

Bimetallic Ni–Pt nanoparticles immobilized on mesoporous N-doped carbon as highly efficient catalysts for complete hydrogen evolution from hydrazine borane

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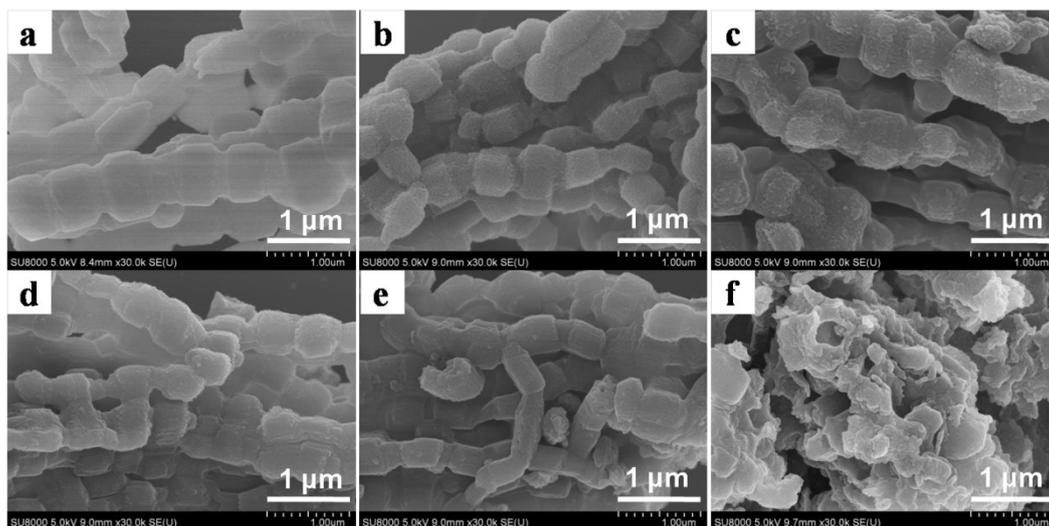


Figure S1. SEM images of (a) SBA-15, (b) MNC-500, (c) MNC-600, (d) MNC-700, (e) MNC-800, and (f) MNC-900.

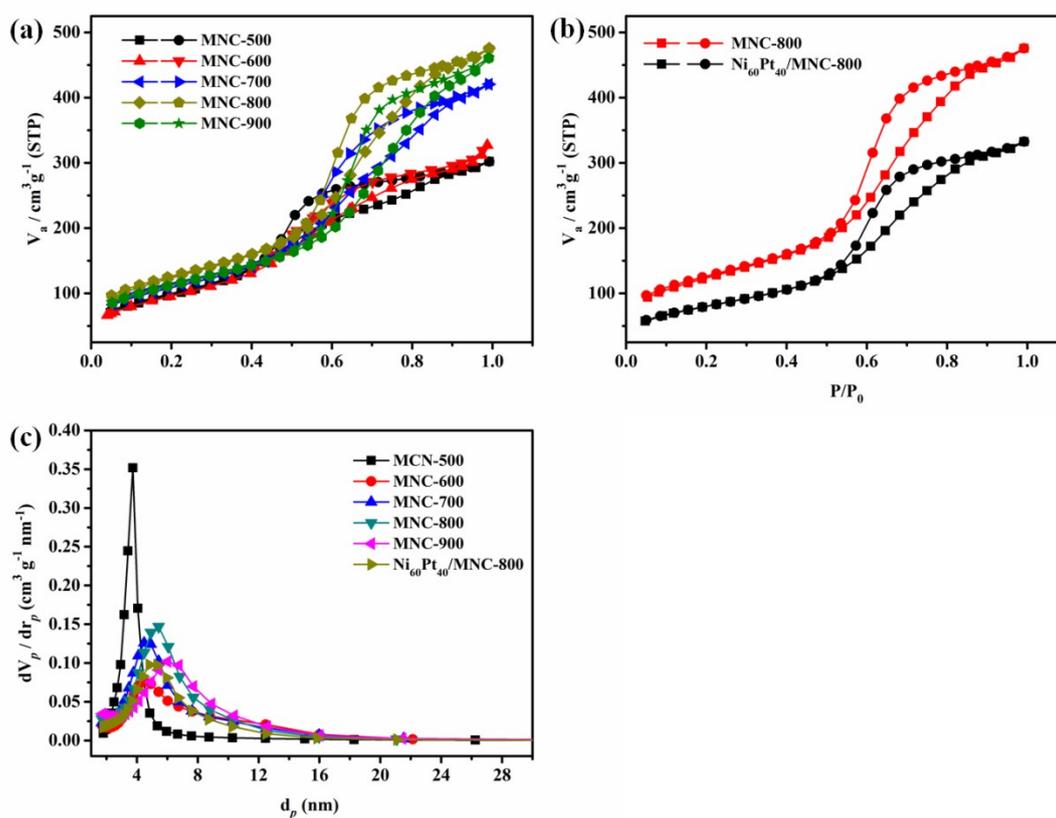


Figure S2. Nitrogen adsorption-desorption isotherms of (a) MNC-500, MNC-600, MNC-700, MNC-800, MNC-900, (b) $\text{Ni}_{60}\text{Pt}_{40}/\text{MNC-800}$; (c) the corresponding pore size distribution.

