

1 *Supporting Information for*

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3 **Cold plasma-activated AgCo surface in situ alloying for
4 enhancing CO₂ electroreduction to ethanol**

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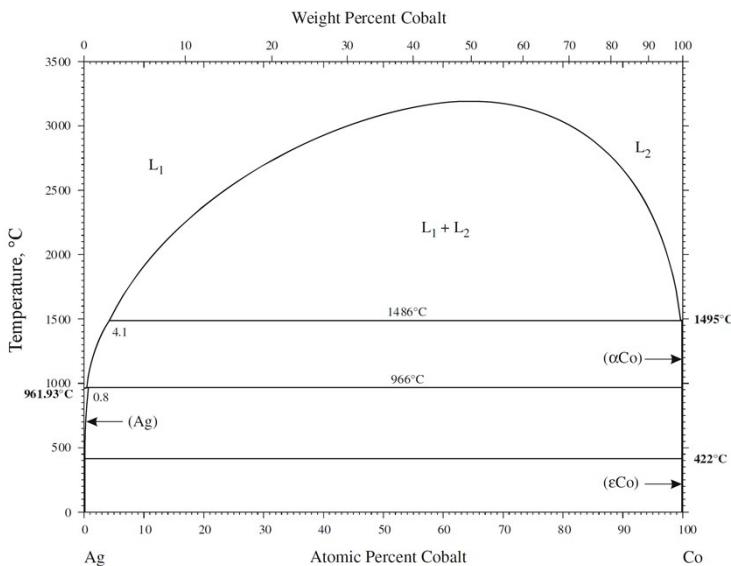
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3 **Fig. S1** Ag-Co phase diagram.^[1]

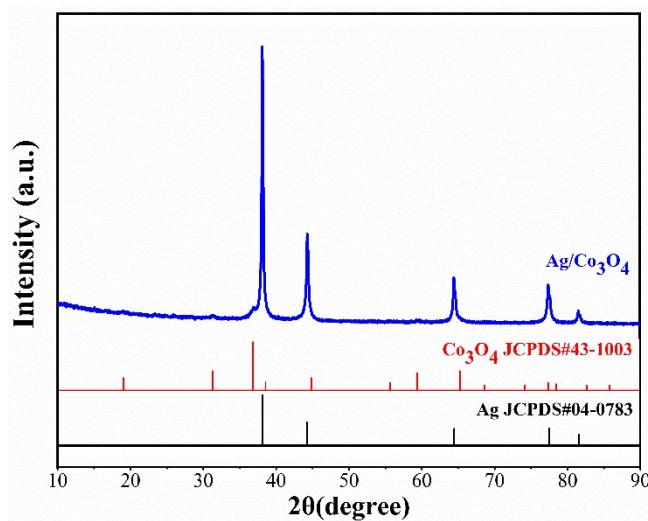
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5 When the content of cobalt atoms is 0.8%, the Ag-Co partial miscible alloying
6 requires a very high temperature (961.93°C).^[1] The high temperature leads to
7 agglomerate the metal catalyst, which is not conducive to the catalytic reaction. In order
8 to solve this problem, we used a cold plasma (200 W 10 min) technology under room
9 temperature to obtain AgCo surface alloy.

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3 **Fig. S2** XRD pattern of as-synthesized Ag/Co₃O₄ nanocubes.

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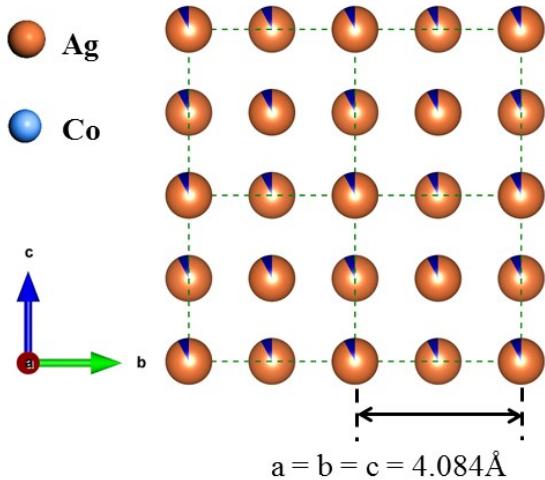
5 The diffraction peaks of the Ag/Co₃O₄ nanocubes at 38.1°, 44.2°, 64.4°, 77.4° and
6 81.5° can be readily assigned to the (111), (200), (220), (311) and (222) crystal planes
7 of Ag (JCPDS#04-0783, space group: *Fm-3m*(225)). The peak at 31.2°, 36.8° and 59.3°
8 is also corresponding to the crystal planes of (220), (311) and (511) of Co₃O₄
9 (JCPDS#15-0806, space group: *Fm-3m*(225)).

