

## Supplementary Information

### Promotional effect of indium on Cu/SiO<sub>2</sub> catalysts for the hydrogenation of dimethyl oxalate to ethylene glycol

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Table S1. Textural Properties of Cu<sub>x</sub>In/SiO<sub>2</sub> Catalysts.

In (wt%)	Cu (wt%) <sup>a</sup>	In (wt%) <sup>a</sup>	S <sub>BET</sub> (m <sup>2</sup> /g) <sup>b</sup>	Vp (cm <sup>3</sup> /g) <sup>b</sup>	Dp(nm) <sup>b</sup>
0	28.45	0	473	0.83	5.8
0.5	30.30	0.53	510	0.98	6.3
1	29.06	1.02	482	0.86	5.8
1.5	29.64	1.49	497	0.95	6.4

<sup>a</sup>Determined by ICP-OES analysis. <sup>b</sup>Determined by N<sub>2</sub> isotherm adsorption.

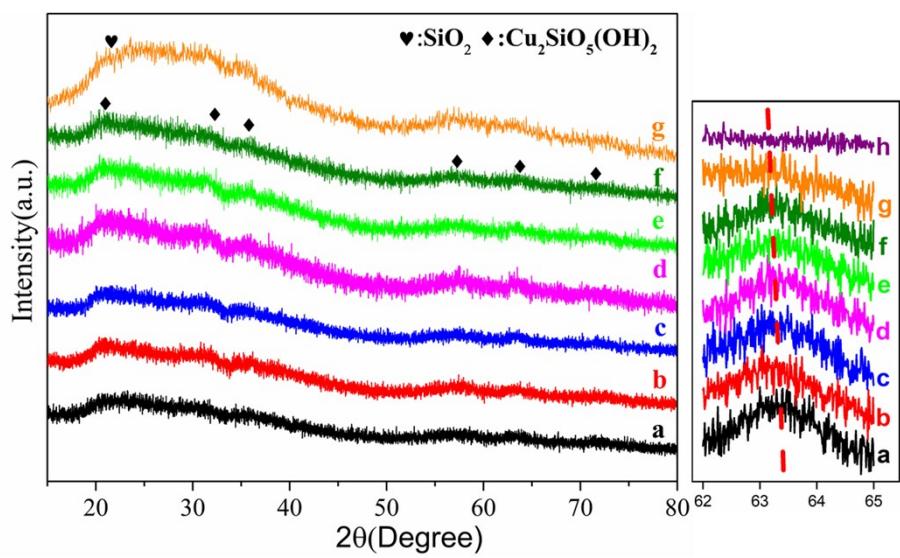


Figure S1. XRD for calcined catalysts and the fine scanning XRD at 62-65 degree for  $\text{CuxIn/SiO}_2$  catalysts (a-g:  $x=0, 0.5, 1, 1.5, 2, 5, 10$ ) and  $6.7\text{In/SiO}_2$  (h).

