

## Supporting Information

### Catalytic transformations of citral in a continuous flow over bifunctional Ru-MCM-41 extrudates

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## EXPERIMENTAL

### Definitions

Normalized time is defined as follows:

$$t_N = t \cdot m_{cat} \cdot \frac{c_{Ru} \cdot D_{Ru}}{Mr_{Ru}} [h \cdot mol_{Ru(surface)}] \quad (1)$$

where  $t$  is reaction time,  $m_{cat}$  is mass of catalyst,  $c_{Ru}$  is the concentration of Ru in the entire catalyst volume,  $D_{Ru}$  is Ru distribution and  $Mr_{Ru}$  is the molecular weight of ruthenium.

The liquid phase mass balance closure is defined as a sum of the concentration of citronellal at a certain time and the concentrations of products visible in the GC chromatogram divided by the initial concentration of citronellal, denoted as MB:<sup>1-3</sup>

$$MB (\%) = \frac{\Sigma m_i}{\Sigma m_0} * 100 \quad (2)$$

$\Sigma m_i$  = sum of mass concentration of all components at different sampling times

$\Sigma m_0$  = sum of mass concentration of all components at time = 0

The reaction rates ( $r$ ) and turnover frequency (TOF) are calculated as follows:

$$r_{extrudates} = \frac{\Delta \dot{n}}{m_{cat}} \left[ \frac{mol}{s \cdot g} \right] \quad (3)$$

$$r_{powder\ catalyst} = \frac{\Delta n}{\Delta t \cdot m_{cat}} \left[ \frac{mol}{s \cdot g} \right] \quad (4)$$

$$TOF_{extrudates} = \frac{\dot{n}_{in} - \dot{n}_{out}}{n_{metal(surface)}} \left[ \frac{1}{s} \right] \quad (5)$$

$$TOF_{powder\ catalyst} = \frac{\Delta n \cdot V_l}{\Delta t \cdot n_{metal(surface)}} \left[ \frac{1}{s} \right] \quad (6)$$

where  $r_{extrudates}$  is obtained over extrudates in trickle-bed reactor and  $r_{powder\ catalyst}$  is obtained over powder catalyst in a batch reactor,  $\Delta \dot{n}$  denotes the change in molar flow rate of the feed at time zero and time  $t$  in a trickle bed reactor,  $\Delta n / \Delta t$  reacted moles per time interval  $\Delta t$  in a batch

reactor,  $m_{\text{cat}}$  is catalyst mass,  $V_l$  is liquid volume and  $n_{\text{metal}(\text{surface})}$  is moles of exposed measured metal.<sup>1-4</sup> Cumulative reaction rate and turn-over-frequency ( $r_{\text{cum}}$ ,  $\text{TOF}_{\text{cum}}$ ) at time  $t$  was calculated as differences to time zero, while the instantaneous reaction rate and turn-over-frequency ( $r_{\text{inst}}$ ,  $\text{TOF}_{\text{inst}}$ ) at time  $t$  were related to time  $t-1$ .

## RESULTS AND DISCUSSION

### Catalyst characterization results

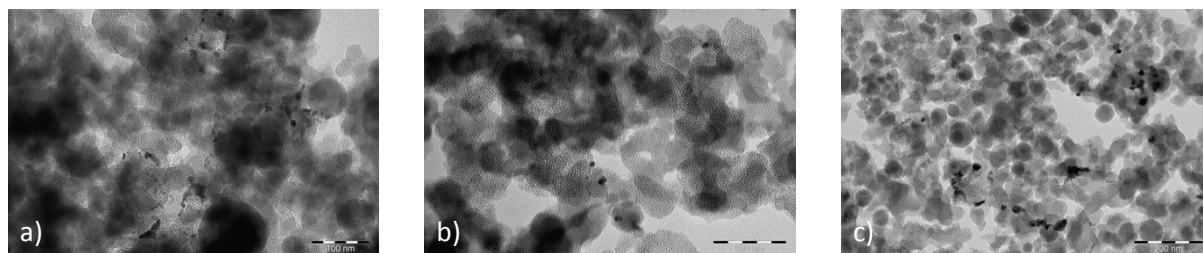


Figure S1. TEM images of powder catalysts: a) Ru/(H-MCM-41+Bindzil) (**P-B**);<sup>3</sup> b) (Ru/Bindzil)+H-MCM-41 (**P-C**); c) (Ru/H-MCM-41)+Bindzil (**P-D**).