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3 **Fig. S3** General view of the face-centered-cubic crystal structure with parameters of a
4 $= b = c = 10.08 \text{ \AA}$. Zeolithic water is omitted for clarity.

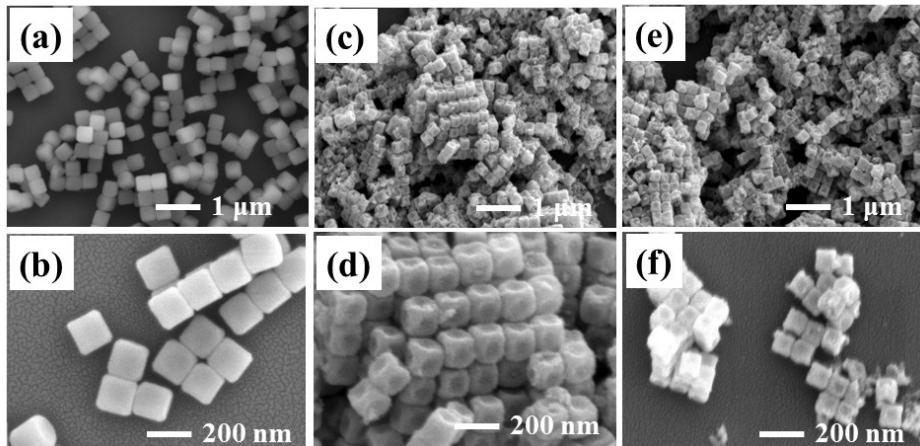
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6 According to Rietveld calculations, the lattice parameter of AgCo SA ($a=b=c=$
7 4.084 \AA) is slightly smaller than pure Ag ($a=b=c= 4.086 \text{ \AA}$), which can indicate that Co
8 atom has been doped into the Ag lattice. The refined atomic coordinates and thermal
9 parameters of AgCo SA are listed in Table S1. The occupancy of Ag is 0.92, and the
10 occupancy of Co is only 0.08.

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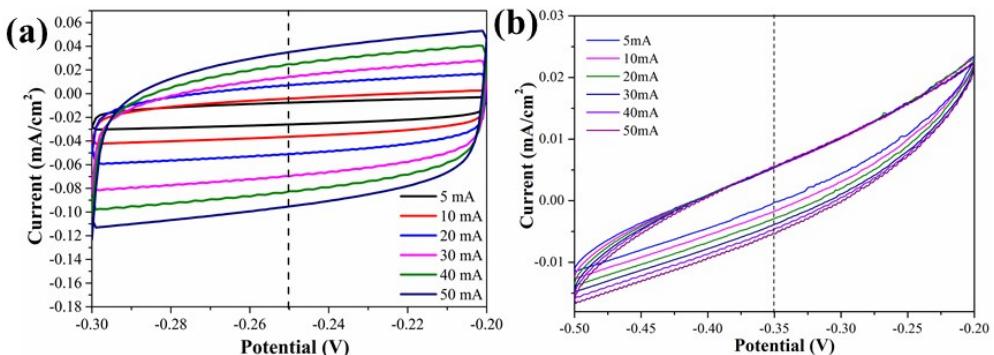
3 **Fig. S4** FESEM images of the precursor $\text{Ag}_3\text{Co}(\text{CN})_6$ (a-b), $\text{Ag}/\text{Co}_3\text{O}_4$ (c-d) and AgCo
4 SA (e-f) at different magnification.

5 The FESEM images revealed that $\text{Ag}_3\text{Co}(\text{CN})_6$ boxes were uniform in size with
6 diameters $\approx 100\text{-}200$ nm with smooth surface. After pyrolysis, $\text{Ag}/\text{Co}_3\text{O}_4$
7 submicroboxes were formed, which maintained the precursor's morphology with cube
8 faces becoming concave, as a result of decomposition and volatilization of organic
9 compounds. Moreover, after cold H_2 -plasma treatment, resulting AgCo SA retained the
10 submicroboxes shape with concave and the surfaces became very rough as shown in
11 Fig. S4e-f.

