

**Sublayer-enhanced atomic sites of single atom catalysts through in-situ  
atomization of metal oxide nanoparticles**

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## **Experimental Section**

### ***1.1 Materials synthesis***

The graphene adopted in present study was obtained from the Institute of Coal Chemistry, Chinese Academy of Sciences (single layer with average thickness of 0.4 nm). The as-received graphene was purified following the procedure reported. The purified graphene was functionalized with PEI, and the PEI functionalized graphene (100 mg) was firstly ultrasonicated in 100 mL EG solution for 1 h, followed by the addition of iron (III) acetylacetonate. The dispersion was ultrasonicated for 15 min and then stirred for another hour before being placed in a three-neck bottle and heated for 5 min, followed by stirring overnight. The solution was then filtered using a nylon membrane and washed for several times. Similarly, the  $\text{CoO}_x$  was synthesized as well with the aim to demonstrate the universal trend.

$\text{FeO}_x/\text{G}$  (10 mg) was dispersed in 20 mL ethanol under ultrasonic for 30 min before being mixed with  $\text{C}_2\text{H}_4\text{N}_2$  (10 g) by grinding till the mixture was dried. Subsequently, the mixed powder was heated at 350 °C for 3 h and then at 650 °C for 3 h before being heated at 900 °C for 1 h under Ar with a flow rate of 50 mL min<sup>-1</sup>. The obtained products are washed with acid and then the iron content was tested adopting inductively coupled plasma - optical emission spectrometer (ICP-OES), and denoted as X-FeSA (X is the actual loading of the iron).

### ***1.2. Characterization***

The obtained materials were firstly analysed by X-ray powder diffraction. The morphology of the catalysts was studied by scanning electron microscopy (SEM), transmission electron microscopy (TEM) and high angle annular dark field (HAADF) scanning TEM (STEM) with elemental mapping on a Titan G2 60-300 at 80 kV. The annular dark field images (ADF) were collected using a Nion UltraSTEM100 microscope operated at 60 kV at a beam current of 60 pA. The convergence half angle of the electron beam was set to 30 mrad and the inner collection half angle of the ADF images was 51 mrad. Diffraction data was collected with a Bruker D8 Advance diffractometer operated at 40 kV and 40 mA with Cu K $\alpha$  ( $\lambda = 1.5406 \text{ \AA}$ ) in the range of 20-90 $^\circ$  2 $\theta$ . X-ray photoelectron spectroscopy (XPS) were conducted on a Kratos Axis Ultra DLD spectrometer using a monochromatic AlK $\alpha$  (1486.6 eV) irradiation source operated at 225 W.

X-ray absorption spectroscopy (XAS) measurements were performed at the wiggler XAS Beamline (12ID) at the Australian Synchrotron in Melbourne, Australia using a set of liquid nitrogen cooled Si (111) monochromator crystals. With the beamline optics employed (Si-coated collimating mirror and Rh-coated focussing mirror) the harmonic content of the incident X-ray beam was negligible. XAS measurements were performed at the Fe K-edge (7.1 keV) at < 10 K to minimize thermal disorder and to ensure that the samples were not radiation damaged (This was confirmed via repetitive quick scanning of the absorption edge for up to 2 h, i.e., 12 scans. Note that a single complete XAS scan took ~1 h). For these samples were prepared as pellets via mechanical grinding in a cellulose binder using a mortar/pestle. Both fluorescence and transmission

spectra were recorded depending on the concentration of Fe in each sample (the validity of this approach was confirmed by comparing the fluorescence and transmission spectrum for one of the samples for which both methods yielded comparable signal-to-noise data).

### ***1.3 Electrochemical characterization***

Electrochemical measurements were conducted in an electrochemical station of Auto Lab in a typical three-electrode system. Graphite rod and Ag/AgCl (saturated KCl) electrode with electrolytic bridge were used as the counter and reference electrodes. The catalysts materials (4 mg) were ultrasonically mixed in 1 mL of ethanol nafion mixture (with Ethanol: Nafion 19:1) to form a homogeneous ink, followed by dropping certain amount of active material ink onto the surface of rotating disk electrode (RDE, 0.19625 cm<sup>2</sup>). The X-FeSA catalyst loading was ~0.408 mg cm<sup>-2</sup>, and Pt loading was ~0.2 mg cm<sup>-2</sup> for Pt/C. Linear scan voltammetry (LSV) curves of X-FeSA and Pt/C (20 % Pt, JM) were obtained in N<sub>2</sub> or O<sub>2</sub>-saturated 0.1 M KOH or 0.1 M HClO<sub>4</sub> solution using RDE with rotating rate of 1600 rpm. The IR-corrected Tafel plots were recorded at a scan rate of 1 mV s<sup>-1</sup>. All potentials in the present study were given versus RHE reference electrode ( $E = E_{AgCl}^0 + 0.197 + 0.059 \text{ pH}$ , here 0.197 V is the potential for Ag/AgCl at 20 °C). The electron transfer number (n) of catalysts was calculated through the Koutecky–Levich (K–L) equations:

$$\frac{1}{J} = \frac{1}{J_L} + \frac{1}{J_K} = \frac{1}{B\omega^{1/2}} + \frac{1}{J_K} \quad (1)$$

$$B = 0.62nFD_0^{2/3}v^{-1/6}C_0 \quad (2)$$

where  $J$ ,  $J_L$ , and  $J_k$  is the measured, diffusion-limiting, and the kinetic current density, respectively.  $\omega$  is the electrode-rotating angular velocity,  $F$  is the Faraday constant (96485 C mol<sup>-1</sup>),  $D_0$  represents the diffusion coefficient of O<sub>2</sub> and is  $1.9 \times 10^{-5}$  cm<sup>2</sup> s<sup>-1</sup> in 0.1 M KOH,  $\nu$  represents kinetic viscosity of the electrolyte and is 0.01 cm<sup>2</sup> s<sup>-1</sup>, and  $C_0$  represents the density of O<sub>2</sub> and is  $1.2 \times 10^{-6}$  mol cm<sup>-3</sup>.

Moreover, The H<sub>2</sub>O<sub>2</sub> yield and the electron transfer number are calculated from the LSV of rotating ring disk electrode (RRDE, 0.2475 cm<sup>2</sup>) measurement at 1600 rpm according to the formulas:

$$H_2O_2\% = \frac{200 \frac{I_R}{N}}{\left(\frac{I_R}{N} + I_D\right)} \quad (3)$$

$$n = \frac{4I_D}{N\left(\frac{I_R}{N} + I_D\right)} \quad (4)$$

Where  $I_D$  and  $I_R$  is the disk current and the ring current, respectively.  $N$  is the collection efficiency (37%) and  $n$  is the electron transfer number.

#### ***1.4 Quantification of the active sites.***

The SD and turnover frequency were obtained according to the method presented by Shui et al.<sup>1</sup> Briefly, extensive cycling in pH 5.2 acetate buffer alternatively in O<sub>2</sub> and N<sub>2</sub> was performed to obtain nonchanging cyclic voltammetry curves in N<sub>2</sub>. Then the catalyst was poisoned by NaNO<sub>2</sub>. The ORR performance was recorded before, during

and after the nitrite absorption. Nitrite stripping was conducted in the region of 0.7 to  $-0.5$  V versus the reversible hydrogen electrode. The excess in cathodic charge ( $Q_{strip}$ ) was proportional to the SD, and the turnover frequency was calculated by dividing the difference of kinetic current before and after nitrite absorption by SD:

$$SD(mol\ g^{-1}) = \frac{Q_{strip}(C\ g^{-1})}{n_{strip}F(C\ mol^{-1})} \quad (5)$$

$$TOF(s^{-1}) = \frac{n_{strip}\Delta j_k(mA\ cm^{-2})}{Q_{strip}L_c(mA\ cm^{-2})} \quad (6)$$

where  $n_{strip}$  ( $= 5$ ) is the number of electrons associated with the reduction of one nitrite

per site,  $j_k = \frac{j_{lim} \times j}{j_{lim} - j}$  is the kinetic current density, where  $j_{lim}$  was taken as the current density achieved @0.2V versus RHE,  $L_c$  is the catalyst loading ( $0.27\ mg\ cm^{-2}$ ).

### 1.5 DTF calculations

The density functional theory (DFT) calculations were carried out employing the VASP<sup>2, 3</sup> within the generalized gradient approximation (GGA) using the Perdew-Burke-Ernzerhof (PBE)<sup>4</sup> formulation. The projected augmented wave (PAW) potentials<sup>5</sup> have been chosen to describe the ionic cores. Take valence electrons into account using a plane wave basis set with a kinetic energy cutoff of 520 eV. Partial occupancies of the Kohn-Sham orbitals were allowed using the Gaussian smearing method and a width of 0.05 eV. The electronic energy was considered self-consistent

when the energy change was smaller than  $10^{-5}$  eV. A geometry optimization was considered convergent when the energy change was smaller than 0.03 eV/Å. The Brillouin zone is sampled with  $3 \times 3 \times 1$  Monkhorst mesh.<sup>6</sup> Gibbs free energy can be obtained by adding corrections including entropic ( $TS$ ) and zero-point energy (ZPE) to calculated DFT energy, so that  $\Delta G = \Delta E_{\text{DFT}} + \Delta \text{ZPE} - T\Delta S - eU$ . where the  $E_{\text{DFT}}$  is the calculated DFT reaction energy,  $\Delta \text{ZPE}$  is the change in ZPE calculated from the vibrational frequencies and  $\Delta S$  is the change in the entropy referring to thermodynamics databases. The electrode potential is adopted with respect to the reversible hydrogen electrode, which makes the standard electrochemical potential of electron involved in reaction ( $G_e$ ) equal to  $-eU$ , and the standard electrochemical potential of the proton ( $G_{\text{H}^+}$ ) equal to that of the hydrogen atom in gaseous  $\text{H}_2$  ( $1/2G_{\text{H}_2}$ ). Considering that the triplet state of the  $\text{O}_2$  molecule is poorly described in the current DFT scheme, the free energy of the  $\text{O}_2$  molecule was derived according to  $G_{\text{O}_2} = 2G_{\text{H}_2\text{O}} - 2G_{\text{H}_2} + 4.92$ .

## 1.6 Zn-air battery and Fuel cell

### 1.6.1 Zn-air battery

**Aqueous ZABs measurement.** The aqueous Zn-air battery was assembled using a home-made two electrode device, in which the self-assembled sandwich-like structure electrode, made up of catalyst layer ( $1.0 \text{ cm} \times 1.0 \text{ cm cm}^{-2}$ ), water-proof breathable membrane and Ni foam layer, was adopted as the air cathode and a polished Zn plate (purity 99.9 wt%, 0.3 mm thickness) was used as the anode. The catalyst layer was prepared by sufficiently mixed catalyst (60 mg), acetylene black (10 mg) and the

polytetrafluoroethylene (PTFE) emulsion (60 wt%, 40  $\mu\text{L}$ ) in ethanol solution. Then, the catalyst layer was cut into 1.0 cm  $\times$  1.0 cm  $\text{cm}^{-2}$  pieces after removing excess ethanol at room temperature, and combined with water-proof breathable membrane and Ni foam layer form sandwich structure by roller press. 6M KOH + 0.2M Zn(Ac)<sub>2</sub> was used as electrolyte and applied in rechargeable ZABs. Meanwhile, the commercial Pt/C or Pt/C+RuO<sub>2</sub> catalyst was also used as air electrode for comparison. The galvanostatic curves (LSVs, scan rate of 5mV S<sup>-1</sup>) and the rate performance and discharge-charge cycling (10 min discharge, 1 min shelving, 10 min charge followed by 1 min shelving) stability were recorded by NEWARE testing system. Both the current density and power density were normalized to the effective surface area of air electrode.

**Quasi-solid-state ZABs measurement.** The structure of quasi-solid-state ZABs the same as that of aqueous ZABs, which are typical sandwich-like structures. The variation is that the as-prepared air electrode and Zn plate were placed on the two sides of PAM-based gel electrolyte. Moreover, the stack pressure was employed for maintain good interfacial contact during battery measurement.

