

Electronic Supporting Information

Development of Robust and Superamphiphobic Membranes using Reduced Graphene Oxide (rGO)/PVDF-HFP Nanocomposite Mats for Membrane Distillation

Environmental Science: Nano

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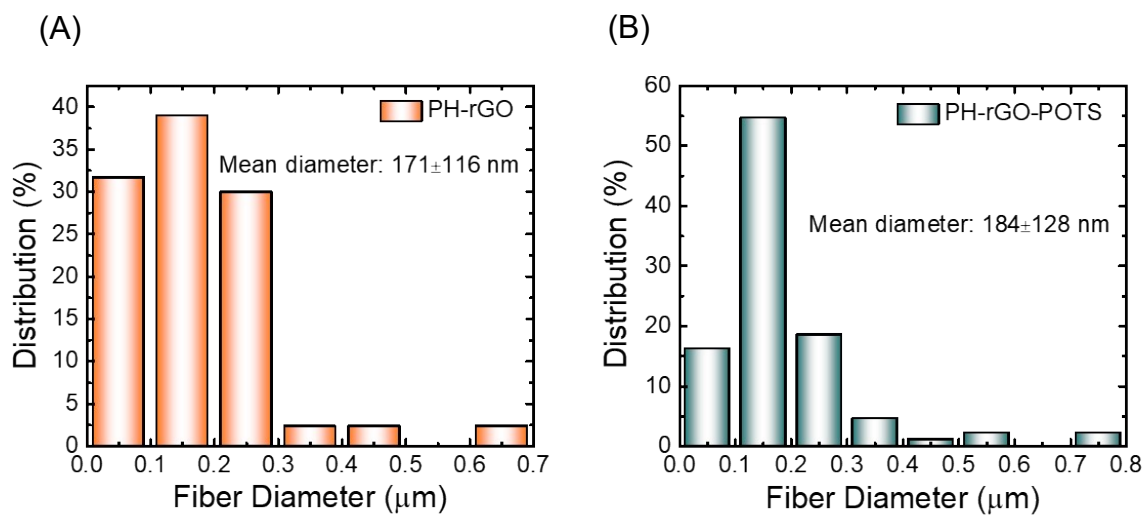


Fig. S1 Fiber diameter distribution of (A) PH-rGO membrane (B) PH-rGO-POTS membrane.

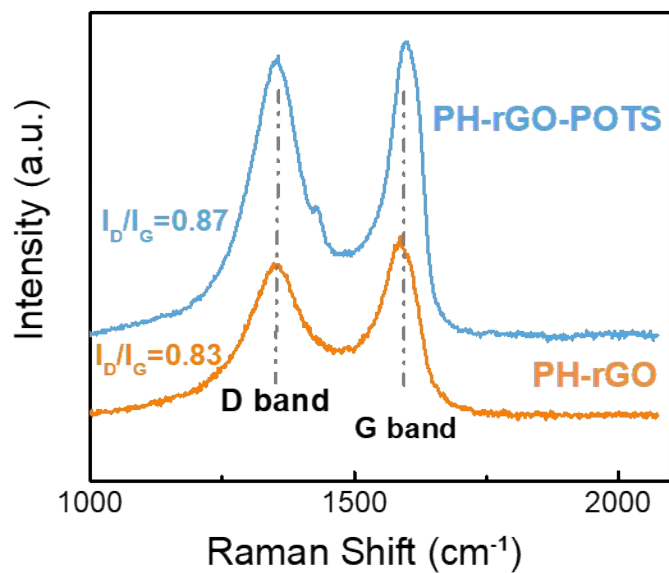


Fig. S2 Raman spectra of (A) PH-rGO membrane and (B) PH-rGO-POTS membrane.