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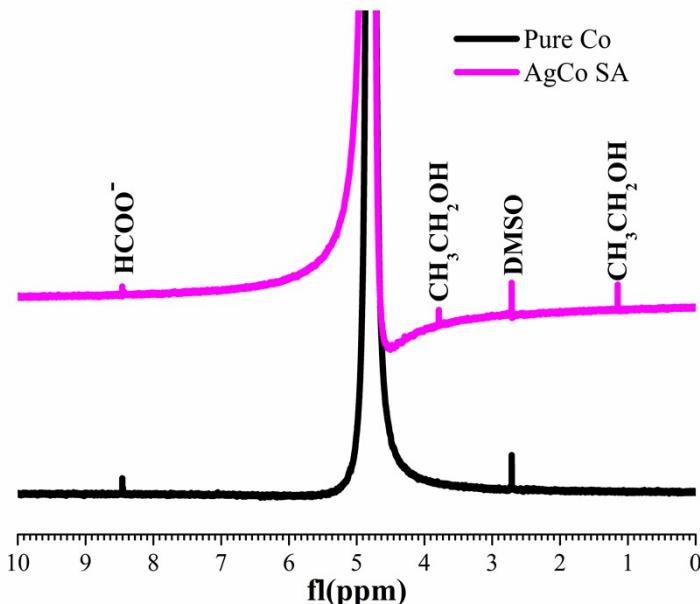
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3 **Fig. S5** CV curve of (a) AgCo SA and (b) pure Co electrode in 0.1 M KHCO₃ saturated
4 with CO₂ over under different scan rate.

5 The high activity of AgCo SA is partly ascribed to the high electrochemical active
6 area (ECSA), which represents the amount of active sites to a certain degree, normally,
7 the ECSA can be approximated to the electrochemical double layer capacitance
8 (EDLC). Not surprisingly, AgCo SA exhibits a higher EDLC than pure Co, indicating
9 larger ECSA, followed by a great number of active sites on AgCo SA, which is an
10 important contributor to the enhanced activity.

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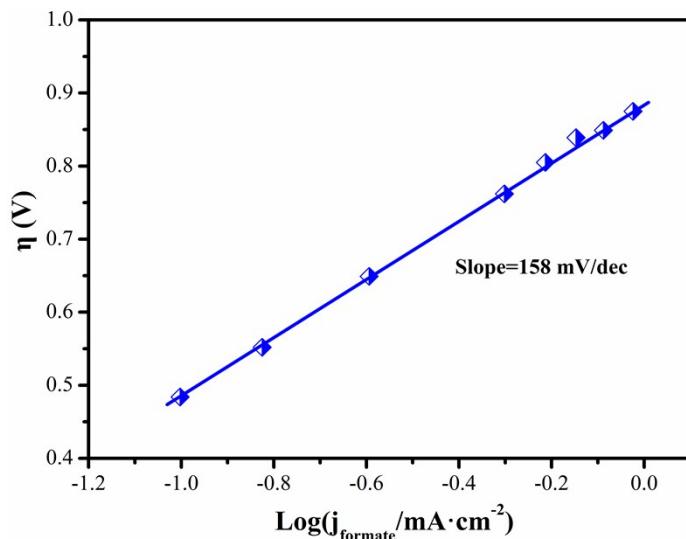
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Fig. S6 ^1H -NMR of the aqueous products after the CO_2RR for 5 h at -0.8 V vs. RHE over AgCo SA and pure Co electrodes. The ^1H spectrum was tested with water suppression by a pre-saturation method. Typically, 0.1 mL of KHCO_3 solution after electrolysis was mixed with 0.1 mL of D_2O , which contained 0.05 μL of DMSO as an internal standard. The concentrations of formic acid and ethanol, were measured using an internal standard, DMSO (star, 2.5 ppm), to be 0.7 and 2.1 ppm, which were converted to the FEs of each product of 8.4% and 22.2%, respectively, in case of AgCo SA. The concentrations of formic acid were measured using an internal standard, DMSO (star, 2.5 ppm) to be 1.40 ppm, which were converted to the FEs of each product of 0.03%, respectively, in case of pure Co. Both data was analyzed by considering the total volume of the electrolyte (30 mL) and the total current, $7.4 \text{ mA}\cdot\text{cm}^{-2}$ (AgCo SA) and $4.9 \text{ mA}\cdot\text{cm}^{-2}$ (pure Co).

