

Atomic Dispersed Pd site on Ti-SBA-15 for Efficient Catalytic Combustion of Typical Gaseous VOCs

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Synthesis of Pd0.5 NPs/Ti-SBA-15 catalyst

Reference sample, Pd0.5 NPs/Ti-SBA-15, was synthesized by using NaBH₄ as reducing agent. Typically, a certain amount of Pd precursor was added into the PVP (Pd/PVP mass ratio=1:1.2) in the deionized water, stirring for 6 h. Then a moderate amount of Ti-SBA-15 dispersed into methanol was added into the mixed solution. The mixture was further vigorously stirred for 3 h. Then, a considerable amount of NaBH₄ dissolved in deionized water was dropwise added. After continuously stirring for 1 h, the solid sample was filtered and dried at 60 °C in an oven for overnight. Finally, the solid sample was calcined at a ramp of 2 °C/min from room temperature to 500 °C and kept at this temperature for 3h in a muffle furnace, hence obtaining the Pd0.5 NPs/Ti-SBA-15 catalyst. The actual loading amount of Pd0.5 NPs/Ti-SBA-15 was determined by ICP-AES to be 0.52 wt%.

DFT calculation

The adsorption energy (E_{ads}) of styrene, cyclohexane and n-hexane on the Pd site was calculated basing on the adsorption configuration a:

$$E_{\text{ads}} = E_{\text{VOC/surface}} - (E_{\text{VOC}} + E_{\text{surface}})$$

where E_{surface} is the total energy of adsorption configuration a, and the $E_{\text{VOC/surface}}$ is the total energy of the VOC/surface. While, the E_{VOC} is the free energy of styrene, cyclohexane and n-hexane. The more negative value from this equation indicated the stronger adsorption accordingly.

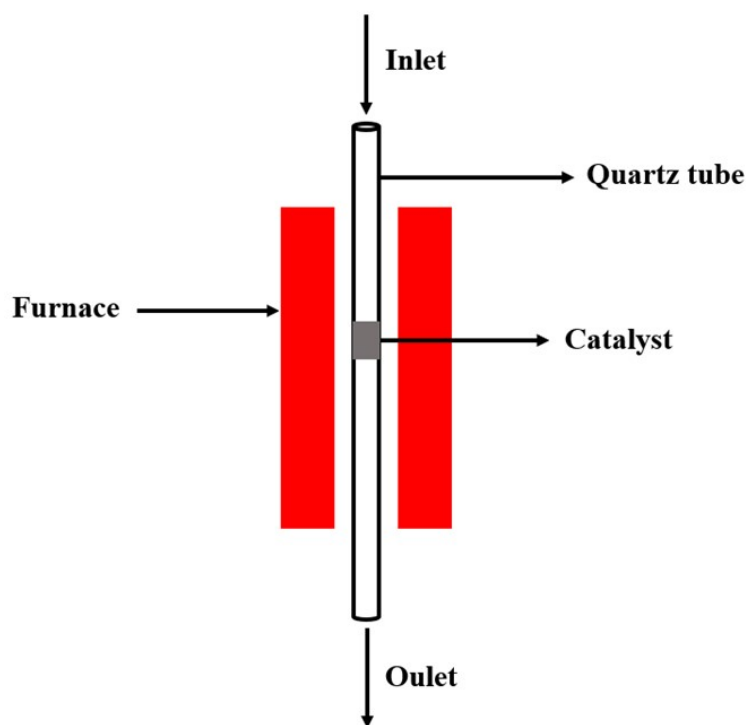


Fig. S1. Schematic diagram of the thermal reactor.