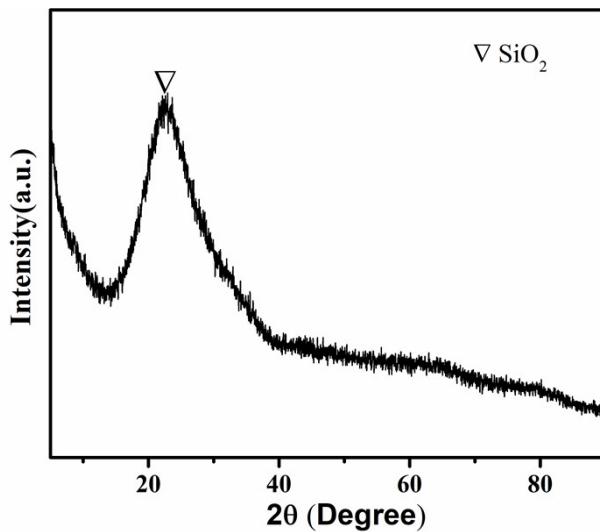


Figure S2. XRD for calcined  $6.7\text{In/SiO}_2$  catalyst

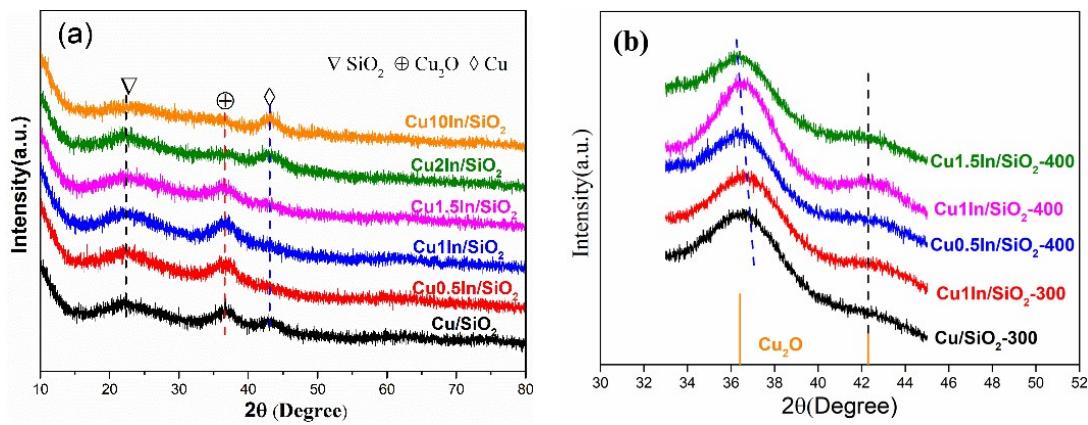


Figure S3. XRD patterns for reduced (a) and fine scanning XRD for reduced catalysts at 33-45 degree (b), Cu<sub>2</sub>O (JCPDS: 05-0667) <sup>1</sup>.

Table S2. Particle sizes calculated from XRD with reduced catalysts.

Catalysts	Reduced(nm)	
	Cu <sup>+</sup>	Cu <sup>0</sup>
Cu/SiO <sub>2</sub>	2.3	2.6
Cu0.5In/SiO <sub>2</sub>	2.1	-
Cu1In/SiO <sub>2</sub>	2.2	-
Cu1.5In/SiO <sub>2</sub>	2.2	-
Cu2In/SiO <sub>2</sub>	1.9	2.2
Cu10In/SiO <sub>2</sub>	-	3.3

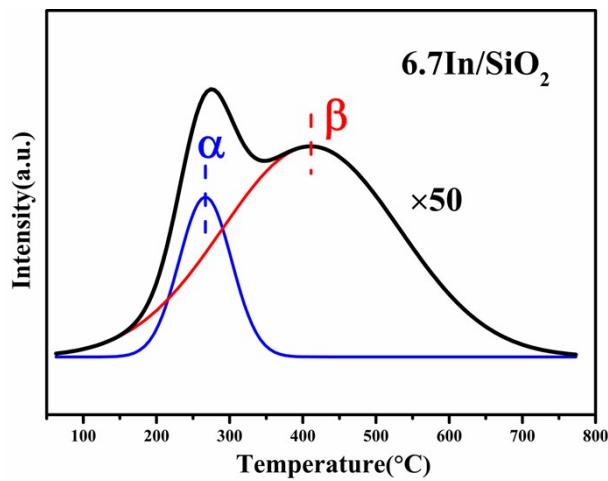


Figure S4. Deconvolution of the enlarged H<sub>2</sub>-TPR curve of 6.7In/SiO<sub>2</sub>.