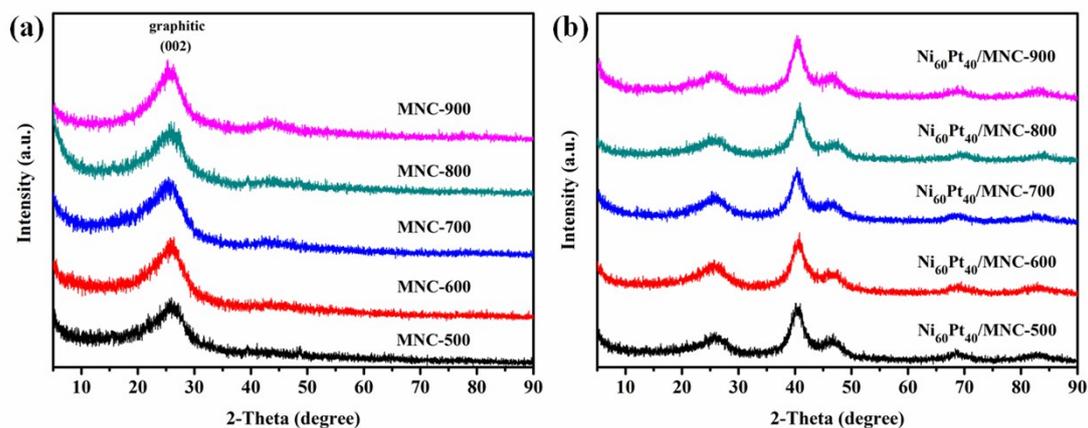


Figure S3. XRD patterns of (a) MNC-500, MNC-600, MNC-700, MNC-800, and MNC-900; and (b) Ni₆₀Pt₄₀/MNC-500, Ni₆₀Pt₄₀/MNC-600, Ni₆₀Pt₄₀/MNC-700, Ni₆₀Pt₄₀/MNC-800, and Ni₆₀Pt₄₀/MNC-900 NCs.

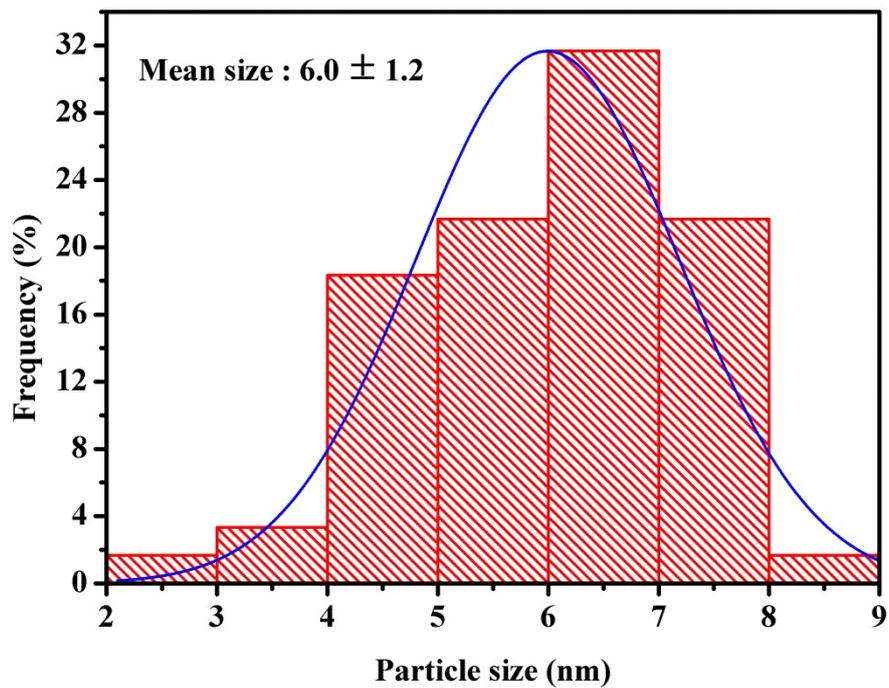


Figure S4. The corresponding distribution size histogram of Ni₆₀Pt₄₀/MNC-800.