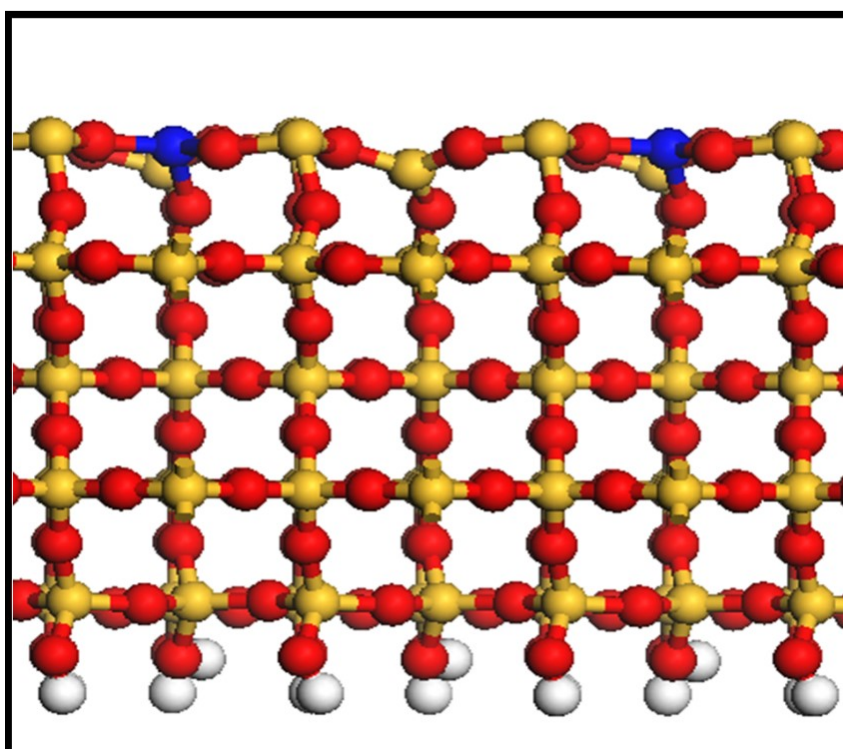


Fig. S2. Optimized configurations of the Ti-SBA-15. The red, yellow, blue and white spheres represent O, Si, Ti and H atoms, respectively.

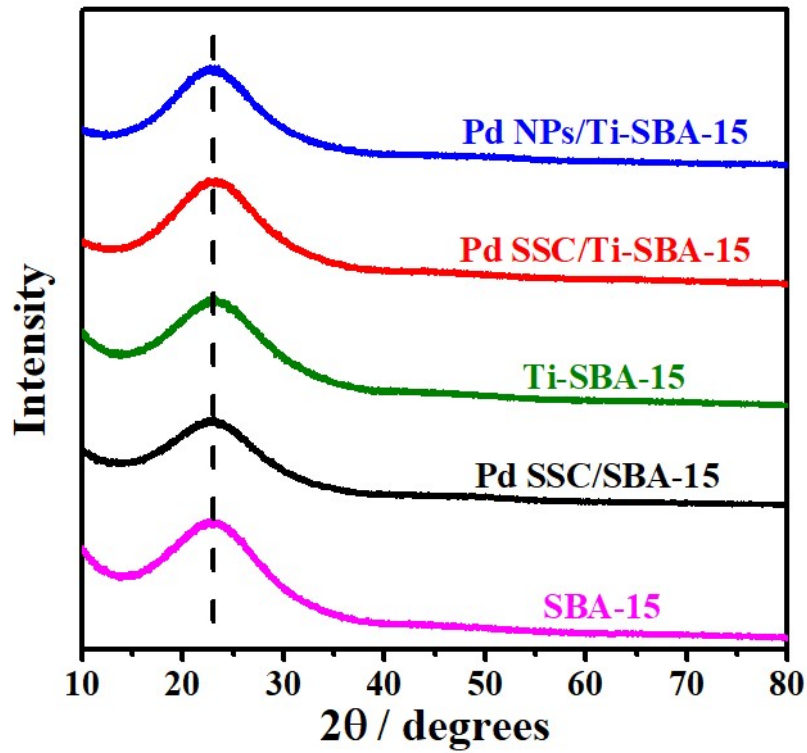


Fig. S3. Wide-angle XRD patterns of the as-prepared samples.

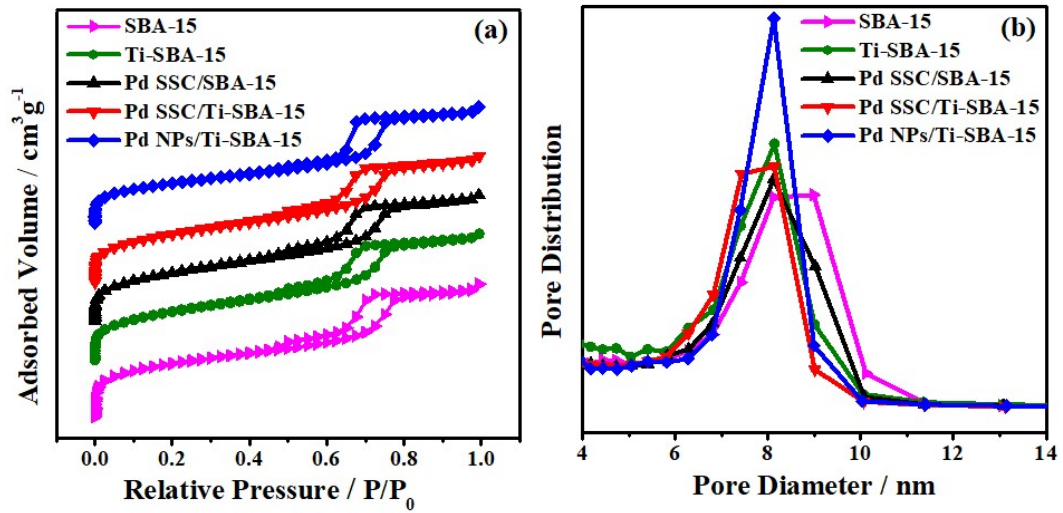


Fig. S4. (a) N_2 adsorption-desorption isotherms and (b) Pore size distributions of as-prepared samples.

