

Supporting Information

A yolk@shell superhydrophobic/superhydrophilic solar evaporator for efficient and stable desalination

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Supporting Discussion: Calculation of heat losses

The heat loss of the solar evaporation device contains three parts: (a) radiation, (b) convection, (c) conduction.

a) Radiation: The radiation loss is calculated by the Stefan-Boltzmann equation.¹

$$Q_{\text{rad}} = \epsilon A \sigma (T_1^4 - T_2^4) \quad (1)$$

Where Q_{rad} represents heat flux, ϵ is the emissivity, A denotes the surface area, σ is the Stefan-Boltzmann constant ($5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$), T_1 (318.15 K) is the average surface temperature of the evaporator for a steady state of ~1 h, and T_2 (310.15 K) is the ambient temperature upward the evaporator under 1 sun irradiation. According to the equation, the radiation heat loss is ~5 %.

b) Convection: The convective heat loss is defined by the Newton' law of cooling.²

$$Q_{\text{conv}} = hA(T_1 - T_2) \quad (2)$$

Where Q_{conv} denotes the heat energy, h is the convection heat transfer coefficient, which is ~5 $\text{W m}^{-2} \text{ K}$. ΔT is the difference between the average surface temperature and the ambient temperature upward the evaporator ($\Delta T = 8 \text{ K}$). According to the equation, the convection heat loss is ~4%.

c) Conduction: The conduction loss was calculated based on.³

$$Q_{\text{cond}} = Cm\Delta T \quad (3)$$

Where Q_{cond} is the heat energy, C is the specific heat capacity of water ($4.2 \text{ J K}^{-1} \text{ g}^{-1}$), m (80 g) is the water weight, and ΔT (0.6 K) is the temperature difference of pure water after and before solar illumination under 1 sun for 1 h. Therefore, the

conduction heat loss is ~3%.

The phenomenon of high efficiency and relatively high heat loss is explained below.

(i) In the continuous irradiation process, the surface temperature of the evaporator, the temperature of the bulk water and the temperature around the environment are constantly changing. The fixed value taken in the calculation makes the calculation result in error.

(ii) The error induced by the infrared temperature measurement.

(iii) The surface of the evaporator is very rough. Thus, the surface area of the evaporator is larger than the projected area for the calculation of the efficiency and heat losses.

Table S1. Effect of MWCNTs concentration on evaporation rate.

MWCNTs concentration (mg mL ⁻¹)	0.125	0.25	0.5	1	2
Evaporation rate (kg m ⁻² h ⁻¹)	0.95±0.2	1.23±0.3	1.45±0.3	1.44±0.4	1.45±0.2