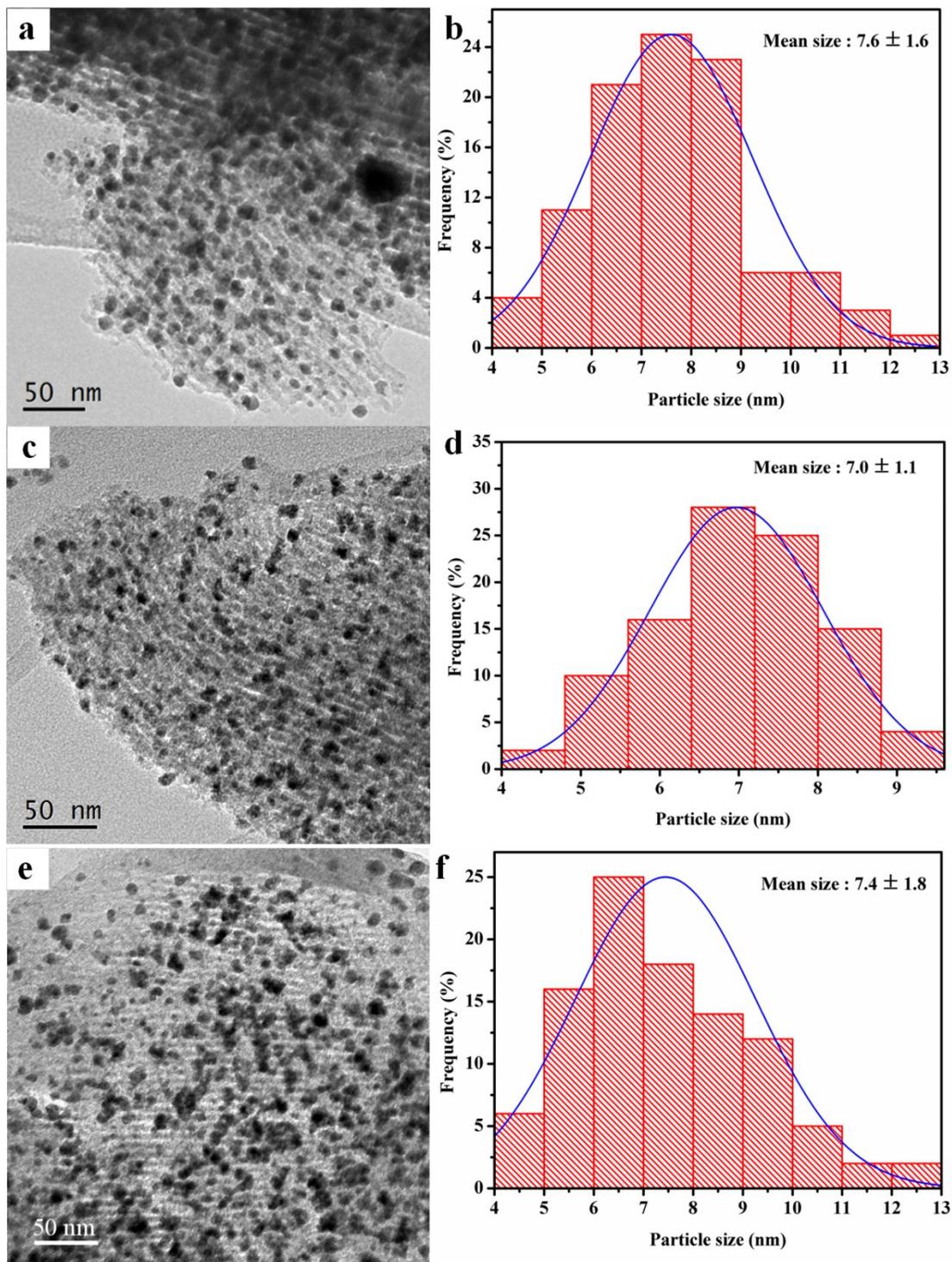


Figure S5. Representative TEM images and the corresponding distribution size histograms of (a and b) Ni₆₀Pt₄₀/MNC-600, (c and d) Ni₆₀Pt₄₀/MNC-700, and (e and f) Ni₆₀Pt₄₀/MNC-900.

