

Supporting Information

Plasma-induced construction of defect-enriched perovskite oxides for catalytic methane combustion

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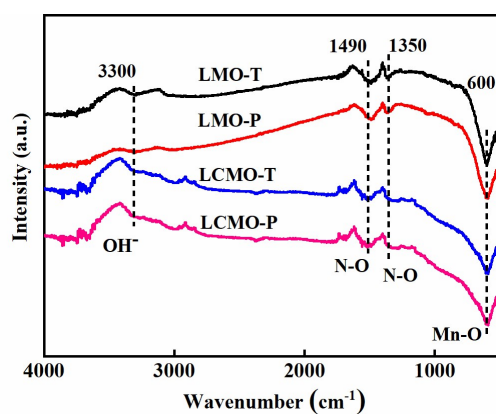


Fig.S1 FTIR spectra of all catalysts.

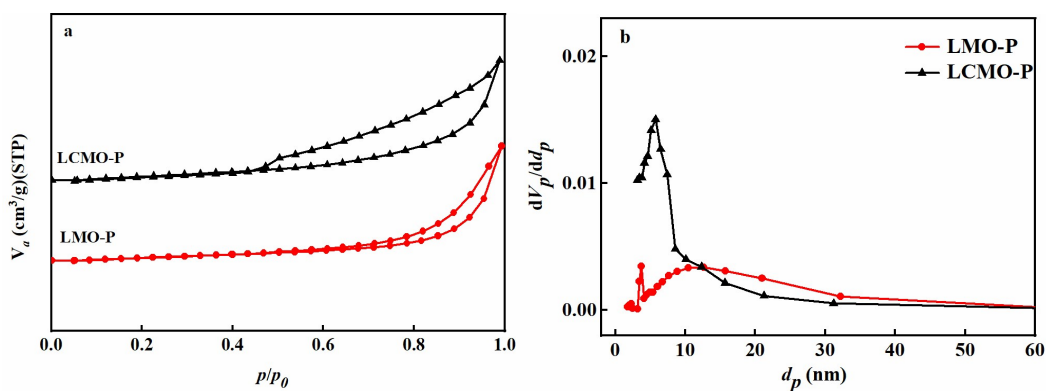


Fig.S2 (a) N₂ adsorption-desorption isotherms and (b) pore-size distributions of LMO-P and LCMO-P catalysts.

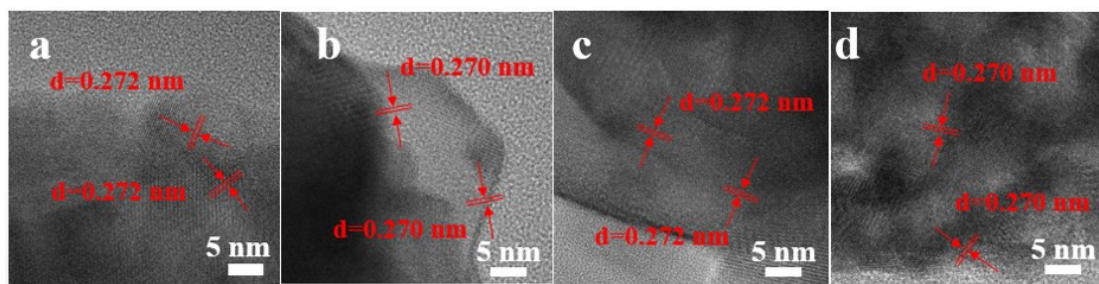


Fig.S3 HRTEM images of (a) LMO-T, (b) LCMO-T, (c) LMO-P and (d) LCMO-P catalysts.

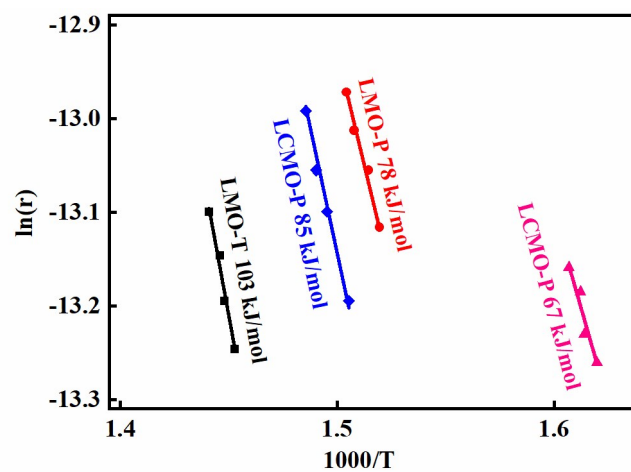


Fig.S4 Arrhenius plots for CH₄ combustion over all catalysts.

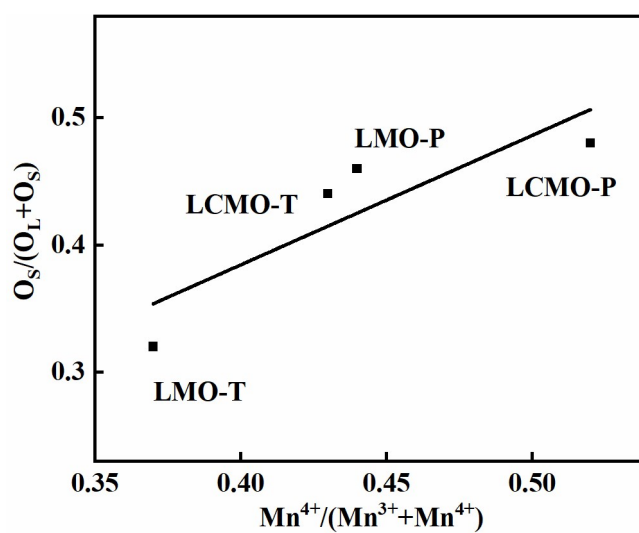


Fig.S5 Relationship among the $Mn^{4+}/(Mn^{3+}+Mn^{4+})$ and $O_S/(O_S+O_L)$ of all catalysts.