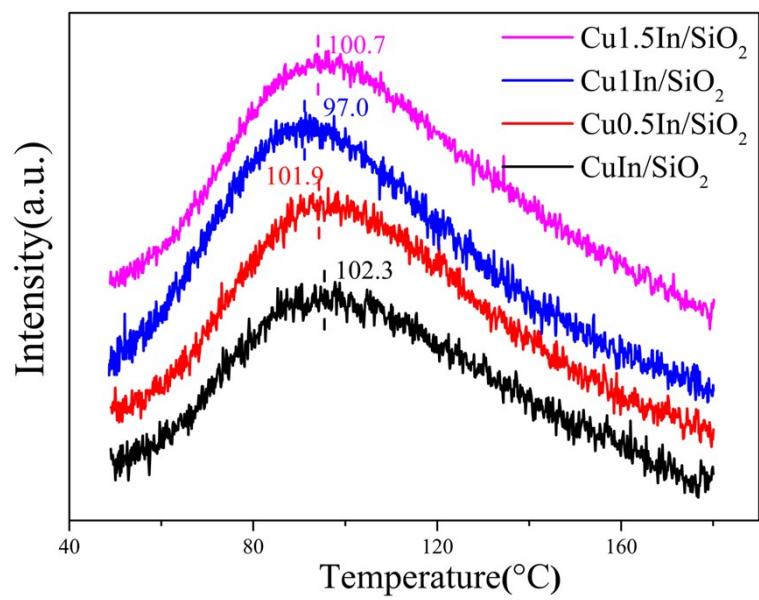


Figure S5. H<sub>2</sub>-TPD curves of CuxIn/SiO<sub>2</sub> catalysts.

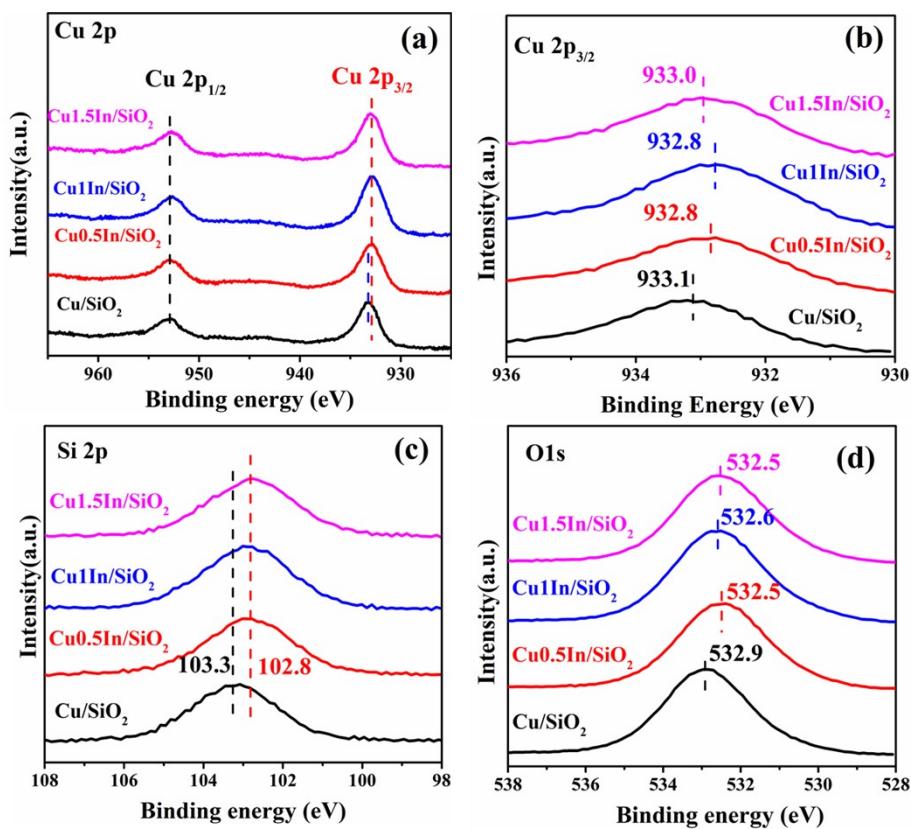


Figure S6. XPS for Cu 2p(a), Cu 2p<sub>3/2</sub>(b), Si 2p(c), O 1s(d).