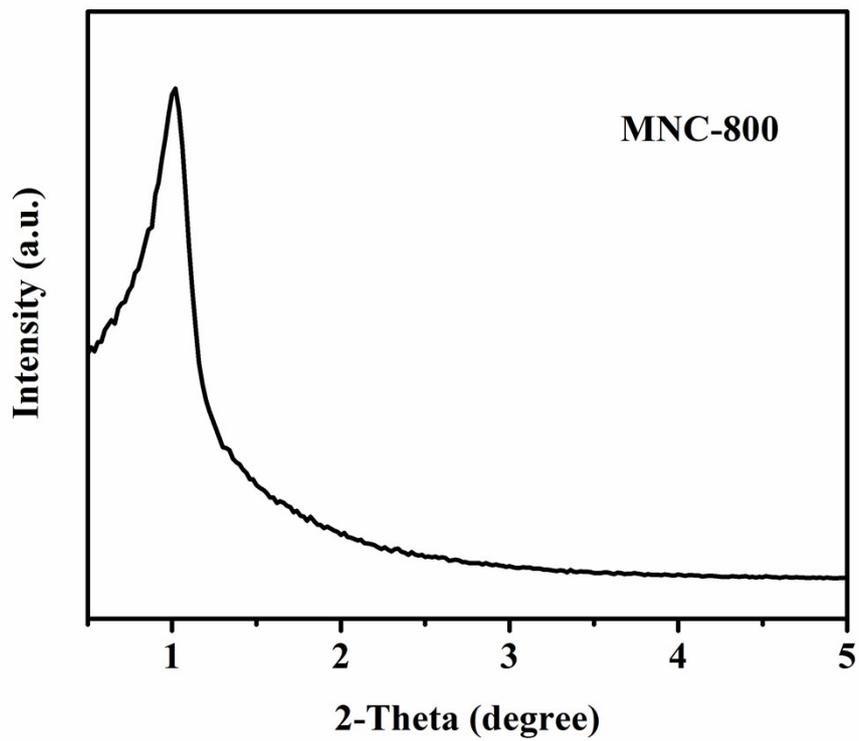


Figure S6. Low-angle XRD pattern of MNC-800.

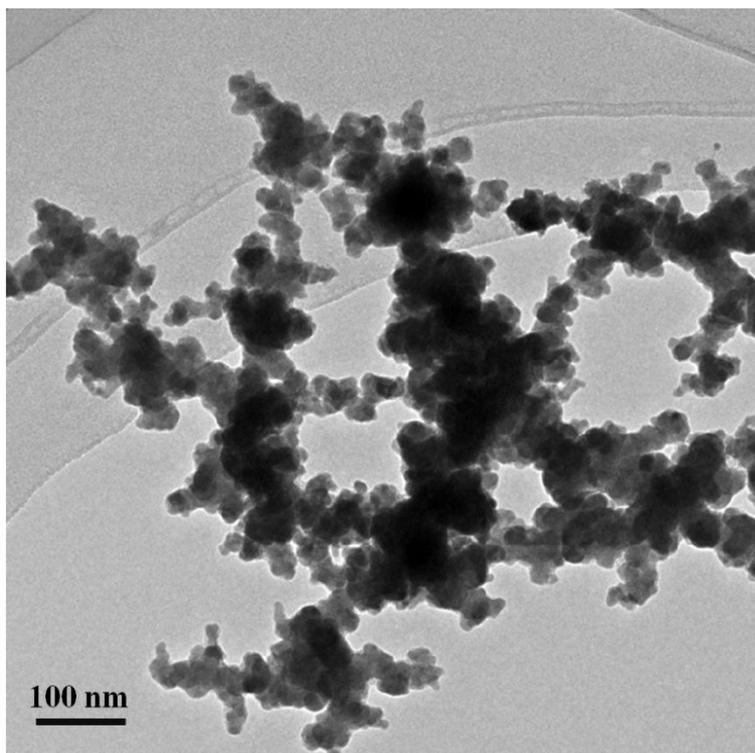


Figure S7. Representative TEM image of MNC-free Ni₆₀Pt₄₀ NPs.

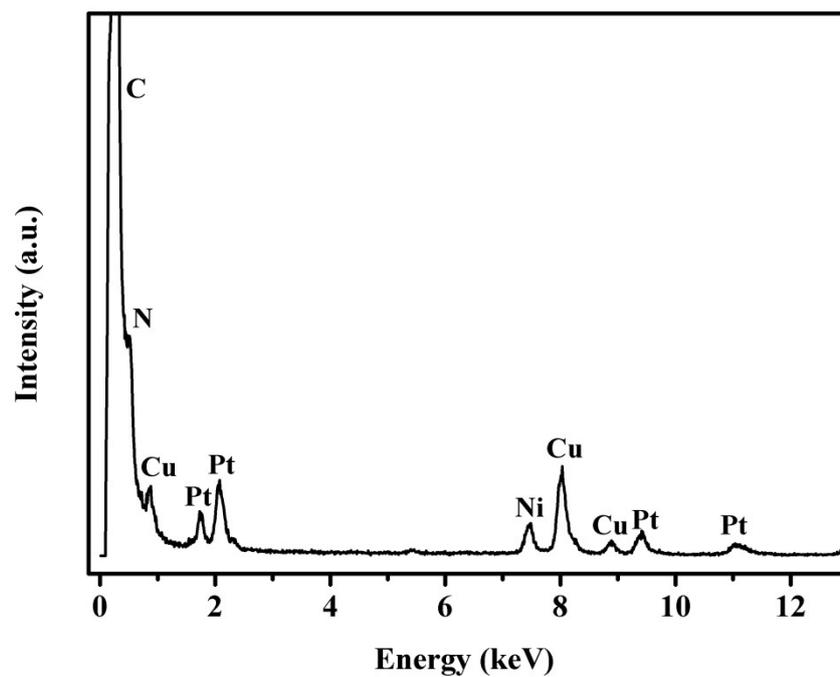


Figure S8. EDX spectrum of Ni₆₀Pt₄₀/MNC-800 NCs. The Cu signal originates from Cu grid.