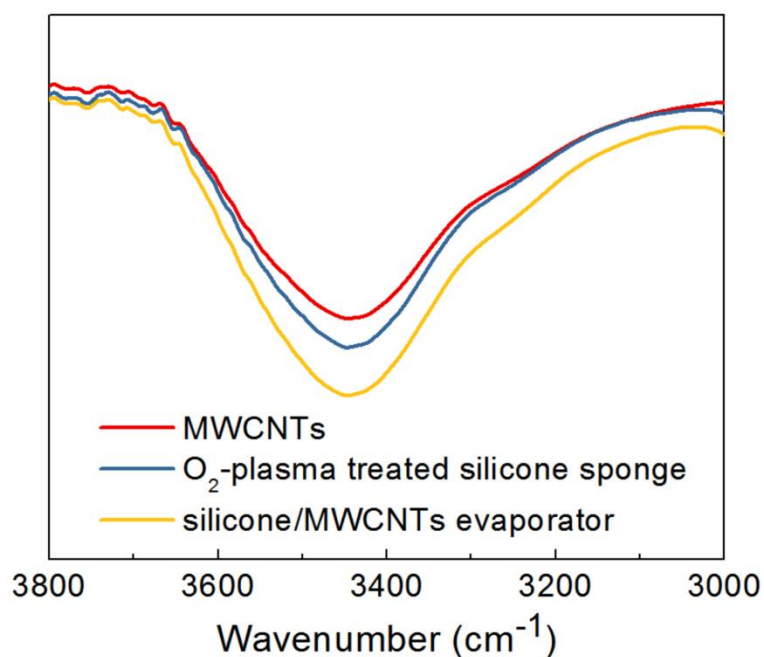


Fig. S1 FTIR spectra of acid activated MWCNTs, O₂-plasma treated silicone sponge and the silicone/MWCNTs evaporator. The bands at 3300~3500 cm⁻¹ are attributed to stretching vibrations of hydroxyl groups. Compared to the bands of MWCNTs and O₂-plasma treated silicone sponge, the band of the silicone/MWCNTs evaporator is widened and enhanced. This means hydrogen bonding between MWCNTs and silicone sponge, which increased polarization degree of the O-H bond.⁴