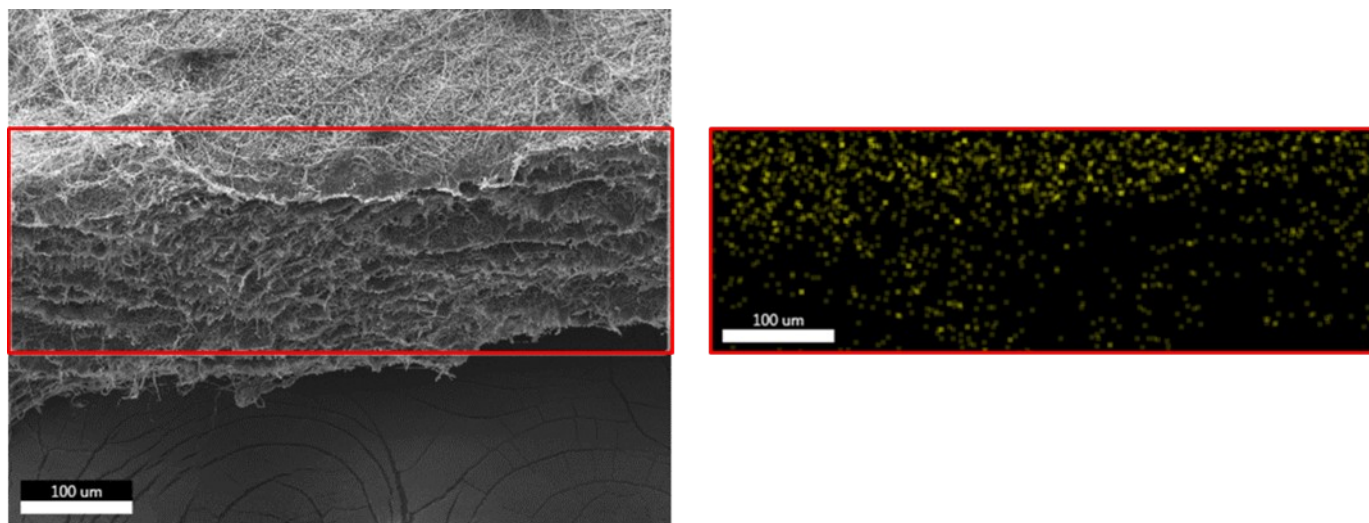


Fig. S3 The cross-sectional EDS mapping images of Si element on the PH-rGO-POTS membrane.



Video 1.MOV

Video S1: Non-sticky test, PH-rGO-POTS membrane was inserted into dye solution and then taken out.



Video 2.MOV

Video S2: The roll-off behavior of the water droplets on the PH-rGO-POTS membrane at the horizontal state.