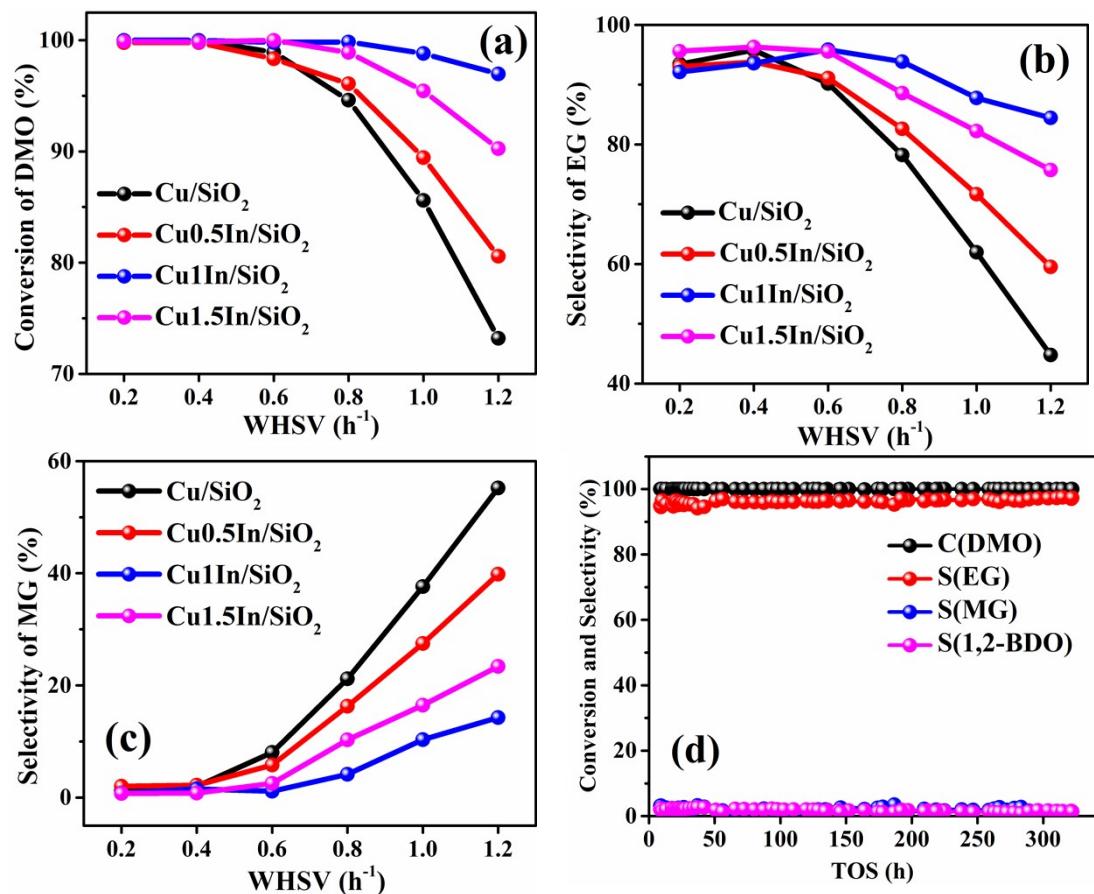


Figure S7. Activity evaluation of  $\text{CuxIn/SiO}_2$  catalysts ( $x=0, 0.5, 1, 1.5$ ), conversion of DMO (a), selectivity of EG (b), selectivity of MG (c) at reaction conditions of 2.5 MPa, 180 °C,  $\text{H}_2/\text{DMO} = 80$  (mole) and stability evaluation of  $\text{Cu1In/SiO}_2$  catalyst (d) at reaction conditions of 2.5 MPa, 180 °C,  $\text{H}_2/\text{DMO} = 80$  (mole) and  $\text{WHSV}=0.8 \text{ h}^{-1}$ .

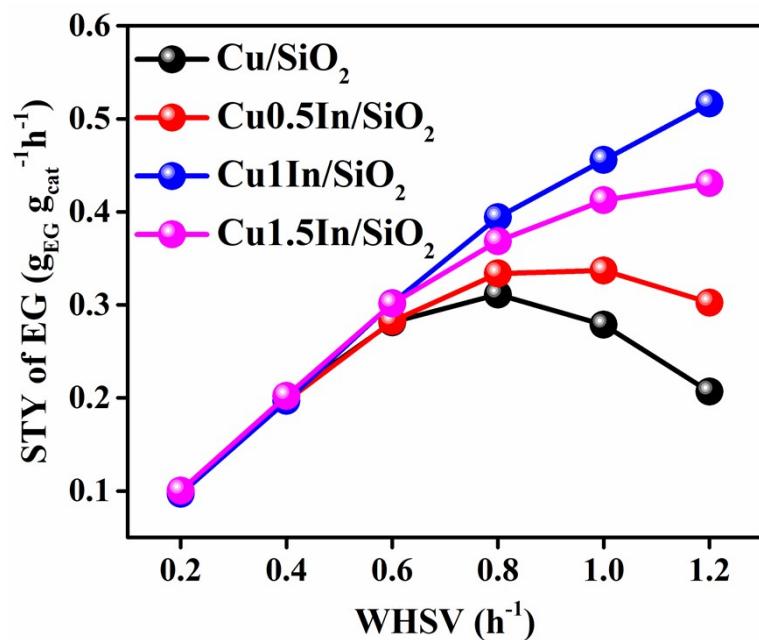


Figure S8. STY of EG at different WHSV, reaction conditions: 2.5 MPa, 180 °C, H<sub>2</sub>/DMO = 80 (mole).