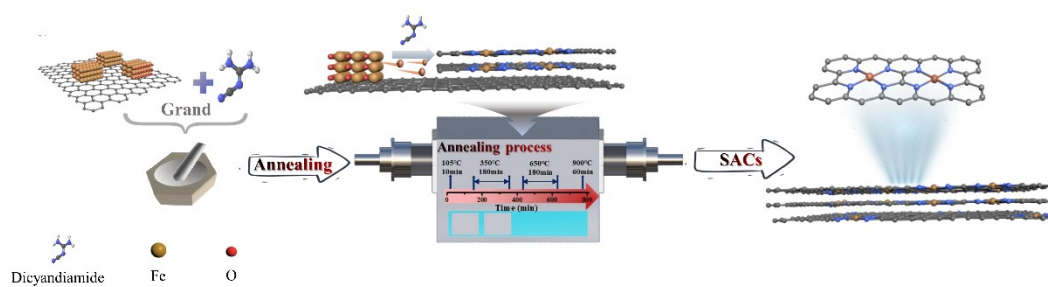
### ***1.6.2 Fuel cell test***

The performance of fuel cells was tested on a fuel cell fixture from Hephass Energy. Anhydrous H<sub>2</sub> (Industrial, BOC) and O<sub>2</sub> (High Purity, BOC) were fed to the fuel cell at a flow rate of 150 sccm and 100 sccm, respectively. Electrochemical measurements were conducted in a standard electrochemical cell using a Princeton potentiostat (Versastat3 , USA). Pt foil (3.0 cm<sup>2</sup>) and saturated calomel electrode (SCE) with electrolytic bridge were used as the counter and reference electrodes, respectively.<sup>7</sup>

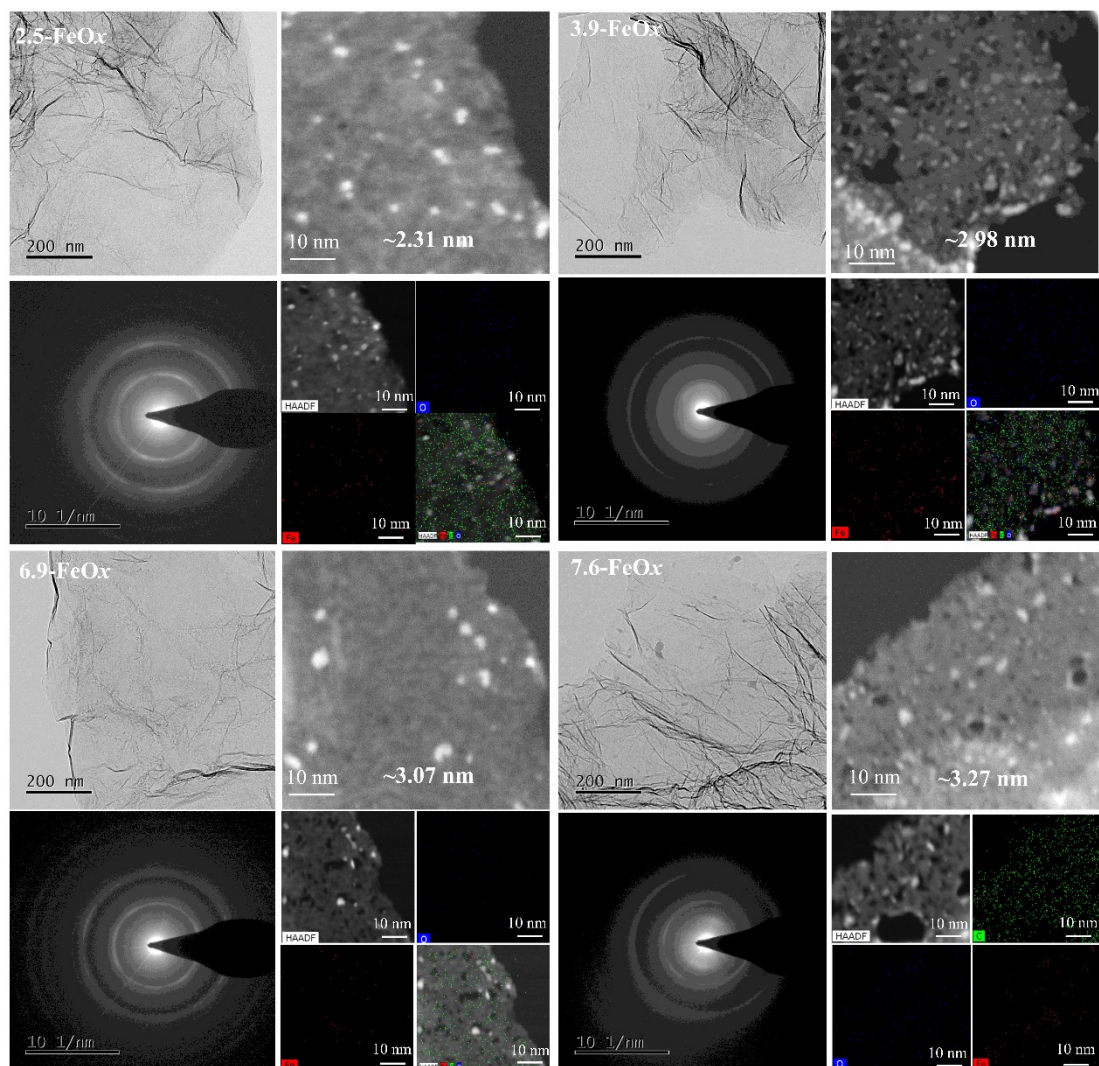


Membrane-electrode assemblies (MEAs) with an active area of 4 cm<sup>2</sup> were fabricated by sandwiching the phosphoric acid doped membrane between two pieces of gas diffusion electrodes with Pt/C anode and cathode followed by hot-pressing at 4.9 MPa and 180 °C for 10 minutes. The performance of PA/PBI/SiO<sub>2</sub>-based membrane cells was measured at 230 °C using a fuel cell fixture from Hephass Energy. Hydrogen (Industrial, BOC) at a flow rate of 100 mL min<sup>-1</sup> and oxygen (High Purity, BOC) at a flow rate of 100 mL min<sup>-1</sup> were supplied to the anode and cathode of the cell, respectively. Stability test of cells was undertaken at a cell voltage of 0.5 V and 160 °C using a flow rate of 100 mL min<sup>-1</sup> for H<sub>2</sub> in the anode and 100 mL min<sup>-1</sup> for oxygen in the cathode. For comparison, a fuel cell using Pt on both anode and cathode with Pt loading of 1.0 mg<sub>Pt</sub> cm<sup>-2</sup> has been assembled and tested following the same procedure.

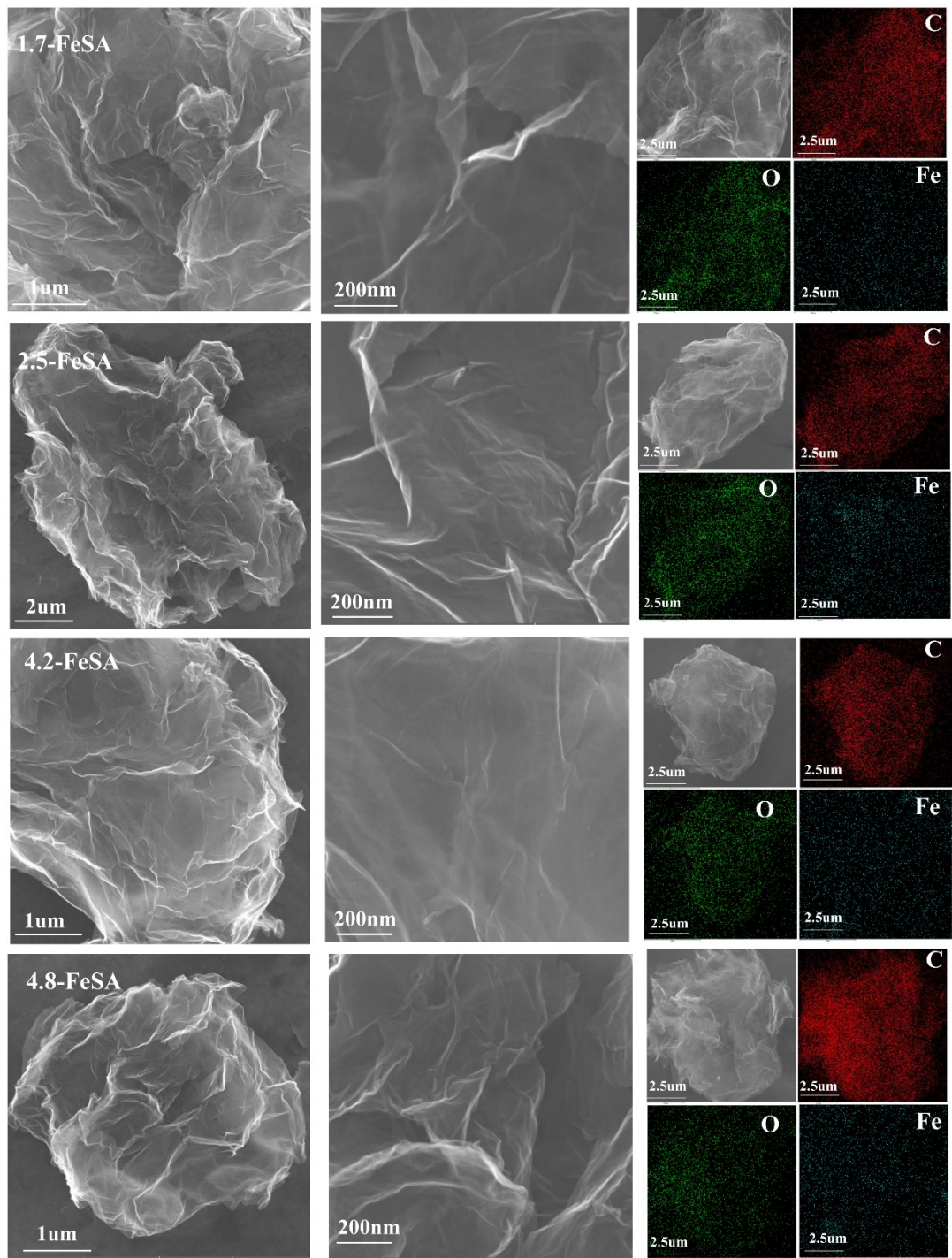
## 2 Supplementary Figures and Tables



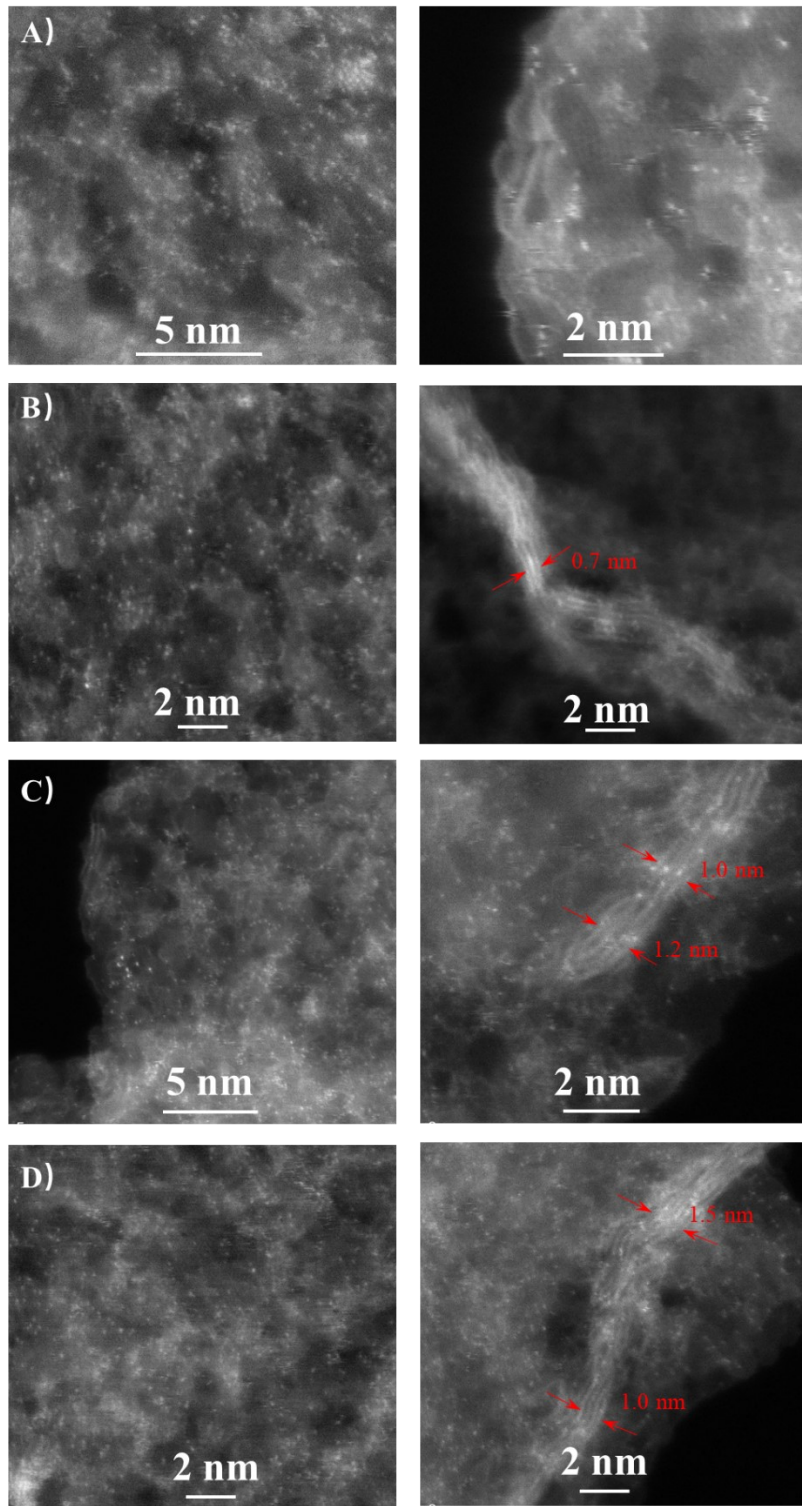
**Schematic S1.** A schematic illustration of synthetic route of the FeSA.



