Application of $\text{ReO}_x/\text{TiO}_2$ catalysts with an excellent SO₂ tolerance in selective catalytic reduction of NO_x by NH₃

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The VASP was used to perform all the spin-polarized density functional theory (DFT) calculations [1, 2] within the generalized gradient approximation (GGA) using the Perdew-Burke-Ernzerhof (PBE) formulation [3]. Projected augmented wave (PAW) potentials were chosen to describe the ionic cores and take valence electrons into account using a plane wave basis set with a kinetic energy cutoff of 450 eV [4, 5]. Partial occupancies of the Kohn-Sham orbitals were allowed using the Gaussian smearing method and a width of 0.02 eV. The electronic energy was considered selfconsistent when the energy change was smaller than 10⁻⁵ eV. A geometry optimization was considered convergent when the energy change was smaller than 3*10⁻² eV/ Å. Grimme's DFT-D3 methodology was used to describe the dispersion interactions among all the atoms in adsorption models of interest [6]. MnO_x/TiO₂, V₂O₅/TiO₂ and ReO_x/TiO₂ surface slab with 8 atomic layers were built first. The surface was chosen since it is the most stable surface among various possible surfaces. This slab was separated by a 15 Å vacuum layer in the z direction between the slab and its periodic images. During structural optimizations of the surface models, a 3×3 \times 1 gamma-point centered k-point grid for Brillouin zone was used and the top 6 atomic layers were allowed to fully relax while the bottom atomic 6 layers were fixed.

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Fig. S1. (a) Catalytic activity of ReTi-3, VWTi and MnTi sample; (b) N_2 selectivity of ReO_x/TiO₂ catalysts. Tested conditions: 1.5 mL catalyst sample, [NO] = [NH₃] = 500 ppm, [O₂] = 4.0%, and N₂ as balanced gas, GHSV = 36 000 h⁻¹.



Fig. S2. (a) Water tolerance experiment of ReTi-3 sample; (b) SO₂ and water tolerance experiment of ReTi-3 sample at 300 °C. Tested conditions: 1.5 mL catalyst sample, $[NO] = [NH_3] = 500$ ppm, $[SO_2] = 500$ ppm (when used), $[H_2O] = 3.0\%$ (when used), $[O_2] = 4.0\%$, and N₂ as balanced gas, GHSV = 36 000 h⁻¹.



Fig. S3. TG results of ReTi-S, VWTi-S and MnTi-S sample.



Fig. S4. XRD result of ReO_x/TiO_2 catalysts with varied Re loading.



Fig. S5. HAADE-STEM and STEM-EDS elemental mapping of ReTi-3 sample.



Fig. S6. The top view for adsorption of SO₂ on (a) MnO_x/TiO_2 model; (b) V_2O_5/TiO_2 model; (c) ReO_x/TiO_2 model. (Ti: grey balls; O: red balls; S: yellow balls; Mn: pink balls; V: deep purple balls; Re: light purple balls)



Fig. S7. In situ DRIFTS of $NH_3 + SO_2 + O_2$ co-adsorption over ReTi-3 sample at 250 °C.



Scheme S1. Proposed E-R mechanism on (a) L acid sites and (b) B acid sites of ReO_x/TiO_2 catalysts.