Supporting Information

Approaching a High-Rate and Sustainable Production of Hydrogen Peroxide: Oxygen Reduction on Co-N-C Single-Atom Electrocatalysts in Simulated Seawater

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Results



Figure S1. Cross-sectional scanning electron microscopy (SEM) image of Co-N-C catalysts on a Sigracet 39BB gas diffusion layer. (A catalyst loading of 2 mg cm⁻² was sprayed on the carbon paper for a clearer image of catalyst distribution.)



Figure S2. Scanning electron microscopy (SEM) images of (a) Co-N-C and (b) N-C samples.



Figure S3. X-ray diffraction (XRD) patterns of the Co-N-C and N-C samples.

Table S1.	Co content	determined	by X-ray	photoelectron	spectroscopy	(XPS)	and
inductively	y coupled pla	ısma mass sp	ectrometry	y (ICP-MS).			

Method	С	N	Со
XPS (at.%)	87.56	11.8	0.64
ICP-MS (wt.%)	-	-	0.97



Figure S4. Top views of anchored Co, graphitic N, pyridinic N, and pyrrolic N.



Figure S5. (a)k²-weighted EXAFS spectra and (b-f) the corresponding fitting curves of Co-N-C, CoPc, Co₃O₄, CoO, and Co foil.



Figure S6. FT-EXAFS fitting curves of (a) CoPc, (b) CoO, (c) Co_3O_4 , and (d) Co foil in R space.

Table S2. EXAFS fitting parameters at the Co K-edge for Co-N-C and standard samples.

	Path	Ν	ΔE (eV)	100×R (Å)	100×σ² (Å ²)	R-
						factor
Co foil	Co-Co	<mark>12.0</mark>	<mark>6.80 (0.51)</mark>	<mark>249.0 (0.3)</mark>	5.67 (0.43)	<mark>0.001</mark>
CoO	Co-O	6.0	-1.10 (<mark>2.08</mark>)	211.0 (1.9)	9.40 (1.71)	<mark>0.008</mark>
	Co-Co	12.0	-3.42 (<mark>1.19</mark>)	300.2 (0.9)	10.22 (0.90)	
	Co-O	<mark>5.3</mark>	-7.35 (1.46)	191.3 (0.8)	2.67 (0.69)	
$\mathrm{Co}_3\mathrm{O}_4$	Co-Co1	4.0	-7.72 (0.77)	285.3 (0.5)	2.54 (0.50)	<mark>0.005</mark>
	Co-Co2	<mark>9.3</mark>	-7.72 (0.77)	358.8 (0.7)	6.10 (0.62)	
CoPc	Co-N	4.0	5.46(1.12)	191.8(2.1)	3.92(0.46)	0.005
Co-N-C	Co-N	<mark>5.2</mark>	-3.72 (1.68)	197.4 (8.3)	11.28 (2.13)	<mark>0.008</mark>
		(0.70)				

The amplitude reduction factor S_0^2 was determined to be 0.72 through fitting the FT-EXAFS of standard Co foil which was measured simultaneously during the experiment. *N*, coordination number; ΔE , threshold energy correction; *R*, distance between absorber and backscatter atoms; σ^2 , Debye-Waller factor to describe the variance due to disorder

K-space and K-space.						
Sample	k space	R space				
Co foil	<mark>3.0≤k≤10.5</mark>	1≤R≤2.7				
CoO	3.2≤k≤11.2	1≤R≤3.4				
Co_3O_4	3.5≤k≤13.1	1≤R≤3.4				
CoPc	3.0≤k≤10.6	1≤R≤2.2				
Co-N-C	3.0≤k≤10.5	1≤R≤2.4				

(both lattice and thermal); the *R*-factor indicates the goodness of the fit. Table S3. The range of the data used in the fitting for Co-N-C and standard samples in k-space and R-space.