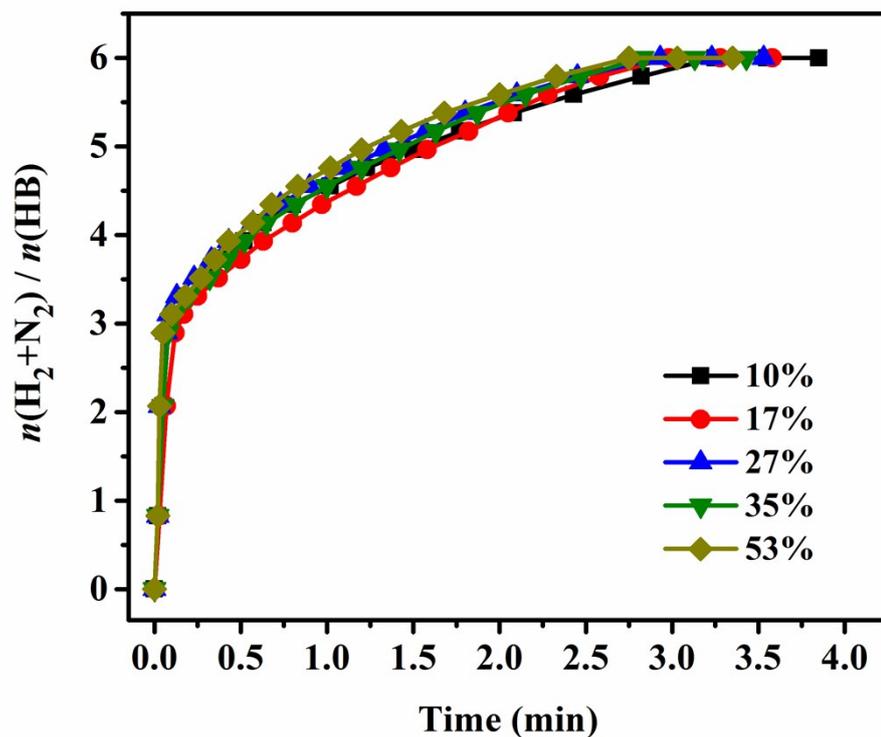


Figure S9. Time course plots for hydrogen generation from HB (200 mM, 5 mL) catalyzed by Ni₆₀Pt₄₀/MNC-800 NCs ($n_{Pt+Ni}/n_{HB} = 0.1$) with different metal loadings at 298 K.

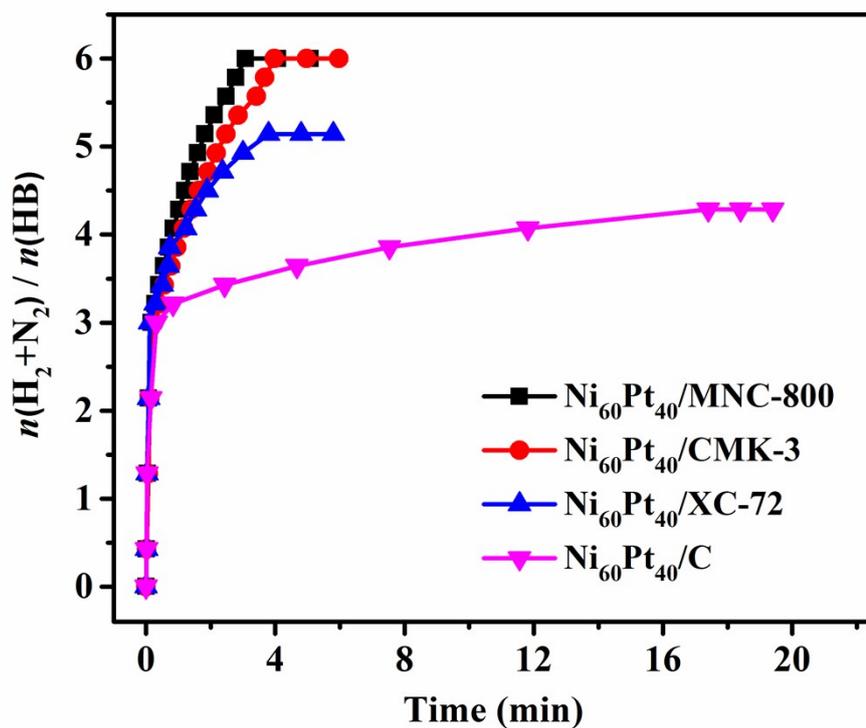


Figure S10. Time course plots for hydrogen generation from HB (200 mM, 5 mL) catalyzed by Ni₆₀Pt₄₀/MNC-800, Ni₆₀Pt₄₀/CMK-3, Ni₆₀Pt₄₀/XC-72, and Ni₆₀Pt₄₀/C NCs ($n_{\text{Pt+Ni}}/n_{\text{HB}} = 0.1$) at 298 K.