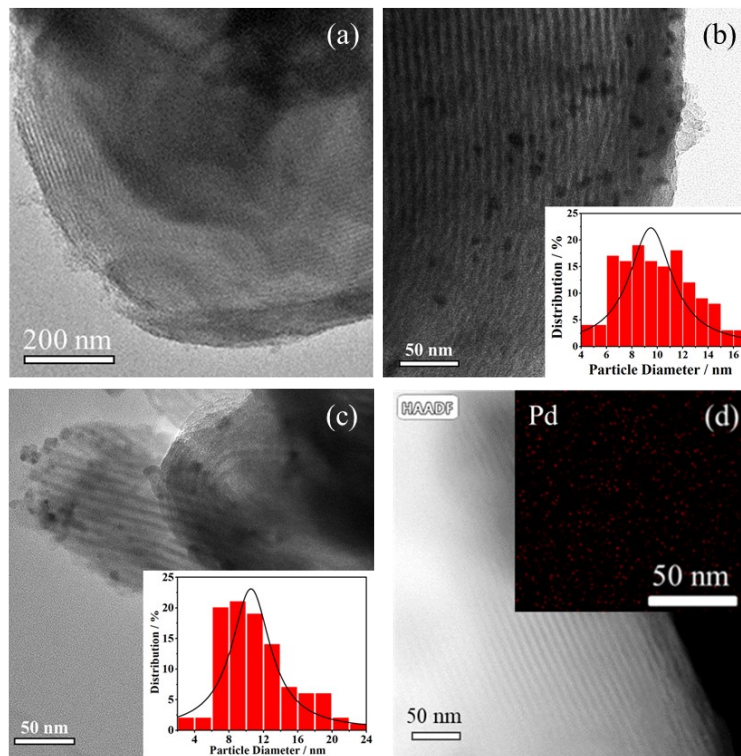


Fig. S5. HR-TEM images of (a) Pd SSC/SBA-15, (b) Pd NPs/Ti-SBA-15, (c) Pd_{0.5} NPs/Ti-SBA-15 and the size distribution images of Pd nanoparticles of Pd NPs/Ti-SBA-15 and Pd_{0.5} NPs/Ti-SBA-15 sample (inset) and (d) HADDF-STEM and EDX elemental mapping of Pd (inset) of recycled Pd SSC/Ti-SBA-15.

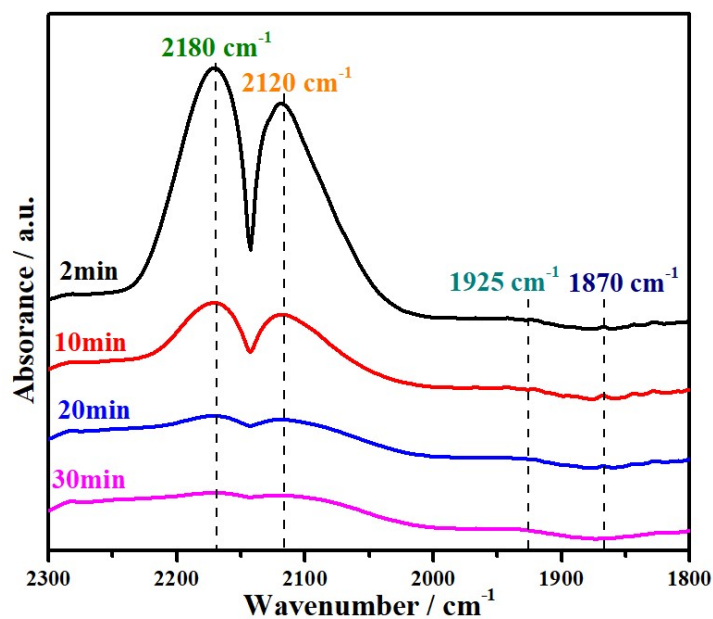


Fig. S6. In-situ DRIFT spectra of CO adsorbed on Pd NPs/Ti-SBA-15 with different time in the N₂ flow (30.0 mL/min) at 30 °C.

