

# Supporting Information

## **Multi-functional composite nitrogen carrier for ammonia production via chemical looping route**

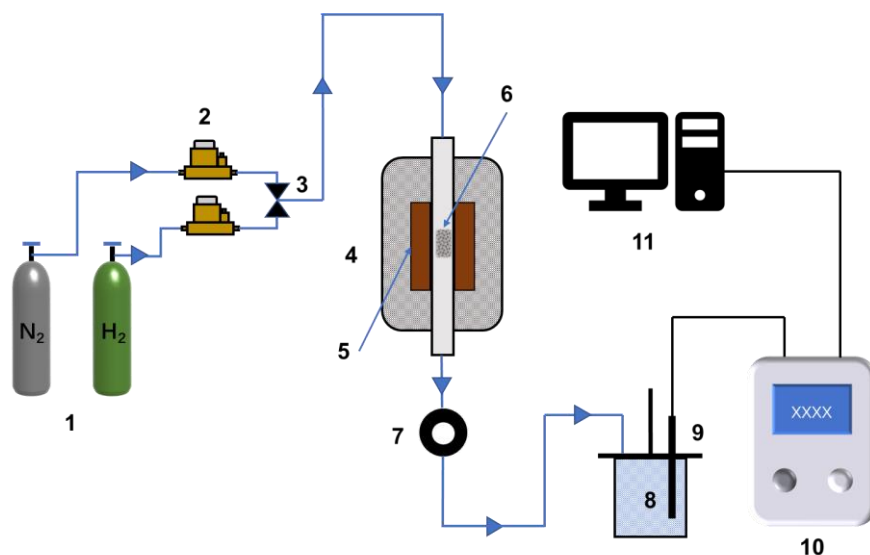
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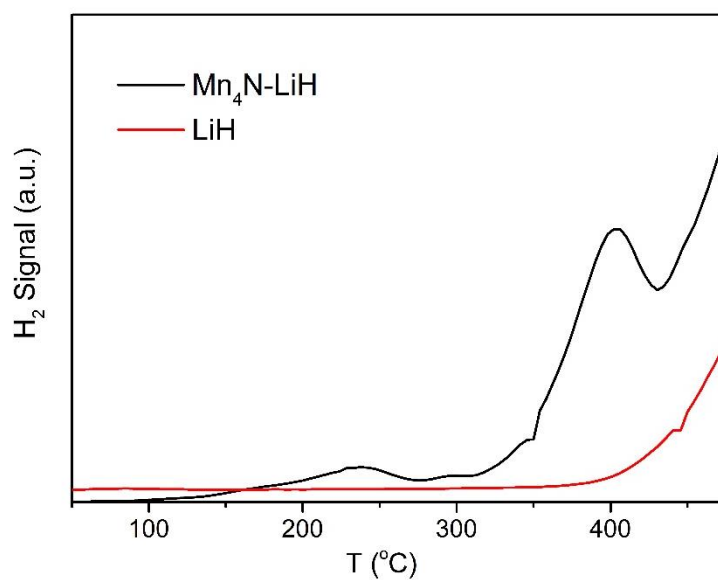
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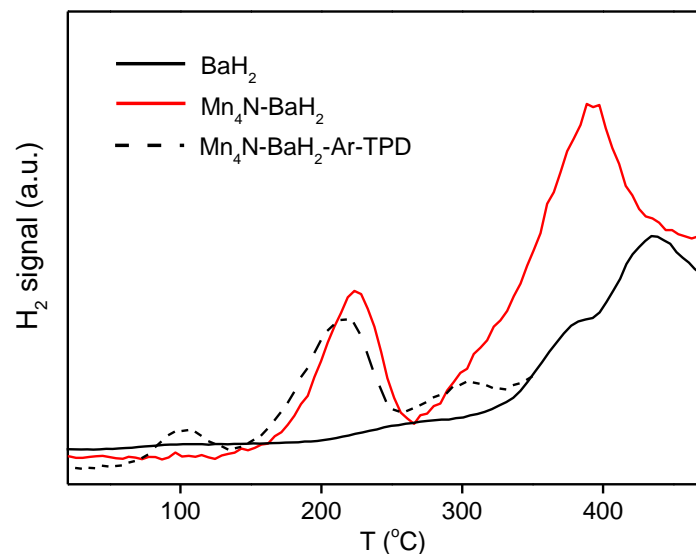
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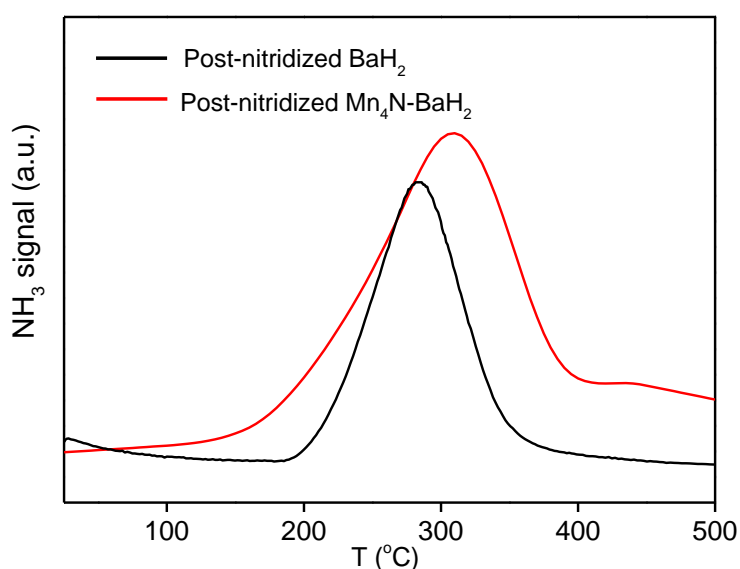
**Fig. S1.** The diagram of evaluation system for chemical looping ammonia synthesis. 1:gas cylinder, 2:mass flowmeter, 3: four-way valve, 4: reactor, 5: heating block, 6: N carrier materials, 7: counterbalance valve, 8: diluted sulfuric acid solution, 9: electrode, 10: conductivity meter, 11: computer.