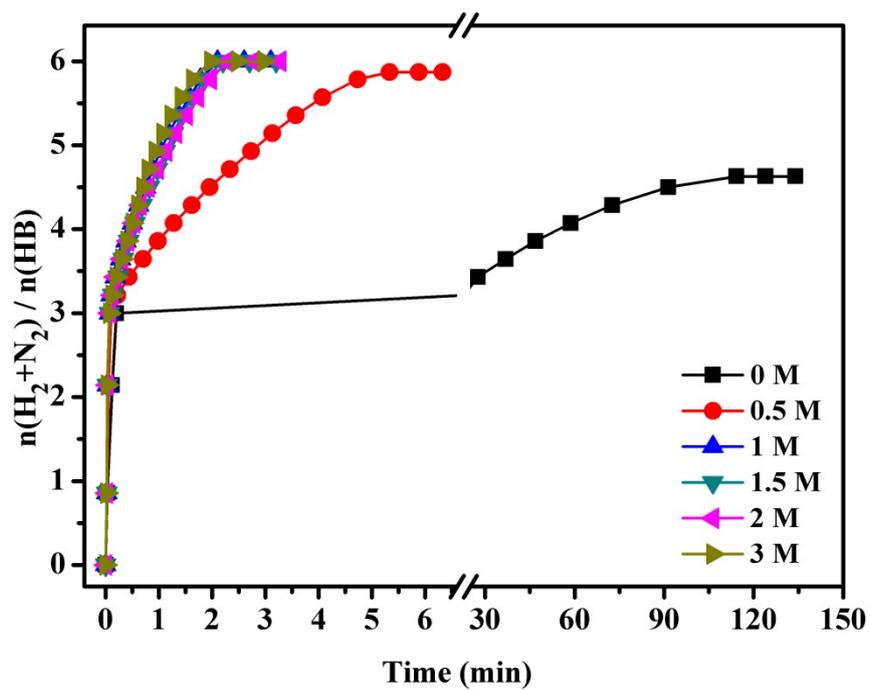


Figure S11. Time course plots for hydrogen generation from HB (200 mM, 5 mL) catalyzed by Ni₆₀Pt₄₀/MNC-800 NCs ($n_{Pt+Ni}/n_{HB} = 0.1$) with different molar concentration of NaOH at 298 K.

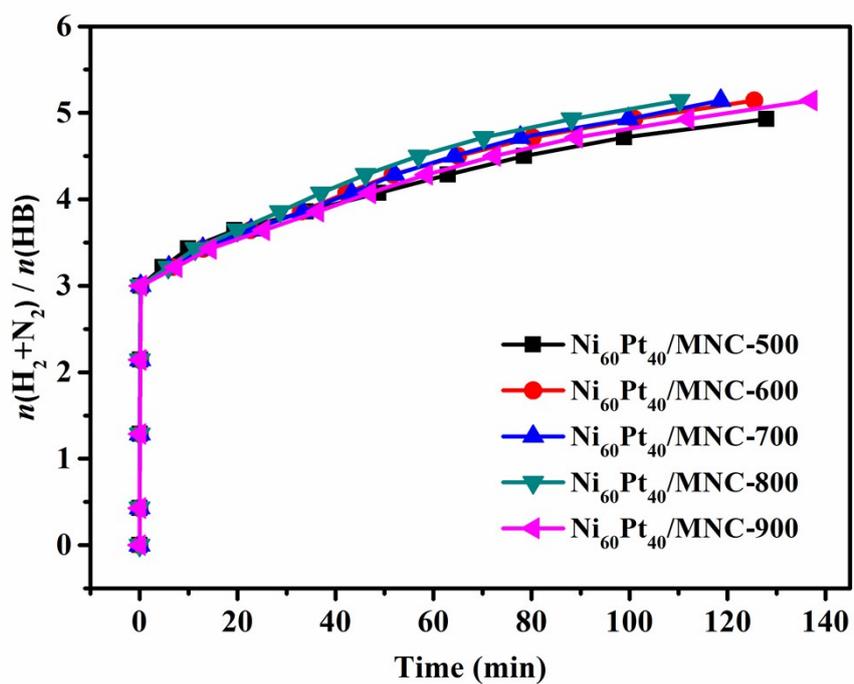


Figure S12. Time course plots for hydrogen generation from HB (200 mM, 5 mL) catalyzed by Ni₆₀Pt₄₀/MNC-500, Ni₆₀Pt₄₀/MNC-600, Ni₆₀Pt₄₀/MNC-700, Ni₆₀Pt₄₀/MNC-800, and Ni₆₀Pt₄₀/MNC-900 NCs ($n_{Pt+Ni}/n_{HB} = 0.1$) without NaOH at 298 K.