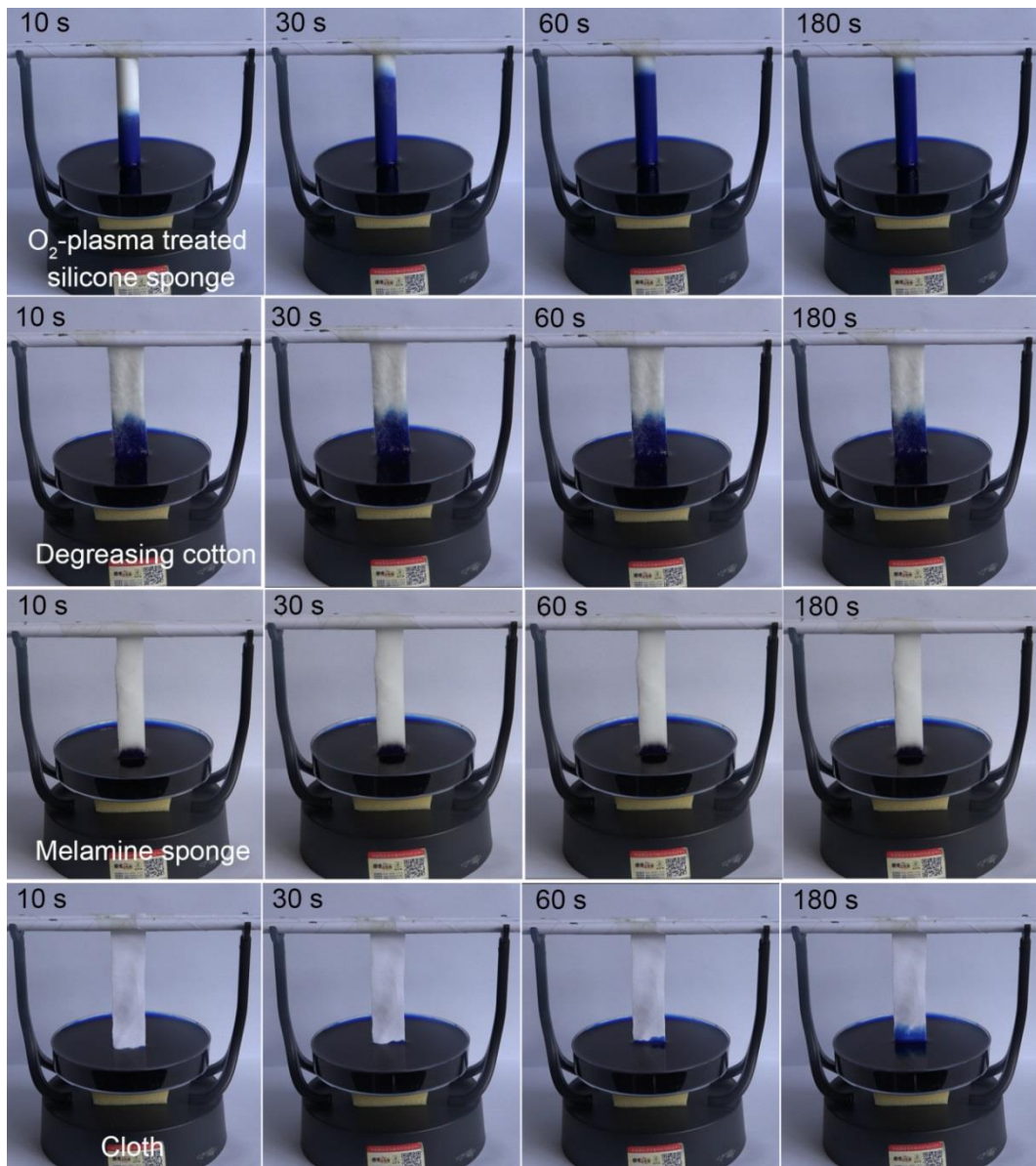


Fig. S2 Climbing behaviors of water dyed with methylene blue in the shell of the O₂-plasma treated silicone sponge and some other conventional matrices for water transport during solar evaporation.

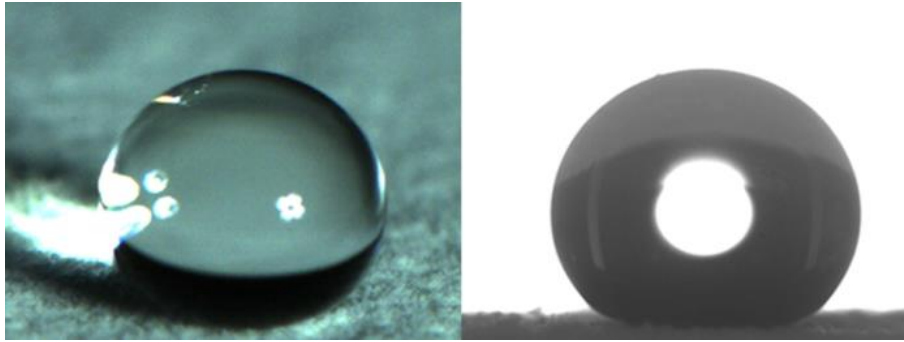


Fig. S3 Photographs of water droplets on the superhydrophobic yolk of the silicone/MWCNTs evaporator.

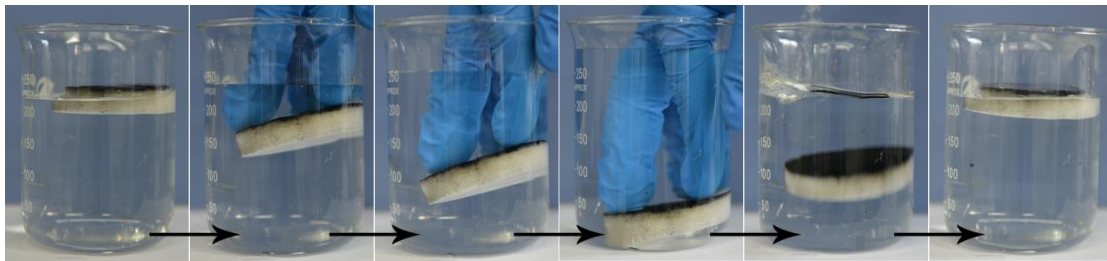


Fig. S4 Representative photographs of the silicone/MWCNTs evaporator in 20 cycles of squeezing and releasing in water.

