

## Supporting Information

### Plasma-induced construction of defect-enriched perovskite oxides for catalytic methane combustion

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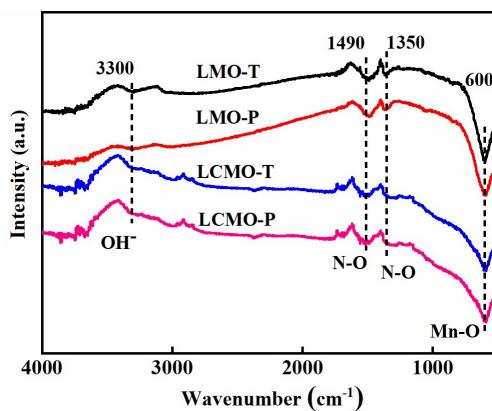
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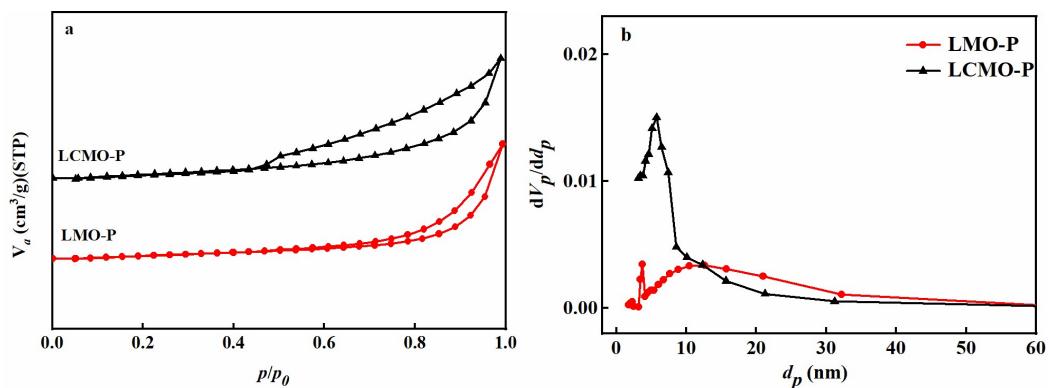
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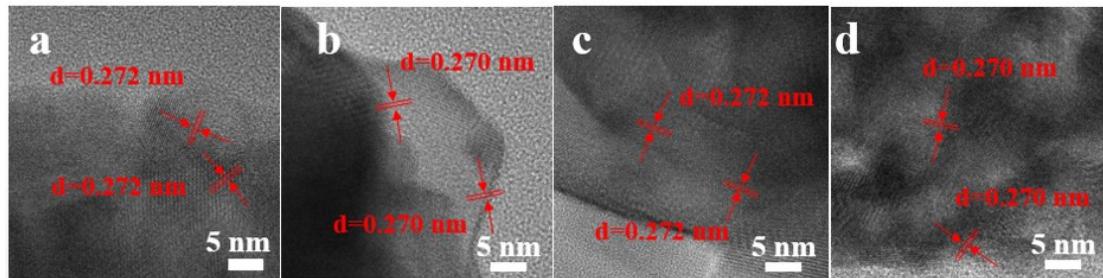
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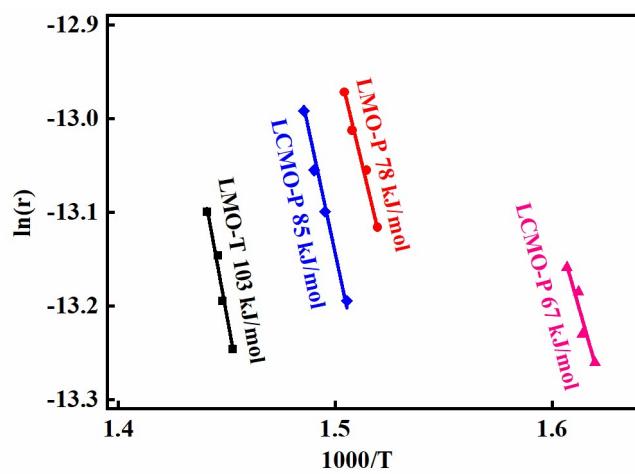
**Fig.S1** FTIR spectra of all catalysts.



