

Supporting Information

A New Multi-Functional Cu(II)-Organic Framework as a Platform for Selective Carbon Dioxide Chemical Fixation and Separation of Organic Dyes

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Table S1. Selected bond lengths (Å) and bond angles (°) for **1**

Complex 1			
Cu(1)-O(2)#2	1.959(3)	O(2)#1-Cu(1)-Cu(1)#1	83.66(14)
Cu(1)-O(2)#1	1.959(3)	O(2)#1-Cu(1)-O(2)#2	89.44(18)
Cu(1)-O(1)	1.962(3)	O(2)#1-Cu(1)-O(1)#3	90.21(14)
Cu(1)-O(1)#3	1.962(3)	O(2)#2-Cu(1)-O(1)	90.21(14)
Cu(1)-O(5)	2.146(8)	O(2)#1-Cu(1)-O(1)	168.22(18)
Cu(1)-O(2)#2	1.959(3)	O(2)#2-Cu(1)-O(1)#3	168.22(18)
O(2)#2-Cu(1)-Cu(1)#1	83.66(14)	O(2)#2-Cu(1)-O(5)	95.3(2)
O(2)#1-Cu(1)-O(5)	95.3(2)	O(1)#3-Cu(1)-O(5)	96.5(2)
O(1)#3-Cu(1)-Cu(1)#1	84.60(14)	O(5)-Cu(1)-Cu(1)#1	178.5(2)
O(1)-Cu(1)-Cu(1)#1	84.60(14)	O(1)-Cu(1)-O(1)#3	87.7(2)
O(1)-Cu(1)-O(5)	96.5(2)		

Symmetrical codes: #1 -x+1/2, -y+3/2, -z+1/2; #2 -x+1/2, y, -z+1/2; #3 x, -y+3/2, z; #4 -y+5/4, -x+5/4, -z+3/4.

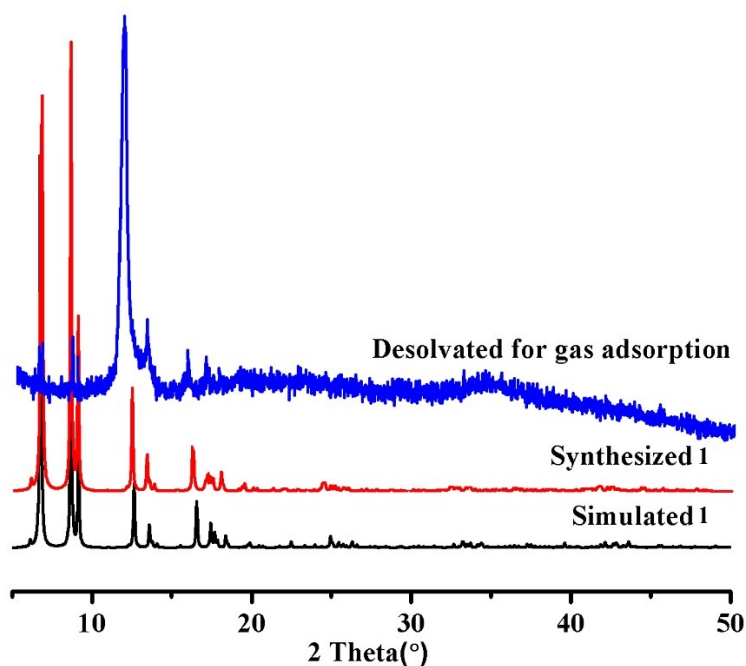


Fig. S1. PXRD patterns of **1** simulated from the X-ray single-crystal structure, experimental samples and desolvated samples (**1a**).

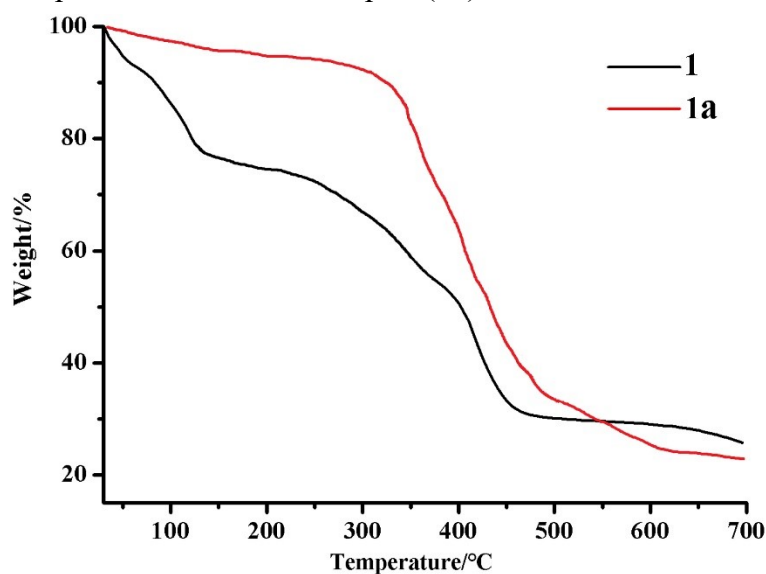


Fig. S2. TGA plots of complex **1** and **1a**.