**Fig. S1.** The TEM image of FeOx.



**Fig. S2.** The SEM image of FeSA



**Fig. S3.** The AC-TEM image of 2.5-FeSA, 5-FeSA, 10-FeSA and 20-FeSA.

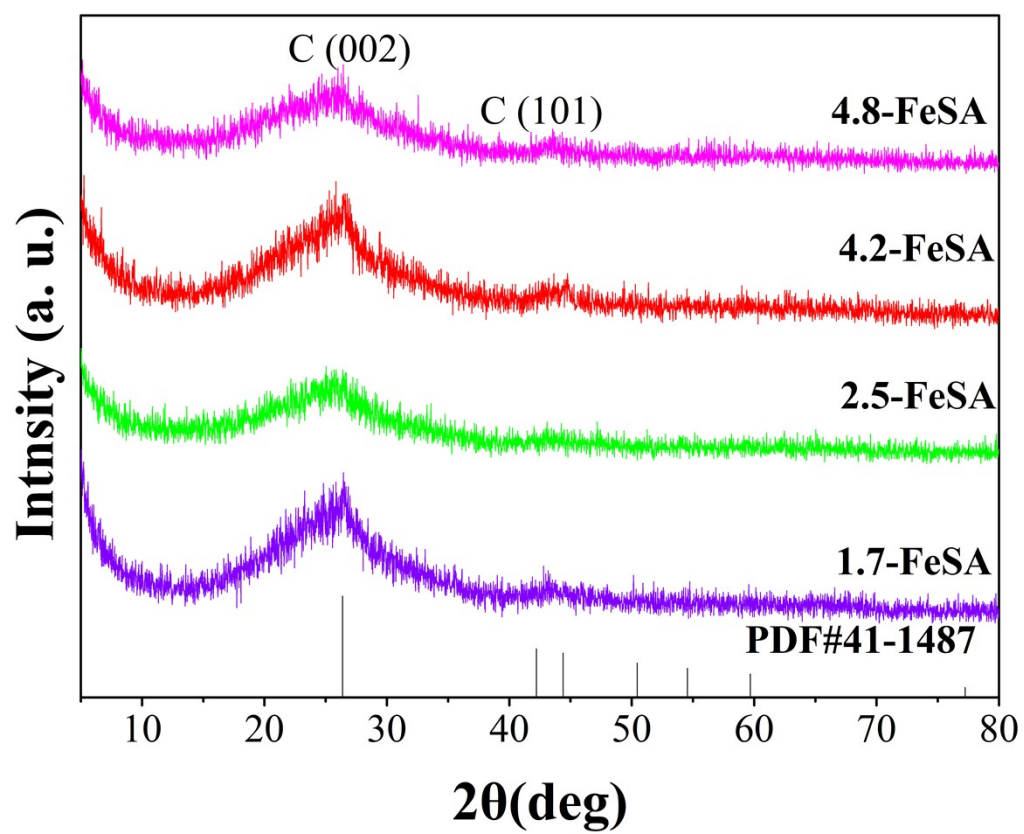
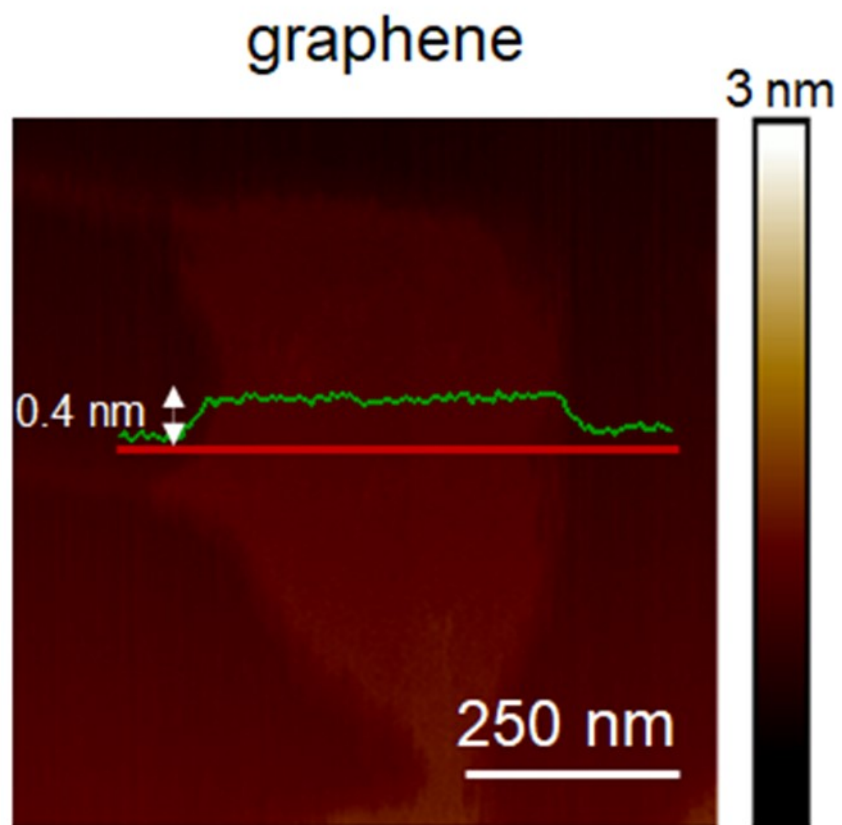
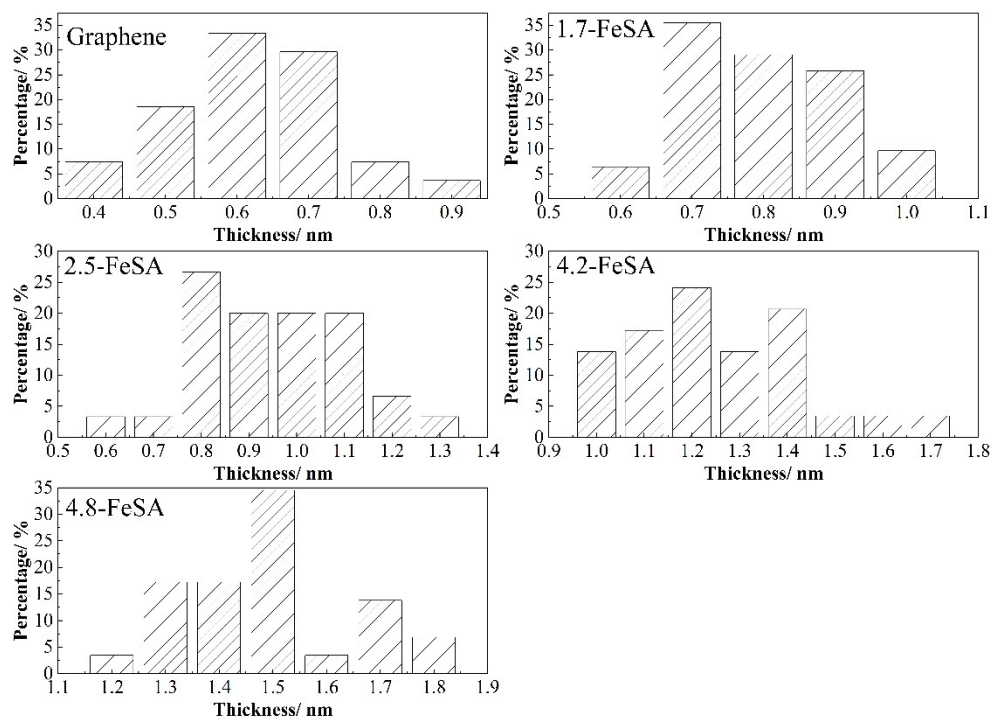


Fig. S4. The XRD of FeSA.

