Supporting information

Conformality of atomic layer deposition in microchannels: impact of process

parameters on the simulated thickness profile

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Figure S 1. Distribution of the partial pressure of Reactant A within the distance *x*. When  $x < x_t$ , partial pressure of Reactant A decreases linearly (Eq. 8). Linearly extrapolated partial pressure becomes zero at  $x_s$  (Eq. 10). When  $x > x_t$ , different simplification is used to describe the partial pressure (Eq. 9) within the distance. Halfthickness penetration depth is expressed as  $x_p$ .



Figure S 2. Effect of channel height *H* on ALD thickness profile after 1000 cycles was simulated by MATLAB by using the parameter values applied to obtain Fig 4. from Ylilammi et al.<sup>1</sup> Parameter values used: W = 0.1 mm,  $p_{A0} = 100 \text{ Pa}$ ,  $M_A = 0.0749 \text{ kg mol}^{-1}$ ,  $d_A = 5.91 \times 10^{-10} \text{ m}$ ,  $M_I = 0.028 \text{ kg mol}^{-1}$ ,  $d_I = 3.74 \times 10^{-10} \text{ m}$ ,  $p_I = 300 \text{ Pa}$ ,  $q = 5 \text{ nm}^{-2}$ , T = 500 K,  $K = 100 \text{ Pa}^{-1}$ , c = 0.01, and  $gpc_{sat} = 1.06 \times 10^{-10} \text{ m}$ .



Figure S 3. (a) Example of Type 1 normalized thickness profile. (b) Details of the part of panel (a) marked with a green box. Half-thickness penetration depth  $\square_{50\%}$  and slope at half-thickness penetration depth are interpolated linearly between points ( $x_i$ , $y_i$ ), where  $x_i$  equal to or smaller than half-thickness penetration depth, and ( $x_{i-1}$ , $y_{i-1}$ ).



Figure S 4. Illustration of the effect of varying individual parameters on the scaled thickness profile in microchannels, simulated with the Ylilammi et al.<sup>1</sup> model re-implemented in this work. The parameter values used in the simulation are presented in Table 1; the simulation with the baseline values is shown as a solid blue line. The effect of (a) initial partial pressure of the Reactant A  $p_{A0}$ , (b) pulse length of Reactant A  $t_1$ , (c) molecular mass of Reactant A  $M_A$ , (d) film density  $\Box$ , (e) adsorption capacity q, (f) desorption probability  $P_d$ , (g) (lumped) sticking coefficient c, (h) ALD process temperature T, and (i) inert gas pressure  $p_l$ .

Table S 1. The fraction of channel filled depending on varied original channel height *H* with 250 cycles and varied number of cycles *N* within the original channel height of 500 nm, half-thickness penetration depth  $\Box_{50\%}$  (-) and absolute value of the slope at  $\Box_{50\%}$  (-) of scaled thickness profile.<sup>\*</sup>

Н	N (-)	Fraction of channel	□ <sub>□□%</sub> (-)	$\left \square(\square/\square)/\square\square\right _{\square_{\square\square_{\%}}}(-)$	Kn (-
(nm)		filled (-)		22,0	)
100	250	0.4744	206.1	0.0007	38
200	250	0.2372	236.4	0.0015	19
500	250	0.0949	250.1	0.0026	8
1000	250	0.0474	248.8	0.0030	4
2000	250	0.0237	238.7	0.0032	2
2500	250	0.0190	233.5	0.0033	2
4000	250	0.0119	219.1	0.0035	1
500	5	0.0019	261.5	0.0029	8
500	10	0.0038	261.3	0.0029	8
500	20	0.0076	260.8	0.0030	8
500	50	0.0190	259.4	0.0029	8
500	100	0.0380	257.0	0.0029	8
500	250	0.0950	250.1	0.0026	8
500	500	0.1898	238.5	0.0018	8

\*To satisfy the criteria of a difference between the two discretisation points in the y-axis below 3% out of the whole range, 1500 discretisation points were used for the simulation with the varied original channel height from 100 to 1000 nm and varied number of cycles. 2800 discretisation points were used for the simulation with the original channel height over 1000 nm.



Figure S 5. Scaled thickness profile with (a) varying original channel height *H* with 250 cycles and (b) varying number of cycles *N* within the original channel height of 500 nm. (c) Half-thickness penetration depth  $\Box_{50\%}$  (–) and absolute value of the slope at  $\Box_{50\%}$  of the scaled thickness profile in panel (a) against the fraction of channel filled. (d) Half-thickness penetration depth  $\Box_{50\%}$  (–) and absolute value of the slope at  $\Box_{50\%}$  (–) of the scaled thickness profile in panel (b) against the fraction of channel filled. Knudsen number was calculated for each case. Simulation results with baseline condition is marked in blue.