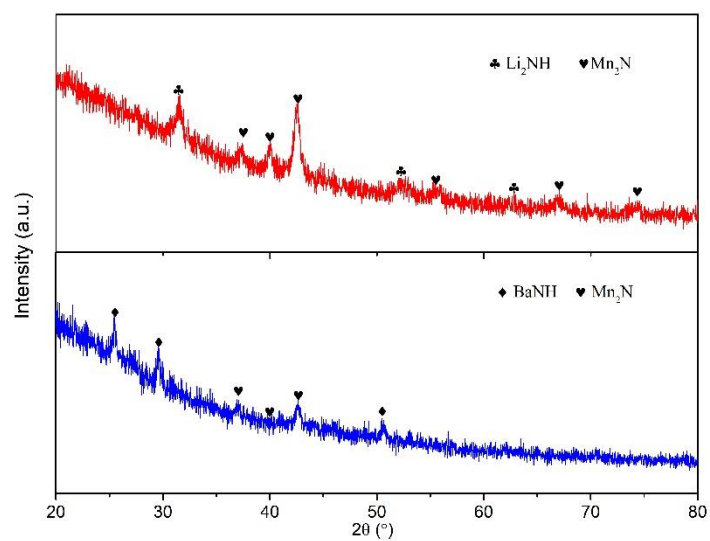
**Fig. S2.**  $N_2$ -TPR-MS profiles of  $LiH$  and  $Mn_4N-LiH$  samples.  $N_2$  flow rate – 30 ml  $min^{-1}$ , ramping rate – 5  $^{\circ}C min^{-1}$ . The data of  $LiH$  was taken from ref. <sup>1</sup>.



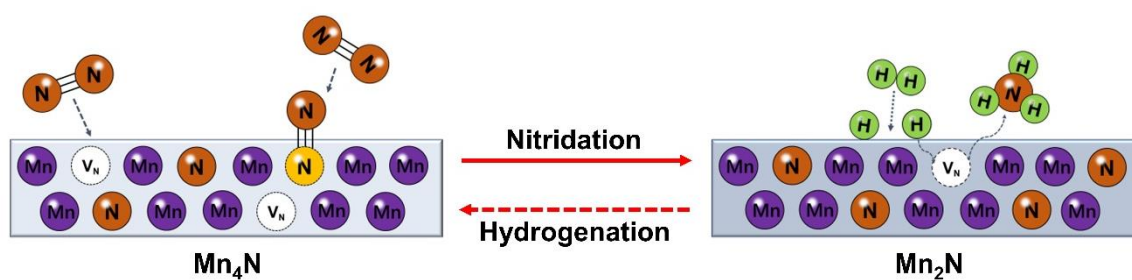
**Fig. S3.**  $\text{N}_2$ -TPR-MS profiles of  $\text{BaH}_2$  and  $\text{Mn}_4\text{N-BaH}_2$  samples (solid lines), and Ar-TPD-MS profile of  $\text{Mn}_4\text{N-BaH}_2$  (dashed line). It is clearly seen that the reaction of  $\text{N}_2$  and  $\text{BaH}_2$  is much easier with the presence of  $\text{Mn}_4\text{N}$ . The  $\text{N}_2$ -TPR-MS profile of  $\text{Mn}_4\text{N-BaH}_2$  shows two apparent  $\text{H}_2$  peaks which are centered around 220 and 390 °C, respectively. By comparing with Ar-TPD-MS profile, it could be concluded that the  $\text{H}_2$  peak at around 220 °C corresponds to the interaction between  $\text{Mn}_4\text{N}$  and  $\text{BaH}_2$ . The peak around 390 °C is mainly due to the fixation of  $\text{N}_2$ , which is at least 50 °C lower than that of  $\text{BaH}_2$ .  $\text{N}_2$  or Ar flow rate – 30 ml  $\text{min}^{-1}$ , ramping rate – 5 °C  $\text{min}^{-1}$ . The data of  $\text{BaH}_2$  were taken from ref. <sup>1</sup>.



