# PtP<sub>2</sub> nanoparticles on N, P doped carbon with self-converting process to coreshell Pt/PtP<sub>2</sub> as efficient and robust ORR catalyst

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## **Theoretical details**

### **Calculations details of the Oxygen Reduction Reaction**

In the acidic solution, the overall ORR reaction is:

$$O_2 + 4H^+ + 4e^- \rightarrow 2H_2O$$

The ORR can proceed through the following elementary steps usually employed to investigate the electrocatalysis of the ORR on various materials:

R1: 
$$O_2(g) + H^+ + e^- + * \rightarrow *OOH$$
  
R2: \*OOH + H<sup>+</sup> +  $e^- \rightarrow *O + H_2O(l)$   
R3: \*O + H<sup>+</sup> +  $e^- \rightarrow *OH$   
R4: \*OH + H<sup>+</sup> +  $e^- \rightarrow H_2O(l) + *$ 

where \* represents an active site on the catalytic surface, and (l) and (g) refer to the liquid and gas phase, respectively.

According to previous studies,<sup>1, 2</sup> the Gibbs free energy of each step is calculated as follows (equation 1):

$$\Delta G = \Delta E + \Delta Z P E - T \Delta S$$

Where the  $\Delta E$  can be obtained by the computation of geometrical structures,  $\Delta ZPE$  is the difference in zero point energies due to the reaction, and the  $\Delta S$  is the change in

entropy calculated using vibrational frequencies analysis.

### **Experimental details**

### Electrochemically active surface area (ESCA)

Cyclic voltammetry (CV) measurements were carried out in 0.1 M HClO<sub>4</sub> solutions under a flow of Ar (Airgas, ultrahigh purity) at a sweep rate of 50 mV/s. The ECSA was estimated by measuring the charge associated with Hupd adsorption (QH) between 0 and 0.37 V and assuming 210  $\mu$ C/cm<sup>2</sup> for the adsorption of a monolayer of hydrogen on a Pt surface (q<sub>H</sub>). The H<sub>upd</sub> adsorption charge (QH) can be determined using QH = 0.5 × Q, where Q is the charge in the H<sub>upd</sub> adsorption/desorption area obtained after double-layer correction. Then, the specific ECSA was calculated based on the following relation:<sup>3</sup>

specific ECSA = 
$$\frac{Q_H}{m * q_H}$$

where QH is the charge for  $H_{upd}$  adsorption, m is the loading amount of metal, and  $q_H$  is the charge required for monolayer adsorption of hydrogen on a Pt surface.

### Number of electron transfer

As for ORR experiment,  $O_2$  was bubbled for 20 min prior to the test and maintained in the headspace of the electrolyte throughout the testing process. The working electrode was scanned cathodically at a rate of 10 mV s<sup>-1</sup> with varying rotating speed from 400 to 2000 rpm in  $O_2$  -saturated 0.1 M HClO<sub>4</sub> aqueous solution. The electron transfer number per oxygen molecule for oxygen reduction can be determined on the basis of the Koutechy-Levich equations:<sup>4</sup>

$$1/J=1/J_{L}+1/J_{K}=1/B\omega^{1/2}+1/J_{K}$$
(1)  
B=0.62nFC<sub>0</sub> (D0)<sup>2/3</sup>v<sup>-1/6</sup> (2)  
$$J_{K=nFkC_{0}}$$
(3)

Where J is the measured current density and is the electrode rotating rate (rad s<sup>-1</sup>). B is determined from the slope of the Koutechy-Levich (K-L) plot based on Levich equation

(2).  $J_L$  and  $J_K$  are the diffusion and kinetic-limiting current densities, n is the transferred electron number, F is the Faraday constant (F= 96485 C mol<sup>-1</sup>), C<sub>0</sub> is the O<sub>2</sub> concentration in the electrolyte (C<sub>0</sub> = 1.26×10<sup>-6</sup> mol cm<sup>-3</sup>), D<sub>0</sub> is the diffusion coefficient of O<sub>2</sub> (D<sub>0</sub> = 1.93×10<sup>-5</sup> cm<sup>2</sup> s<sup>-1</sup>), and v is the kinetic viscosity (v = 0.01009 cm<sup>2</sup> s<sup>-1</sup>). The constant 0.62 is adopted when the rotation speed is expressed in rad s<sup>-1</sup>. For ORR experiments, the LSV curves were obtained at a scan rate of 10 mV s<sup>-1</sup>. In order to obtain a stable current, the LSV data were collected at the second sweep.

#### Mass and specific activities

The ORR measurements were performed in 0.1 M HClO<sub>4</sub> solutions under flow of O<sub>2</sub> (Airgas, Research grade) using the glassy carbon RDE at a rotation rate of 1,600 rpm and a sweep rate of 10 mV/s. In order to produce a clean electrode surface, several potential sweeps between -0.05 and 1.3 V versus RHE were applied to the electrode prior to the ORR measurement. In the ORR polarization curve, current densities were normalized in reference to the geometric area of the glassy carbon RDE (0.196 cm<sup>2</sup>). For the ORR at a RDE, the Koutecky-Levich equation can be described as follows:

$$\frac{1}{i} = \frac{1}{i_k} + \frac{1}{i_d}$$

Where i is the experimentally measured current,  $i_d$  is the diffusion-limiting current, and  $i_k$  is the kinetic current. Then, the kinetic current was calculated based on the following equation:

$$i_k = \frac{i * i_d}{i_d - i}$$

For each catalyst, the kinetic current was normalized to loading amount of metal and ECSA in order to obtain mass and specific activities, respectively. The accelerated durability tests were performed at room temperature in  $O_2$ -saturated 0.1 M HClO<sub>4</sub> solutions by applying cyclic potential sweeps between 0.3 and 1.3 V versus RHE at a sweep rate of 50 mV/s for a given number of cycles.