Video 3.MOV

Video S3: Self-cleaning behavior of the PH-rGO-POTS membrane

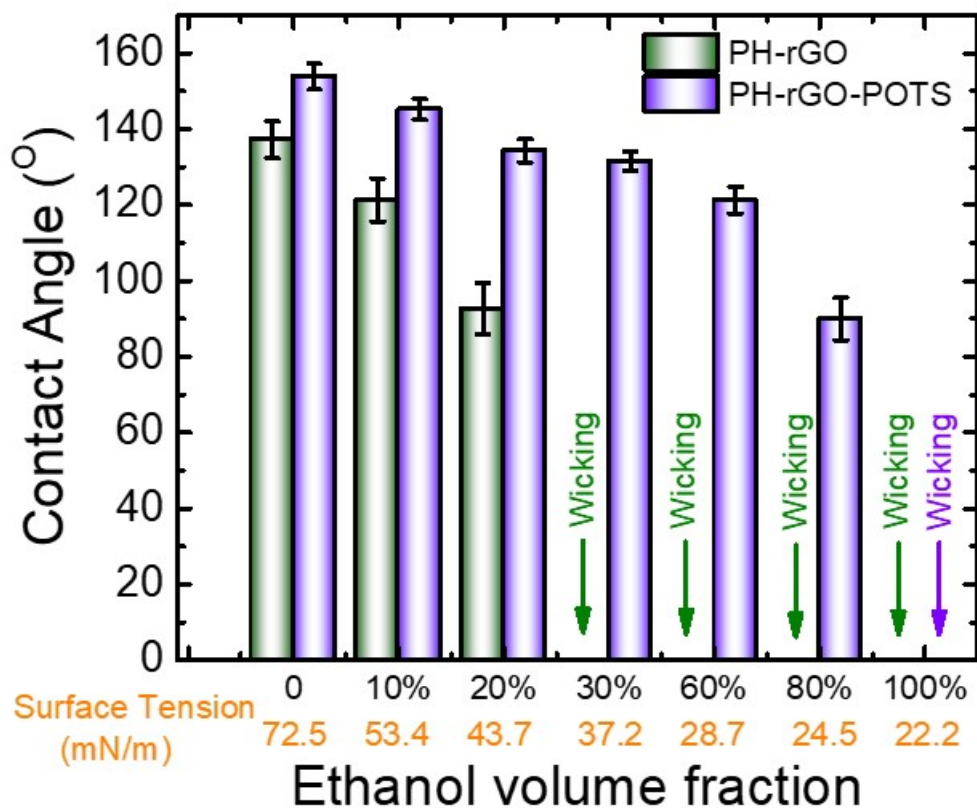


Fig. S4 Contact angles of the PH-rGO-POTS membrane facing with different water-ethanol mixtures. “Wicking” means that the membrane was wetted by the testing liquids immediately, and no stable contact angles could be measured. The error bars stand for the standard deviations of contact angle measurements. The water-ethanol mixtures with different surface tensions are prepared following a published protocol.¹