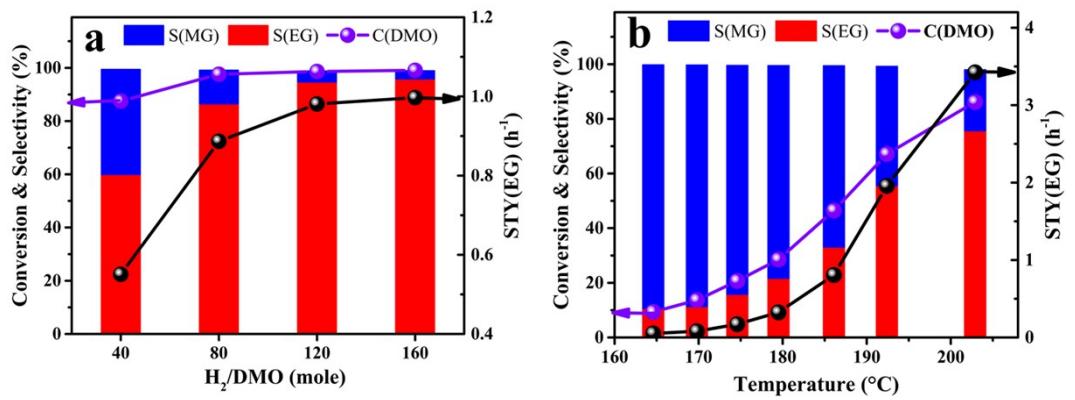


Figure S9. Catalytic performance of Cu<sub>1</sub>In/SiO<sub>2</sub> with different H<sub>2</sub>/DMO (a) at 180 °C, 2 h<sup>-1</sup>, 2.5 MPa, and reaction temperature (b) at 10 h<sup>-1</sup>, 2.5 MPa, H<sub>2</sub>/DMO = 80 (mole).

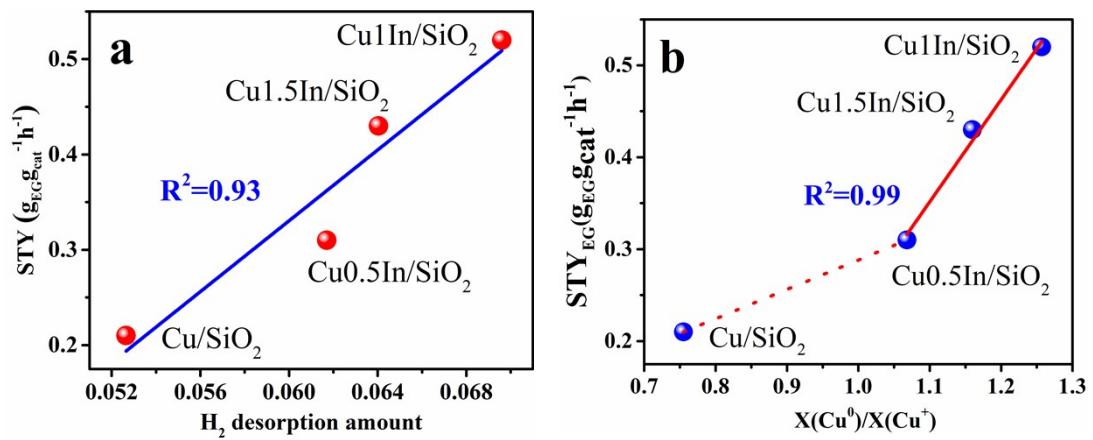


Figure S10. Relationship between  $\text{STY}_{\text{EG}}$  and  $\text{H}_2$  adsorption amount (a) and ratio of  $\text{Cu}^0/\text{Cu}^+$ (b).