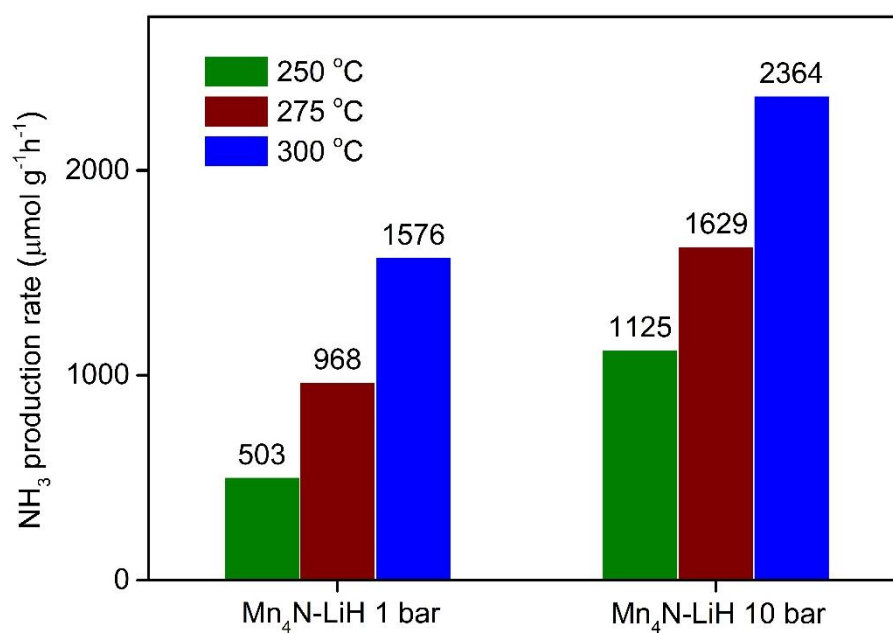
**Fig. S4.**  $\text{H}_2$ -TPR-MS profiles of post-nitridized  $\text{BaH}_2$  (i.e.,  $\text{BaNH}$ ) and  $\text{Mn}_4\text{N-BaH}_2$  samples.  $\text{H}_2$  flow rate – 30 ml  $\text{min}^{-1}$ , ramping rate – 5 °C  $\text{min}^{-1}$ . The data of  $\text{BaH}_2$  was taken from ref. <sup>1</sup>.



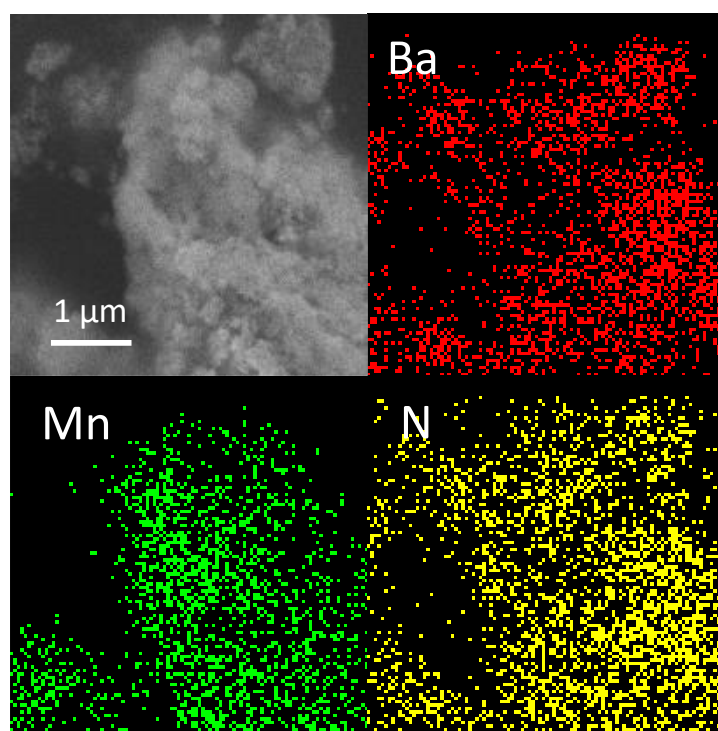
**Fig. S5.** XRD patterns of  $\text{Mn}_4\text{N}$ -LiH and  $\text{Mn}_4\text{N}$ -BaH<sub>2</sub> samples collected after second nitridation step.