Figure S 6. Scaled thickness profiles simulated in free molecular flow regime (Kn >> 1) by implementing Ylilammi et al.<sup>1</sup> model with varying (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability,

(f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (l) diameter of Reactant A, and (m) film density. Parameter values used, if otherwise stated:  $H = 5 \times 10^{-2} \mu m$ , N = 1,  $t_1 = 0.1 \text{ s}$ ,  $p_{A0} = 50 \text{ Pa}$ ,  $M_A = 0.1 \text{ kg mol}^{-1}$ ,  $d_A = 6.0 \times 10^{-10} \text{ m}$ ,  $M_I = 0.028 \text{ kg mol}^{-1}$ ,  $d_I = 4.0 \times 10^{-10} \text{ m}$ ,  $p_I = 250 \text{ Pa}$ ,  $q = 4 \text{ nm}^{-2}$ ,  $\Box = 3500 \text{ kg m}^{-3}$ ,  $M = 0.050 \text{ kg mol}^{-1}$ ,  $P_d = 0.01 \text{ s}^{-1}$ , and c = 0.01.



Figure S 7. Scaled thickness profiles simulated in transition flow regime ( $Kn \approx 1$ ) by implementing Ylilammi et al.<sup>1</sup> model with varying (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability, (f) adsorption density,

(g)temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (I) diameter of Reactant A, and

(m) film density. Parameter values used, if otherwise stated:  $H = 0.5 \ \mu\text{m}$ , N = 1,  $t_1 = 0.1 \ \text{s}$ ,  $p_{A0} = 500 \ \text{Pa}$ ,  $M_A = 0.1 \ \text{kg mol}^{-1}$ ,  $d_A = 6.0 \times 10^{-10} \ \text{m}$ ,  $M_I = 0.028 \ \text{kg mol}^{-1}$ ,  $d_I = 4.0 \times 10^{-10} \ \text{m}$ ,  $p_I = 2500 \ \text{Pa}$ ,  $q = 4 \ \text{nm}^{-2}$ ,  $\Box = 3500 \ \text{kg m}^{-3}$ ,  $M = 0.050 \ \text{kg mol}^{-1}$ ,  $P_d = 0.01 \ \text{s}^{-1}$ , and c = 0.01.



Figure S 8. Type 1 normalized thickness profiles simulated in free molecular flow regime (Kn >> 1) by implementing Ylilammi et al.<sup>1</sup> model with varying (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability,

(f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (l) diameter of Reactant A, and (m) film density. Parameter values used, if otherwise stated:  $H = 5 \times 10^{-6} \mu m$ , N = 1,  $t_1 = 0.1 \text{ s}$ ,  $p_{A0} = 50 \text{ Pa}$ ,  $M_A = 0.1 \text{ kg mol}^{-1}$ ,  $d_A = 6.0 \times 10^{-10} \text{ m}$ ,  $M_I = 0.028 \text{ kg mol}^{-1}$ ,  $d_I = 4.0 \times 10^{-10} \text{ m}$ ,  $p_I = 250 \text{ Pa}$ ,  $q = 4 \text{ nm}^{-2}$ ,  $\Box = 3500 \text{ kg m}^{-3}$ ,  $M = 0.050 \text{ kg mol}^{-1}$ ,  $P_d = 0.01 \text{ s}^{-1}$ , and c = 0.01.



Figure S 9. Type 1 normalized thickness profiles simulated in transition flow regime (Kn  $\approx$  1) by implementing Ylilammi et al.<sup>1</sup> model with varying (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability,

(f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (l) diameter of Reactant A, and (m) film density. Parameter values used, if otherwise stated:  $H = 0.5 \mu m$ , N = 1,  $t_1 = 0.1 \text{ s}$ ,  $p_{A0} = 500 \text{ Pa}$ ,  $M_A = 0.1 \text{ kg mol}^{-1}$ ,  $d_A = 6.0 \times 10^{-10} \text{ m}$ ,  $M_I = 0.028 \text{ kg mol}^{-1}$ ,  $d_I = 4.0 \times 10^{-10} \text{ m}$ ,  $p_I = 2500 \text{ Pa}$ ,  $q = 4 \text{ nm}^{-2}$ ,  $\Box = 3500 \text{ kg m}^{-3}$ ,  $M = 0.050 \text{ kg mol}^{-1}$ ,  $P_d = 0.01 \text{ s}^{-1}$ , and c = 0.01.



