

Comparative sustainability assessment of hydrogen supply network for hydrogen refueling stations in Korea – A techno-economic and life cycle assessment perspective

Malik Sajawal Akhtar ^a, Rofice Dickson ^b, Haider Niaz ^a, Dong Won Hwang ^{c,d}, J. Jay Liu ^{a,*}

^a*Department of Chemical Engineering, Pukyong National University, Busan 48513, Republic of Korea*

^b*Department of Chemistry & Chemical Engineering, SBA School of Science and Engineering, Lahore University of Management Sciences (LUMS), Lahore, 54972, Pakistan*

^c*Green Carbon Research Center, Korea Research Institute of Chemical Technology (KRICT), 141 Gajeongro, Yuseong, Daejeon 34114, Republic of Korea*

^d*Department of Advanced Materials and Chemical Engineering, University of Science and Technology (UST), 217 Gwahangno, Yuseong, Daejeon 34113, Republic of Korea*

^{a*} Corresponding author.

Email address: jayliu@pknu.ac.kr (J. Jay Liu)

Table S.1. Data used for calculating capital cost.

| Equipments | Baseline Purchased Cost USD | Year of quote | Installation factor | Reference |
|-----------------------------------|------------------------------------|----------------------|----------------------------|------------------|
| Air Separation Unit (ASU) | | | | |
| Heat Exchangers | 641,080 | 2010 | 2.17 | 1 |
| Compressors | 549,000 | 2010 | 2.75 | 1 |
| Drivers | 316,740 | 2010 | 1.5 | 1 |
| High Pressure Distillation Column | 120,800 | 2010 | 13.73 | 1 |
| Low Pressure Distillation Column | 153,700 | 2010 | 8.20 | 1 |
| Turbine | 14,590 | 2010 | 6.10 | 1 |
| Water Purification Unit (MVC) | | | | |
| Compressor | 164,050 | 2010 | 2.75 | 1 |
| Driver | 102,630 | 2010 | 1.5 | 1 |
| Evaporator | 1,235,220 | 2010 | 3.0 | 1 |
| Flat Plate HX | 454,940 | 2010 | 2.99 | 1 |
| Flat Plate HX | 1,047,740 | 2010 | 2.99 | 1 |
| Ammonia Synthesis Loop | | | | |
| Heat Exchangers | 2,154,355 | 2010 | 2.17 | 1 |
| Compressors | 4,545,891 | 2010 | 2.75 | 1 |
| Drivers | 1,083,847 | 2010 | 1.5 | 1 |
| Reactors | 1,291,755 | 2010 | 2.45 | 1 |
| Pumps | 363,650 | 2010 | 1.6 | 1 |

Table S.2. Multiplier for calculating direct, indirect costs and capital cost breakdown.²

| Cost distribution | Multiplier |
|---------------------------------------|-------------------|
| Direct costs | |
| Warehouse | 4% of ISBL |
| Site Development | 9% of ISBL |
| Additional piping | 5% of ISBL |
| Indirect Costs | |
| Portable Expenses | 10% of TDC |
| Field Expenses | 10% of TDC |
| Home Office & construction Fee | 20% of TDC |
| Project Contingency | 10% of TDC |
| Other Costs (start-up, permits, etc.) | 10% of TDC |
| Working Capital | 20% of ISBL |

Table S3. Environmental indicators and definition.

| Impact Category (Units per kg emission) | Definition | Relevant LCI Data |
|--|--|---|
| Abiotic Depletion Potential (ADP) (kg Sb eq) | Cumulative quantification of impact caused by extraction of minerals due to inputs in the system | Extraction of mineral resources |
| Abiotic Depletion Potential (fossil fuels) (ADPFF) (MJ) | Surplus energy (lower heating value) per extracted MJ, kg or m ³ fossil fuel, as a result of lower quality resources; unavailable for use by future generations | Extraction of fossil fuel resources |
| Global Warming Potential (GWP 100a) (kg CO ₂ eq) | GWP potential for time horizon 100 years: Impact caused by emissions of greenhouses gases | CO ₂ , NO ₂ , CH ₄ , CFC _s , HCFC _s , CH ₃ BR |
| Ozone Layer Depletion Potential (ODP) (kg CFC-11 eq) | Thinning of ozone layer due to greenhouse gas emissions | CFC _s , HCFC _s , CH ₃ BR, Halons |
| Human Toxicity Potential (HTP) (1,4-dichlorobenzene eq) | Potential detrimental effect of toxic substances within the environment on human health | Human toxic substances |
| Fresh Water Aquatic Ecotoxicity Potential (FETP) (1,4-dichlorobenzene eq) | Potential impact of toxic substances on aquatic ecosystems | Toxic substances with a reported lethal concentration to fish |
| Photochemical Oxidation Potential (PCOP) (kg C ₂ H ₄ eq) | Production of reactive chemical compounds, such as ozone, by the action of sunlight on pollutants in the air | PM10, NH ₃ , SO ₂ , NO _x , and NMVOC |
| Acidification Potential (ACP) (kg SO ₂ eq) | Acidic compounds formation as a result of manufacturing process | SO _x |
| Eutrophication Potential (EP) (kg PO ₄ eq) | Cumulative quantification of phosphorus compounds formation | Nitrogen and Phosphorus compounds |