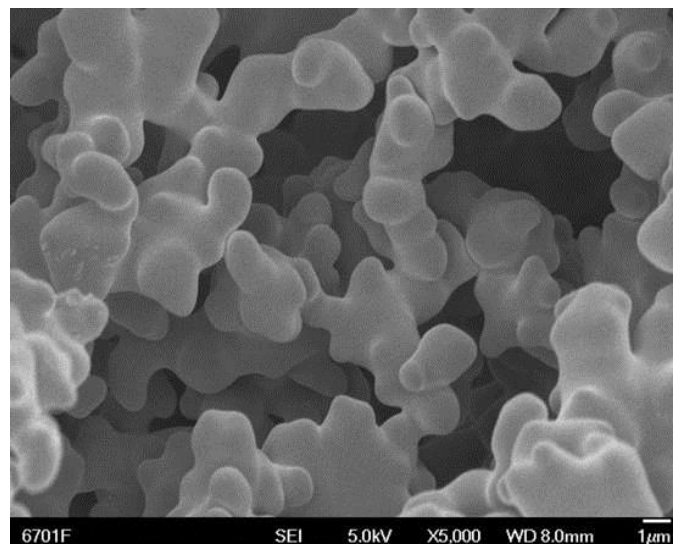


Fig. S5 Cross-sectional SEM image of the silicone/MWCNTs evaporator after 100 compression-release cycles with 50% strain.

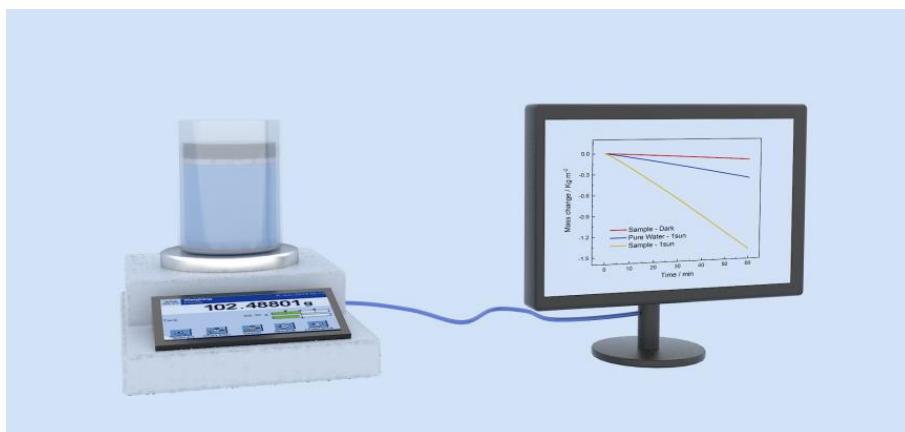


Fig. S6 Photograph of the custom made setup for testing the solar evaporation properties of the silicone/MWCNTs evaporators.



Fig. S7 Photograph of water vapor generated by the silicone/MWCNTs evaporator under 2 sun.

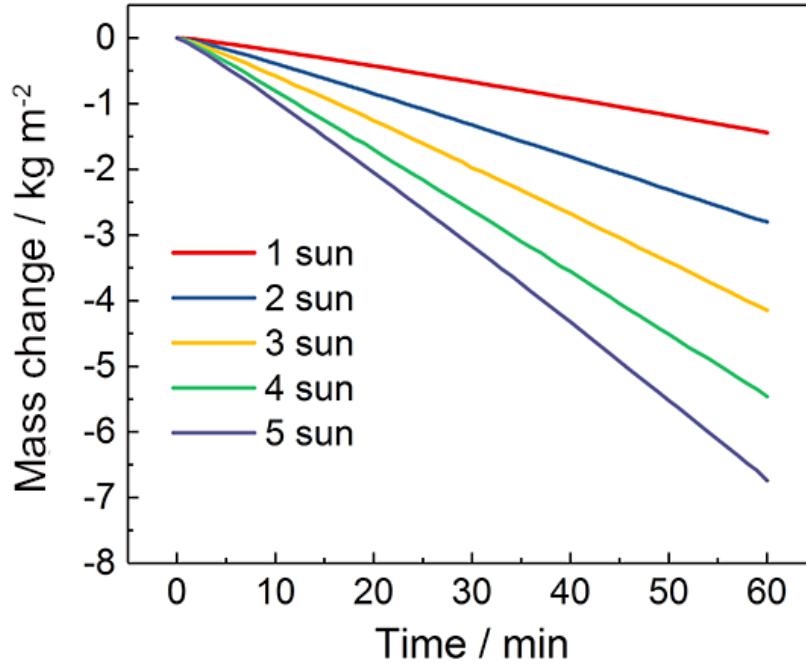


Fig. S8 Water mass changes versus time under different illuminations in the presence of the silicone/MWCNTs evaporator.