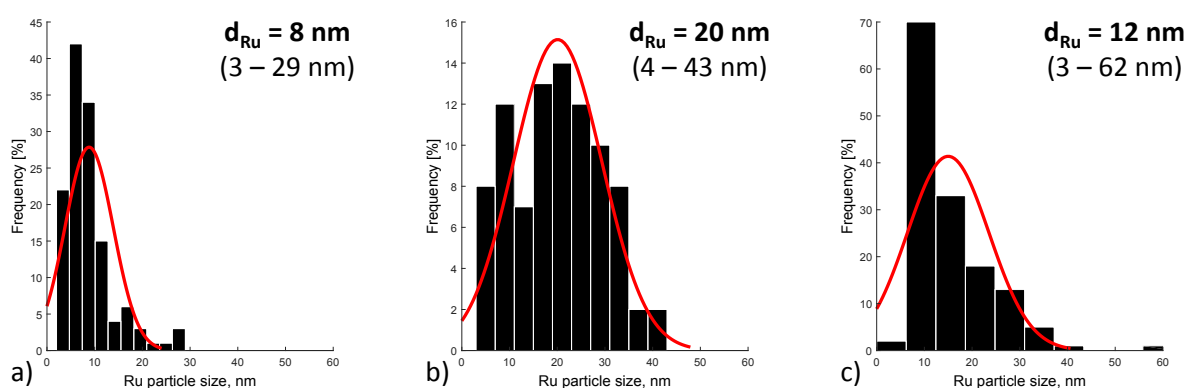


Figure S2. Ru particle size distribution of powder catalysts: a) Ru/(H-MCM-41+Bindzil) (**P-B**);<sup>3</sup> b) (Ru/Bindzil)+H-MCM-41 (**P-C**); c) (Ru/H-MCM-41)+Bindzil (**P-D**).

Table S1. Brønsted and Lewis acid sites. In parenthesis data for theoretical value calculated from the contribution of individual components.

Type	Brønsted acidity, $\mu\text{mol/g}$				Lewis acidity, $\mu\text{mol/g}$				Total acidity $\mu\text{mol/g}$
	weak	medium	strong	$\Sigma$	weak	medium	strong	$\Sigma$	
P <sup>3</sup>	41	19	24	84	20	14	21	56	140
Z	0	0	1	1	1	0	0	1	2
P* <sup>3</sup>	29 (29)	11 (13)	1 (17)	41 (59)	28 (14)	6 (10)	1 (15)	34 (40)	75 (99)
P-B <sup>3</sup>	18	4	0	21	41	3	0	44	65
P-C	37	0	0	37	32	0	0	32	69
P-D	28	0	0	28	15	0	0	15	44
E-A <sup>3</sup>	36	1	0	37	22	2	0	24	60
E-B <sup>3</sup>	31	0	0	31	21	0	0	21	51
E-C <sup>3</sup>	32	3	0	35	23	2	0	25	60

E-D <sup>3</sup>	29	0	0	29	22	0	0	22	52
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P – powder catalyst; E - extrudates; **P-B** – Ru/(H-MCM-41+Bindzil); **P-C** – (Ru/Bindzil)+H-MCM-41; **P-D** – (Ru/H-MCM-41)+Bindzil; **E-A** – Ru/(H-MCM-41+Bindzil) *post* synthesis; **E-B** – Ru/(H-MCM-41+Bindzil) *in-situ* synthesis; **E-C** – (Ru/Bindzil)+H-MCM-41; **E-D** – (Ru/H-MCM-41)+Bindzil.

## Catalytic results

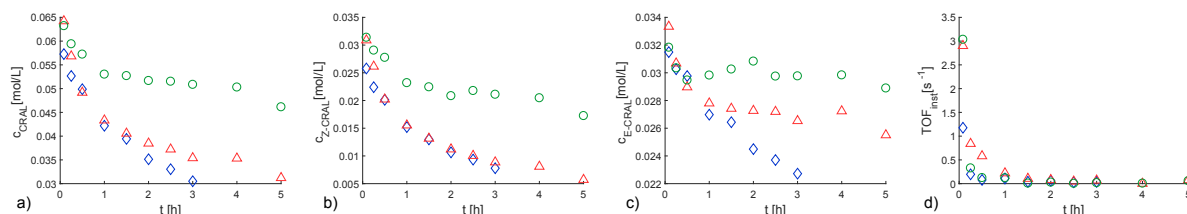


Figure S3. Concentration profile as a function of reaction time: a) racemic mixture of citral, b) Z-citral, c) E-citral; d) Instantaneous turn-over-frequency as a function of reaction time. Legend: Ru/(H-MCM-41+Bindzil) (**P-B**, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (**P-C**, red triangle), Ru/(H-MCM-41)+Bindzil (**P-D**, green circle). Conditions: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst.