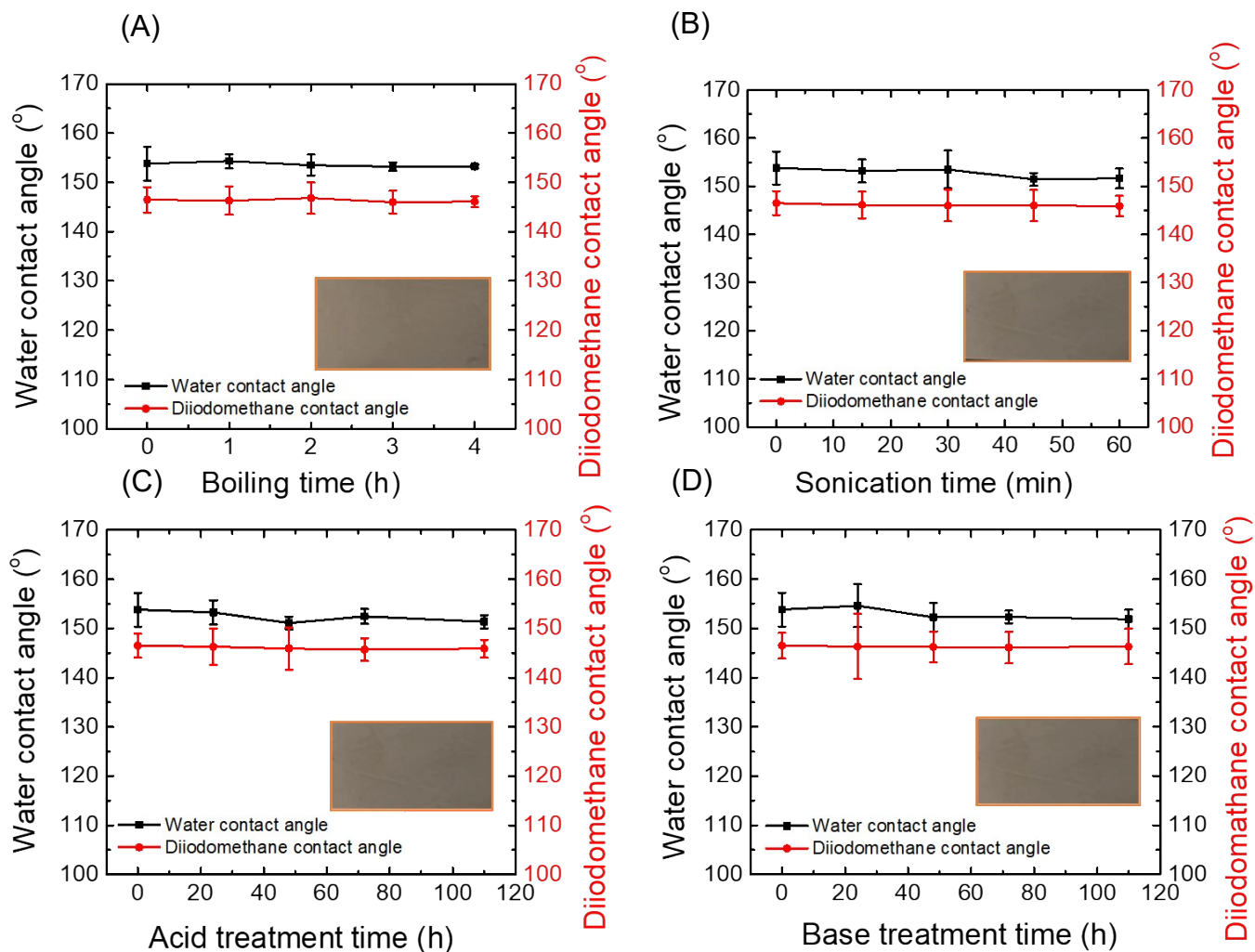


Fig. S5 Water contact angle (black) and Diiodomethane contact angle (red) of PH-rGO-POTS membranes after challenging with (A) boiling water for 4h, (B) sonication for 60 min, (C) strong acid (HCl, pH=2) for 110 h, and (D) base solution (NaOH, pH=12) for 110 h. The error bars in the figures stand for standard deviation. Insets are optical images of PH-rGO-POTS membranes after various treatments.

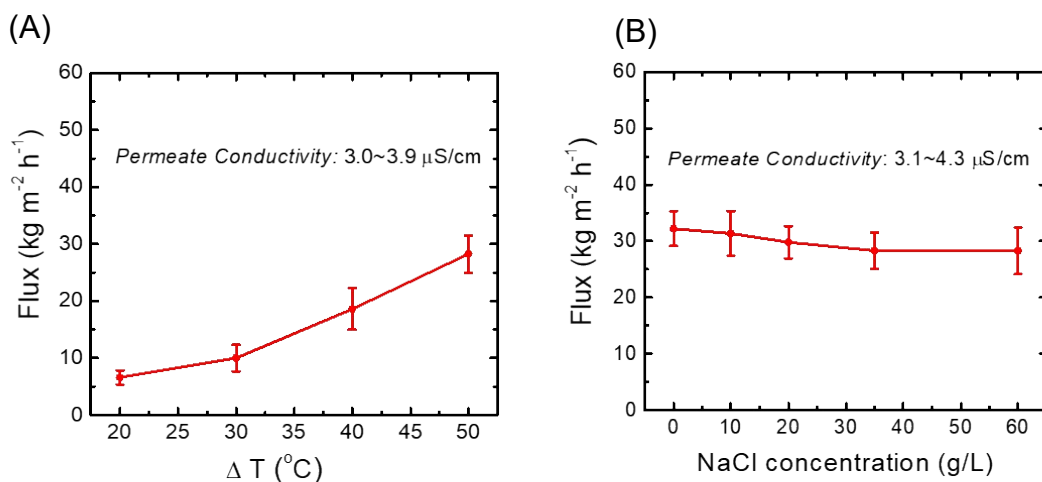


Fig. S6 (A) Water flux of the PH-rGO-POTS membranes under various temperature differences; the temperature of the feed varied from 35 °C to 65 °C, while the permeate side temperature was kept constant at 15.0 °C. (B) Water flux of the PH-rGO-POTS membrane under different NaCl concentrations with the temperature difference maintained at 50 °C. The error bars in the figures stand for standard deviation.