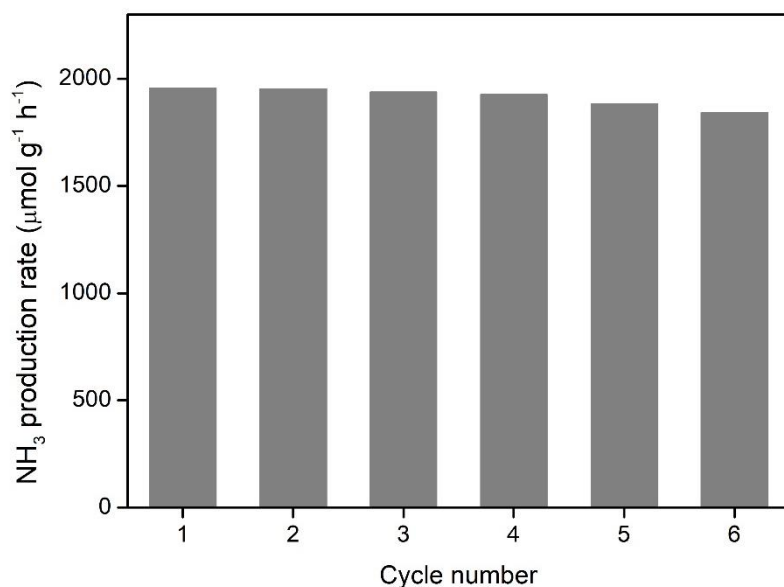
**Fig. S6.** Schematic diagram of CLAS mediated by Mn nitride. The nitrogen vacancies ( $V_N$ ) may function as the active site for the activation and dissociation of  $\text{N}_2$  molecules.



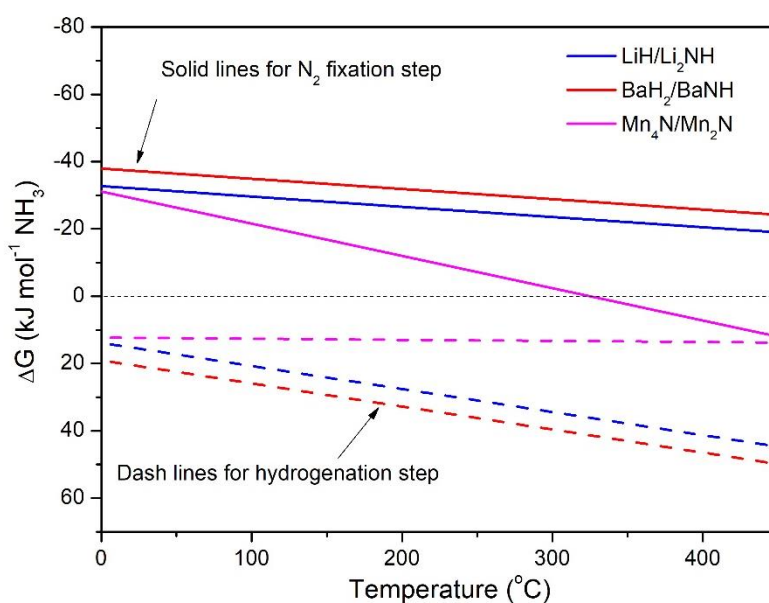
**Fig. S7.**  $\text{NH}_3$  production rates of  $\text{Mn}_4\text{N-LiH}$  under 1 bar and 10 bar of pressure, respectively. Reaction conditions:  $\text{WHSV} = 60000 \text{ ml g}^{-1} \text{ h}^{-1}$ .