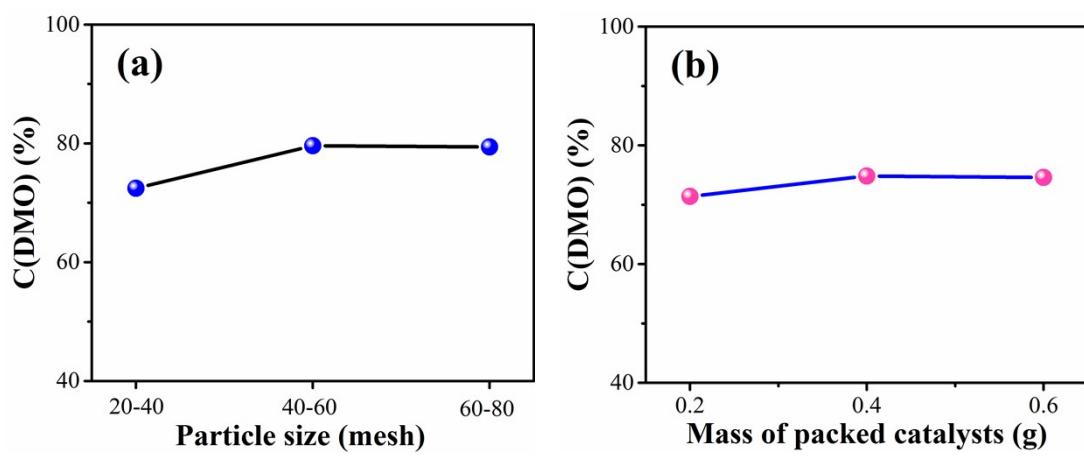


Figure S11. Madon-Boudart test<sup>2</sup> with Cu1In/SiO<sub>2</sub>. Reaction conditions: 180 °C, 2.5 MPa, WHSV = 3 h<sup>-1</sup> and H<sub>2</sub>/DMO = 80 (mole).