Table S4. Costs forecasting.

| Parameter | 2020 | 2025 | 2030 | Reference |
|----------------------------|-------|-------|-------|-----------|
| Solar PV | 902 | 733 | 565 | 3 |
| AWE Capex | 903 | 720 | 588 | 4-6 |
| AWE Opex | 408 | 324 | 240 | 4-6 |
| LCOA | 0.9 | 0.74 | 0.6 | Authors |
| HRS+CSD | 5.66 | 5.32 | 5.1 | Authors |
| Solar PV Electricity price | 0.106 | 0.095 | 0.085 | 7 |
| Grid Integration cost | 0.032 | 0.033 | 0.038 | 7 |

used for LCOH

Table S5. LCA results (Per 1kg H₂) according to CML-IA baseline method.

| Impact category | Unit | Case 1 | Case 2 | Case 3 |
|-----------------|--------------|----------|----------|----------|
| ADP | kg Sb eq | 1.48E-03 | 1.13E-03 | 1.07E-03 |
| ADPFF | MJ | 7.76E+01 | 6.26E+01 | 5.18E+01 |
| GWP | kg CO2 eq | 6.81E+00 | 5.35E+00 | 4.57E+00 |
| ODP | kg CFC-11 eq | 8.10E-07 | 6.63E-07 | 5.37E-07 |
| HTP | kg 1,4-DB eq | 1.46E+01 | 1.12E+01 | 1.05E+01 |
| FETP | kg 1,4-DB eq | 1.20E+01 | 9.15E+00 | 8.74E+00 |
| PCOP | kg C2H4 eq | 1.97E+04 | 1.50E+04 | 1.43E+04 |
| ACP | kg SO2 eq | 2.38E-02 | 1.82E-02 | 1.67E-02 |
| EP | kg PO4 eq | 2.23E-03 | 1.53E-03 | 1.40E-03 |

Table S6. List of Ecoinvent v3.6 databases selected for LCA of studied cases.

| Processes |
|--|
| Calendering, rigid sheets {GLO} market for APOS, S |
| Acrylonitrile-butadiene-styrene copolymer {RoW} production APOS, S |
| Tetrafluoroethylene {GLO} market for APOS, S |
| Polyphenylene sulfide {GLO} market for APOS, S |
| N-methyl-2-pyrrolidone {GLO} market for APOS, S |
| Aniline {RoW} market for aniline APOS, S |
| Purified terephthalic acid {GLO} market for APOS, S |
| Acetic anhydride {GLO} market for acetic anhydride APOS, S |
| Nitric acid, without water, in 50% solution state {RER} market for nitric acid, without water, in 50% solution state APOS, S |
| Hydrochloric acid, without water, in 30% solution state {RER} hydrochloric acid production, from the reaction of hydrogen with chlorine APOS, S |
| Zirconium oxide {GLO} market for APOS, S |
| Carbon monoxide {RoW} market for APOS, S |
| Water, deionised {RoW} water production, deionised APOS, S |
| Industrial machine, heavy, unspecified {RoW} production APOS, S |
| Plaster mixing {GLO} market for APOS, S |
| Water, decarbonised {GB} market for water, decarbonised APOS, S |
| Steel, unalloyed {GLO} market for APOS, S |
| Heat, central or small-scale, other than natural gas {GLO} market group for APOS, S |
| Heat, from steam, in chemical industry {RoW} steam production, as energy carrier, in chemical industry APOS, S |
| Water, deionised {RoW} water production, deionised APOS, S |
| Potassium hydroxide {GLO} market for APOS, S |
| Steam, in chemical industry {RoW} production APOS, S |
| Nitrogen, liquid {RoW} air separation, cryogenic APOS, S |
| Iron ore, crude ore, 63% Fe {GLO} market for iron ore, crude ore, 63% Fe APOS, S |
| Potassium hydroxide {RoW} production APOS, S |
| Aluminium oxide, metallurgical {UN-OCEANIA} aluminium oxide production APOS, S |
| Refinery gas {RoW} refinery gas production, petroleum refinery operation APOS, S |
| Compressed air, 600 kPa gauge {RoW} market for compressed air, 600 kPa gauge APOS, S |
| Electricity, low voltage {RoW} electricity production, photovoltaic, 570kWp open ground installation, multi-Si APOS, S |
| Transport, freight, lorry 7.5-16 metric ton, EURO6 {RoW} transport, freight, lorry 7.5-16 metric ton, EURO6 APOS, S |
| Transport, freight, sea, container ship {GLO} transport, freight, sea, container ship APOS, S |