Table S2. Citral transformation to menthol over Ru catalysts. Legend: t, TOS – reaction time, time-on-stream; X – conversion of citral; r – cumulative reaction rate; TOF – cumulative turnover frequency; η – effectiveness factor; PCU – percentage of catalyst utilization, <sup>0</sup> the initial time for powder catalyst and extrudates was 5 min and 30 min, respectively. Conditions for the batch experiment over the powder catalysts: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst. Conditions for the continuous experiment over the extrudates: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.

Catalyst	t, TOS*	X	r <sup>0</sup> <sub>cum</sub>	TOF <sup>0</sup> <sub>cum</sub>	η <sup>0</sup>	r <sub>cum</sub>	TOF <sub>cum</sub>	η	PCU
-	h	%	mol/s/g	l/s	-	mol/s/g	l/s	-	%
P-B	3	59	2.53·10 <sup>-5</sup>	1.449	-	1.81·10 <sup>-6</sup>	0.104	-	-
P-C	5	58	1.52·10 <sup>-5</sup>	2.329	-	1.61·10 <sup>-6**</sup>	0.247**	-	-
P-D	5	40	2.10·10 <sup>-5</sup>	2.445	-	1.09·10 <sup>-6**</sup>	0.127**	-	-
E-A	0.2, 3*	70	4.36·10 <sup>-7</sup>	0.025	0.02	3.62·10 <sup>-7</sup>	0.021	0.20	19.8
E-B	0.2, 3*	66	4.93·10 <sup>-7</sup>	0.056	0.02	3.26·10 <sup>-7</sup>	0.037	0.18	35.8
E-C	0.2, 3*	66	4.65·10 <sup>-7</sup>	0.056	0.03	3.08·10 <sup>-7</sup>	0.037	0.19	15.0
E-D	0.2, 3*	64	4.38·10 <sup>-7</sup>	0.037	0.02	3.15·10 <sup>-7</sup>	0.027	0.29	21.1

\*\*at 3 h of reaction time, P – powder catalyst; E - extrudates; P-B – Ru/(H-MCM-41+Bindzil); P-C – (Ru/Bindzil)+H-MCM-41; P-D – (Ru/H-MCM-41)+Bindzil; E-A – Ru/(H-MCM-41+Bindzil) *post* synthesis; E-B – Ru/(H-MCM-41+Bindzil) *in-situ* synthesis; E-C – (Ru/Bindzil)+H-MCM-41; E-D – (Ru/H-MCM-41)+Bindzil.

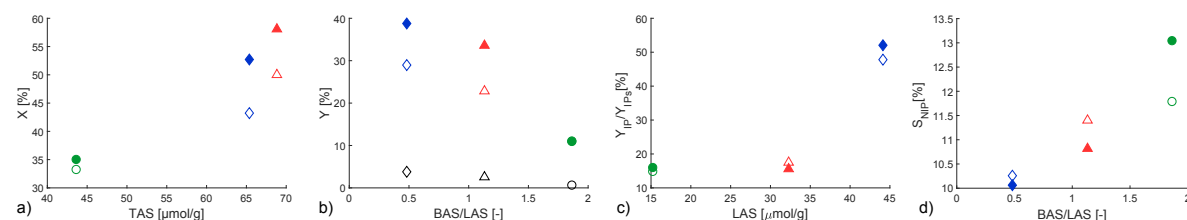


Figure S4. a) Citral conversion as a function of total acidity, b) total yield as a function of Brønsted to Lewis acid sites ratio, c) stereoselectivity of isopulegol as a function of Lewis acidity, d) Selectivity of neoisopulegol as a function of Brønsted to Lewis acid sites ratio. Legend: Ru/(H-MCM-41+Bindzil) (**P-B**, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (**P-C**, red triangle), Ru/(H-MCM-41)+Bindzil (**P-D**, green circle); at normalized time

of  $1.5 \cdot 10^{-6} \text{ h}\cdot\text{mol}_{\text{Ru}(\text{surface})}$  (black open symbols),  $3.5 \cdot 10^{-6} \text{ h}\cdot\text{mol}_{\text{Ru}(\text{surface})}$  (open symbols),  $7 \cdot 10^{-6} \text{ h}\cdot\text{mol}_{\text{Ru}(\text{surface})}$  (filled symbols). Conditions: 70 °C, 10 bar of  $\text{H}_2$ , 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst.