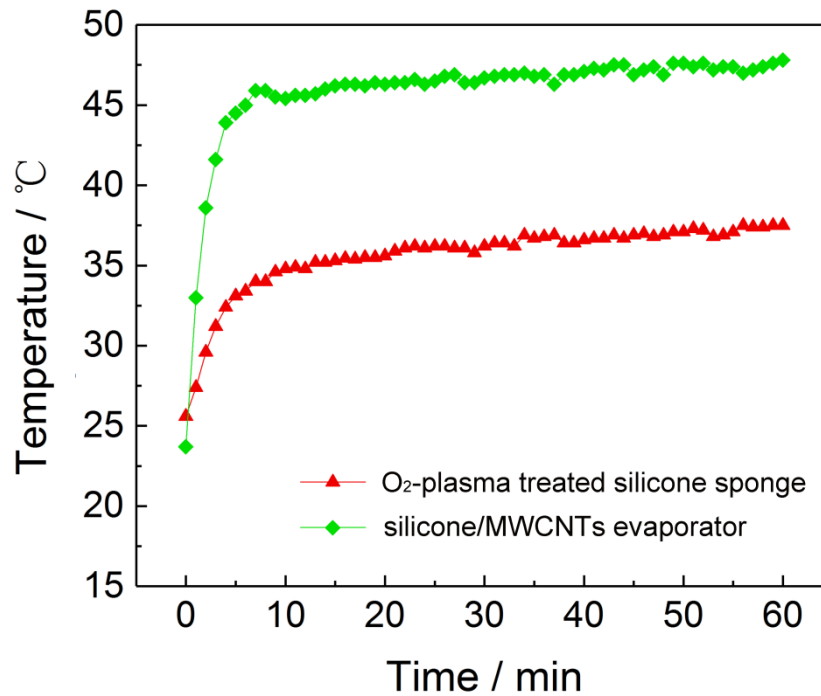


Fig. S9 Variation of top surface temperature of the silicone/MWCNTs evaporator under 1 sun with the O₂-plasma treated silicone sponge for comparison.

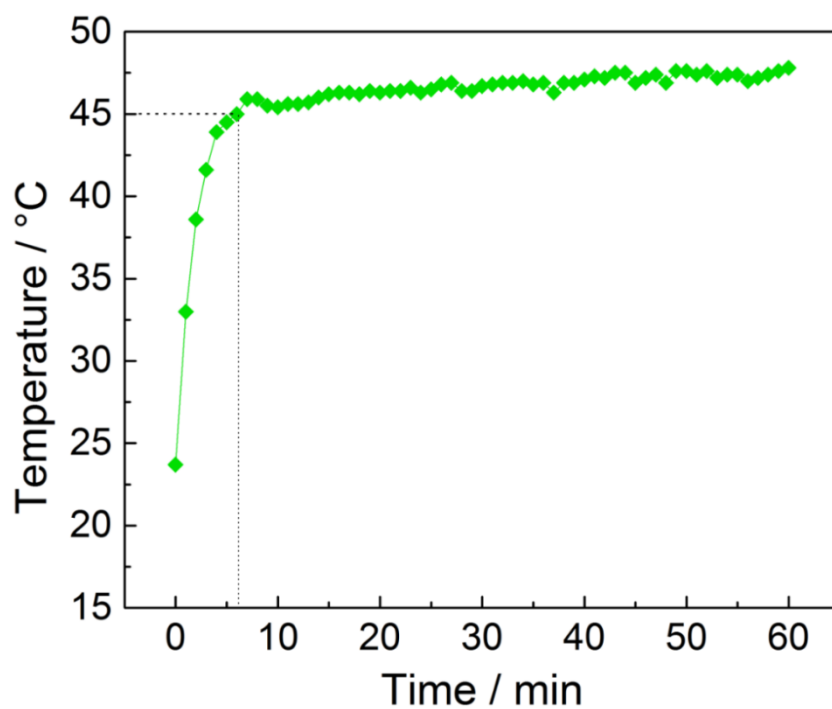


Fig. S10 Variation of top surface temperature of the silicone/MWCNTs evaporator with irradiation time under 1 sun.