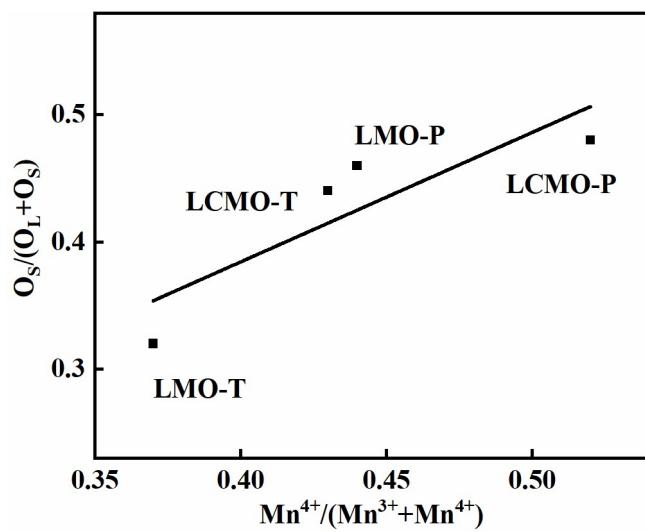
**Fig.S2** (a)  $\text{N}_2$  adsorption-desorption isotherms and (b) pore-size distributions of LMO-P and LCMO-P catalysts.



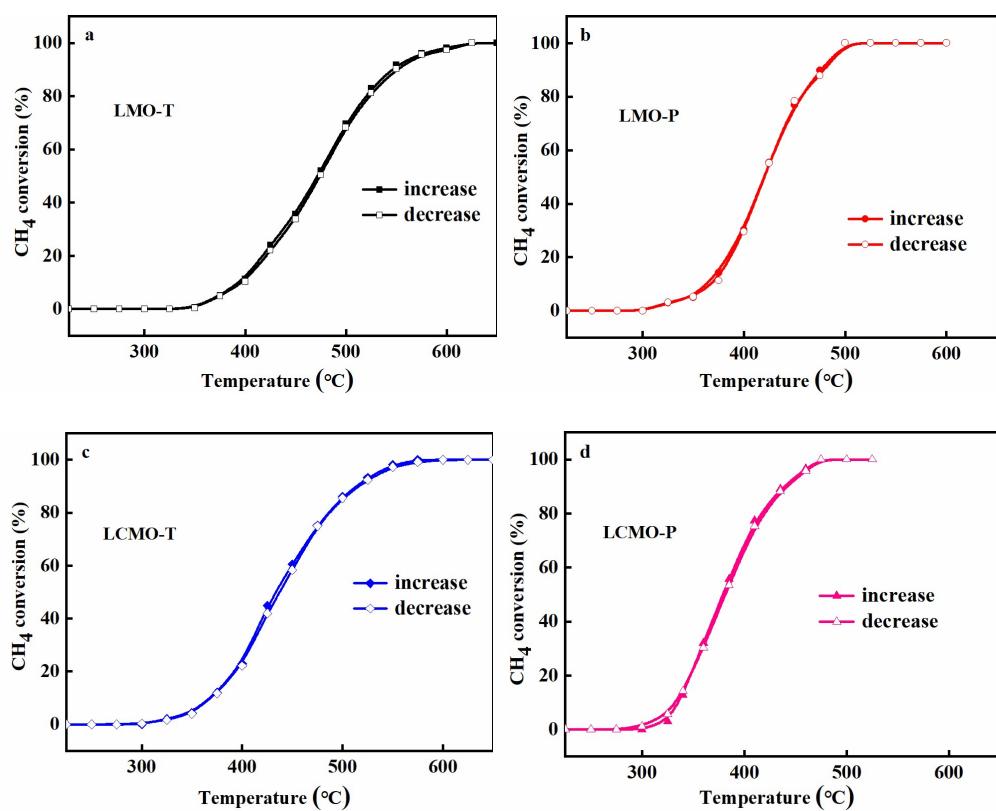
**Fig.S3** HRTEM images of (a) LMO-T, (b) LCMO-T, (c) LMO-P and (d) LCMO-P catalysts.