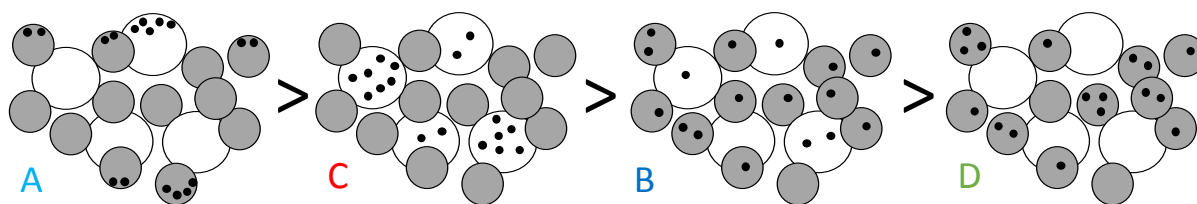


Figure S5. A schematic picture of the catalysts employed in this study, showing different distances between the metal and acid sites: a) A – Ru/(H-MCM-41+bindzil-50/80), post synthesis; b) C – (Ru/bindzil-50/80)+H-MCM-41, in-situ synthesis; c) B – Ru/(H-MCM-41+bindzil-50/80), in-situ synthesis; d) D – (Ru/H-MCM-41)+bindzil-50/80, in-situ synthesis. Legend: H-MCM-41 (grey circle), bindzil-50/80 (white circle), Ru (black dots) <sup>3,5</sup>.

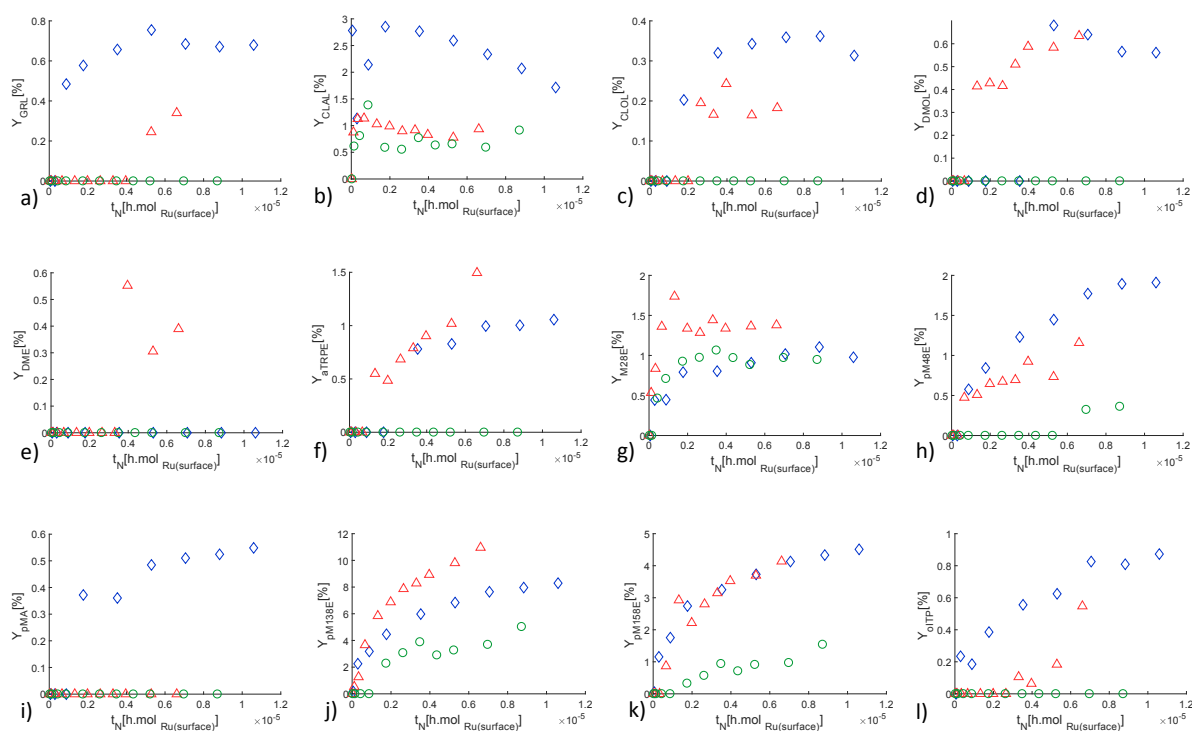


Figure S6. Product distribution in citral transformation to menthol over powder catalyst in a batch reactor: a) geraniol, b) citronellal, c) citronellol, d) 3,7-dimethyloctan-1-ol, e) 2,6-dimethylcyclohexane, f)  $\alpha$ -terpinolene, g) metha-2,8-diene, h) p-menth-4(8)-ene, i) p-menthane, j) p-mentha-1,3,8-triene, k) p-mentha-1,5,8-triene, l) o-isopropenyltoluene. Legend: Ru/(H-MCM-41+Bindzil) (**P-B**, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (**P-C**, red triangle), Ru/(H-MCM-41)+Bindzil (**P-D**, green circle). Conditions: 70 °C, 10 bar of  $\text{H}_2$ , 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst.