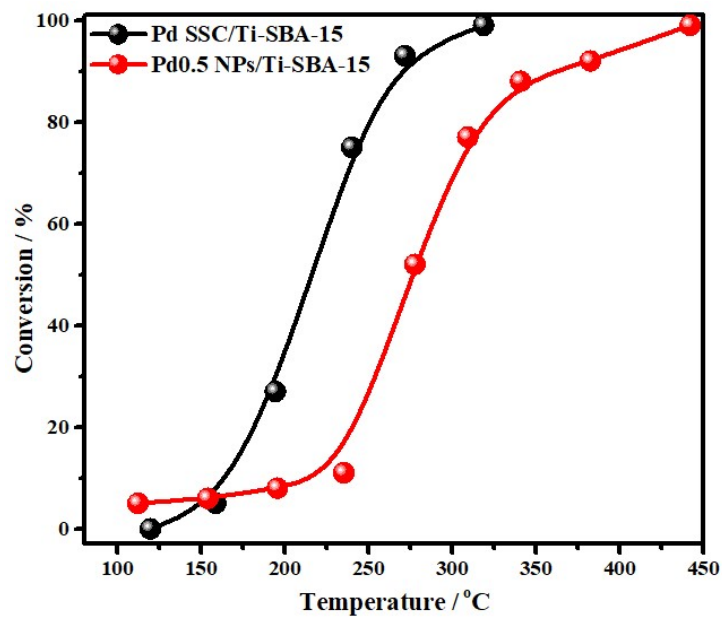


Fig. S7. Cyclohexane conversion as a function of temperature over Pd SSC/Ti-SBA-15 and Pd0.5 NPs/Ti-SBA-15.

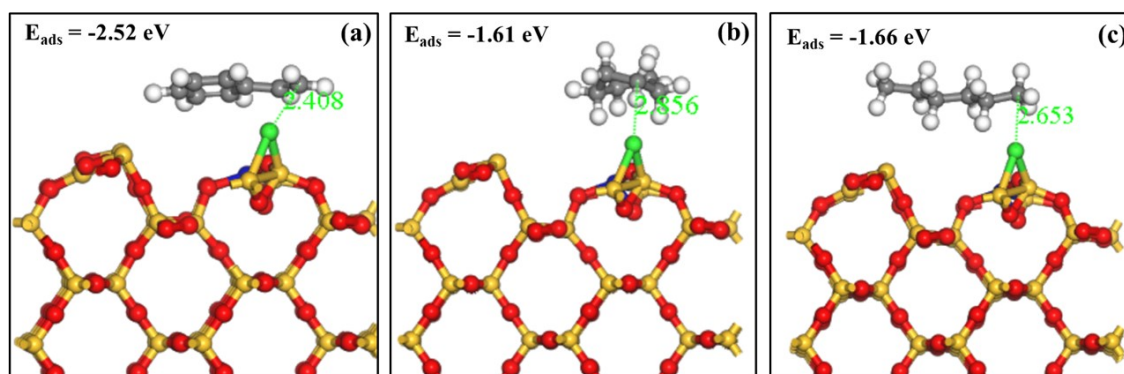


Fig. S8. Configurations for styrene (a), cyclohexane (b) and n-hexane (c) adsorption on the Pd site of Pd SSC/Ti-SBA-15. The red, yellow, blue, green and white spheres represent O, Si, Ti, Pd and H atoms, respectively.

Table S1. Textural parameters of various prepared samples.

Sample	Surface area	Pore diameter	Pore volume	Pd content (wt%)	Ti content (wt%)
SBA-15	1024.081	8.984	0.760	0	0
Ti-SBA-15	911.034	8.318	0.766	0	0.14
Pd SSC/SBA-15	891.906	8.117	0.708	0.05	0
Pd SSC/Ti-SBA-	859.942	8.315	0.683	0.04	0.14
Pd NPs/Ti-SBA-	770.437	8.124	0.753	0.05	0.13

Table S2. Different conversions temperatures of cyclohexane onto the prepared samples.

Catalyst	T ₅₀ (°C)	T ₉₀ (°C)
Pd SSC/SBA-15	340	420
Pd SSC/Ti-SBA-15	220	270
Pd NPs/Ti-SBA-15	350	500
Pd0.5 NPs/Ti-SBA-15	275	370

Table S3. Adsorption energies of Pd atom on different configurations over Pd SSC/Ti-SBA-15.

Configurations	Eads (eV)
a	-4.95
b	-4.57
c	-4.52

Table S4. Different conversions temperatures of different VOCs on Pd SSC/Ti-SBA-15.