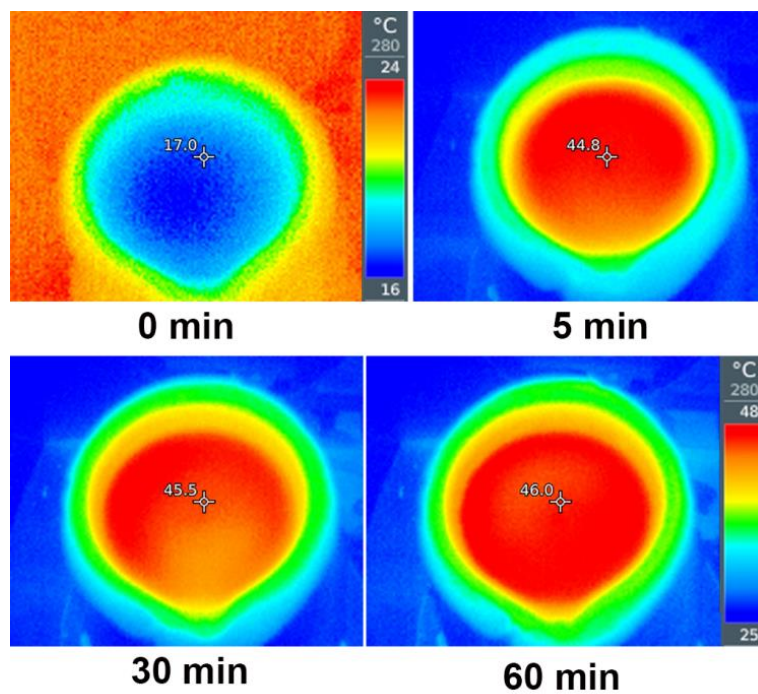


Fig. S11 Infrared images of top surface of the silicone/MWCNTs evaporator under 1 sun.