Table S3. Stereoselectivity to isopulegol isomers in menthol synthesis from citral. Legend: isopulegol (IP), neoisopulegol (NIP), isoisopulegol (IIP), neoisopulegol (NIP). Conditions for the batch experiment over the powder catalysts: 70 °C, 10 bar of  $\text{H}_2$ , 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst. Conditions for the continuous experiment over the extrudates: 70 °C, 10 bar of  $\text{H}_2$ , 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.

	t, TOS*	Y <sub>IPs</sub>	Y <sub>IP</sub> /Y <sub>IPs</sub>	Y <sub>NIP</sub> /Y <sub>IPs</sub>	Y <sub>IIP</sub> /Y <sub>IPs</sub>	Y <sub>NIIP</sub> /Y <sub>IPs</sub>
	h		%			
P-B	3	13.0	54	33	14	0
P-C	5	5.4	15	67	19	0
P-D	5	3.9	15	46	21	18

E-A	0.2, 3*	6.7	55	36	9	0
E-B	0.2, 3*	4.4	45	39	14	0
E-C	0.2, 3*	3.6	33	47	19	0
E-D	0.2, 3*	4.5	42	42	16	0

P – powder catalyst; E - extrudates; P-B – Ru/(H-MCM-41+Bindzil); P-C – (Ru/Bindzil)+H-MCM-41; P-D – (Ru/H-MCM-41)+Bindzil; E-A – Ru/(H-MCM-41+Bindzil) *post* synthesis; E-B – Ru/(H-MCM-41+Bindzil) *in-situ* synthesis; E-C – (Ru/Bindzil)+H-MCM-41; E-D – (Ru/H-MCM-41)+Bindzil.

Table S4. Stereoselectivity to menthol isomers in menthol synthesis from citral. Legend: menthol (ME), neomenthol (NME), isomenthol (IME), neoisomenthol (NIME). Conditions for the batch experiment over the powder catalysts: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst. Conditions for the continuous experiment over the extrudates: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.

	t, TOS*	Y <sub>MEs</sub>	Y <sub>ME</sub> /Y <sub>MEs</sub>	Y <sub>NME</sub> /Y <sub>MEs</sub>	Y <sub>IME</sub> /Y <sub>MEs</sub>	Y <sub>NIME</sub> /Y <sub>MEs</sub>
	h	%				
P-B	3	1.8	22	0	44	33
P-C	5	2.8	21	0	61	21
P-D	5	1.0	0	0	100	0
E-A	0.2, 3*	9.1	66	23	0	12
E-B	0.2, 3*	2.9	66	14	0	21
E-C	0.2, 3*	1.3	62	0	38	0
E-D	0.2, 3*	2.3	52	0	22	26

P – powder catalyst; E - extrudates; P-B – Ru/(H-MCM-41+Bindzil); P-C – (Ru/Bindzil)+H-MCM-41; P-D – (Ru/H-MCM-41)+Bindzil; E-A – Ru/(H-MCM-41+Bindzil) *post* synthesis; E-B – Ru/(H-MCM-41+Bindzil) *in-situ* synthesis; E-C – (Ru/Bindzil)+H-MCM-41; E-D – (Ru/H-MCM-41)+Bindzil.