IAST adsorption selectivity calculation

The experimental isotherm data for pure CO₂ and CH₄ (measured at 273 and 298 K) were fitted using a Langmuir-Freundlich (L-F) model

$$q = \frac{a * b * p^c}{1 + b * p^c}$$

Where q and p are adsorbed amounts and pressures of component i , respectively. The adsorption selectivities for binary mixtures of CO₂/CH₄ at 273 and 298 K and CO₂/N₂ at 298 K., defined by

$$S_{ads} = (q_1 / q_2) / (p_1 / p_2)$$

Where q_i is the amount of i adsorbed and p_i is the partial pressure of i in the mixture.

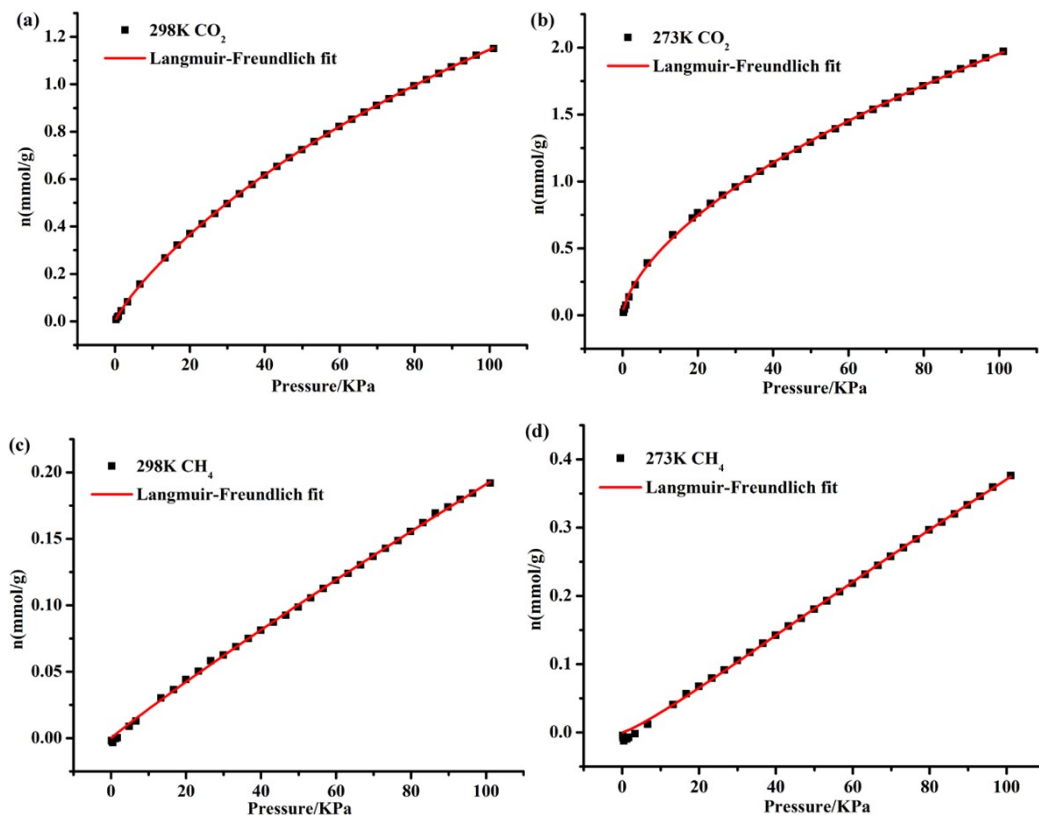


Fig. S3. CO₂ adsorption isotherms of **1a** at 273K with fitting by L-F model: $a = 15.652$, $b = 0.0071$, $c = 0.6510$, $\text{Chi}^2 = 1.75 \times 10^{-4}$, $R^2 = 0.99951$; CO₂ adsorption isotherms of **1a** at 298K with fitting by L-F model: $a = 4.0308$, $b = 0.0076$, $c = 0.8568$, $\text{Chi}^2 = 6.18 \times 10^{-6}$, $R^2 = 0.99995$; CH₄ adsorption isotherms of **1a** at 273K with fitting by L-F model: $a = 2.04506$, $b = 9.47 \times 10^{-4}$, $c = 1.18421$, $\text{Chi}^2 = 2.24 \times 10^{-5}$, $R^2 = 0.99856$; CH₄ adsorption isotherms of **1a** at 298K with fitting by L-F model: $a = 4.18026$, $b = 5.7768$, $c = 0.95923$, $\text{Chi}^2 = 3.24 \times 10^{-6}$, $R^2 = 0.99918$.