FIGURES.

CAPEX and OPEX breakdown

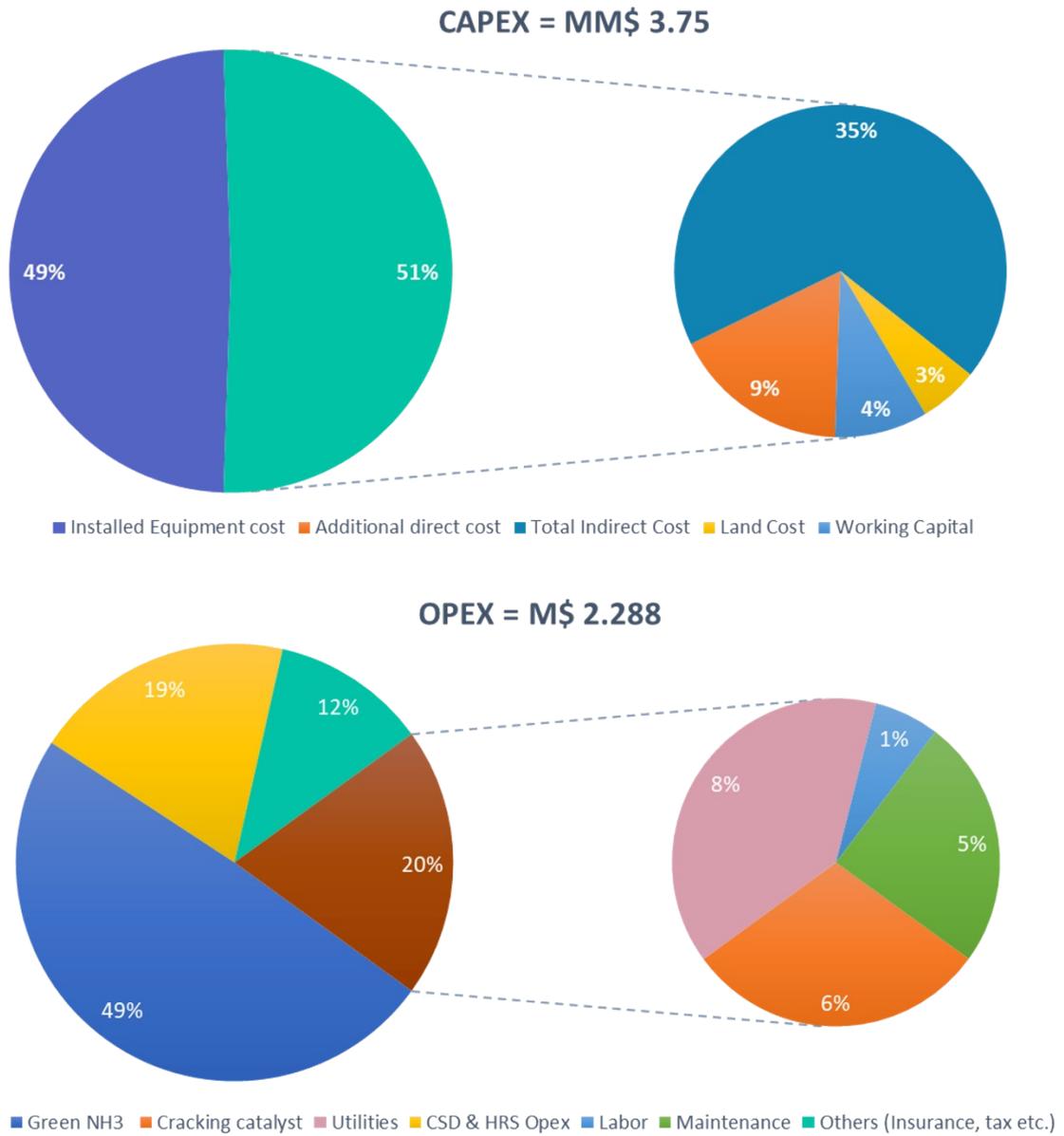
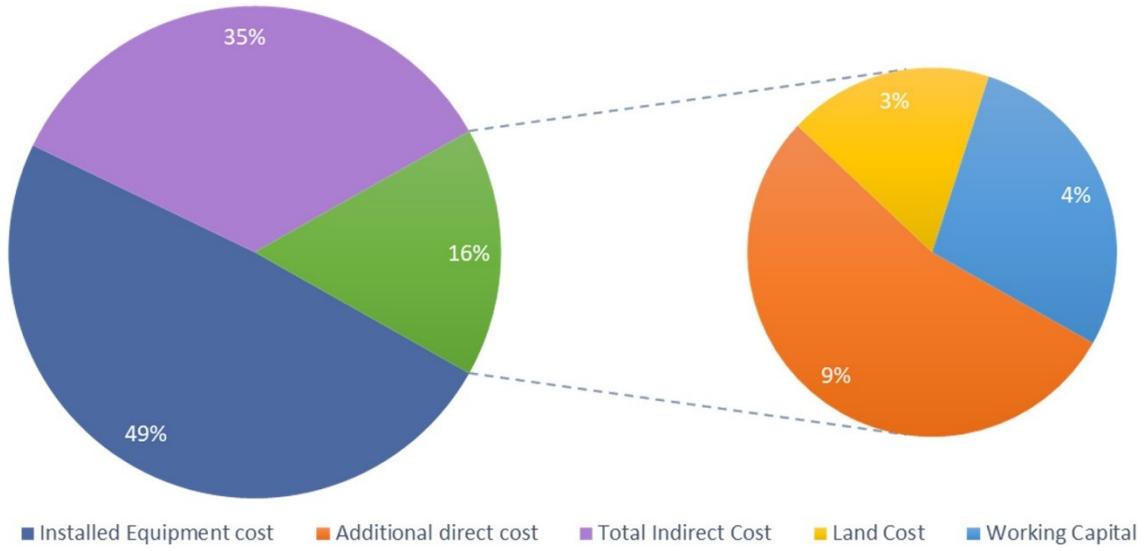