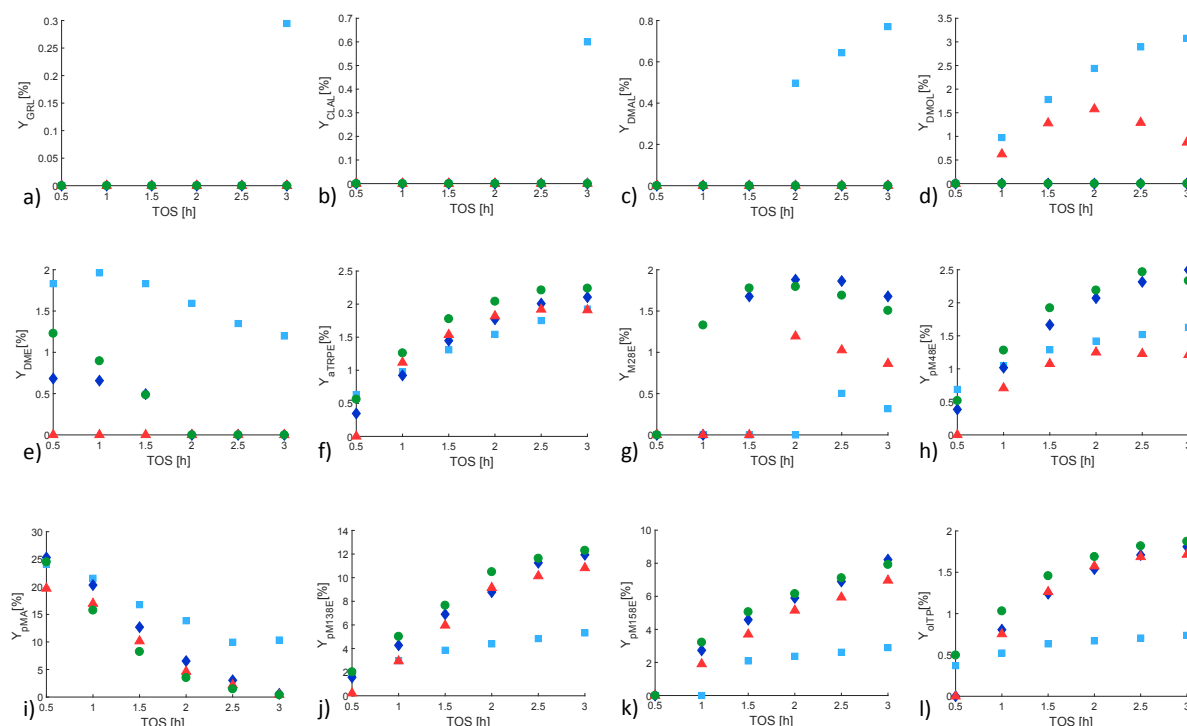


Figure S7. Product distribution in citral transformation to menthol over extrudates in a trickle-bed reactor: a) geraniol, b) citronellal, c) 3,7-dimethyloctanal, d) 3,7-dimethyloctan-1-ol, e) 2,6-dimethyloctane, f)  $\alpha$ -terpinolene, g) mentha-2,8-diene, h) *p*-menth-4(8)-ene, i) *p*-menthane, j) *p*-mentha-1,3,8-triene, k) *p*-mentha-1,5,8-triene, l) *o*-isopropenyltoluene. Legend: Ru/(H-MCM-41+Bindzil), *post* synthesis (E-A, light blue square), Ru/(H-MCM-41+Bindzil), *in-situ* synthesis (E-B, dark blue diamond), (Ru/Bindzil)+H-MCM-41 (E-C, red triangle), Ru/(H-

*MCM-41)+Bindzil (E-D, green circle). Conditions: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.*

Tables 5 and 6 present the collected catalytic results of citral transformation from both the batch and trickle-bed reactor over Ru-powder catalysts (0.2 g) and extrudates (1 g) with controlled metal location, respectively, under 70 °C, 10 bar with 0.086 M of the initial citral (Z-/E-CRAL = 1) concentration in cyclohexane.

*Table S5. Citral transformation to menthol over Ru catalysts. Legend: t – reaction time, TOS – time-on-stream, X – conversion, MB – liquid phase mass balance closure, Y – total yield, Y<sub>ACP</sub> – yield of acyclic hydrogenation products, Y<sub>DFP</sub> – yield of defunctionalization products, Y<sub>CP</sub> – yield of cyclic products (MES+IPs+DFP), Y<sub>DM</sub> – yield of dimeric ethers and heavy components, Y<sub>MES</sub> – yield of menthols, Y<sub>IPs</sub> – yield of isopulegols. Conditions for the batch experiment over the powder catalysts: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst. Conditions for the continuous experiment over the extrudates: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.*

Cat.	t, TOS*	X	MB	Y	Y <sub>ACP</sub>	Y <sub>DFP</sub>	Y <sub>CP</sub>	Y <sub>DM</sub>	Y <sub>MES</sub>	Y <sub>IPs</sub>	CP/ACP	IP/ME	Z-/E-CRAL
-	<i>h</i>	%									-		
P-B	3.0	59	81	40	3.3	22.3	37.1	0.0	1.8	13.0	11	7.2	0.34
P-C	5.0	58	76	34	3.8	21.5	29.7	0.0	2.8	5.4	8	1.9	0.22
P-D	5.0	40	74	14	0.9	8.4	13.3	0.0	1.0	3.9	15	3.9	0.60
E-A	0.2, 3*	70	79	49	5.9	27.2	43.0	0.0	9.1	6.7	7	0.7	0.64
E-B	0.2, 3*	66	82	48	0.0	31.6	38.9	9.4	2.9	4.4	-	1.5	0.35
E-C	0.2, 3*	66	65	32	0.9	25.7	30.6	0.0	1.3	3.6	34	2.8	0.28
E-D	0.2, 3*	64	78	42	0.0	31.3	38.1	4.4	2.3	4.5	-	2.0	0.31