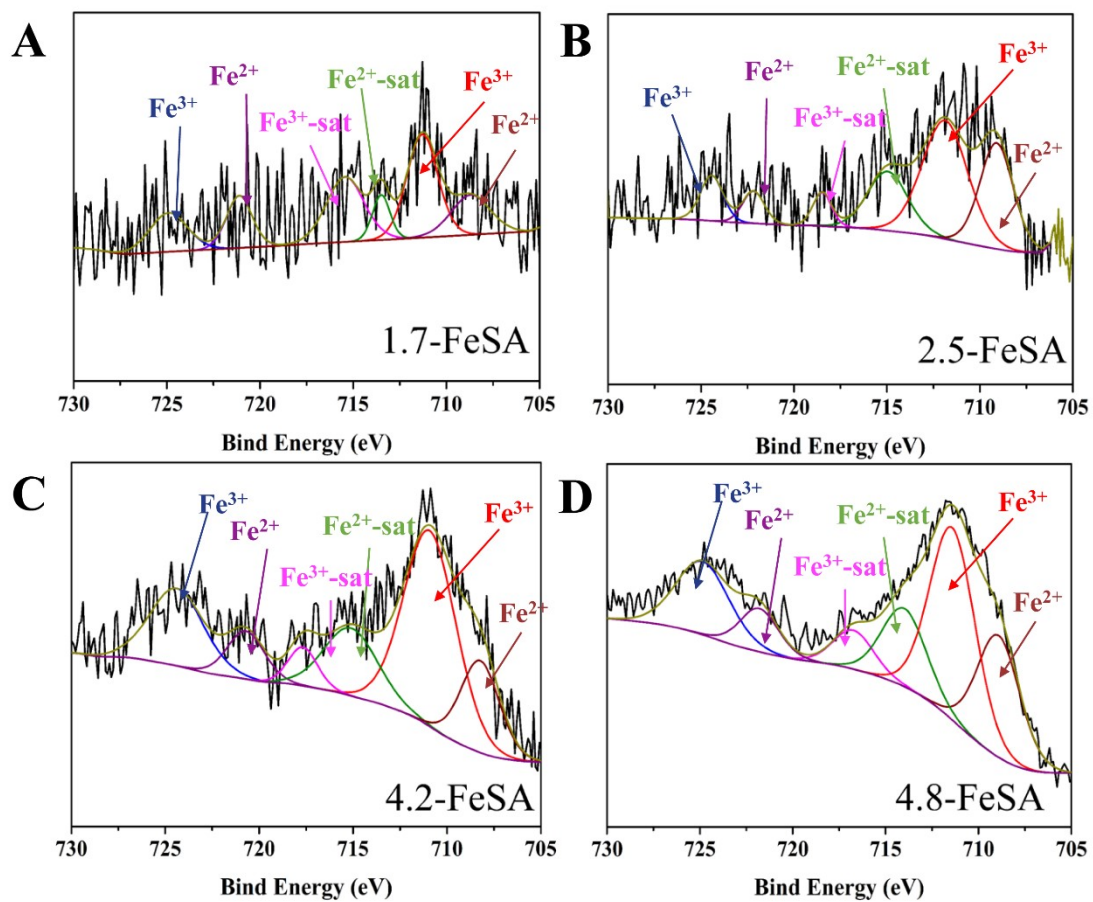


**Fig. S5** The AFM image of the pristine graphene.

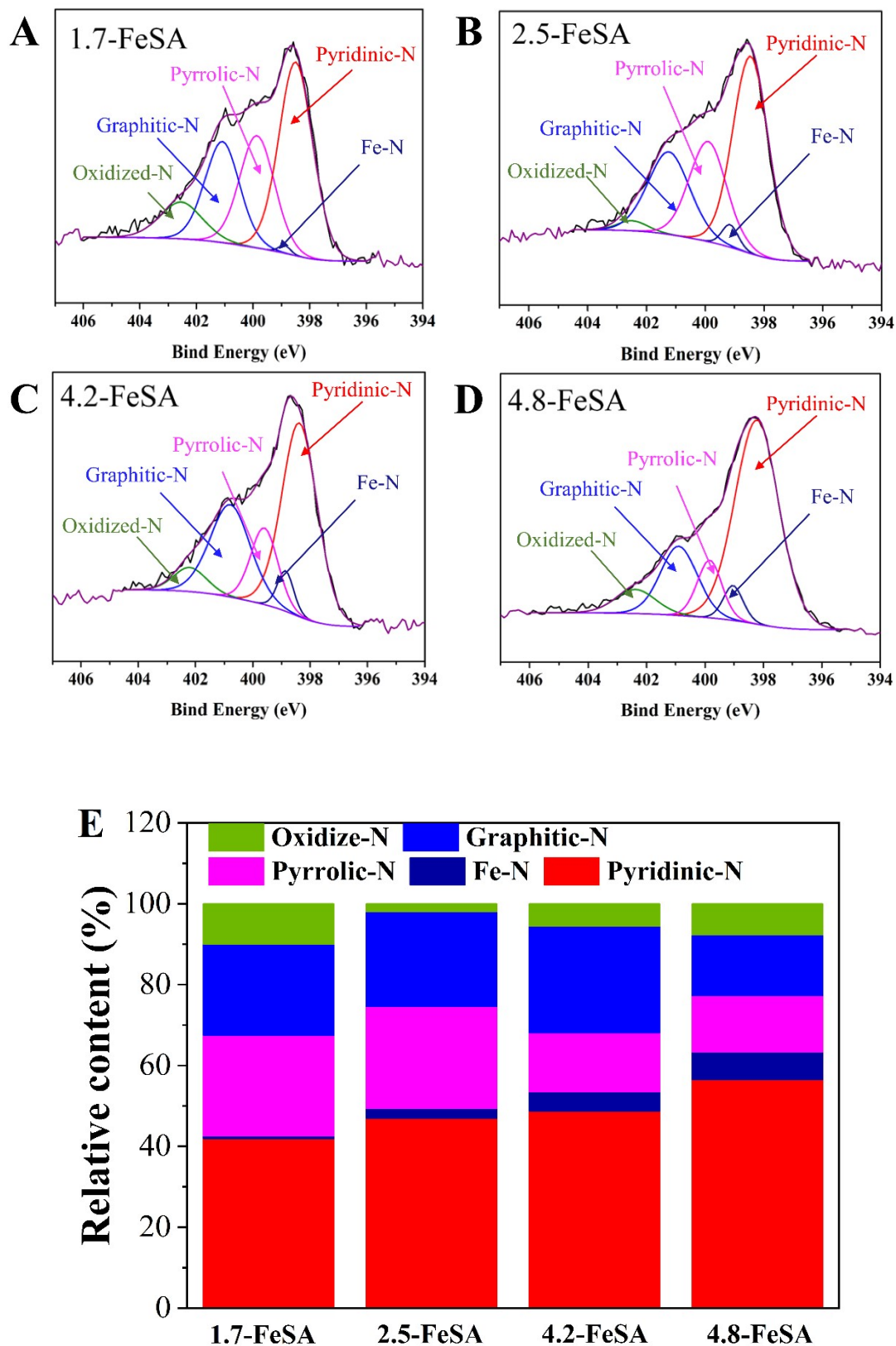


**Fig. S6** The thickness of the graphene sheets before and after supported with single atoms.

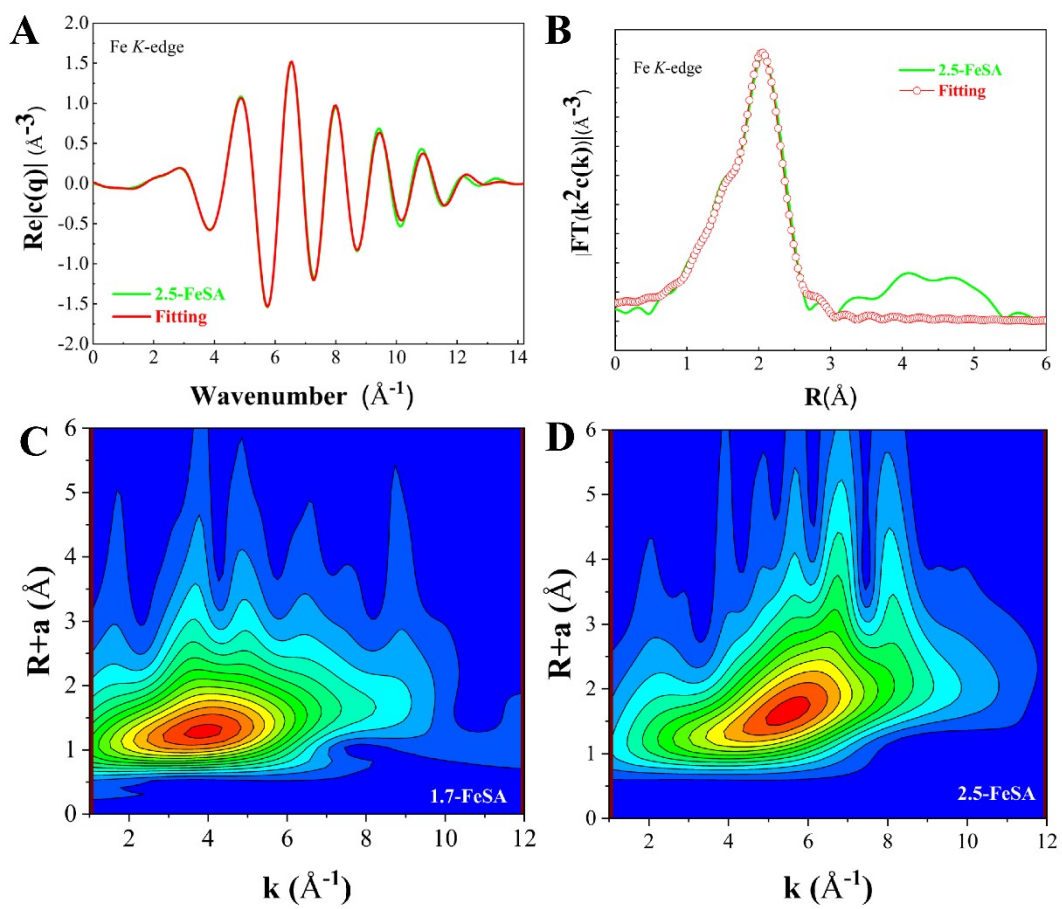




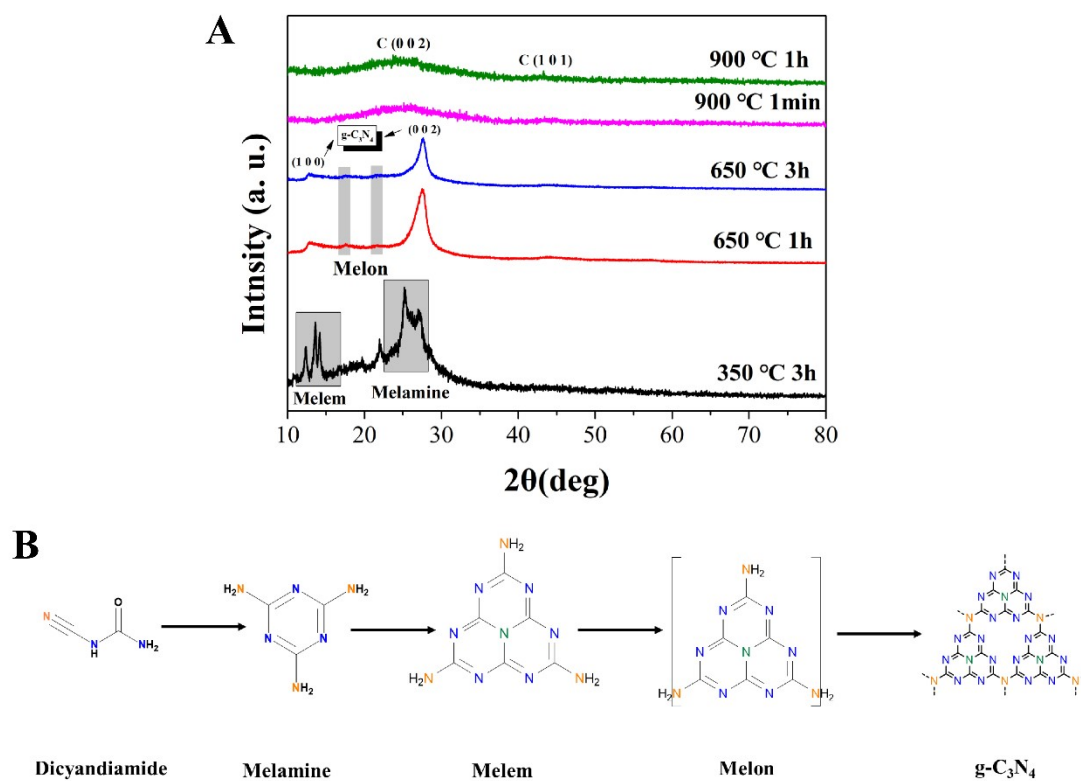
**Fig. S7.** The Fe 2p high resolution XPS spectra of FeSA (A-1.7-FeSA; B-2.5-FeSA; C-4.2-FeSA; D-4.8-FeSA)



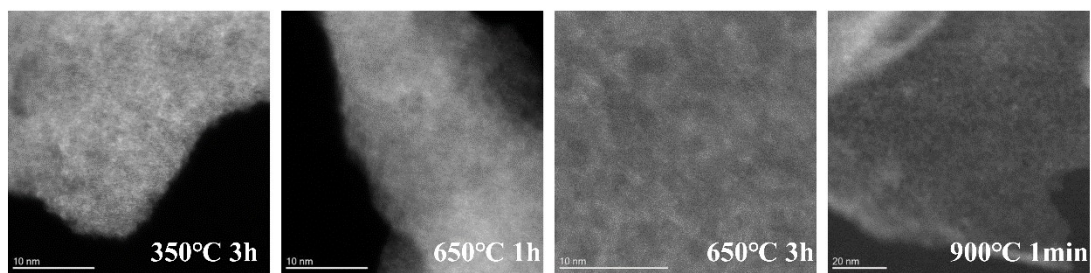
**Fig. S8.** The N 1s high resolution XPS spectra of FeSA (A-1.7-FeSA; B-2.5-FeSA; C-4.2-FeSA; D-4.8-FeSA), and the N relative content (%) of FeSA (E).