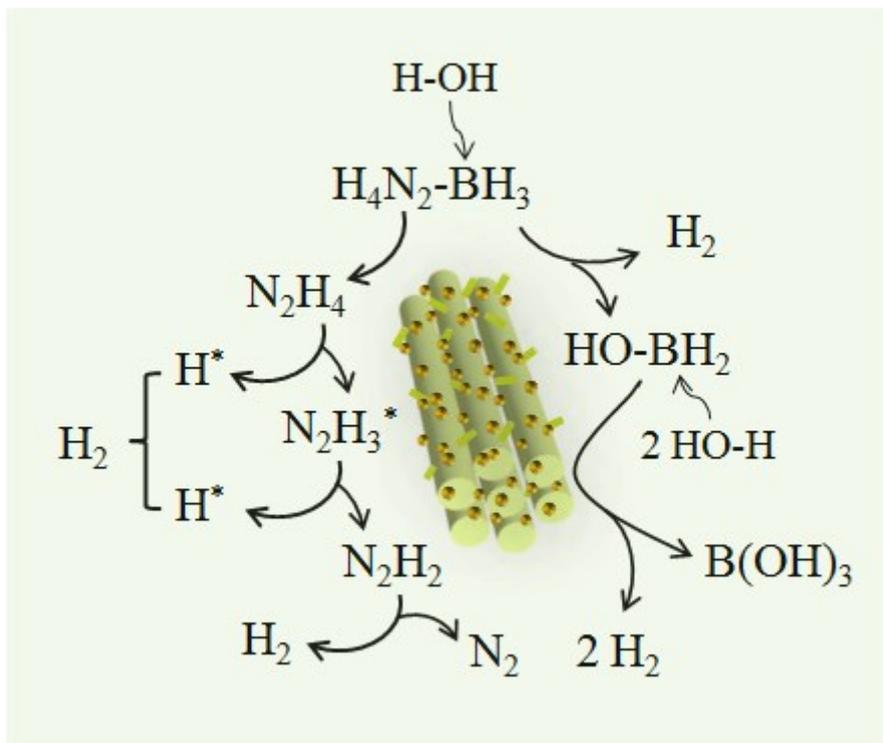


Figure S13. Schematic representation of H₂ generation from HB over Ni₆₀Pt₄₀/MNC-800 catalysts.

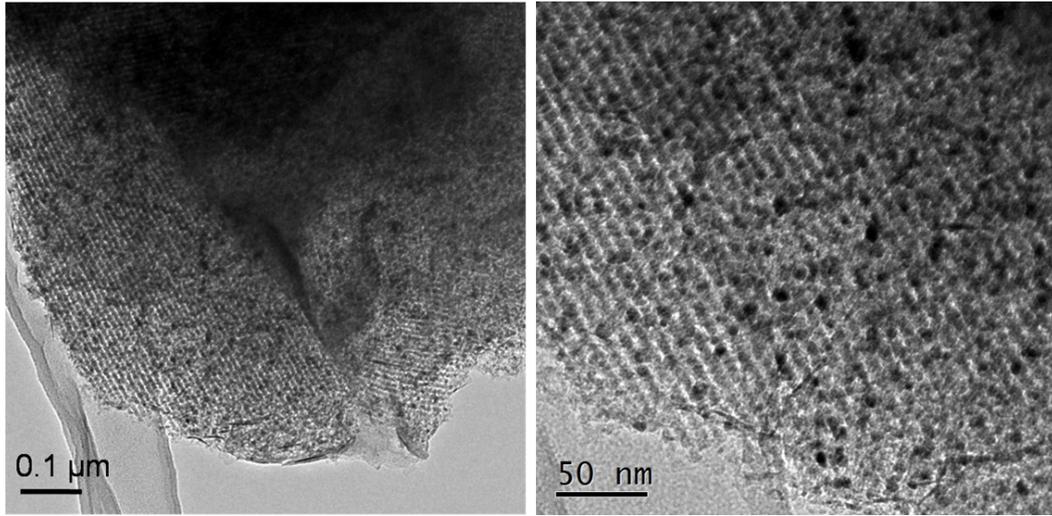


Figure S14. TEM images of the Ni₆₀Pt₄₀/MNC-800 NCs after the reusability test.