P – powder catalyst; E – extrudates; P-B – Ru/(H-MCM-41+Bindzil); P-C – (Ru/Bindzil)+H-MCM-41; P-D – (Ru/H-MCM-41)+Bindzil; E-A – Ru/(H-MCM-41+Bindzil) *post* synthesis; E-B – Ru/(H-MCM-41+Bindzil) *in-situ* synthesis; E-C – (Ru/Bindzil)+H-MCM-41; E-D – (Ru/H-MCM-41)+Bindzil.

*Table S6. Citral transformation to menthol over Ru catalysts. Legend: t – reaction time, TOS – time-on-stream, ACP – acyclic hydrogenation products, DFP – defunctionalization products, Y<sub>GRL</sub> – yield of geraniol, Y<sub>CLAL</sub> – yield of citronellal, Y<sub>DMAL</sub> – yield of 3,7-dimethyloctanal, Y<sub>CLOL</sub> – yield of citronellol, Y<sub>DMOL</sub> – yield of 3,7-dimethyloctan-1-ol, Y<sub>DME</sub> – 2,6-dimethyloctane, Y<sub>αTRPE</sub> – α-terpiolene, Y<sub>LMN</sub> – yield of limonene, Y<sub>M28E</sub> – yield of mentha-2,8-diene, Y<sub>pM48E</sub> – yield of p-mentha-4(8)-ene, Y<sub>pMA</sub> – yield of p-menthane, Y<sub>pM138E</sub> – yield of p-mentha-1,3,8-triene, Y<sub>pM158E</sub> – yield of p-mentha-1,5,8-triene, Y<sub>oC</sub> – yield of o-cymene, Y<sub>oIPT</sub> – yield of o-isopropenyltoluene. Conditions for the batch experiment over the powder catalysts: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst. Conditions for the continuous experiment over the extrudates: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.*

Cat.	t, TOS*	ACP						DFP								
		Y <sub>GRL</sub>	Y <sub>CLAL</sub>	Y <sub>DMAL</sub>	Y <sub>CLOL</sub>	Y <sub>DMOL</sub>	Y <sub>DME</sub>	Y <sub>αTRPE</sub>	Y <sub>LMN</sub>	Y <sub>M28E</sub>	Y <sub>pM48E</sub>	Y <sub>pMA</sub>	Y <sub>pM138E</sub>	Y <sub>pM158E</sub>	Y <sub>oC</sub>	Y <sub>oIPT</sub>
-	<i>h</i>	%														
P-B	3.0	0.7	1.7	0.0	0.3	0.6	0.0	1.1	0.0	1.0	1.9	0.5	8.3	4.5	2.4	0.9
P-C	5.0	0.3	0.9	0.0	0.2	0.6	0.4	1.5	0.0	1.4	1.2	0.0	11.0	4.1	0.0	0.5

P-D	5.0	0.0	0.9	0.0	0.0	0.0	0.0	0.0	0.0	0.9	0.4	0.0	5.0	1.5	0.0	0.0
E-A	0.2, 3*	0.3	0.6	0.8	0.0	3.1	1.2	1.9	1.9	0.3	1.6	10.4	5.3	2.9	1.8	0.7
E-B	0.2, 3*	0.0	0.0	0.0	0.0	0.0	0.0	2.1	0.0	1.7	2.5	0.6	11.9	8.2	2.2	1.8
E-C	0.2, 3*	0.0	0.0	0.0	0.0	0.9	0.0	1.9	0.0	0.9	1.2	0.4	10.8	7.0	1.3	1.7
E-D	0.2, 3*	0.0	0.0	0.0	0.0	0.0	0.0	2.2	0.0	1.5	2.3	0.4	12.3	7.9	2.1	1.9

P – powder catalyst; E - extrudates; P-B – Ru/(H-MCM-41+Bindzil); P-C – (Ru/Bindzil)+H-MCM-41; P-D – (Ru/H-MCM-41)+Bindzil; E-A – Ru/(H-MCM-41+Bindzil) *post* synthesis; E-B – Ru/(H-MCM-41+Bindzil) *in-situ* synthesis; E-C – (Ru/Bindzil)+H-MCM-41; E-D – (Ru/H-MCM-41)+Bindzil.