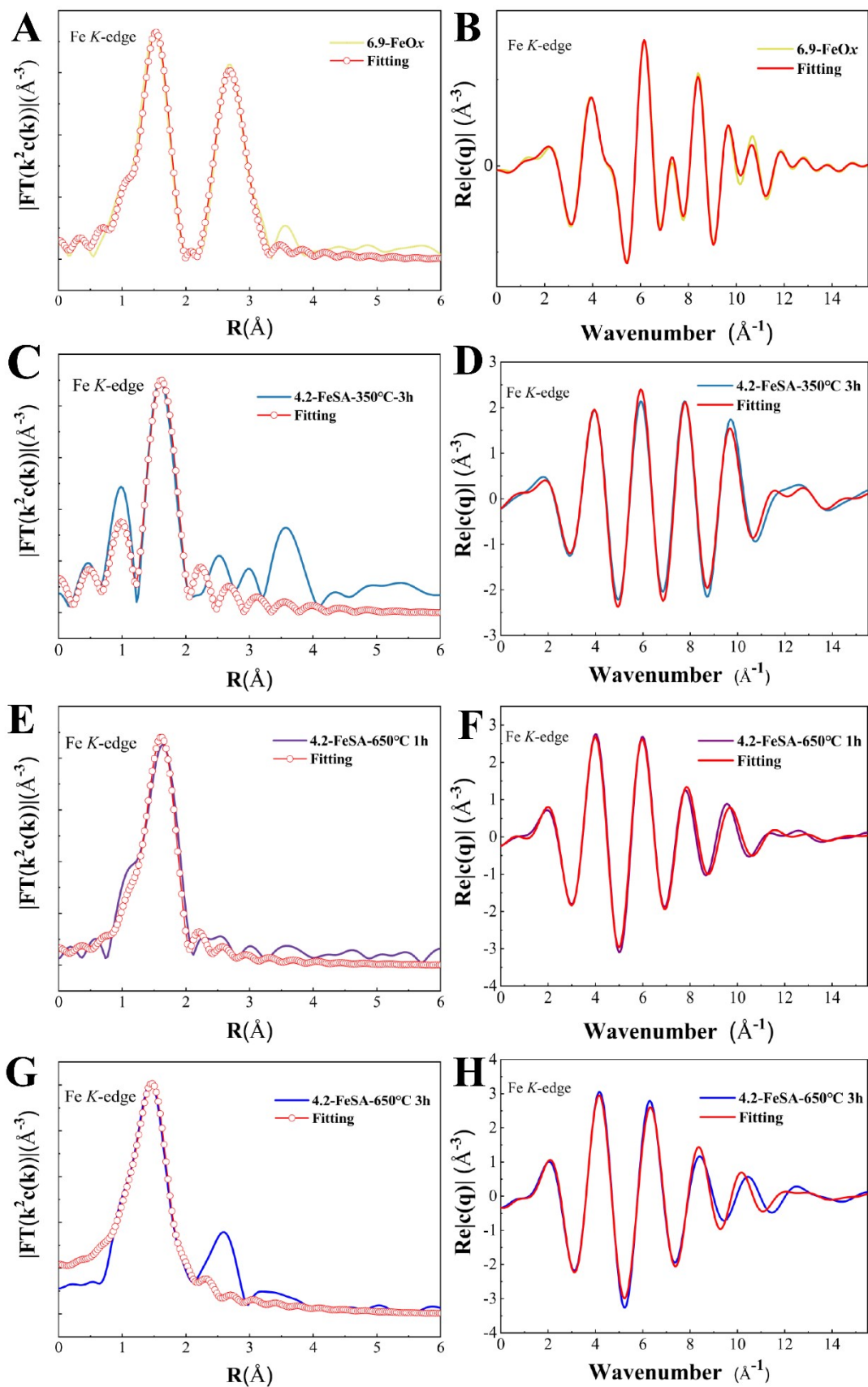
**Fig. S9.** Fitting results of the EXAFS spectra of 2.5-FeSA at R space (A) and K space (B), respectively. WT of the Fe K-edge of 1.7-FeSA (C) and 2.5-FeSA (D).



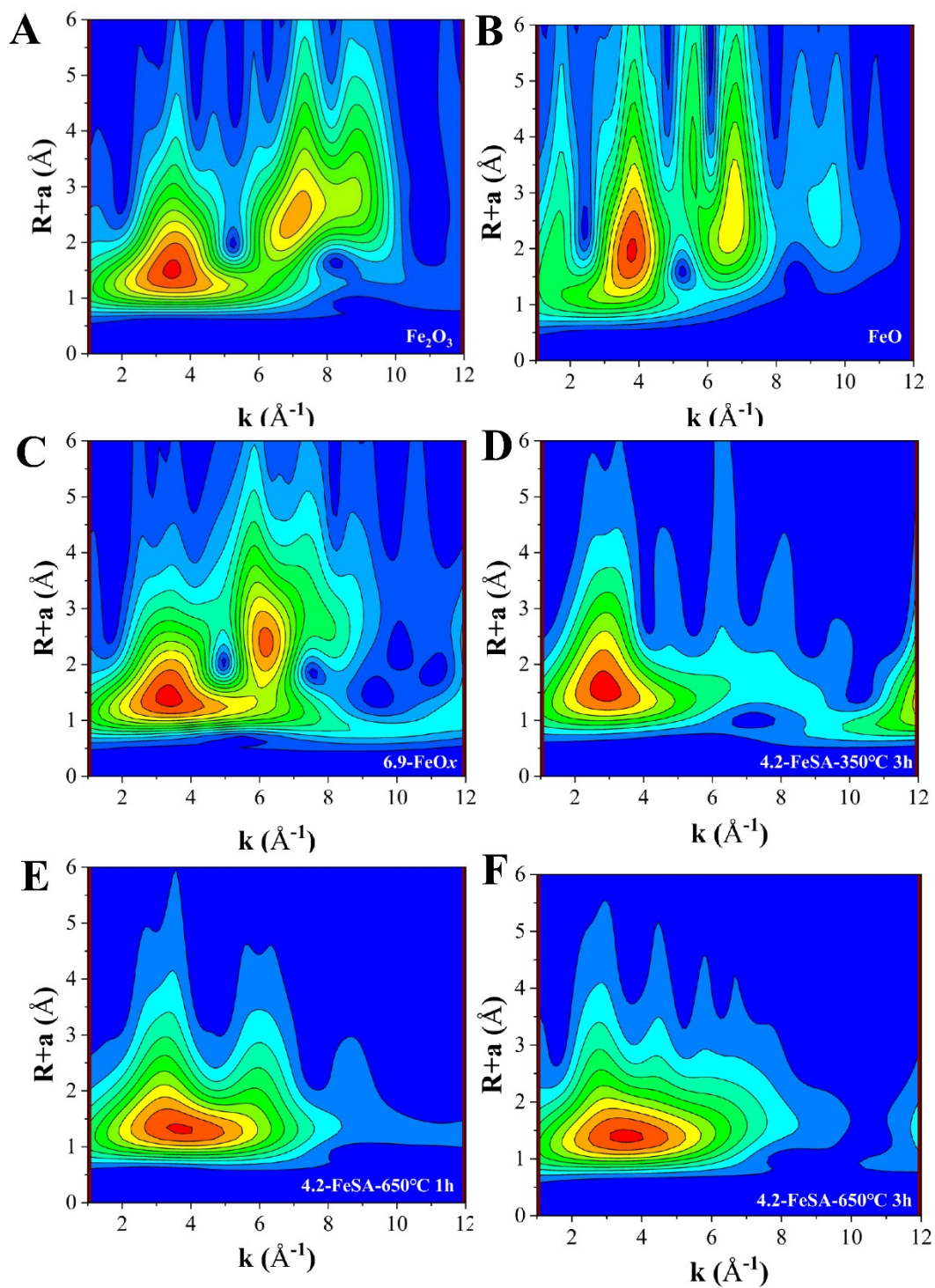
**Fig. S10.** The XRD results of 10-FeSA with different temperature (A) and the transformation of dicyandiamide in this experiment (B).



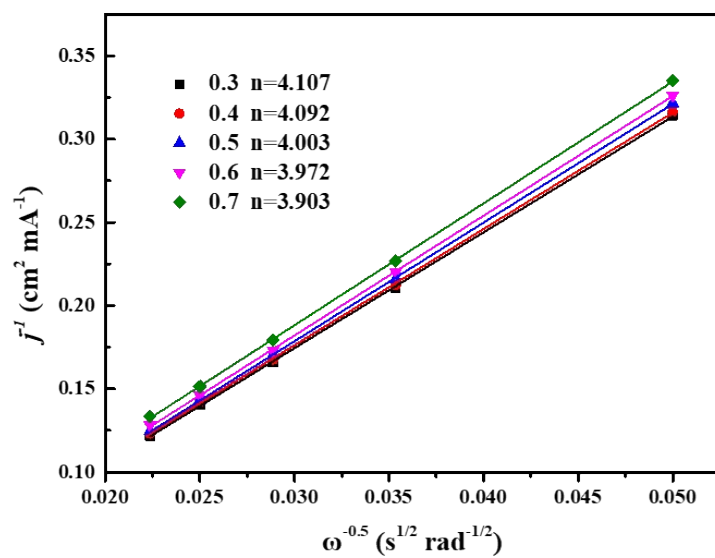
**Fig. S11.** The AC-STEM image of 4.2-FeSA at different temperature.



**Fig. S12.** In the process of pyrolysis, fitting results of the EXAFS spectra of 4.2-FeSA at R space (A, C, E, G) and K space (B, D, F, H), respectively

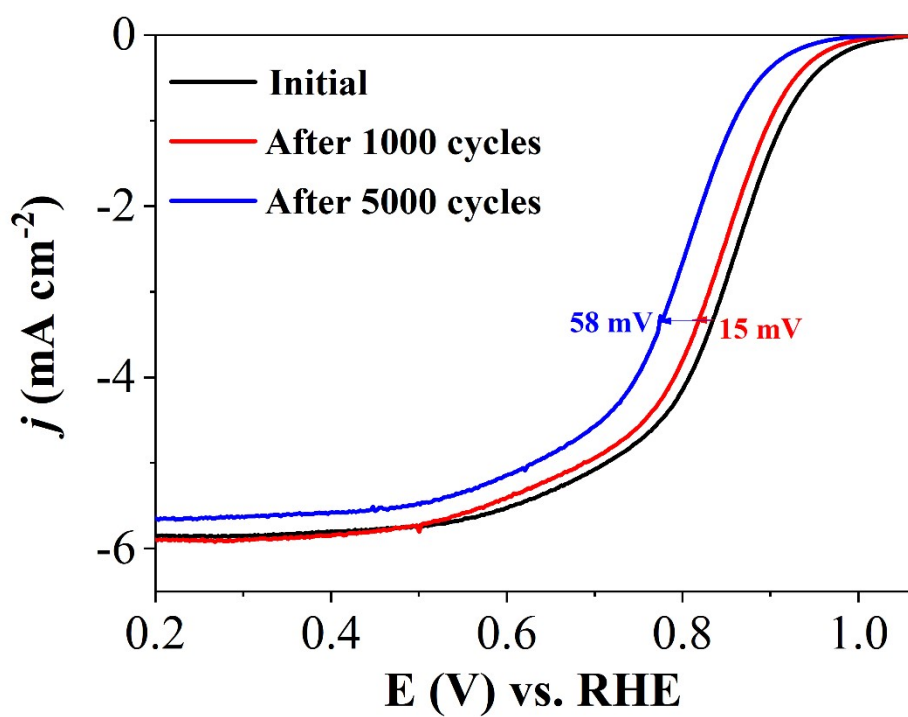


**Fig. S13.** In the process of pyrolysis, WT of the Fe K-edge of 4.2-FeSA, referenced  $\text{Fe}_2\text{O}_3$  and  $\text{FeO}$ .