Fig.S 1. CAPEX and OPEX breakdown for Case 1.

CAPEX = Billion \$ 0.331



OPEX = M\$ 39.33

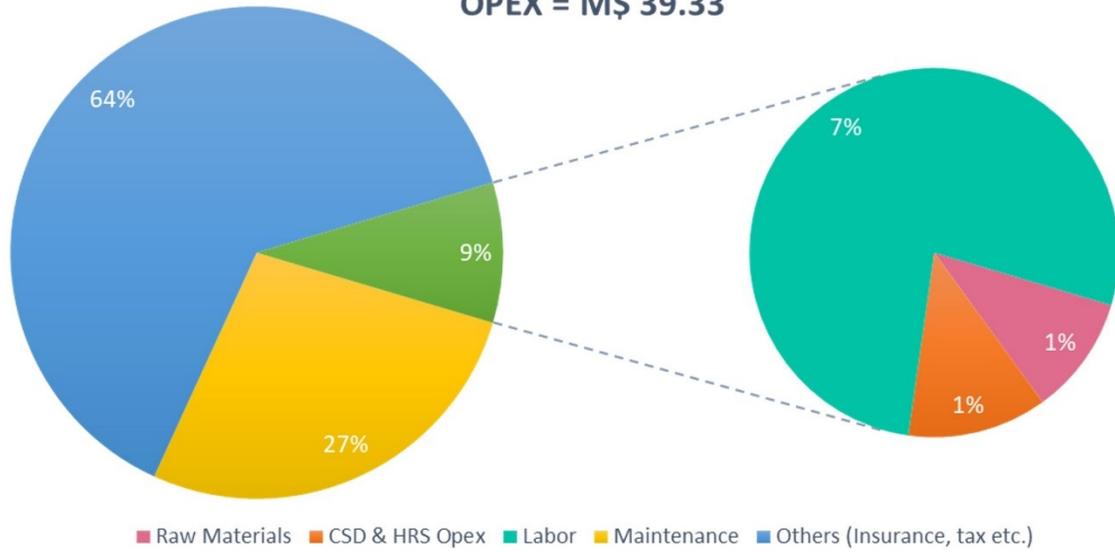


Fig.S 2. CAPEX and OPEX breakdown for Case 2.