Figure S1. Optimized bulk PtP<sub>2</sub> model. Atom colors: blue: Pt, purple: P.



**Figure S2.** The theoretical models used in DFT calculations of Pt (111), PtP<sub>2</sub> (111) and Pt/PtP<sub>2</sub> (111), respectively. Atom colors: blue: Pt, purple: P.



Figure S3. XRD pattern of as-synthesized Pt@NPC.



Figure S4. XRD pattern of synthesized  $PtP_2@NPC$  before etching process of SiO<sub>2</sub> template. The residual peaks can be assigned to SiO<sub>2</sub>.



Figure S5. Raman spectrum of Pt @NPC.



Figure S6. SEM image of the synthesized SiO<sub>2</sub> spheres.



Figure S7. (a) Nitrogen absorption/desorption curve and (b) the pore size distribution of  $PtP_2@NPC$  with using of SiO<sub>2</sub> spheres as template.



Figure S8. (a) Nitrogen absorption/desorption curve and (b) the pore size distribution of  $PtP_2@NPC$  without using of SiO<sub>2</sub> spheres as template.



**Figure S9.** SEM image of Pt/PtP<sub>2</sub>@NPC after etching of SiO<sub>2</sub> template.



Figure S10. SEM image of  $PtP_2$ @NPC without using SiO<sub>2</sub> as template. We can see the solid and aggregated morphology of the carbon support.



**Figure S11.** SEM image of bubble-like carbon framework after stability test. No deformation after reaction confirms stability of the porous morphology.



Figure S12. (a) and (b) magnified SEM or HAADF-STEM image of  $PtP_2@NPC$  after etching of SiO<sub>2</sub> template



**Figure S13.** SEM image and corresponding particle size distribution plot of Pt/PtP<sub>2</sub> NPs.



Figure S14. XRD data (a) and TEM image (b) of Pt/PtP<sub>2</sub> after durability test



Figure S15. (a) HAADF-STEM imaging of a representative as-synthesized  $PtP_2@NPC$ . (b) STEM line scans crossing the representative as-synthesized  $PtP_2@NPC$ .



**Figure S16.** (a) HAADF-STEM imaging of a representative as-synthesized  $Pt/PtP_2@NPC$ . (b) STEM line scans crossing the representative as-synthesized  $Pt/PtP_2@NPC$ . We can see that Pt content on the surface area (approximately 1 nm) of  $Pt/PtP_2$  is comparatively higher than that of  $PtP_2$  counterpart, confirming the surface concentration of Pt on the surface.



Figure S17. XPS spectra of P (2p) of Pt/PtP<sub>2</sub>@NPC (a) and Pt@NPC (b).



Figure S18. XPS spectra of C (1s) of Pt/PtP<sub>2</sub>@NPC (a) and Pt@NPC (b).



Figure S19. XPS spectra of N (1s) of  $Pt/PtP_2@NPC$  (a) and Pt@NPC (b).



Figure S20. LSV curves of  $PtP_2$  at initial, 2000, 3000 and 4000 circles.



Figure S21. LSV curves of NPC at 400, 800, 1200, 1600 and 2000 rpm with a sweep rate of 10 mV s<sup>-1</sup> in O<sub>2</sub>-saturated 0.1 M HClO<sub>4</sub> solutions. (c) K–L plots of NPC at the potential of 0.55, 0.60, 0.65, 0.70 and 0.75 V (n = 3.65).



Figure S22. CV curves of Pt/PtP<sub>2</sub>@NPC and Pt@NPC before and after different potential cycles.

Sample	$E_{half}$	jecsa,0.90v	j <sub>mass,0.90V</sub>	ECSA $(m^2 a^{-1})$	
	(V vs RHE)	(mA cm <sup>-2</sup> )	$(A mg^{-1}Pt)$	LCSA (III g )	
Pt@NPC	0.872	0.178	0.149	83.89	
PtP2@NPC	0.883	0.438	0.466	106.43	
Pt/PtP2@NPC	0.899	0.508	0.724	142.55	
Pt/C	0.866	0.142	0.098	64.25	

**Table S1.** Comparison of ORR parameters for the Pt@NPC, PtP2@NPC,Pt/PtP2@NPC and commercial Pt/C catalyst in 0.1M HClO4.

Sample	a (Å)	b (Å)	α (°	β (°	γ (°
			)	)	)
Pt	8.41940	8.41940	90.000	90.000	120.0000
PtP <sub>2</sub>	8.12620	8.12620	90.000	90.000	120.0000

**Table S2.** lattice parameters of Pt (111),  $PtP_2(111)$  and  $Pt/PtP_2(111)$ 

Table S3. ORR activity comparasion of core-shell structure in acid environment from	1
previous literatures.	

Sample	Mass activity	Specific	Ref
	(A/mg <sub>Pt</sub> )	activity	
		(mA/cm <sup>2</sup> )	
Core-shell Pt/PtP <sub>2</sub>	0.685	1.35	This work
Core-shell-like Pt <sub>3</sub> Co		0.14	5
Ti-Au@Pt/C	3.0	1.32	6
Pd–Pt Core–Shell	2.66	3.31	7
Co@Pt core-shell	0.17	0.41	8
Pt <sub>ML</sub> /AuNi <sub>0.5</sub> Fe	0.18	1.12	9
Core-shell Ni/Pt	0.49	1.95	10
Core-Shell Pt-Cu		0.45	11

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