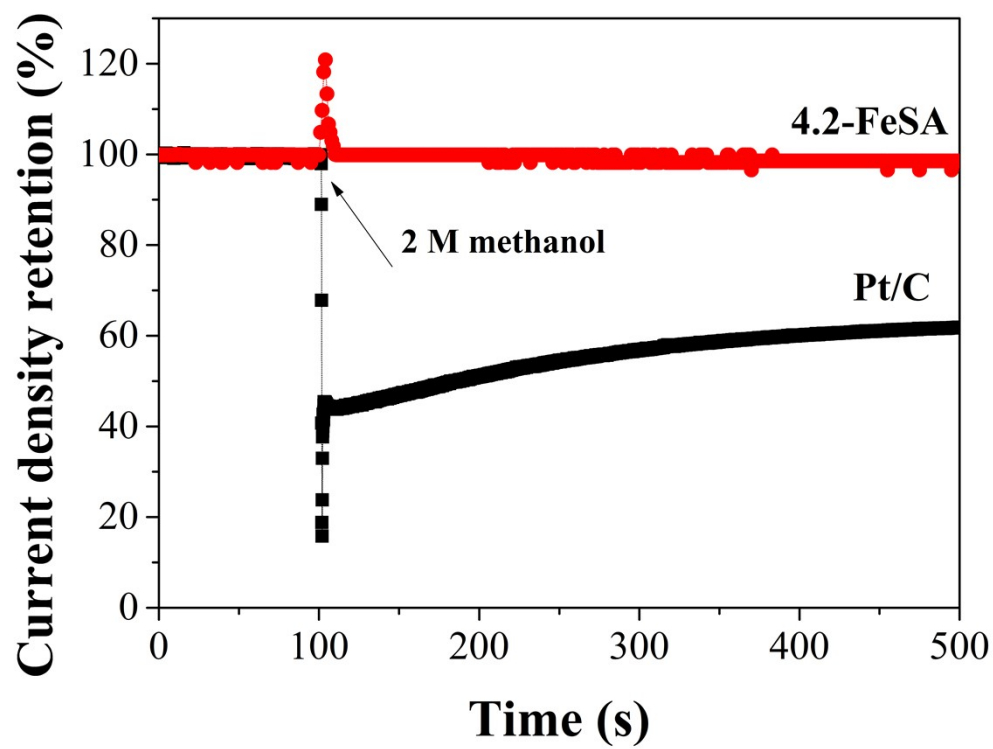


**Fig. S14.** The Koutecky-Levich (K-L) of 4.2-FeSA at potential 0.3, 0.4, 0.5, 0.6 and 0.7 V.

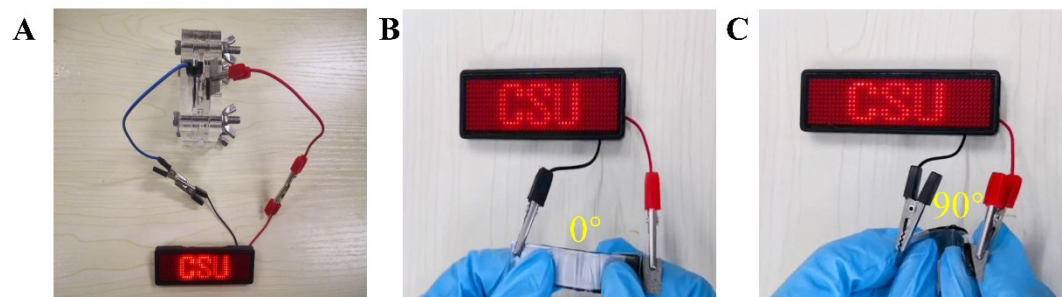




**Fig. S15** RDE polarization curves of Pt/C before and after 1,000 and 5,000 cycles of accelerated durability testing



**Fig. S16** Current density retention curves of 4.2-FeSA and Pt/C at 0.3 V in 0.1 m KOH with re-addition of 2 M methanol.



**Fig. S17** Photograph of aqueous (A) and quasi-solid-state (B and C) Zn-air batteries.

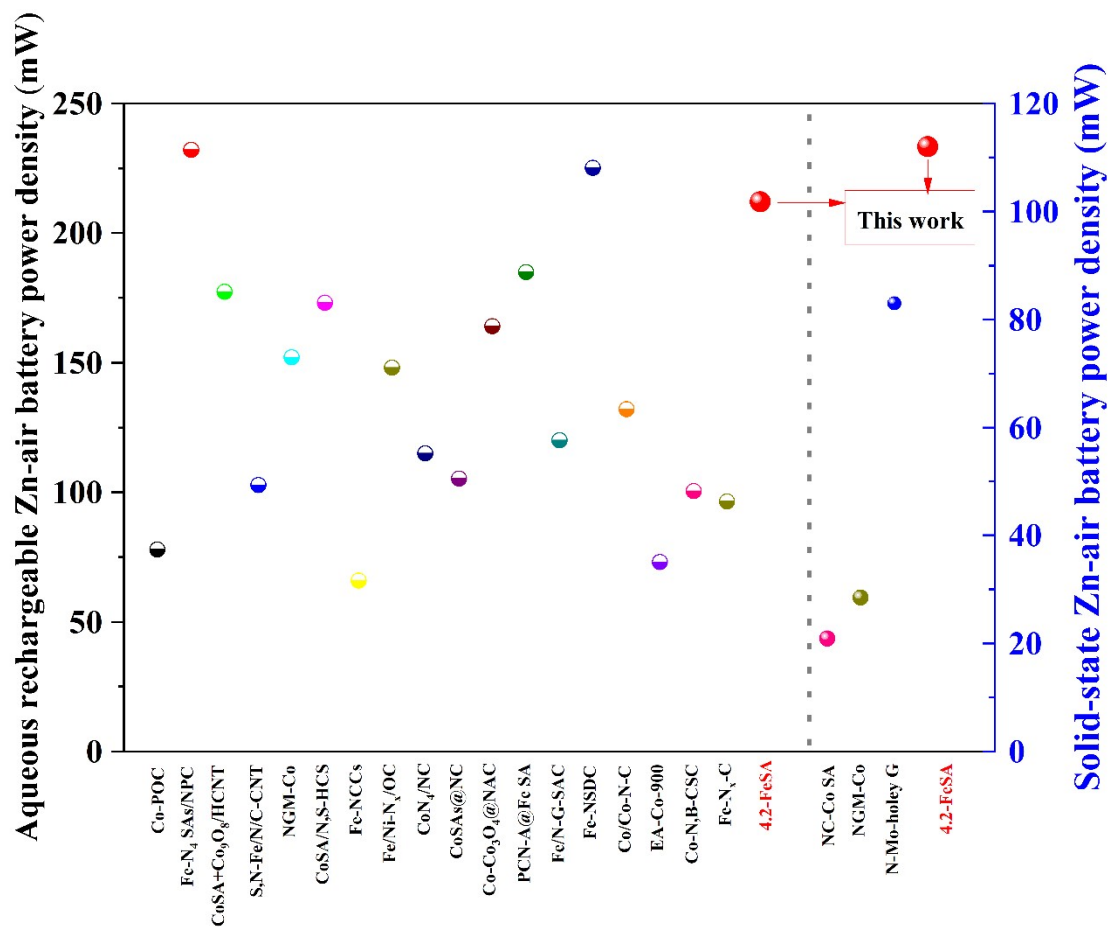
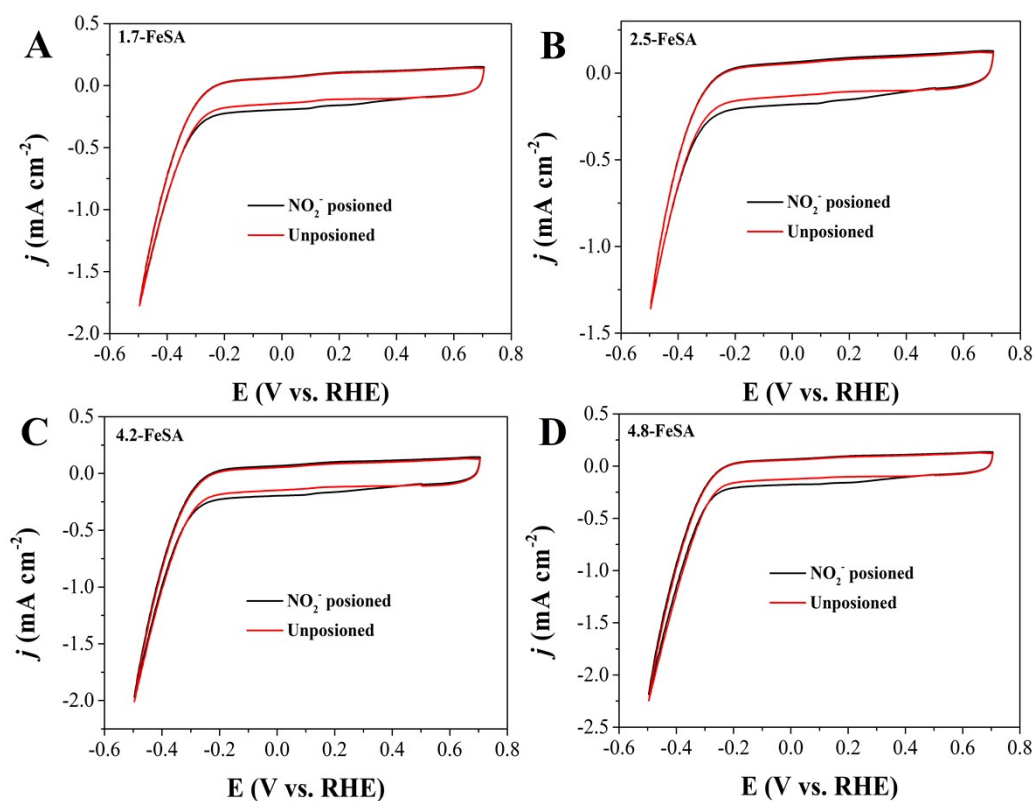
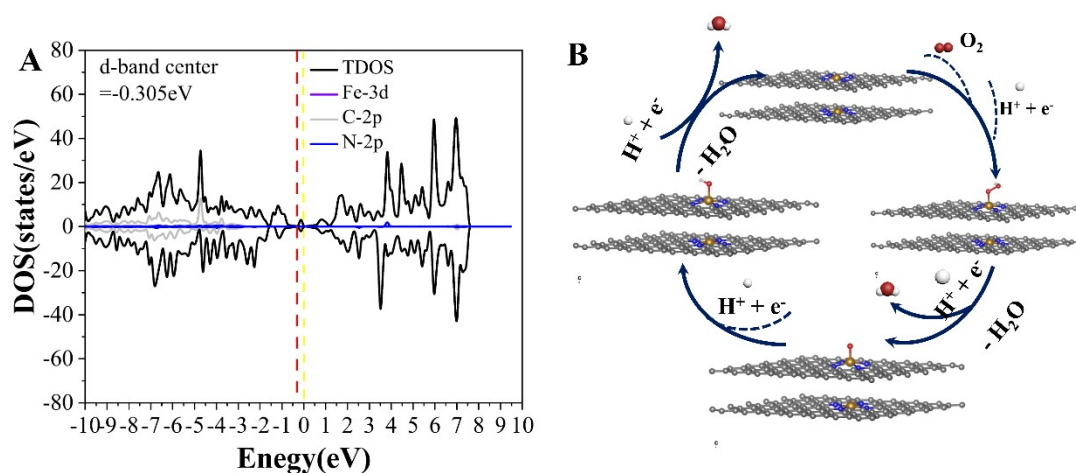


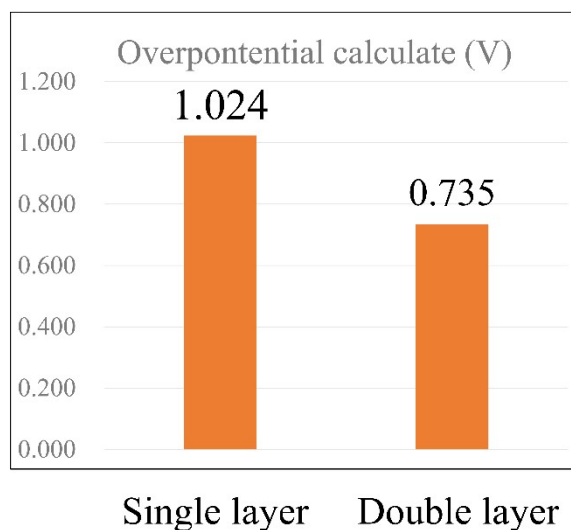
Fig. S18. The Maximum power density of 4.2-FeSA comparison with previous works.



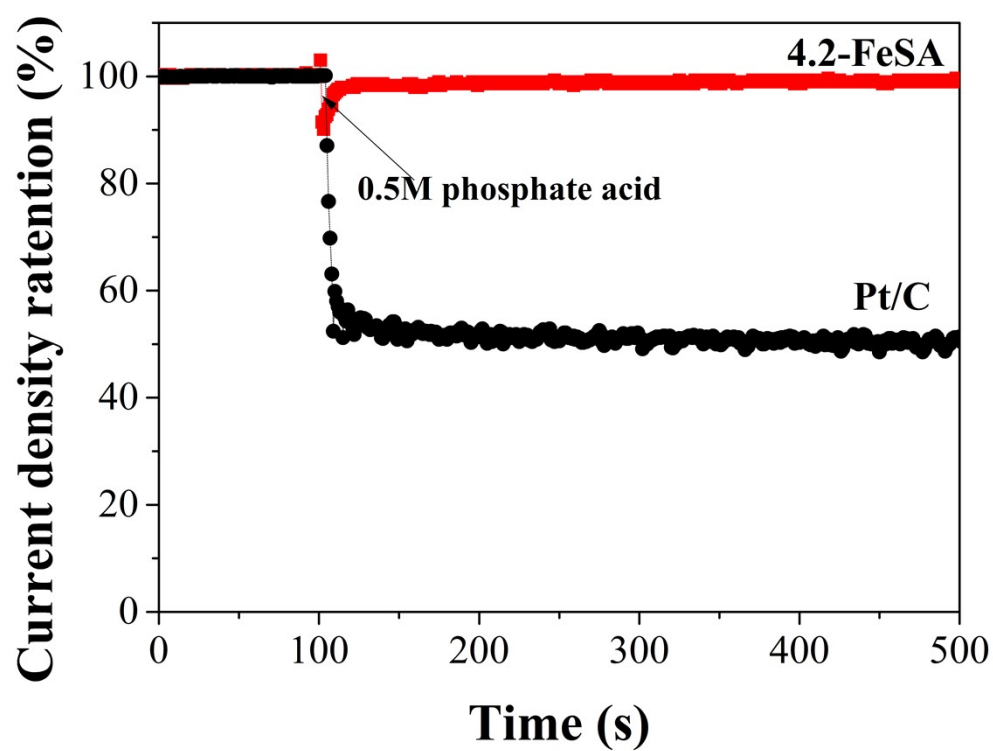
**Fig. S19** Determination of site density and turnover frequency of FeSA through reversible nitrite poisoning. CV curves before and during nitrite adsorption in the nitrite reductive stripping region in a 0.5 M acetate buffer at pH 5.2 (A-D).