Calculation of sorption heat for CO₂ uptake using Virial 2 model

$$\ln P = \ln N + 1/T \sum_{i=0}^m aiN^i + \sum_{i=0}^n biN^i \quad Q_{st} = -R \sum_{i=0}^m aiN^i$$

The above equation was applied to fit the combined CO₂ isotherm data for desolvated **1a** at 273 and 298 K, where P is the pressure, N is the adsorbed amount, T is the temperature, ai and bi are virial coefficients, and m and n are the number of coefficients used to describe the isotherms. Q_{st} is the coverage-dependent enthalpy of adsorption and R is the universal gas constant.

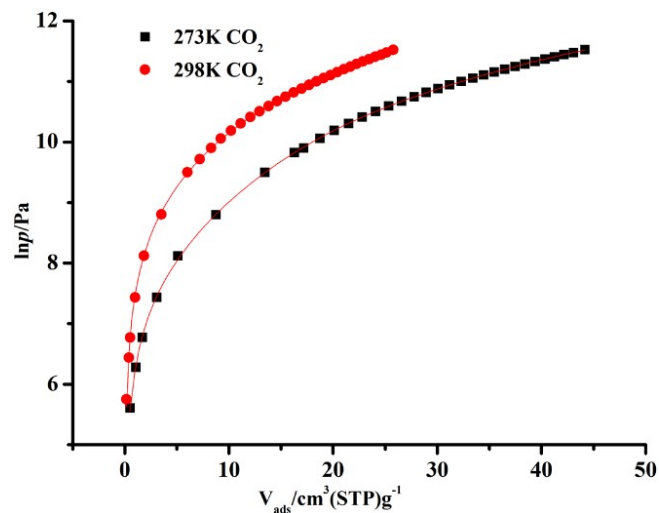


Fig. S4. Virial analysis of the CO₂ adsorption data at 273 and 298 K for **1a**. Fitting results: $a_0 = -3989.33$, $a_1 = -32.37$, $a_2 = 8.24$, $a_3 = -0.24$, $a_4 = 0.0014$, $\chi^2 = 0.00064$, $R^2 = 0.9997$.

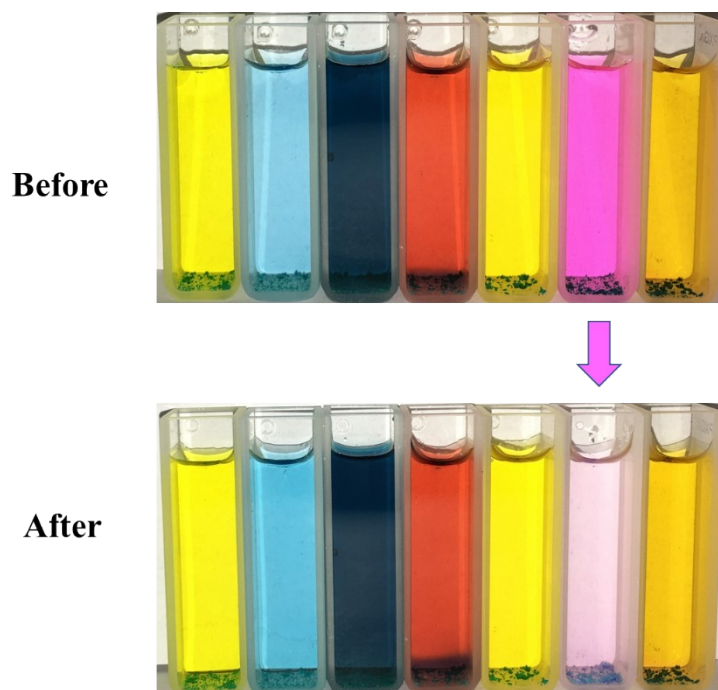


Fig. S5. Color differences of the H₂O solutions with complex **1** in various dyes.

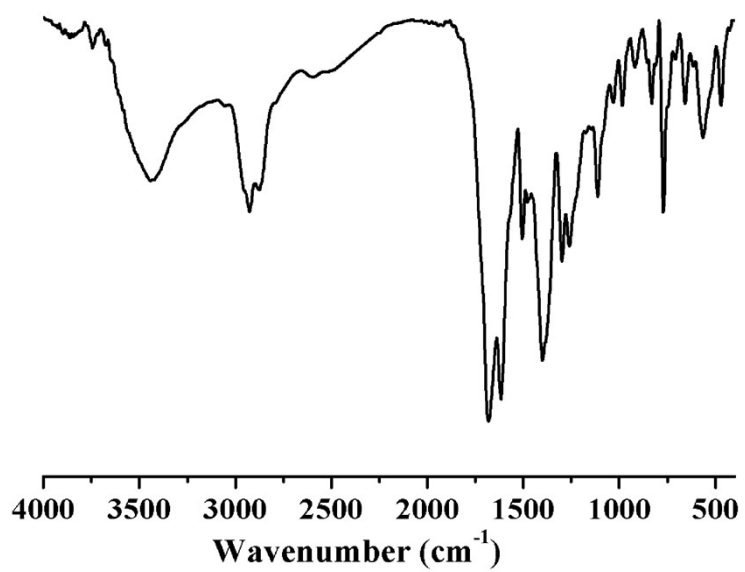


Fig. S6. The FT-IR spectra of complex 1.