## Supporting Information for

## Advanced Composite Sorbent with High Thermal Stability and Superior Sorption Capacity without Hysteresis for a Better Thermal Battery

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**Figure S1.** Test procedures of thermodynamic measurement, using condition of 0.87 MPa as example.



Figure S2. Test procedures of kinetic measurement, using condition of 0.87 MPa as example.



**Figure S3.** Comparison of NH<sub>4</sub>Cl and EWN-Mec during pretreatment with Rubotherm balance: (a) pure NH<sub>4</sub>Cl under the condition of vacuum and heating temperature of 60°C, (b) EWN-Mec under the condition of vacuum and heating temperature of 120°C.



Figure S4. TG curves (solid lines) and DSC curves (dash lines) of ENG-TSA and EWNs.



Figure S5. The SEM images: (a) EWN-Mag, (b) EWN-Ult.



**Figure S6.** The nitrogen adsorption isotherms of: (a) ENG-TSA, (b) EWN-Mec, (c) EWN-Mag, (d) EWN-Ult.



Figure S7. The BJH adsorption dV/dD pore size distribution of ENG-TSA and EWNs.



Figure S8. The XRD patterns of EWN-Mec before and after ammonia sorption test.



Figure S9. The FTIR spectra of EWN-Mec before and after ammonia sorption test.



**Figure S10.** The ammonia sorption isotherms of EWN-Mec deduced from the D-A equation and Clapeyron equation.



**Figure S11.** The kinetic characteristics of EWN-Mec-NH<sub>3</sub>: (a) desorption processes with the ending  $T_{oil}$  ranging from 30°C to 60°C, under 0.63 Mpa, (b) sorption processes with the ending  $T_{oil}$  ranging from 20°C to 35°C, under 0.63 Mpa, (c) desorption processes with the ending  $T_{oil}$  ranging from 30°C to 50°C, under 0.44 Mpa, (d) sorption processes with the ending  $T_{oil}$  ranging from 20°C to 25°C, under 0.44 Mpa.



**Figure S12.** Kinetic simulation results: (a) the first stage desorption process, (b) the second stage desorption process, (c) the sorption process.

Summary Report	ENG-TSA	EWN-Mec	EWN-Mag	EWN-Ult
BET Surface Area (m <sup>2</sup> ·g <sup>-1</sup> )	18	7	11	14
Total pore volume ( $cm^3 \cdot g^{-1}$ )	0.033	0.013	0.019	0.028
Pore diameter (nm)	2.5	2.4	2.5	2.4

Table S1. Surface area, pore volume and pore size of the composites

**Table S2.** Kinetic model for EWN-Mec- $NH_3$ , where *k*, *m* and *n* are the reaction rate, reaction order and pressure potential parameter, subscripts s and d represent sorption and desorption, respectively.

Process	Conditions	Kinetic model
Des. $\frac{\mathrm{d}x_{\mathrm{m}}}{\mathrm{d}t}$	$T_{\rm s} < T_{\rm c}$	$-k_{\mathrm{ld}} \cdot \left[ x_{\mathrm{m}}(T_{\mathrm{s}}) - x_{\mathrm{eq}}(T_{\mathrm{s}}) \right]^{m_{\mathrm{ld}}} \cdot \left( \frac{p_{\mathrm{s}}}{p_{\mathrm{c}}} \right)^{n_{\mathrm{ld}}}$
	$T_{\rm s} > T_{\rm c}$	$-k_{2d} \cdot \left[x_{m}(T_{s}) - 0\right]^{m_{2d}} \cdot \left(\frac{p_{s}}{p_{c}}\right)^{n_{2d}}$
Sor. $\frac{\mathrm{d}x_{\mathrm{m}}}{\mathrm{d}t}$	$T_{\rm s} > T_{\rm c}$	0
	$T_{\rm s} < T_{\rm c}$	$k_{\rm s} \cdot \left[ x_{\rm eq}(T_{\rm s}) - x_{\rm m}(T_{\rm s}) \right]^{m_{\rm s}} \cdot \left( 1 - \frac{p_{\rm s}}{p_{\rm c}} \right)^{n_{\rm s}}$