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Supporting Information

Sandwich-like multi-scale hierarchical porous carbon with highly hydroxylated surface

for flow batteries

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Fig. S1 Withered platanus leafs in Wutong West Road of Xi'an Jiaotong University.

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Fig. S2 digital photographs of (a) pristine GF and (b) SPHC modified GF.



Fig. S3 N₂ adsorption-desorption isotherms of SPHC-600, SPHC-800 and SPHC-1000.

As shown in Fig. S3, a strong adsorption in low pressure region (P/P₀=0-0.1) and an obvious hysteresis loop in medium pressure region (P/P₀=0.4-0.8) for the SPHC-X are respectively attributed to the appearance of the mesopore and micropore. Similar to some biomass-derived carbons^[18, 19], it is found that the N₂ adsorption-desorption isotherms of SPHC-X are not closed, which may be caused by the destruction of some pore structures in the N₂ adsorption-desorption process.



Fig. S4 XPS spectra of the SPHC-1000.



Fig. S5 Chemical composition ratio of oxygen and carbon atoms for SPHC-600, SPHC-800

and SPHC-1000.



Fig. S6 Chemical composition ratio of SPHC-600, SPHC-800 and SPHC-1000 from C1s spectra.



Fig. S7 (a) XPS spectra of the SPHC-600; XPS analysis and its fitting from high resolution (b)

C1s peak, (c) O1s peak for SPHC-600.



Fig. S8 (a) XPS spectra of the SPHC-800; XPS analysis and its fitting from high resolution (b)

C1s peak, (c) O1s peak for SPHC-800.



Fig. S9 Energy efficiency of VFBs with pristine GF and SPHC electrodes at different current densities.



Fig. S10 Performance comparison of VFBs with SPHC electrode, and the VFB performance in the open literature.

Ref.	Sample	electrode size	membrane	electrolyte	flow rate
			5		

 Table. S1 Experimental parameters from the open literature.

1	Wood-derived carbon	9 cm ²	N115	1.5M	53.4 mL min ⁻¹
2	Lignin-derived carbon	5.0625 cm ²	N116	1.6M	30 mL min ⁻¹
3	CNF-CNT/GF	5 cm^2	N117	2.0M	20 mL min ⁻¹
4	Cocoon-derived carbon	4 cm ²	212	1M	46 mL min ⁻¹
5	Corn-derived carbon	25 cm ²	N115	2.0M	60 mL min ⁻¹
6	NiCoO ₂ /GF	4 cm^2	GN-114C	1M	20 mL min ⁻¹
7	rGO/GF	25 cm ²	N117	3.0M	30 mL min ⁻¹
8	EMIM-coated GF	4 cm^2	N115	1.6M	20 mL min ⁻¹
9	Nb-WO ₃ /GF	10 cm ²	N115	2.0M	20 mL min ⁻¹
10	TiNb ₂ O ₇ -rGO/GF	-	-	0.5M	-
11	P-O-doped GF	25 cm ²	ACS	1.6m	30 mL min ⁻¹
12	P-F-doped GF	12 cm^2	N115	1.5M	20 mL min ⁻¹
13	ZrO ₂ /GF	4 cm^2	N211	1.1M	-
14	Dopamine-coated GF	4 cm ²	N212	1M	46 mL min ⁻¹
15	FeOOH-actived GF	4 cm^2	N115	0.75M	-



Fig. S11 Charge-discharge curves for ZBFBs with SPHC electrode.



Fig. S12 Capacities during cycling test for VFBs with SPHC at 200 mA cm⁻².





Fig. S13 (a) Efficiencies and (b) capacities during cycling test for ZBFBs with SPHC at 80 mA cm⁻².



Fig. S14 digital photographs of SPHC-GF electrodes (a) before and after cycling chargedischarge test.

Computational method

Two kinds of porous computational domains in flow battery were investigated by numerical method. Porous materials in different regions were illustrated in Fig. S14. The simulation was carried at the electrode scale and catalyst scale, respectively. First, simulate the flow of the porous medium that fits the flow channel to obtain the flow velocity in the porous medium. Second, further study the flow in secondary pores in porous media. The basic design parameters and operation conditions are shown in Table 1.

- 1. Assumptions
 - (1)The flow battery operates in steady state
 - (2)Flow in all areas is considered as laminar flow due to the low velocity

(3) The porous domain is considered to be homogeneous.

2. Conservation equations

The Flows in channel was described by Naiver-Stokes equation:

$$\rho(\vec{u} \cdot \nabla)\vec{u} = \nabla \cdot [-pI + \mu(\nabla \vec{u} + (\nabla \vec{u})^T)]$$
$$\rho \nabla \cdot \vec{u} = 0$$

where ρ , μ , u are density, viscosity and velocity respectively

For the flow in porous domain, Naiver-Stokes equation is replaced by the Brinkman equation which takes into account the porosity correction.

$$\frac{1}{\epsilon}\rho(\vec{\mathbf{u}}\cdot\nabla)\vec{u}\frac{1}{\epsilon} = \nabla\cdot\left[-pI + \frac{\mu}{\epsilon}(\nabla\vec{u} + (\nabla\vec{u})^T)\right] - \frac{\mu}{k}\vec{u}$$

where ϵ is porosity and k is permeability.

 k_0 is known at porosity ϵ_0 . When the porosity changes to ϵ , the permeability can be known from the following equation:

$$\mathbf{k} = \mathbf{k}_0 \frac{(1 - \epsilon_0)^2}{\epsilon_0^3} \frac{\epsilon^3}{(1 - \epsilon)^2}$$



Fig. S15 Computational domains of (a) electrode under flow channel and (b) sandwich-like porous structure.

Parameter	Symbols	Value	Ref.
Electrolyte flow rate	Q _{in}	46ml min ⁻¹	Experiment
Graphite porosity	ϵ_{f}	0.9	Experiment
Secondary porosity	$\epsilon_{\rm s}$	0.5	Experiment
Outlet pressure	Pout	1 atm	Experiment
Original fluid permeability	k ₀	$2 * 10^{-10} m^2$	[16]
Original porosity	ϵ_0	0.6	[16]
Fluid density	ρ	$1400 \ \text{kg} \ \text{m}^{-3}$	[17]
Fluid Viscosity	μ	0.0044 Pa s	[17]

Table S2 Modeling parameters related to electrode and electrolyte properties.

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