSe}_x(\text{inter})\text{Fe}_3\text{O}_4$  was obtained by pretreating fresh  $\text{MoSe}_x(\text{inter})\text{Fe}_3\text{O}_4$  under  $500 \mu\text{g m}^{-3} \text{Hg}^0$  for 12 h].

**Kinetic models.** pseudo-first-order and pseudo-first-order kinetic models were chosen to study the Hg<sup>0</sup> uptake rate over MoSe<sub>x</sub>(inter)Fe<sub>3</sub>O<sub>4</sub>. In the pseudo-first-order model, the Hg adsorption rate was proportional to the difference between the equilibrium capacity and the adsorbed amount at any time, as described as follows:

$$\frac{dQ_t}{dt} = k_1(Q_e - Q_t) \quad (S1)$$

Equation (3) could be modified to the following equation based on the initial conditions of t=0, Q<sub>t</sub>=0:

$$Q_t = Q_e(1 - e^{-k_1 t}) \quad (S2)$$

where the pseudo-first-order kinetic constant (k<sub>1</sub>, min<sup>-1</sup>) can be determined by fitting the adsorption breakthrough curve.

The pseudo-second-order model represents that the surface diffusivity is inversely proportional to the square of concentration variation on sorbent surface, which could be described by equation (S3):

$$\frac{dQ_t}{dt} = k_2(Q_e - Q_t)^2 \quad (S3)$$

Equation (S3) could be modified to the following equation based on the initial conditions of t=0, Q<sub>t</sub>=0:

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{1}{Q_e} t \quad (S4)$$

where the pseudo-second-order kinetic constant (k<sub>2</sub>, mg g<sup>-1</sup> min<sup>-1</sup>) can be determined by fitting the adsorption breakthrough curve.

**Thermodynamics.** The activation energy for Hg<sup>0</sup> adsorption over MoSe<sub>x</sub>(inter)Fe<sub>3</sub>O<sub>4</sub> was determined by Arrhenius equation with the assistance of k<sub>2</sub>:

$$\ln k_2 = \frac{E_a}{R} \left( \frac{1}{T} \right) + C \quad (\text{S5})$$

in which R = 8.314 J mol<sup>-1</sup> K<sup>-1</sup>, T (K) is the reaction temperature, and the activation energy (E<sub>a</sub>, kJ mol<sup>-1</sup>) could be hence obtained by simulating a linear relationship between different ln k<sub>2</sub> and 1/T.

**Mercury temperature programmed desorption/decomposition (Hg-TPD).** To properly determine the  $\text{Hg}^0$  species over Hg-laden  $\text{MoSe}_x(\text{inter})\text{Fe}_3\text{O}_4$ , a Hg-TPD test was conducted. In a typical procedure, 10 mg of  $\text{MoSe}_x(\text{inter})\text{Fe}_3\text{O}_4$  mixed with 500 mg of  $\text{SiO}_2$  was pretreated in the presence of  $500 \mu\text{g m}^{-3}$  of  $\text{Hg}^0$  feed for a continuous 30 min at  $50 \text{ }^\circ\text{C}$ . Then, the  $\text{Hg}^0$  feed was cut off and the Hg-laden sorbent was purged by pure  $\text{N}_2$  until the outlet  $\text{Hg}^0$  concentration equaled zero. The Hg-TPD test was hence started from  $50 \text{ }^\circ\text{C}$  to  $450 \text{ }^\circ\text{C}$  with a heating rate of  $10 \text{ }^\circ\text{C min}^{-1}$  to monitor the possible decomposition of both HgSe and HgO. The outlet  $\text{Hg}^0$  concentration was unceasingly recorded by the mercury analyzer.

List of Tables:

**Table S1.** Experimental conditions.

**Table S2.** Adsorption performance comparison of various magnetic sorbents.

**Table S1.** Experimental conditions.

Experiments	Materials	Carrier gas (1 L min <sup>-1</sup> )	Reaction temperature (°C)	Mass loaded (mg)	C <sub>in</sub> (µg m <sup>-3</sup> )
Set I	Bare Fe <sub>3</sub> O <sub>4</sub> ; Bare MoSe <sub>x</sub> ; MoSe <sub>x</sub> /Fe <sub>3</sub> O <sub>4</sub> ; MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub>	50	10	500
Set II	MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub>	25-125	10	500
Set III	MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub> ; N <sub>2</sub> + 4%-20% O <sub>2</sub> ; N <sub>2</sub> +0.1%-1% SO <sub>2</sub> (+4% O <sub>2</sub> ); N <sub>2</sub> +8%-20% H <sub>2</sub> O (+4% O <sub>2</sub> )	50	10	500
Set IV	MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub>	50	10	50-1500
Set V	MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub>	50	2-50	500
Set VI	MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub>	50	10	500
Set VII	Recycled MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub>	Pure N <sub>2</sub>	50	As recycled	500

**Table S2. Adsorption performance comparison of various magnetic sorbents.**

Sorbents	$C_{in}$ ( $\mu\text{g m}^{-3}$ )	Sorbent mass (mg)	Hg <sup>0</sup> adsorption capacities ( $\mu\text{g g}^{-1}$ )	Hg <sup>0</sup> adsorption rate ( $\mu\text{g g}^{-1}\cdot\text{min}^{-1}$ )	Reference
MoSe <sub>x</sub> (inter)Fe <sub>3</sub> O <sub>4</sub> (100%)	500	10	134250	28.3	This work
Fe <sub>3</sub> O <sub>4</sub> @CuS (100%)	90	5	80730	13.2	11
FeS <sub>x</sub> (4%)	120	200	220	0.3	36
H <sub>2</sub> S modified Fe-Ti spinel (5%)	100-120	200	690	1.9	37
H <sub>2</sub> S modified ilmenite (6%)	100-120	200	170	0.5	38
Mn/ $\gamma$ -Fe <sub>3</sub> O <sub>4</sub> (19%)	1000	30	3640	-	40
(Fe <sub>3-x</sub> Mn <sub>x</sub> ) <sub>1-<math>\delta</math></sub> O <sub>4</sub> (100%)	670-1130	25	5100	-	39
Magnetic zeolite supported Ag <sup>0</sup> (20%)	310	~50	44	-	41
Co-MF (100%)	85	500	30	-	42
Magnetic biochar (100%)	85	50	950	-	43

The ratios in the bracelets represent to which extent the sorbents were penetrated.