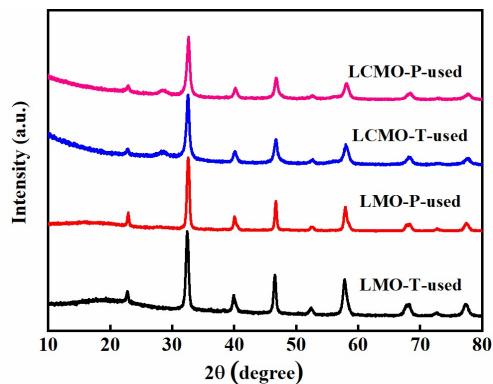
**Fig.S4** Arrhenius plots for  $\text{CH}_4$  combustion over all catalysts.



**Fig.S5** Relationship among the  $\text{Mn}^{4+}/(\text{Mn}^{3+} + \text{Mn}^{4+})$  and  $\text{O}_s/(\text{O}_s + \text{O}_L)$  of all catalysts.



**Fig.S6** Cycle performance tests of all catalysts.



**Fig.S7** XRD patterns of all used catalysts.

**Tab.S1** Detailed data of pore volume ( $V_p$ ), average pore size ( $D_p$ ), ICP results and surface atomic concentration of all catalysts

Catalysts	$V_p^a$ ( $\text{cm}^3 \cdot \text{g}^{-1}$ )	$D_p^a$ (nm)	Ce content <sup>b</sup> (wt.%)	Surface atomic concentration (%)		
				Mn	La	Ce
LMO-T	-	-	-	16.1	22.0	-
LMO-P	0.12	27.9	-	17.0	23.2	-
LCMO-T	-	-	11.7	17.6	16.2	3.2
LCMO-P	0.23	11.0	11.2	19.5	16.6	2.1

<sup>a</sup> The data were calculated by BJH method according to the desorption branch.

<sup>b</sup> The data were calculated by ICP analysis.

**Tab.S2** Comparison of  $\text{CH}_4$  catalytic oxidation over other catalysts reported in the literature.

Catalysts	Reaction conditions	$T_{50}$	$T_{90}$	Reaction rate	Ref.
		(°C)	(°C)	( $\mu\text{mol} \cdot \text{g}^{-1} \cdot \text{s}^{-1}$ ) <sup>a</sup>	
LCMO-P	2.5 vol.% $\text{CH}_4$ , 30000 $\text{h}^{-1}$	380	440	1.47	This work
$\text{LaMn}_{0.8}\text{Mg}_{0.2}\text{O}_3$	1 vol.% $\text{CH}_4$ , 30000 $\text{h}^{-1}$	450	525	0.47	[1]
$\text{LaMnO}_3$	3 vol.% $\text{CH}_4$ , 30000 $\text{h}^{-1}$	480	570	1.31	[2]
$\text{La}_{1-x}\text{FeO}_{3-\delta}$	0.5 vol.% $\text{CH}_4$ , 240000 $\text{h}^{-1}$	500	625	0.75	[3]
$\text{NiO/LaNiO}_3$	10 vol.% $\text{CH}_4$ , 36000 $\text{h}^{-1}$	480	575	0.79	[4]
$\text{La}(\text{Mn, Fe})\text{O}_{3+\lambda}$	1 vol.% $\text{CH}_4$ , 15000 $\text{h}^{-1}$	439	493	0.32	[5]

<sup>a</sup> Reaction rate calculated from the active test at 350 °C.

## References:

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- [2] Guo G, Lian K, Wang L, et al. High specific surface area  $\text{LaMO}_3$  ( $\text{M} = \text{Co, Mn}$ ) hollow spheres: synthesis, characterization and catalytic properties in methane combustion. RSC Advances, 2014, 4(102):58699-58707.
- [3] Faye J, Baylet A, Trentesaux M, et al. Influence of lanthanum stoichiometry in  $\text{La}_{1-x}\text{FeO}_{3-\delta}$  perovskites on their structure and catalytic performance in  $\text{CH}_4$  total oxidation. Applied Catalysis B-Environmental, 2012, 126:134-143.
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- [5] Miao F, Wang F, Mao D, et al. Effect of different reaction conditions on catalytic activity of  $\text{La}(\text{Mn, Fe})\text{O}_{3+\lambda}$  catalyst for methane combustion. Materials Research Express, 2019, 6(5) :15.