Figure S7. CV curve of Co-N-C catalyst in an N_2 saturated 0.5M NaCl containing 0.2M H_2O_2 .



Figure S8. Linear sweep voltammetry (LSV) curves of Co-N-C at different electrolytes with various pH values in a RRDE setup with the ring current was collected on the Pt ring at a constant potential of +1.26 V_{RHE}.



Figure S9. Linear sweep voltammetry (LSV) curves of (a) Co-N-C and (b) CoPc in 0.5M NaCl and 0.5M NaClO₄ in a RRDE setup with the ring current was collected on the Pt ring at a constant potential of +1.26 V_{RHE}.



Figure S10. (a) Raman spectra of 0.5M NaCl and the interfaces between Co-N-C or CoPc and 0.5M NaCl or H_2O (* indicates signals from the environmental light), and (b) adsorption of chloride ion on Co-N₅ and Co-N₄ surfaces with adsorption energies (E_{ads}) computed by DFT (color notation: dark blue-Co, brown-C, light blue-N, green-Cl).



Figure S11. (a) LSV curves of Co-N-C cathode with a mass loading of 0.2 mg cm⁻² in flow cell under the flow of O_2 and Ar (the red dash line was obtained by subtracting the current under the flow of Ar); (b) LSV curves of Co-N-C cathode with a mass loading of 0.2, 1.6, 3.2 mg cm⁻² in flow cell under the flow of O_2 .



Figure S12. (a) Production rate (left) and Faradaic efficiency (right) of Cl_2 in the anode in a triple-phase flow cell under the flow of O_2 in 0.5M NaCl and (b) electrocatalytic degradation of 1 mL Rhodamine B (RhB, 20 ppm) or tetracycline (TC, 20 ppm) in one minute using different amounts of anolyte after 1 h of electrolysis at 50 mA cm⁻².



Figure S13. Electrochemical impedance spectroscopy of the flow cell at the open circuit potential.



Figure S14. Images of rotating ring-disk electrode (RRDE) setup: (a) the connection to measure disk current only and (b) the connection to measure both disk current and ring current.

Catalyst	k _{H2O2}	$\mathrm{FE}_{\mathrm{H2O2}}$	Electrolyte	j	Ref No. in
	(mol g ⁻¹ _{catalyst} h ⁻¹)	(%)		(mA cm ⁻	Figure 4c
				²)	
Co-N-C	4.5	95.6	0.5M NaCl	50	This work
Co-C	0.056	30	PEM*	30	[50] ¹
CB-10%	3.66	~90	SE*	200	[51] ²
NADE	0.227	66.8	0.05M Na ₂ SO ₄	240	[52] ³
CMK3-20s	0.837	78	$0.1 \text{ M K}_2 \text{SO}_4$	~14	[55] ⁴
CoTPP/KB	0.475	50	PEM*	95	[56] ⁵
CoTPP/VGCF	0.1458	32	PEM*	80	[57] ⁶
(1073 K)					
MnCl-OEP/AC	0.018	34.1	$0.6 \ M \ H_2 SO_4$	56.1	[53] ⁷
(823 K)					
AC(HNO ₃ 3.8	0.036	31	${\sim}0.6~M~H_2SO_4$	~30	[54] ⁸
M)+VGCF					
Co-N-C	4.33	50	0.1M KOH	~50	[15] ⁹
N-FLG-8	3.11	99.8	0.1M KOH	36.1	[58] ¹⁰
Ni-N ₂ O ₂	5.9	90	0.1M KOH	70	[20] ¹¹
N-O-P-C-800	0.54	93.1	0.1M KOH	~14	[59] ¹²
VGCF+XC72	0.0325	94	2M NaOH	100	[60] ¹³

Table S4. Comparison of this work and recently reported catalysts for H_2O_2 production via ORR in flow cell.

*PEM: proton exchange membrane with neutral DI water as carrier flow

*SE: solid electrolyte with neutral DI water flow

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