Figure S 10. Half-thickness penetration depth of scaled thickness profile simulated in free molecular flow regime (Kn >> 1) against varied parameters: (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability,

(f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (l) diameter of Reactant A, and (m) film density. The scaled thickness profiles, on which this data is based, are in Figure S 6.



Figure S 11. Absolute value of the slope at half-thickness penetration depth of scaled thickness profile simulated in free molecular flow regime (Kn >> 1) against varied parameters: (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability, (f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A,

(K) molar mass of inert gas, (I) diameter of Reactant A, and (m) film density. The scaled thickness profiles, on which this data is based, are in Figure S 6.



Figure S 12. Absolute value of the slope at half-thickness penetration depth of Type 1 normalized thickness profile simulated in free molecular flow regime (Kn >> 1) against varied parameters: (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability, (f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (l) diameter of Reactant A, and (m) film density. The Type1 normalized thickness profiles, on which this data is based, are in Figure S 8.



Figure S 13. Half-thickness penetration depth of scaled thickness profile simulated in transition flow regime ( $Kn \approx 1$ ) against varied parameters: (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability, (f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (I) diameter of Reactant A, and (m) film density. The scaled thickness profiles, on which this data is based, are in Figure S 7.



Figure S 14. Absolute value of the slope at half-thickness penetration depth of scaled thickness profile simulated in transition flow regime ( $Kn \approx 1$ ) against varied parameters: (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability, (f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A, (K) molar mass of inert gas, (l) diameter of Reactant A, and (m) film density. The scaled thickness profiles, on which this data is based, are in Figure S 7.



Figure S 15. Absolute value of the slope at half-thickness penetration depth of Type 1 normalized thickness profile simulated in transition flow regime ( $Kn \approx 1$ ) against varied parameters: (a) original channel height, (b) initial partial pressure of Reactant A, (c) pulse length, (d) (lumped) sticking coefficient, (e) desorption probability, (f) adsorption density, (g) temperature, (h) total pressure, (i) ratio between initial partial pressure of Reactant A to total pressure, (j) molar mass of Reactant A,

(K) molar mass of inert gas, (I) diameter of Reactant A, and (m) film density. The Type 1 normalized thickness profiles, on which this data is based, are in Figure S 9.



Figure S 16. Type 1 normalized thickness profiles simulated in a wide microchannel in free molecular flow with varying (a) different process temperature, (b) molar mass of reactant A, and (c) sticking coefficient. Sticking coefficient values back-extracted from these thickness profiles by the slope method<sup>2</sup> are listed in Table 3. Parameters used if not otherwise stated:  $H = 0.2 \mu m$ , N = 1, W = 10 mm, T = 523.15 K,  $t_1 = 2 \text{ s}$ ,  $p_{A0} = 10 \text{ Pa}$ ,  $M_A = 0.1 \text{ kg mol}^{-1}$ ,  $d_A = 600 \text{ pm}$ ,  $M_1 = 0.028 \text{ kg mol}^{-1}$ ,  $d_1 = 374$ 

pm,  $p_1 = 50$  Pa, q = 4 nm<sup>-2</sup>,  $\Box = 3500$  kg m<sup>-3</sup>, M = 0.050 kg mol<sup>-1</sup>,  $P_d = 10^{-5}$  s<sup>-1</sup>, and c = 0.01.



Figure S 17. Evolution of (left) partial pressure of Reactant A and (right) surface coverage in HAR was simulated by Ylilammi et al.<sup>1</sup> model (Model A) and by Yanguas-Gil and Elam<sup>3</sup> model (Model B).

Simulations were made with varied sticking coefficients and other parameters as the baseline conditions defined in Table 1 of the main manuscript. In the diffusion-limited regime (sticking coefficients  $10^{-2}$  and  $10^{-4}$ ), the two models gave rather similar results, while in the reaction-limited case (sticking coefficient  $10^{-6}$ ) the results differed significantly. The reason behind the differences is in the specific treatment of the partial pressure  $p_A$  in Model A, which is poorly applicable for simulations in the reaction-limited regime. According to a reference,<sup>3</sup> the process is in reaction- limited regime when Thiele modulus  $h_T << 1$ . In this work, the case with the sticking coefficient of  $10^{-6}$  was clearly in the reaction-limited regime although Thiele modulus value was not far from 1 (ca. 0.9).

## References

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