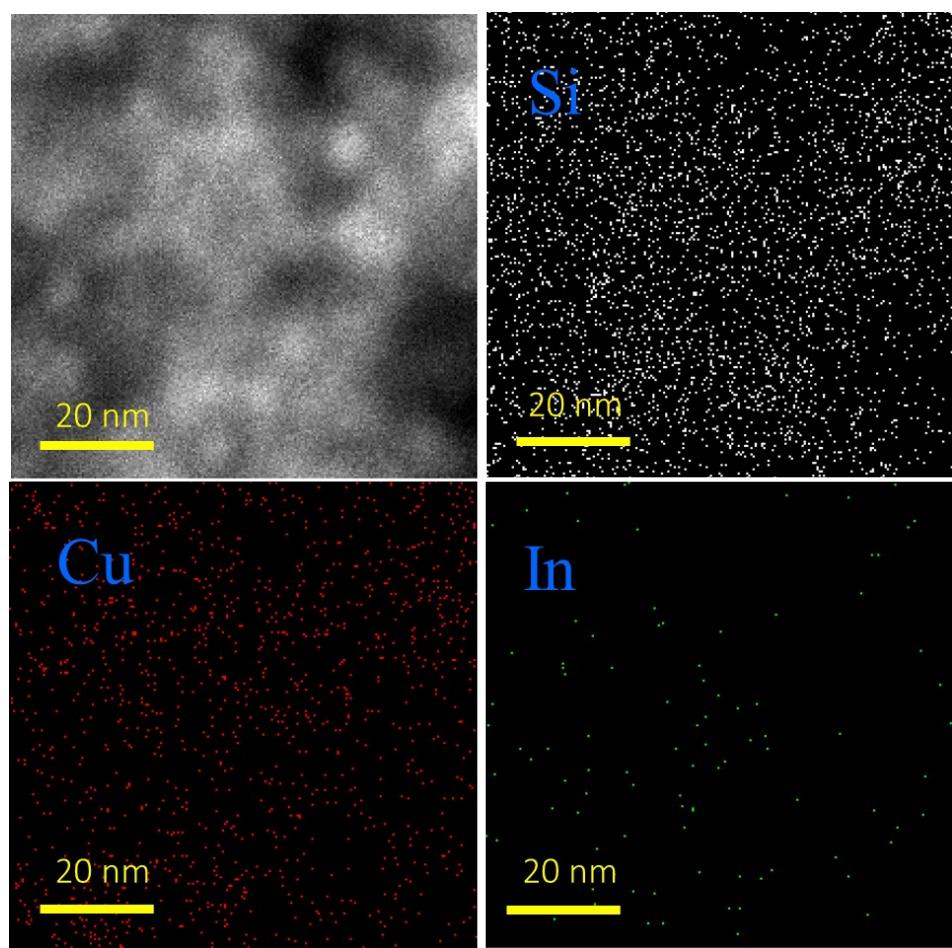


Figure S12. Elemental mapping of Si, O, Cu and In for Cu<sub>1</sub>In/SiO<sub>2</sub>

Table S3. The evaluation results for Cu/SiO<sub>2</sub> when calculating the Ea.

T/°C	WHSV/h <sup>-1</sup>	C(DMO)/%	S(EG)/%
184.8	6	35.3	19.0
180.0	6	23.9	12.7
175.1	6	16.3	10.2
170.4	6	11.4	9.6
165.4	6	7.5	6.6

Table S4. The evaluation results for Cu0.5In/SiO<sub>2</sub> when calculating the Ea.

T/°C	WHSV/h <sup>-1</sup>	C(DMO)/%	S(EG)/%
184.3	10	27.7	14.9
180.9	10	20.8	13.6
175.2	10	13.4	10.1
170.1	10	9.3	7.9
164.8	10	6.2	5.2

Table S5. The evaluation results for Cu1In/SiO<sub>2</sub> when calculating the Ea.

T/°C	WHSV/h <sup>-1</sup>	C(DMO)/%	S(EG)/%
185.4	14	20.4	12.1
180.0	14	13.9	8.7
175.2	14	9.8	5.8
170.3	14	7.1	7.2
165.4	14	5.0	6.4

Table S6. The evaluation results for Cu1.5In/SiO<sub>2</sub> when calculating the Ea.

T/°C	WHSV/h <sup>-1</sup>	C(DMO)/%	S(EG)/%
185.3	10	24.2	15.9
180.6	10	16.4	11.2
175.8	10	11.4	8.8
169.9	10	7.7	8.3
165.0	10	5.1	6.5

Table S7 Catalytic performance of DMO hydrogenation for Cu5In/SiO<sub>2</sub> and Cu10In/SiO<sub>2</sub>.

Catalysts	C(DMO)/%	S(EG)/%	S(MG)/%
Cu5In/SiO <sub>2</sub>	41.5	16.9	83.1
Cu10In/SiO <sub>2</sub>	24.4	5.7	94.3

Reaction conditions: 2.5 MPa, 180 °C, WHSV=0.4 h<sup>-1</sup>, H<sub>2</sub>/DMO = 80 (mole)

Table S8. Catalytic performance of copper-based catalysts in DMO hydrogenation to EG.