**Fig. S8.** SEM and elemental mapping images of the nitridized  $\text{Mn}_4\text{N-BaH}_2$  sample.



**Fig. S9.** Cyclic test of Mn<sub>4</sub>N-BaH<sub>2</sub> sample for chemical looping ammonia synthesis at 275 °C and 1 bar of N<sub>2</sub> and H<sub>2</sub>.



**Fig. S10.** Thermodynamic analyses of N<sub>2</sub> fixation and hydrogenation steps for LiH/Li<sub>2</sub>NH, BaH<sub>2</sub>/BaNH and Mn<sub>4</sub>N/Mn<sub>2</sub>N pairs. The solid lines are the temperature dependences of  $\Delta G$  for N<sub>2</sub> fixation over BaH<sub>2</sub>, LiH and Mn<sub>4</sub>N forming BaNH, Li<sub>2</sub>NH and Mn<sub>2</sub>N, respectively. The dashed lines are the temperature dependences of  $\Delta G$  for hydrogenation of BaNH, Li<sub>2</sub>NH and Mn<sub>2</sub>N. The entropies of solids are not considered. The thermodynamic data used in this figure are given in Tables S1 and S2.

**Table S1.** Thermodynamic calculations of the nitridation of AH and Mn<sub>4</sub>N. The entropies of solids are not considered. The standard enthalpies of formation ( $\Delta_f H^\circ$ ) of Li<sub>2</sub>NH (ref.<sup>2</sup>) and BaNH (ref.<sup>3</sup>) are taken from the literatures. The standard enthalpies of formation of other substances are taken from “NIST Standard Reference Database Number 69”.<sup>4</sup>

Reaction	2LiH	+	1/2N <sub>2</sub>	→	Li <sub>2</sub> NH	+	1/2H <sub>2</sub>	$\Delta_r H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta_r S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
$\Delta_f H^\circ$ (kJ mol <sup>-1</sup> )	-90.5		0		-222		0	-41	---
$S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )	---		191.6		---		130.7	---	-30.5

Reaction	BaH <sub>2</sub>	+	1/2N <sub>2</sub>	→	BaNH	+	1/2H <sub>2</sub>	$\Delta_r H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta_r S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
$\Delta_f H^\circ$ (kJ mol <sup>-1</sup> )	-178.7		0		-224.9		0	-46.2	---
$S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )	---		191.6		---		130.7	---	-30.5

Reaction	Mn <sub>4</sub> N	+	1/2N <sub>2</sub>	→	2Mn <sub>2</sub> N	$\Delta_r H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta_r S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
$\Delta_f H^\circ$ (kJ mol <sup>-1</sup> )	-128.7		0		-93	-57.3	---
$S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )	0		191.6		0	---	-95.8

**Table S2.** Thermodynamic calculations of the hydrogenation of ANH and Mn<sub>2</sub>N. The entropies of solids are not considered.

Reaction	Li <sub>2</sub> NH	+	2H <sub>2</sub>	→	2LiH	+	NH <sub>3</sub>	$\Delta_r H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta_r S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
$\Delta_f H^\circ$ (kJ mol <sup>-1</sup> )	-222		0		-90.5		-45.9	-4.9	---
$S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )	---		130.7		---		192.8	---	-68.6

Reaction	BaNH	+	2H <sub>2</sub>	→	BaH <sub>2</sub>	+	NH <sub>3</sub>	$\Delta_r H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta_r S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
$\Delta_f H^\circ$ (kJ mol <sup>-1</sup> )	-224.9		0		-178.7		-45.9	0.3	---
$S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )	---		130.7		---		192.8	---	-68.6

Reaction	2Mn <sub>2</sub> N	+	3/2H <sub>2</sub>	→	Mn <sub>4</sub> N	+	NH <sub>3</sub>	$\Delta_r H^\circ$ (kJ mol <sup>-1</sup> )	$\Delta_r S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )
$\Delta_f H^\circ$ (kJ mol <sup>-1</sup> )	-93		0		-128.7		-45.9	11.4	---
$S^\circ$ (J mol <sup>-1</sup> K <sup>-1</sup> )	---		130.7		0		192.8	---	-3.25



## References

1. W. Gao, J. Guo, P. Wang, Q. Wang, F. Chang, Q. Pei, W. Zhang, L. Liu and P. Chen, *Nat. Energy*, 2018, **3**, 1067-1075.
2. P. Chen, Z. Xiong, J. Luo, J. Lin and K. L. Tan, *Nature*, 2002, **420**, 302-304.
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