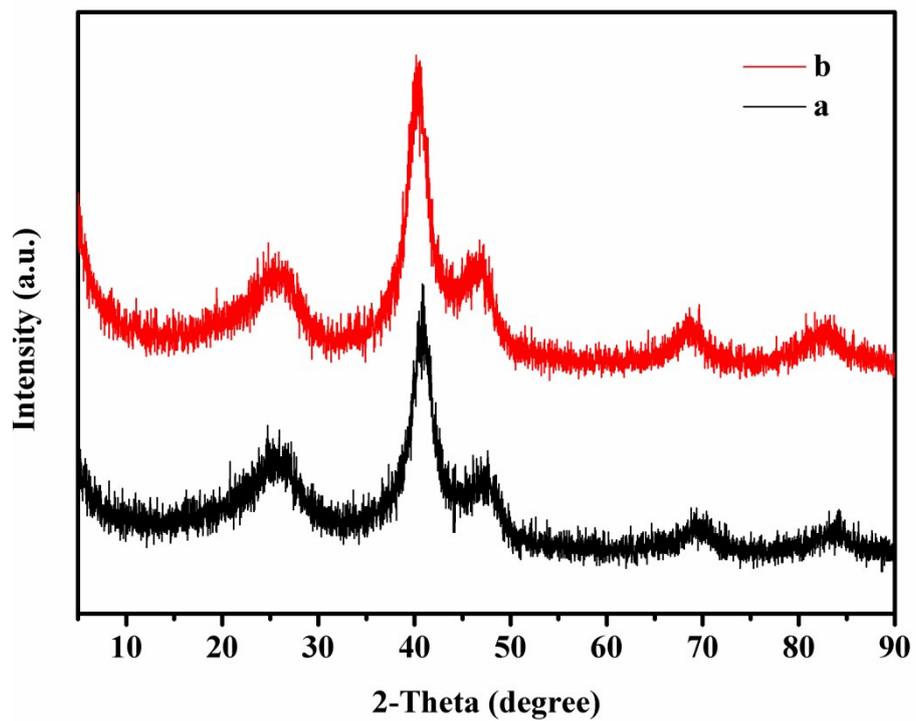


Figure S15. Powder XRD patterns of (a) fresh synthesized Ni₆₀Pt₄₀/MNC-800 NCs and (b) the Ni₆₀Pt₄₀/MNC-800 NCs after the durability and reusability test.

Table S1. Texture Parameters of MNC-500, MNC-600, MNC-700, MNC-800, MNC-900 and Ni₆₀Pt₄₀/MNC-800.

sample	S_{BET} (m² g⁻¹)	pore volume (cm³ g⁻¹)	pore size (nm)
MNC-500	354	0.47	4.44
MNC-600	364	0.51	5.56
MNC-700	385	0.65	5.78
MNC-800	438	0.74	5.82
MNC-900	396	0.71	6.49
Ni ₆₀ Pt ₄₀ /MNC-800	289	0.51	5.78

Table S2. Element analysis of MNC-500, MNC-600, MNC-700, MNC-800, and MNC-900.

Sample	N wt%	C wt%	C/N mole ratio
MNC-500	18.46	61.70	3.85
MNC-600	18.07	65.90	4.17
MNC-700	13.62	71.82	6.25
MNC-800	9.75	73.02	9.09
MNC-900	8.67	78.26	10.52

Table S3. The catalysts composition determined by inductively coupled plasma atomic emission spectroscopic (ICP-AES).

Catalysts	Ni (wt%)	Pt (wt%)	Ni/Pt initial composition	Ni/Pt final composition
Ni/MNC-800	9.2	-	-	-
Ni ₈₀ Pt ₂₀ /MNC-800	7.0	6.1	80:20	79:21
Ni ₇₀ Pt ₃₀ /MNC-800	6.2	9.0	70:30	69:31
Ni ₆₀ Pt ₄₀ /MNC-800	5.3	11.8	60:40	60:40
Ni ₅₀ Pt ₅₀ /MNC-800	4.3	14.4	50:50	50:50
Ni ₄₀ Pt ₆₀ /MNC-800	3.4	16.9	40:60	40:60
Ni ₃₀ Pt ₇₀ /MNC-800	2.5	19.4	30:70	30:70
Pt/MNC-800	-	26.2	-	-
Ni ₆₀ Pt ₄₀	31.6	68.4	60:40	61:39
Ni ₆₀ Pt ₄₀ /MNC-800 after five cycles	5.2	11.7	60:40	60:40

Table S4. The relationship between the performance of the catalyst and the C/N mole ratio and the mean particle size of the metal particles.

Sample	C/N mole ratio	Mean particle size / nm	TOF / h⁻¹ (298K)
Ni ₆₀ Pt ₄₀ /MNC-600	4.17	7.6	508
Ni ₆₀ Pt ₄₀ /MNC-700	6.25	7.0	882
Ni ₆₀ Pt ₄₀ /MNC-800	9.09	6.0	1111
Ni ₆₀ Pt ₄₀ /MNC-900	10.52	7.4	857

Calculation method for *TOF*:

The total turnover frequency (*TOF*) reported in this work is an apparent *TOF* value based on the number of metal atoms in catalyst, which is calculated from the equation as follow:

$$TOF = \frac{n_{H_2}}{n_{metal} \times t}$$

Where n_{H_2} is the mole number of generated H_2 , n_{metal} is the mole number of metal (Ni and Pt) in catalyst and t is the completed reaction time in hour.