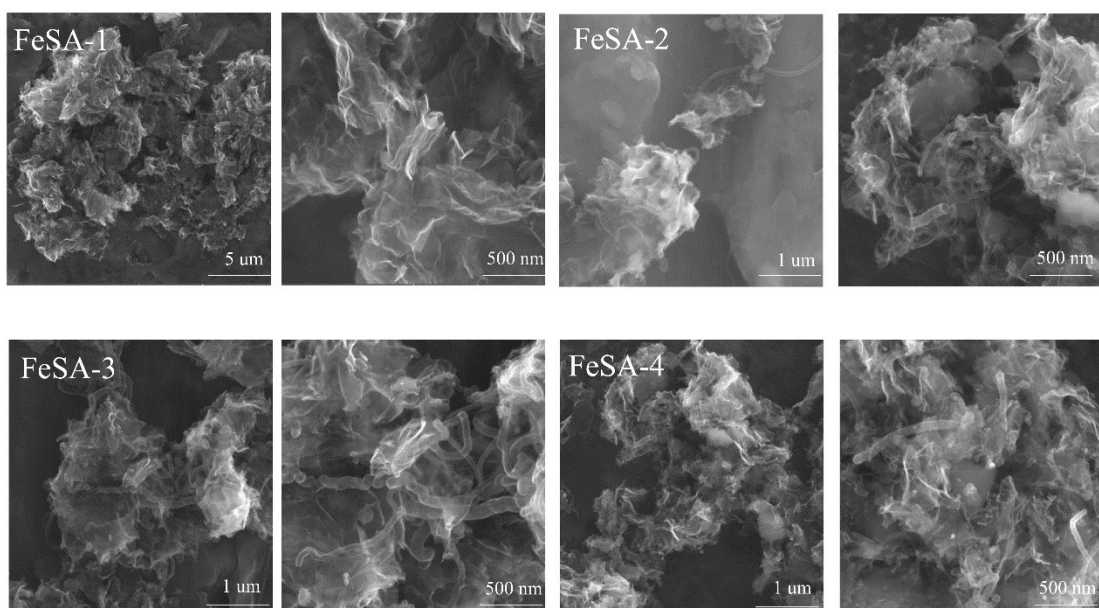
**Fig. S20** The density of state of single lauer FeN<sub>4</sub> (A) and the ORR catalytic cycle path on duble layer FeN<sub>4</sub> (B).



**Fig. S21** The overpotential calculated from DFT simulation reveal that the overpotential for doublbe layer active center exhibit significantly lower overpotential in comparison to single layer.

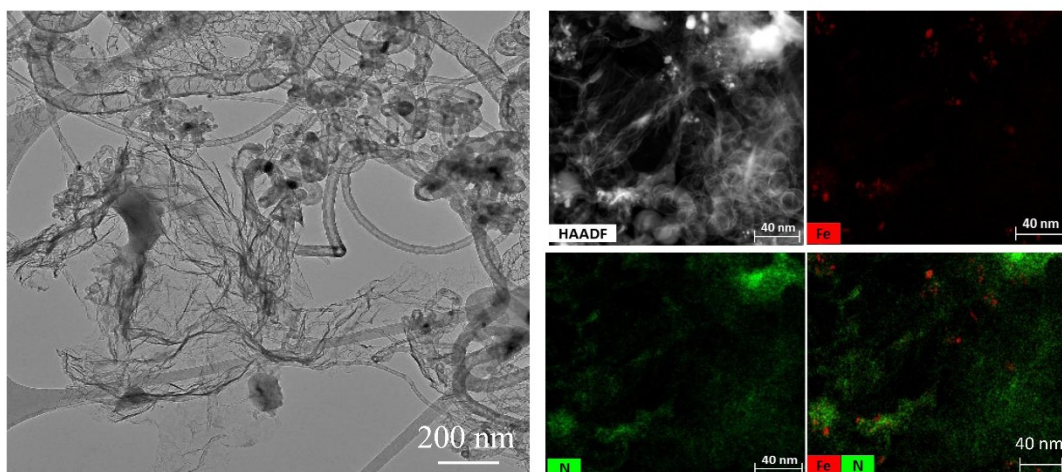


**Fig. S22** Current density retention curves of 4.2-FeSA and Pt/C at 0.3 V in 0.1 m HClO<sub>4</sub> with re-addition of 0.5 M phosphate acid.

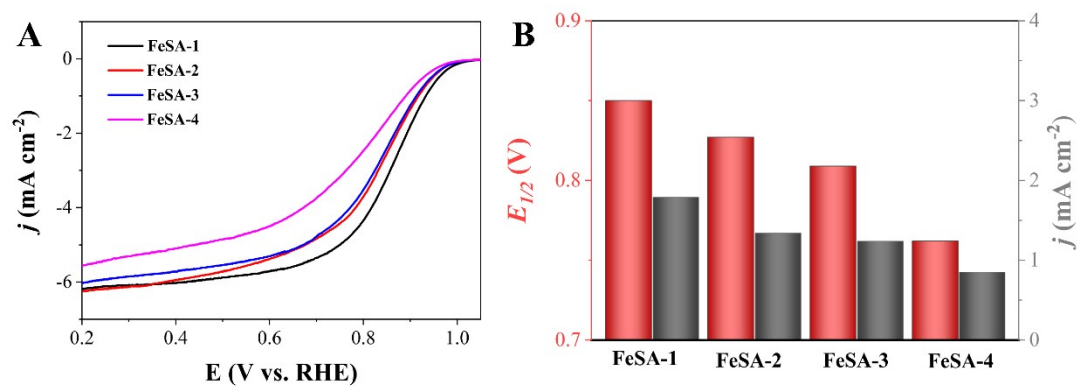


**Fig. S23** The SEM image of FeSA through pyrolysis a blend of metal\nitrogen\carbon precursors (iron acetylacetonate,  $C_2H_4N_4$  and graphene) with the same precursor amount of  $x$ -FeSA.

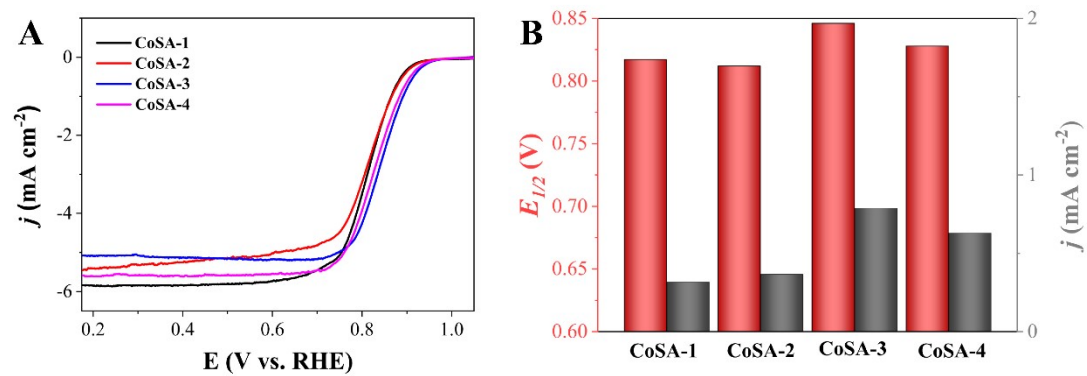




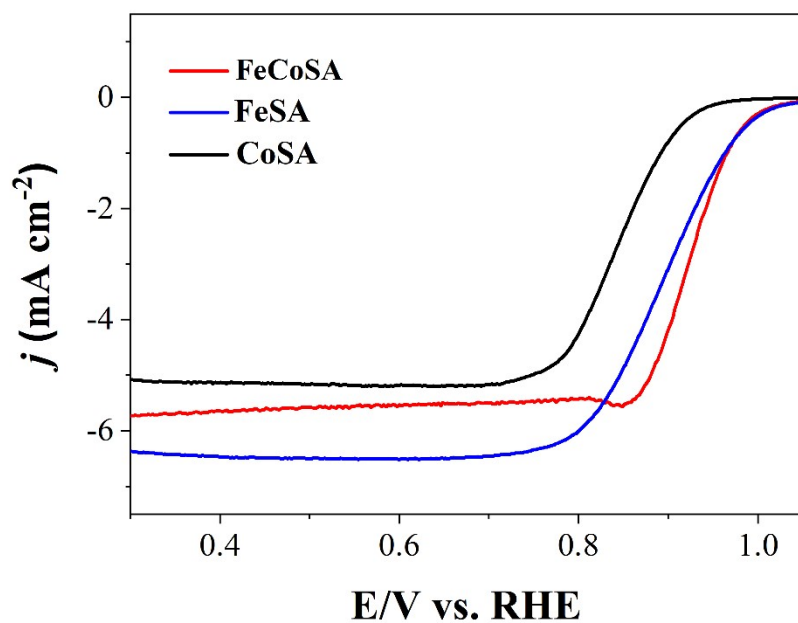
**Fig. S24** The elemental mapping images and TEM image of FeSA-3.



**Fig. S25** The RDE polarization curves of Pt/C, FeSA-1, FeSA-2, FeSA-3 and FeSA-4 in 0.1 M KOH. Scan rate: 5 mV s<sup>-1</sup> (A); comparison of the kinetic current density at 0.9V ( $J_k$ ) and  $E_{1/2}$  (B).



**Fig. S26** The RDE polarization curves of Pt/C, CoSA-1, CoSA-2, CoSA-3 and CoSA-4 in 0.1 M KOH. Scan rate: 5 mV s<sup>-1</sup> (A); comparison of the kinetic current density at 0.9V ( $J_k$ ) and  $E_{1/2}$  (B).



**Fig. S27** The RDE polarization curves of FeSA, CoSA and FeCoSA in 0.1 M KOH.  
Scan rate:  $5 \text{ mV s}^{-1}$

**Table S1.** The Fe content of FeOx

<b>Sample</b>	<b>Loading by ICP-OES</b>
<b>2.5-FeOx</b>	2.5wt%
<b>3.9-FeOx</b>	3.9wt%
<b>6.9-FeOx</b>	6.9wt%
<b>7.6-FeOx</b>	7.6wt%

**Table S2.** The average thickness of graphene, 1.7-FeSA, 2.5-FeSA, 4.2-FeSA and 4.8-FeSA, and the Fe content of FeSA.

<b>Sample</b>	<b>Average thickness of 30 sections (nm)</b>	<b>Loading by ICP-OES</b>
Graphene	0.632857nm	
1.7-FeSA	0.801563nm	1.7wt%
2.5-FeSA	0.945nm	2.5wt%
4.2-FeSA	1.24333nm	4.2wt%
4.8-FeSA	1.47667nm	4.8wt%

**Table S3.** XPS elemental surface analysis.

<b>Catalysts</b>	<b>pyridinic N (content %)</b>	<b>Fe-N (content %)</b>	<b>pyrrolic N (content %)</b>	<b>graphitic N (content %)</b>	<b>oxidized N (content %)</b>
1.7-FeSA	41.93	0.58	24.98	22.509	9.997
2.5-FeSA	46.94	2.478	25.127	23.421	2.03
4.2-FeSA	48.746	4.717	14.596	26.411	5.528
4.8-FeSA	56.444	6.9	13.937	15.033	7.677

**Table S4.** Structural parameters of the samples obtained from EXAFS fitting.

<b>Sample</b>	<b>Bond type</b>	<b>N</b>	<b>R (Å)</b>	<b><math>\Delta E_0</math> (eV)</b>	<b><math>\sigma^2 \times 10^3</math> (Å<sup>2</sup>)</b>	<b>R-factor</b>
1.7-FeSA	Fe-N	3.5	2.07±0.02	12.7±3.8	17.0±1.0	0.0147
	Fe-C	2.2	2.47±0.03	10.8±5.7	12.1±3.1	
2.5-FeSA	Fe-N	3.6	1.97±0.01	3.7±6.3	28.9±1.5	0.0025
	Fe-Fe	1.0±0.1	2.48±0.01	13.0±3.0	5.4±13.5	
	Fe-C	1.7±0.3	2.64±0.01	4.2±2.6	5.4±13.5	
4.2-FeSA	Fe-N	3.7	2.02±0.01	8.1±9.0	28.5±2.7	0.0027
	Fe-Fe	0.9±0.2	2.48±0.01	14.6±5.2	4.6±1.9	
	Fe-C	1.8±0.5	2.64±0.01	5.5±4.3	4.6±1.9	

N, coordination number; R, distance between absorber and backscatter atoms;  $\Delta E_0$ , inner potential correction to account for the difference in the inner potential between the sample and the reference compound.  $\sigma^2$ , Debye–Waller factor;  $S_0^2$  fitting from Fe sample defined as 0.75.