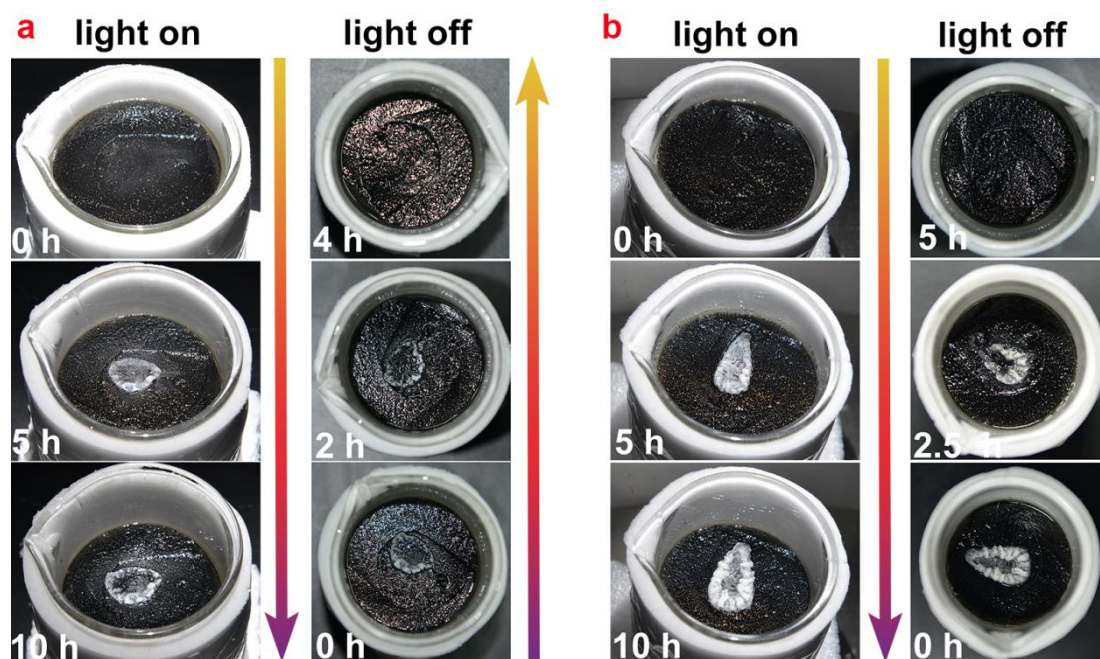


Fig. S12 Salt precipitation (1 sun) and salt ablation (room conditions) processes of seawater from (a) the Bohai Sea and (b) the Yellow Sea on the top surface of the silicone/MWCNTs evaporator.

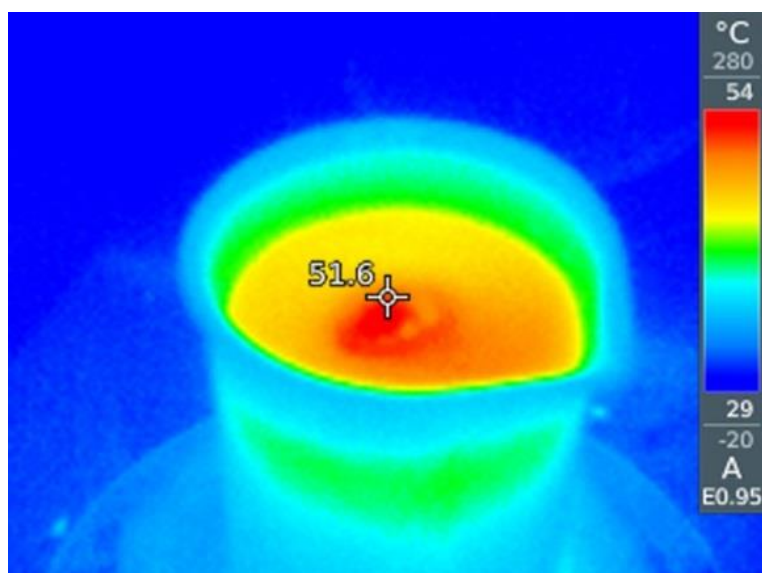


Fig. 13 Infrared image of the evaporator surface after continuous irradiation for 2 h under 1 sun.



Fig. 14 Measurement of water CA of the shell of the silicone/MWCNTs evaporator after being soaked in 3.5 wt% NaCl solution for 30 d.