catalyst	C <sub>DMO</sub> /%	S <sub>EG</sub> /%	P/ MPa	T/ °C	H <sub>2</sub> /DMO	LHSV /h <sup>-1</sup>	Yield/%	STY/ h <sup>-1</sup>	TOF/h <sup>-1</sup> (RT <sup>a</sup> )
Cu/MMO-S3 <sup>3</sup>	98.2	96.1	2	165	50	1	94.4	0.602	23.6(165)
20Cu-OMS <sup>4</sup>	100	98.2	2.5	180	80	1	98.2	0.477	-
Cu1In/SiO <sub>2</sub> (this work)	100	96	2.5	180	80	0.6	96	0.52	27.6(180)
6Cu1.9Au/SBA-15 <sup>5</sup>	100	99.1	3	180	80	0.6	99	1.5	121(180)
Cu/ZrO <sub>2</sub> -x-S3 <sup>6</sup>	100	99.5	2	180	50	2	99.5	1.05	42.4(180)
CuZr1/SiO <sub>2</sub> <sup>7</sup>	100	95	2.5	180	80	0.6	-	-	35.6(180)
1B-Cu-SiO <sub>2</sub> <sup>8</sup>	99.7	93	3	190	80	0.75	92.7	1.6	-
Cu@SiO <sub>2</sub> @CNT <sup>9</sup>	100	~99	3	190	100	0.6	99	-	22(190)
0.05D-Cu-SiO <sub>2</sub> <sup>10</sup>	99.9	96.9	2	190	50	1	96.8	-	11.4(160)
Cu-Ag.05/SiO <sub>2</sub> <sup>11</sup>	100	97	3	190	80	0.6	97	-	20.6(190)
CuSiZr1-850 <sup>12</sup>	100	99	3	190	150	0.3	99	-	30(190)
Cu/SiO <sub>2</sub> -3HZ-38	99.8	94.4	3	190	80	2	94.2	1.50	-
6Cu1-Pt0.1/SBA-15 <sup>13</sup>	100	98	3	190	80	0.6	98	0.31	62.1(190)
Cu/SiO <sub>2</sub> <sup>14</sup>	100	95.0	2.5	200	200	2	95.0	-	-
Cu/SiO <sub>2</sub> <sup>15</sup>	95.0	90.0	3	200	80	0.6	85.5	-	-
Cu/10-SiO <sub>2</sub> <sup>16</sup>	100	94.7	2.5	200	120	2.5	94.7	-	30.6(195)
Cu-PSNT@m-SiO <sub>2</sub> <sup>17</sup>	100	98.0	3	200	80	2	98.0	-	40.6(200)
Cu/NAHS	100	95.0	2.5	200	20	2	95.0	-	160(200)
Cu-0.5%Pd/SiO <sub>2</sub> <sup>18</sup>	100	95.0	2.5	200	100	0.5	95	-	-
Cu-0.6%Sn/SiO <sub>2</sub> <sup>19</sup>	100	96.0	2.5	200	90	1	96	-	-
15CNTs-Cu-SiO <sub>2</sub> <sup>20</sup>	100	95.0	3	200	80	1.2	95.0	2.6	-
Cu/SiO <sub>2</sub> -TiO <sub>2</sub> <sup>21</sup>	100	97	3	200	100	0.3	97	-	-
Cu/H1S1 <sup>22</sup>	100	98	2.5	200	100	1.5	98	-	1.89(200)
20Cu-HMS <sup>23</sup>	100	98	2.5	200	50	0.45	98	-	3.8
20Cu-MCM-41 <sup>24</sup>	100	92	2.5	200	80	3	92	-	-
CuB/HMS(2/1) <sup>25</sup>	100	98	2.5	200	120	2.5	98	-	-
Cu <sub>3</sub> Ni/HMS <sup>26</sup>	100	98	2.5	200	100	1	98	-	19.7(200)
Cu-Ni/ZrO <sub>2</sub> -DBD <sup>27</sup>	100	96	2.5	200	120	0.3	96	-	-
Cu/SiO <sub>2</sub> -MOF <sup>28</sup>	99.9	95.0	2	210	50	0.82	94.9	0.424	19.3(190)
0.1CD-Cu-SiO <sub>2</sub> <sup>29</sup>	~99.9	~95.0	2	210	50	0.72	94.9	~0.36	11.4(170)
10%Cu-Co/HMS <sup>30</sup>	100	>95.0	3	220	150	1.2	95.0	-	5.5(220)
Cu/Al-ZrO <sub>2</sub> <sup>31</sup>	100	97.1	2.5	220	120	0.8	97.1	-	16.9(220)
CuZnAl-773 <sup>32</sup>	100	>95.0	3	220	100	0.3	95.0	-	-
CuZnZr-0.2 <sup>33</sup>	>95.0	>95.0	3	220	150	0.3	90	-	-
CoCu-ZnO-450 <sup>34</sup>	100	93	2.5	220	110	2	93	-	-
CuZnAl-LDH <sup>35</sup>	100	94.7	2.5	220	160	0.3	94.7	-	-
20Cu/P25-823 <sup>36</sup>	100	99	2.5	220	100	0.3	99	-	4.5(220)
Cu@CNTs-350 <sup>37</sup>	99.4	87.4	2.5	240	200	0.2	86.9	-	-
20Cu/HAP <sup>38</sup>	100	90.0	2.5	240	150	0.4	90	0.72	14.6(210)

<sup>a</sup>RT: reaction temperature when calculating the TOF values.

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