**Table S5** Structural parameters of the samples obtained from EXAFS fitting.

<b>Sample</b>	<b>Bond type</b>	<b>N</b>	<b>R (Å)</b>	<b><math>\Delta E_0</math> (eV)</b>	<b><math>\sigma^2 \times 10^3</math> (Å<sup>2</sup>)</b>	<b>R-factor</b>
6.9-FeOx	Fe-O	4.7±0.5	2.00±0.01	-2.8±1.3	6.9±1.8	0.0081
	Fe-Fe	4.3±1.0	3.09±0.01	-0.5±2.1	7.8±2.3	
4.2-FeSA- 350°C 3h	Fe-N	1.0	1.94±0.02	-30.6±9.6	4.2±1.7	0.014
	Fe-O	3.0	2.05±0.02	-6.1±2.8	4.2±1.7	
4.2-FeSA- 650°C 1h	Fe-/N	3.0	2.02±0.02	-2.2±5.3	6.9±2.0	0.014
	Fe-O	1.1	2.14±0.01	3.6±4.9	5.5±1.9	
4.2-FeSA- 650°C 3h	Fe-C/N	6.6±0.9	2.00±0.01	-2.1±1.6	10.8±2.3	0.013

N, coordination number; R, distance between absorber and backscatter atoms;  $\Delta E_0$ , inner potential correction to account for the difference in the inner potential between the sample and the reference compound.  $\sigma^2$ , Debye–Waller factor;  $S_0^2$  fitting from Fe sample defined as 0.85.



**Table S6.** Summary of various recently reported advanced ORR electrocatalysts in 0.1M KOH.

Materials	Loading (mg cm <sup>-2</sup> )	E <sub>1/2</sub> (V)	Metal loading (wt%)	Synthesis strategy	REF.
FeAB-O	0.2	0.9	/	Coordination chemistry	Nat. Commun. (2020) <sup>8</sup>
N/Fe-CG	0.17	0.86	/	Electrospinning based approach	Nano energy (2019) <sup>9</sup>
Cu/C	0.4	0.847	5.4 (Cu)	Unique confined self-initiated dispersing protocol	Nano energy (2019) <sup>10</sup>
Fe-SAs/NPS-HC	0.1	0.912	1.54 (Fe)	Novel MOF@polymer	Nat. Commun. (2018) <sup>11</sup>
A-CoPt-NC	0.262	0.96	1.72 (Co)/0.16 (Pt)	Metal–organic framework derived single-atom catalyst, electrochemically activation	J. Am. Chem. Soc. (2018) <sup>12</sup>
Cu SAs/N-C-900	0.102	0.87	1.9 (Co)	Ionic exchange	Small (2020) <sup>13</sup>
Co-pyridinic N-C	0.25	0.87	2.14 (Co)	Modification of a lysozyme-modified zeolitic imidazolate framework	Adv. Energy Mater. (2020) <sup>14</sup>
Fe/Mn-Nx-C	0.396	0.88	/	Metal ions adsorption, pyrolysis	Appl. Catal. B (2021) <sup>15</sup>
Fe <sub>SA</sub> -N-C	0.28	0.891	1.76 (Fe)	Mixed-ligand strategy in MOF system	Angew. Chem. Int. Ed. (2018) <sup>16</sup>
SA-Fe/NHPC	0.1	0.87	/	Utilizing the biomass resources	Small (2017) <sup>17</sup>
Cu-SA/SNC	0.102	0.893	4.5 (Cu)	Atomic interfacial engineering	Energy Environ. Sci. (2019) <sup>18</sup>
Fe-N-C-1	0.5	0.88	5.64 (Fe)	Controlling the annealing rate of metal precursor at 1 °C/min	Angew. Chem. Int. Ed. (2019) <sup>19</sup>
CAN-Pc (Fe/Co)	0.2	0.84	10.7 (Fe/Co)	One-step ball milling method	Angew. Chem. Int. Ed. (2019) <sup>20</sup>
PSTA-Co-1000	0.142	0.878	/	Template-free approach to construct cross-linked polyphosphazene nano-spheres with tunable hollow structures	Angew. Chem. Int. Ed. (2020) <sup>21</sup>
Zn/CoN-C	0.2551	0.861	0.33 (Zn)/0.14 (Co)	Competitive complexation	Angew. Chem. Int. Ed. (2019) <sup>22</sup>
Fe-ISA/NC	0.51	0.896	0.947 (Fe)	Pyrrole–thiophene copolymer pyrolysis	Adv. Mater. (2018) <sup>23</sup>
FeSAs/NSC	0.2	0.87	0.87 (Fe)	Template-assisted method	J. Am. Chem. Soc. (2019) <sup>24</sup>
Fe SAs-N/C-20	0.408	0.909	0.2 (Fe)	Metal–organic framework derived single-atom catalyst	J. Am. Chem. Soc. (2018) <sup>25</sup>
Pt/NBF-ReS <sub>2</sub> /Mo <sub>2</sub> CT	0.204	0.911	1.26 (Pt)	Wet chemistry, pyrolysis	Energy Storage Mater. (2021) <sup>26</sup>

Fe <sup>x</sup> /OES	0.4	0.85	0.11 (Fe)	Silica-mediated MOF-templated	Angew. Chem. Int. Ed. (2020) <sup>27</sup>
Co <sub>1</sub> -N <sub>3</sub> PS/HC	0.51	0.92	0.39 (Co)	Metal–organic framework derived single-atom catalyst	Angew. Chem. Int. Ed. (2021) <sup>28</sup>
4.2-FeSA	0.408	0.901	4.2	In-situ atomization of metal oxide nanoparticles	This work
FeCoSA	0.408	0.924	5.2 (Fe)/0.4 (Co)	In-situ atomization of metal oxide nanoparticles	This work

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**Table S7.** Summary of single atom catalyzed in zinc-air batteries

Materials	Open circuit voltage (V)	Power density (mw cm <sup>-2</sup> )	Durability	REF.
4.2-FeSA	1.60	212	450h@5 mA cm <sup>-2</sup> for 2200 cycles	This work
Co-POC	/	78	2 mA cm <sup>-2</sup> for 25 cycles	Adv. Mater. (2019) <sup>29</sup>
Fe-N <sub>4</sub> SAs/NPC	/	232	36h@2 mA cm <sup>-2</sup> for 108 cycles	Angew. Chem. Int. Ed. (2018) <sup>30</sup>
CoSA+ Co <sub>9</sub> S <sub>8</sub> /HCNT	1.45	177.33	5 mA cm <sup>-2</sup> for 24h	Small (2020) <sup>31</sup>
S, N-Fe/N/C-CNT	1.35	102.7	5 mA cm <sup>-2</sup> for 100 cycles	Angew. Chem. Int. Ed. (2017) <sup>32</sup>
NGM-Co	1.439	152	60h@2 mA cm <sup>-2</sup> for 180 cycles	Adv. Mater. (2017) <sup>33</sup>
CoSA/N, S-HCS	1.5	173.1	320h@10 mA cm <sup>-2</sup> for 1000 cycles	Adv. Energy Mater. (2020) <sup>34</sup>
Fe-NCCs	1.36	66	/	ACS Appl. Energy Mater. (2018) <sup>35</sup>
Fe/Ni-N <sub>x</sub> /OC	1.525	148	/	Adv. Mater. (2020) <sup>36</sup>
CoN <sub>4</sub> /NG	1.51	115	100h@10 mA cm <sup>-2</sup>	Nano energy (2018) <sup>37</sup>
Fe SAs/MC (950)	1.521	/	100h@5 mA cm <sup>-2</sup>	ACS Energy Lett. (2018) <sup>38</sup>
N-Mo-holely G	1.37	83	(Solid-State) 80h@2 mA cm <sup>-2</sup> for 500 cycles	Appl. Catal. B (2020) <sup>39</sup>
CoSAs@NC	1.46	105.3	81.5h@10 mA cm <sup>-2</sup> for 250 cycles	Angew. Chem. Int. Ed. (2019) <sup>40</sup>
Co-Co <sub>3</sub> O <sub>4</sub> @NAC	1.449	164	35h@5 mA cm <sup>-2</sup>	Appl. Catal. B (2020) <sup>41</sup>
PCN-A@Fe SA	/	185	/	J. Energ. Chem. (2021) <sup>42</sup>
Fe/N-G-SAC	/	120	10 mA cm <sup>-2</sup> for 240 cycles	Adv. Mater. (2020) <sup>43</sup>
Fe-NSDC	1.52	225.1	66.5h@4 mA cm <sup>-2</sup> for 400 cycles	Small (2019) <sup>44</sup>
Co/Co-N-C	1.41	132	/	Adv. Mater. (2019) <sup>45</sup>
EA-Co-900	1.37	73	100h@20 mA cm <sup>-2</sup>	Appl. Catal. B (2019) <sup>46</sup>
Co-N, B-CSC	1.43	100.4	14h@5 mA cm <sup>-2</sup> for 128 cycles	ACS Nano (2018) <sup>47</sup>
Fe-N <sub>x</sub> -C	1.51	96.4	10 mA cm <sup>-2</sup> for 2000 min	Adv. Funct. Mater. (2019) <sup>48</sup>
NC-Co SA	1.411	20.9	(Solid-State) 2500 min, 125	ACS Catal. (2018) <sup>49</sup>

NGM-Co	1.439	28.5	cycles (Solid-State) 1h@1mA cm <sup>-2</sup> for 18 cycles	Adv. Mater. (2017) <sup>33</sup>
4.2-FeSA	1.43	112	(Solid-State) 60h@2 mA cm <sup>-2</sup>	This work

**Table S8.** The value of site density and turnover

Sample	SD (umol g <sup>-1</sup> )	TOF (s <sup>-1</sup> )	
		0.95V	0.9V
<b>1.7-FeSA</b>	27.66	0.61	2.32
<b>2.5-FeSA</b>	29.65	0.76	2.80
<b>4.2-FeSA</b>	31.25	1.05	3.57
<b>4.8-FeSA</b>	30.45	1.31	3.75

**Table S9.** Summary of power density in HT-PEMFCs

<b>Materials</b>	<b>Power density (mW cm<sup>-2</sup>)</b>	<b>REF.</b>
PBI-Fe/C	60	J. Mater. Chem. A (2015) <sup>50</sup>
BP-FeNC	189.2	Appl. Catal. B (2018) <sup>51</sup>
Pt-Ru/MWCNT-GNP	280	Int. J. Energy Res.(2019) <sup>52</sup>
Pt/SiCTiC	227.4	Appl. Catal. B (2016) <sup>53</sup>
FeSA-G	276	Adv. Sci. (2019) <sup>54</sup>
Pt/FeP/C	465	Adv. Funct. Mater. (2021) <sup>55</sup>
Cu-PtFe/NC	432.6	Adv. Funct. Mater. (2021) <sup>56</sup>
20% Pt/C	250	J. Power Sources (2009) <sup>57</sup>
10% Pt/C	320	J. Power Sources (2019) <sup>58</sup>
4.2-FeSA	351.1	This work

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