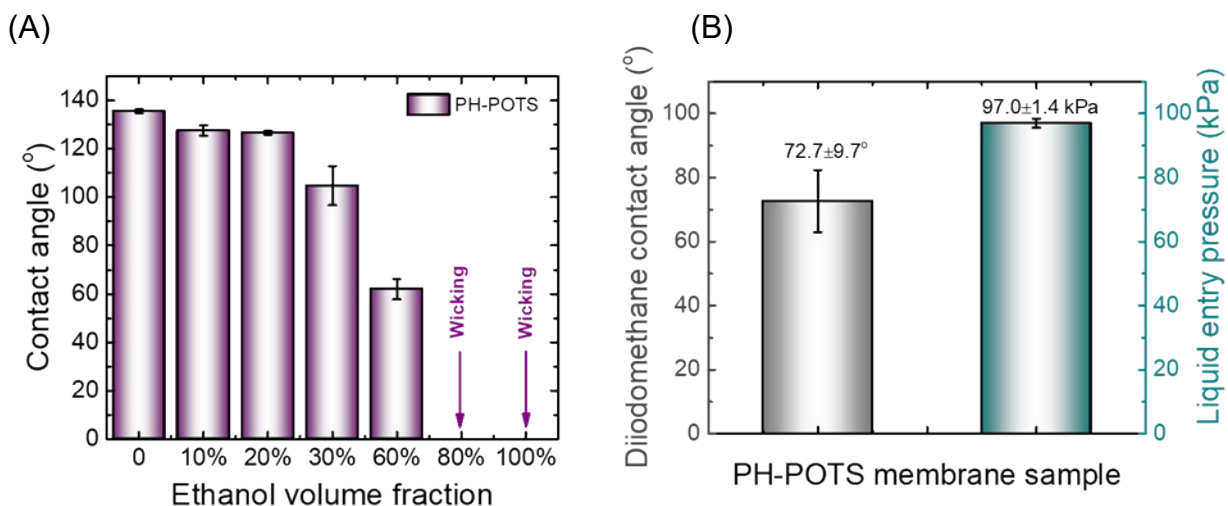


Fig. S7 (A) Contact angles of the PH-POTS membrane with different ethanol concentrations. (B) Diiodomethane contact angle (grey) and LEP (blue) of the PH-POTS membrane.

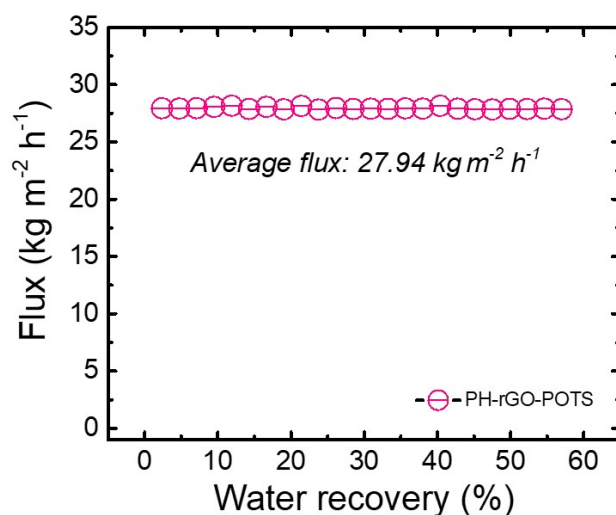


Fig. S8 Water flux as the function of the water recovery for the PH-rGO-POTS membrane during the long-term stability in presence of mixed foulants (35 g/L NaCl, 20 mM CaCl₂, 20 mM Na₂SO₄, 100 mg/L humic acid sodium salt, 10 mg/L machine oil, and 0.05 mM SDS). The feed solution temperature was maintained at 65 °C and the permeate side temperature was maintained at 15 °C.

Supplementary References

- 1 W. Wang, X. Du, H. Vahabi, S. Zhao, Y. Yin, A. K. Kota, T. Tong, Trade-off in membrane distillation with monolithic omniphobic membranes. *Nat. Commun.*, 2019, 10, 1-9.