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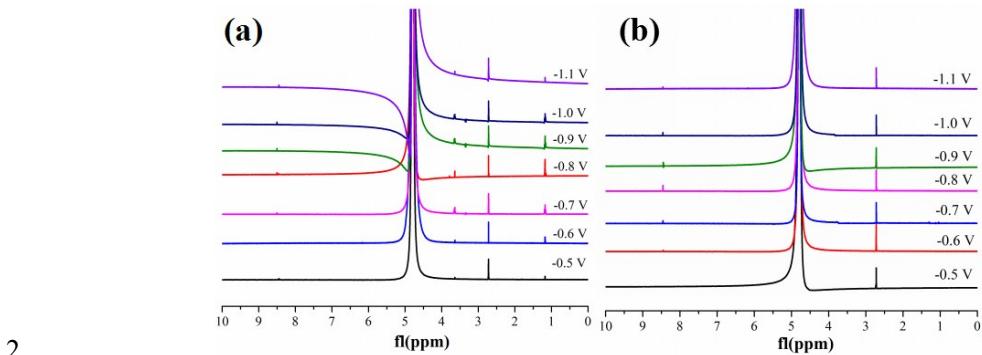
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3 Fig. S7 Tafel plot for formate on pure Co electrodes in 0.1 M KHCO_3 solution.

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3 **Fig. S8** ^1H -NMR of the aqueous products after the CO_2RR for 5 h at different potentials

4 over AgCo SA (a) and pure Co (b).

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2 **Table S1** Structural parameters for AgCo SA in cubic system

Atom	x	y	z	g	Ueq(Å ²)
Ag1	0	0	0	0.92(3)	0.00009
Co1	0	0	0	0.08(3)	0.00158

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4 **Table S2** Electrochemical CO₂RR properties of AgCo SA compared with other
5 electrocatalysts for ethanol production.

Catalysts		Electrolyte	Work potential	Current density (mA/cm ²)	Ethanol faradaic efficiency	Stability	Ref.
Bimetallic Alloy catalysts	CuAg alloy	1 M KOH	-0.7 V vs. RHE	300	25%	N.R.	2
	Cu _x Zn alloy	0.1 M KHCO ₃	-1.05 V vs. RHE	8.2	~29.1%	5 h	3
	Au ₃₆ Cu ₆₄	0.5 M KHCO ₃	-0.9 V vs. SCE	N.R.	~12%	N.R.	4
	AgCo SA	0.1 M KHCO₃	-0.8 V vs. RHE	7.4	72.3%	~48 h	This work
Other catalysts	Ag-G-NCF	0.1 M KHCO ₃	-0.6 V vs. RHE	0.31	82.1%	10 h	5
	N-doped mesoporous carbon	0.1 M KHCO ₃	-0.56 V vs. RHE	~0.25	77%	24 h	6
	Ag/Cu	1 M KHCO ₃	-0.67 V vs. RHE	250	~41%	N.R.	7
	Plasma-activated Cu nanocube	0.1 M KHCO ₃	-1.0 V vs. RHE	~34	~22%	N.R.	8
	Cu nanoparticles	0.1 M KHCO ₃	-0.85 V vs. RHE	10	~17%	10 h	9
	Cu ₂ O	0.1 M KHCO ₃	-0.99 V vs. RHE	35	~16%	60 h	10
	N-doped graphene quantum dots	1 M KOH	-0.78 V vs. RHE	~23	~16%	N.R.	11
	Cu(B)-2	0.1 M KHCO ₃	-1.1 V vs. RHE	~70	~27%	~36 h	12
	Cu ₂ S-Cu-V	1 M KOH	-0.92 V vs. RHE	120	~24.7%	~16 h	13
	Ag-Co ₃ O ₄ -CeO ₂ /LGC	0.1 M KHCO ₃	-0.85 V vs. RHE	12.8	54.2%	60 h	14
	Cu/TiO ₂ /NG	0.2 M KI	-0.75 V vs. RHE	0.65	43.6%	20 h	15
	CuO/TiO ₂	0.5 M KHCO ₃	-0.85 V vs. RHE	8.03	27.4%	25 h	16

6 N.R. : not reported

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