VOC	T ₅₀ (°C)	T ₉₀ (°C)
Styrene	180	210
Cyclohexane	220	270
n-hexane	275	310

Table S5. Recent works of catalytic VOCs combustion over different catalysts.

Sample	VOC	Concentration ppm	Loading Amount (wt%)	T ₅₀ (°C)	T ₉₀ (°C)	Ref
Pt/Al ₂ O ₃	cyclopentane	6200	0.26	312	-	1
Au/TiO ₂	n-hexane	125	3	350	-	2
Pt/Al ₂ O ₃	n-hexane	1500	0.12	300	400	3
Ce _{0.99} Cu _{0.01} O ₂	n-hexane	260	-	-	400	4
CuO/Al ₂ O ₃	styrene	1000	8.2	240	325	5
PtCu/CeO ₂	n-pentane	50	0.08	300	400	6
Pd/SBA-15	toluene	650	0.3	261	292	7
Pd/C	toluene	1000	0.5	280	360	8
Pd/TiO ₂	toluene	1000	0.5	230	250	9
Pd/ V ₂ O ₅ /Al ₂ O ₃	benzene	482	5	280	310	10
Pd SSC/Ti-SBA-15	styrene	50	0.04	180	210	this work
Pd SSC/Ti-SBA-15	cyclohexane	40	0.04	220	270	this work
Pd SSC/Ti-SBA-15	n-hexane	40	0.04	275	310	this work

Reference

1. T. F. Garetto and C. R. Apesteguia, Oxidative catalytic removal of hydrocarbons over Pt/Al₂O₃ catalysts, *Catalysis Today*, 2000, **62**, 189-199.
2. C. Cellier, S. Lambert, E. M. Gaigneaux, C. Poleunis, V. Ruaux, P. Eloy, C. Lahousse, P. Bertrand, J. P. Pirard and P. Grange, Investigation of the preparation and activity of gold catalysts in the total oxidation of n-hexane, *Applied Catalysis B: Environmental*, 2007, **70**, 406-416.
3. M. Anic, N. Radic, B. Grbic, V. Dondur, L. Damjanovic, D. Stoychev and P. Stefanov, Catalytic activity of Pt catalysts promoted by MnO_x for n-hexane oxidation, *Appl Catal B-Environ*, 2011, **107**, 327-332.
4. V. D. Araujo, M. M. de Lima, Jr., A. Cantarero, M. I. B. Bernardi, J. D. A. Bellido, E. M. Assaf, R. Balzer, L. F. D. Probst and H. V. Fajardo, Catalytic oxidation of n-hexane promoted by Ce_(1-x)Cu_(x)O₂ catalysts prepared by one-step polymeric precursor method, *Materials Chemistry and Physics*, 2013, **142**, 677-681.
5. H. Pan, Z. He, Q. Lin, F. Liu and Z. Li, The effect of copper valence on catalytic combustion of styrene over the copper based catalysts in the absence and presence of water vapor, *Chinese Journal of Chemical Engineering*, 2016, **24**, 468-474.
6. J. Kong, G. Li, M. Wen, J. Chen, H. Liu and T. An, The synergic degradation mechanism and photothermocatalytic mineralization of typical VOCs over PtCu/CeO₂ ordered porous catalysts under simulated solar irradiation, *Journal of Catalysis*, 2019, **370**, 88-96.
7. C. He, J. J. Li, J. Cheng, L. D. Li, P. Li, Z. P. Hao and Z. P. Xu, Comparative Studies on Porous Material-Supported Pd Catalysts for Catalytic Oxidation of Benzene, Toluene, and Ethyl Acetate, *Industrial & Engineering Chemistry Research*, 2009, **48**, 6930-6936.
8. J. Bedia, J. M. Rosas, J. Rodriguez-Mirasol and T. Cordero, Pd supported on mesoporous activated carbons with high oxidation resistance as catalysts for toluene oxidation, *Appl Catal B-Environ*, 2010, **94**, 8-18.
9. J. C. Rooke, T. Barakat, S. Siffert and B. L. Su, Total catalytic oxidation of toluene using Pd impregnated on hierarchically porous Nb₂O₅ and Ta₂O₅ supports, *Catalysis Today*, 2012, **192**, 183-188.
10. R. S. G. Ferreira, P. G. P. de Oliveira and F. B. Noronha, Characterization and catalytic activity of Pd/V₂O₅/Al₂O₃ catalysts on benzene total oxidation, *Applied Catalysis B: Environmental*, 2004, **50**, 243-249.