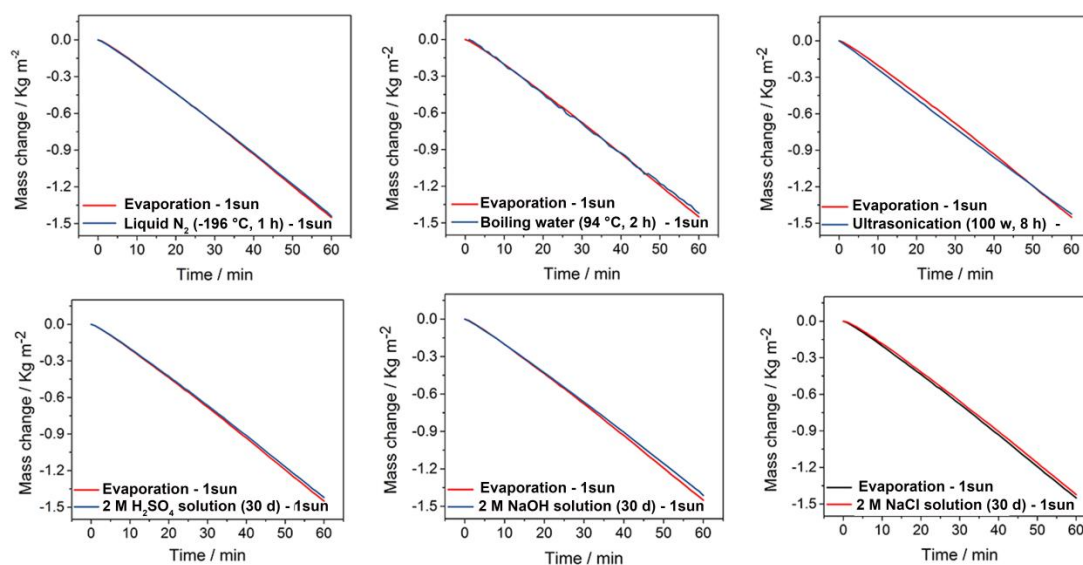


Fig. S15 Water mass changes of the silicone/MWCNTs evaporator after immersion in liquid N₂ (-196 °C, 1 h), boiling water (94 °C, 2 h), deionized water under ultrasonication (100 w, 8 h), 2 M H₂SO₄ solution (30 d), 2 M NaOH solution (30 d) and 2 M NaCl solution (30 d).

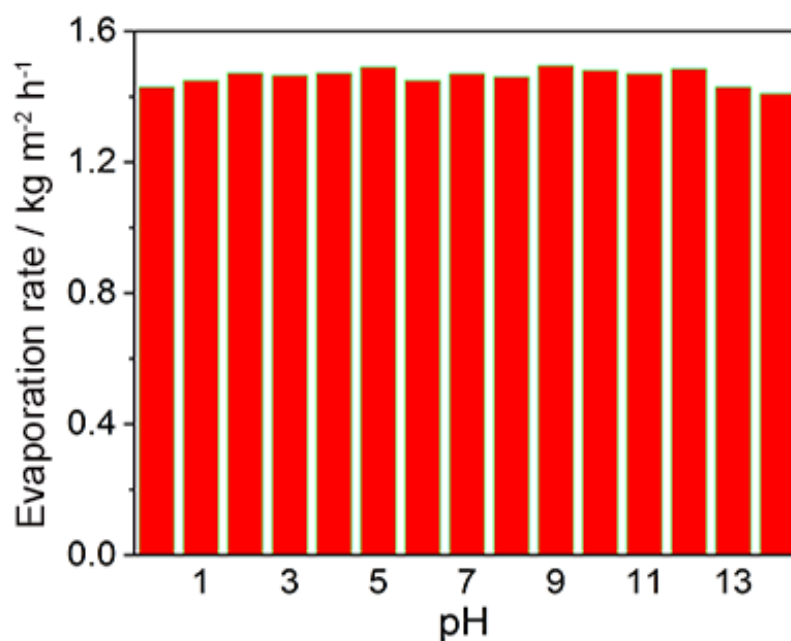


Fig. S16 Evaporation rate of aqueous solutions with different pH under 1 sun illumination. The pH of the aqueous solutions was regulated using 1 M H₂SO₄ solution and 1 M NaOH solution.

Movie S1. Impacting of a 10 μ L water droplet from a height of 10 mm on the shell of the evaporator. This video highlights the superhydrophilicity of the shell and ultrafast water transport in the shell.

Movie S2. Climbing behaviors of water dyed with methylene blue in the shell of the O₂-plasma treated silicone sponge and some other conventional matrices for water transport during solar evaporation. This video highlights the much faster water transport in the shell of the O₂-plasma treated silicone sponge than the others.

Movie S3. Impacting of a 10 μ L water droplet from a height of 10 mm on the yolk of the evaporator. This video highlights the superhydrophobicity of the yolk.

References

1. G. Ni, G. Li, Svetlana V. Boriskina, H. Li, W. Yang, T. Zhang and G. Chen, *Nat. Energy*, 2016, **1**, 16126.
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