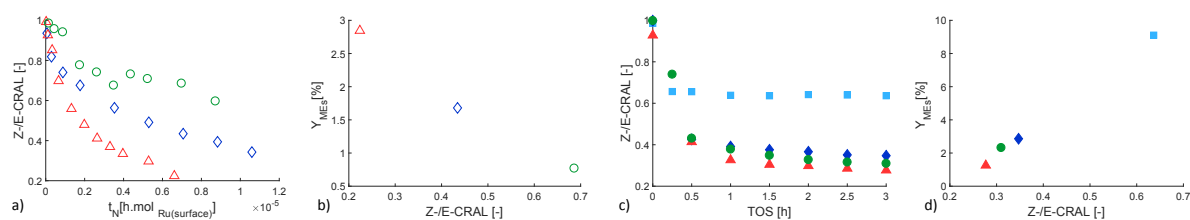


Figure S8. Ratio of Z-citral to E-citral as a function of the time for: a) powder catalysts, c) extrudates. Yield of menthols as a function of the ratio of Z-citral to E-citral: b) powder catalysts at normalized time of  $7 \cdot 10^{-6}$  h·mol<sub>Ru(surface)</sub>, d) extrudates at 3 h of TOS. Legend of powder catalyst: Ru/(H-MCM-41+Bindzil) (P-B, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (P-C, red triangle), Ru/(H-MCM-41)+Bindzil (P-D, green circle). Legend of extrudates: Ru/(H-MCM-41+Bindzil), post synthesis (E-A, light blue square), Ru/(H-MCM-41+Bindzil), in-situ synthesis (E-B, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (E-C, red triangle), Ru/(H-MCM-41)+Bindzil (E-D, green circle). Conditions for the batch experiment over the powder catalysts: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst. Conditions for the continuous experiment over the extrudates: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 1 g of catalyst, 12.5 min of residence time.

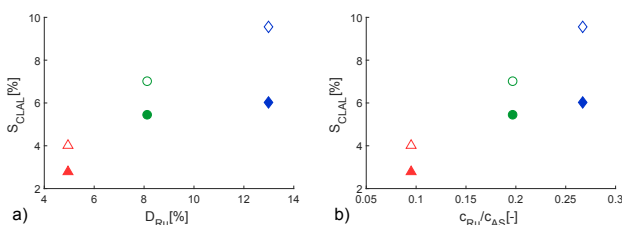


Figure S9. Selectivity of citronellal as a function of a) Ru dispersion, b) ratio of Ru concentration to acidity. Legend: Ru/(H-MCM-41+Bindzil) (P-B, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (P-C, red triangle), Ru/(H-MCM-41)+Bindzil (P-D, green circle); at normalized time of  $3.5 \cdot 10^{-6}$  h·mol<sub>Ru(surface)</sub> (open symbols),  $7 \cdot 10^{-6}$  h·mol<sub>Ru(surface)</sub> (filled symbols). Conditions: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst.

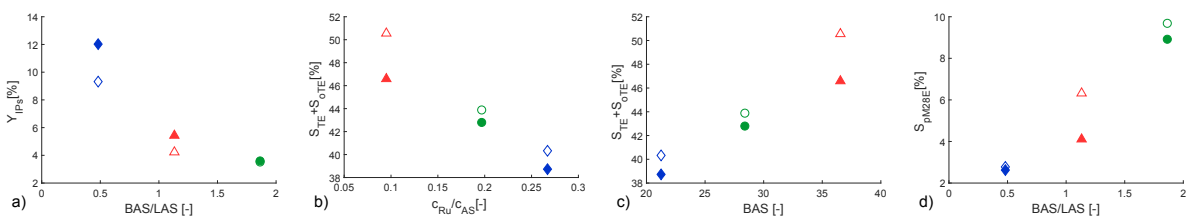


Figure S10. a) Yield of isopulegols as a function of Brønsted to Lewis acid sites ratio, b, c) Selectivity of p-menthatrienes, o-cymene and o-isopropenyltoluene as a function of ratio of Ru concentration to acidity and Brønsted acidity, d) Selectivity of p-mentha-2,8-diene as a function of Brønsted to Lewis acid sites ratio. Legend: Ru/(H-MCM-41+Bindzil) (P-B, dark blue diamond), Ru/(Bindzil)+H-MCM-41 (P-C, red triangle), Ru/(H-MCM-41)+Bindzil (P-D, green circle); at normalized time of  $3.5 \cdot 10^{-6}$  h·mol<sub>Ru(surface)</sub> (open symbols),  $7 \cdot 10^{-6}$  h·mol<sub>Ru(surface)</sub> (filled symbols). Conditions: 70 °C, 10 bar of H<sub>2</sub>, 0.086 M initial concentration of citral in cyclohexane, 0.2 g of catalyst.

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