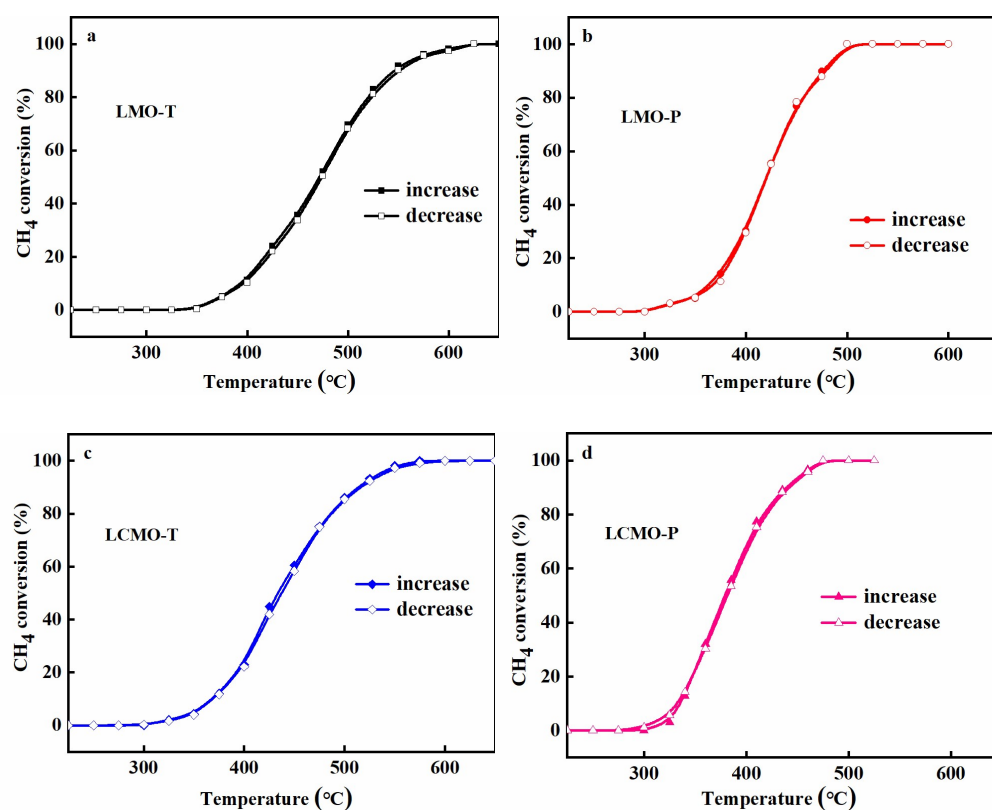


Fig.S6 Cycle performance tests of all catalysts.

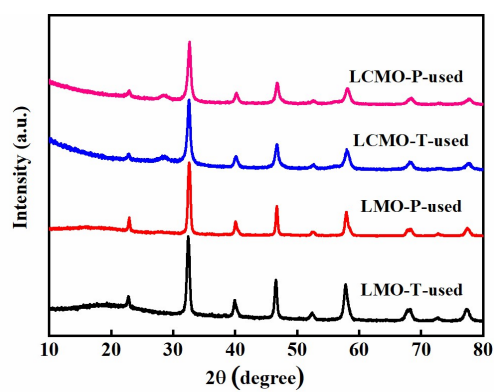


Fig.S7 XRD patterns of all used catalysts.

Tab.S1 Detailed data of pore volume (V_p), average pore size (D_p), ICP results and surface atomic concentration of all catalysts

Catalysts	V_p^a ($\text{cm}^3 \cdot \text{g}^{-1}$)	D_p^a (nm)	Ce content ^b (wt.%)	Surface atomic concentration (%)		
				Mn	La	Ce
LMO-T	-	-	-	16.1	22.0	-
LMO-P	0.12	27.9	-	17.0	23.2	-
LCMO-T	-	-	11.7	17.6	16.2	3.2
LCMO-P	0.23	11.0	11.2	19.5	16.6	2.1

^a The data were calculated by BJH method according to the desorption branch.

^b The data were calculated by ICP analysis.

Tab.S2 Comparison of CH_4 catalytic oxidation over other catalysts reported in the literature.

Catalysts	Reaction conditions	T_{50}	T_{90}	Reaction rate ($\mu\text{mol} \cdot \text{g}^{-1} \cdot \text{s}^{-1}$) ^a	Ref.
		(°C)	(°C)		
LCMO-P	2.5 vol.% CH_4 , 30000 h^{-1}	380	440	1.47	This work
$\text{LaMn}_{0.8}\text{Mg}_{0.2}\text{O}_3$	1 vol.% CH_4 , 30000 h^{-1}	450	525	0.47	[1]
LaMnO_3	3 vol.% CH_4 , 30000 h^{-1}	480	570	1.31	[2]
$\text{La}_{1-x}\text{FeO}_{3-\delta}$	0.5 vol.% CH_4 , 240000 h^{-1}	500	625	0.75	[3]
NiO/LaNiO_3	10 vol.% CH_4 , 36000 h^{-1}	480	575	0.79	[4]
$\text{La}(\text{Mn, Fe})\text{O}_{3+\lambda}$	1 vol.% CH_4 , 15000 h^{-1}	439	493	0.32	[5]

^a Reaction rate calculated from the active test at 350 °C.

References:

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