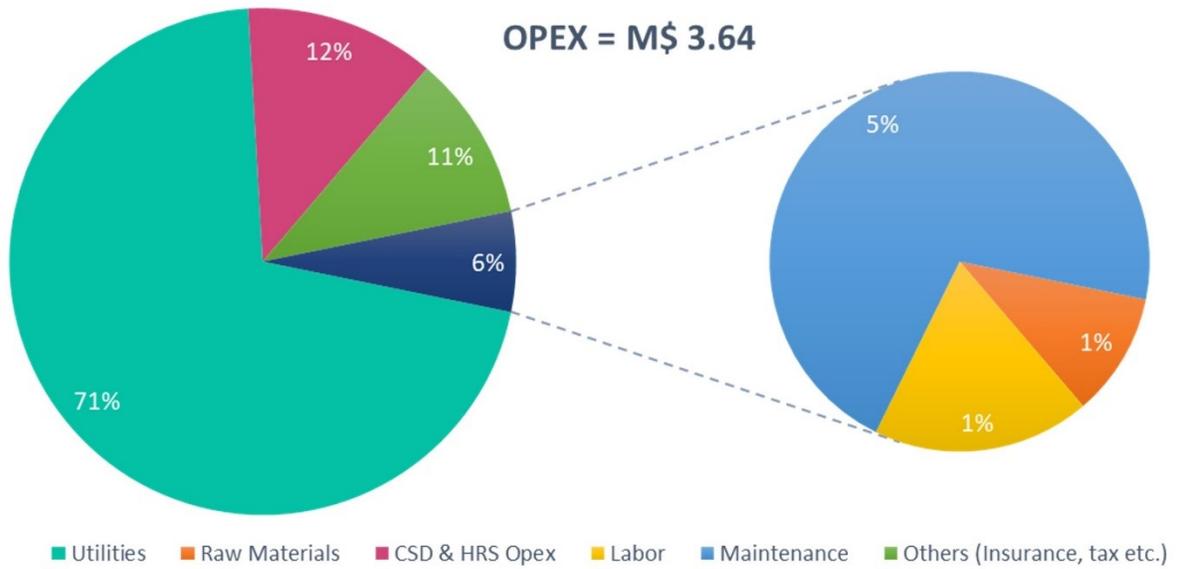
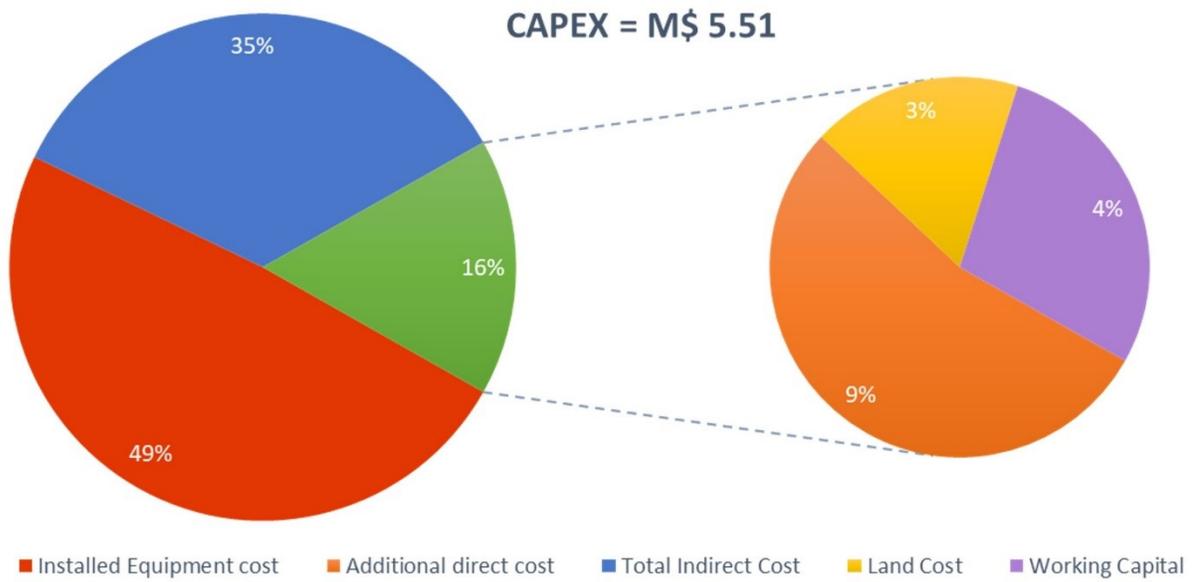


Fig.S 3. CAPEX and OPEX breakdown for Case 3.

Hydrogen delivery by tube trailer.

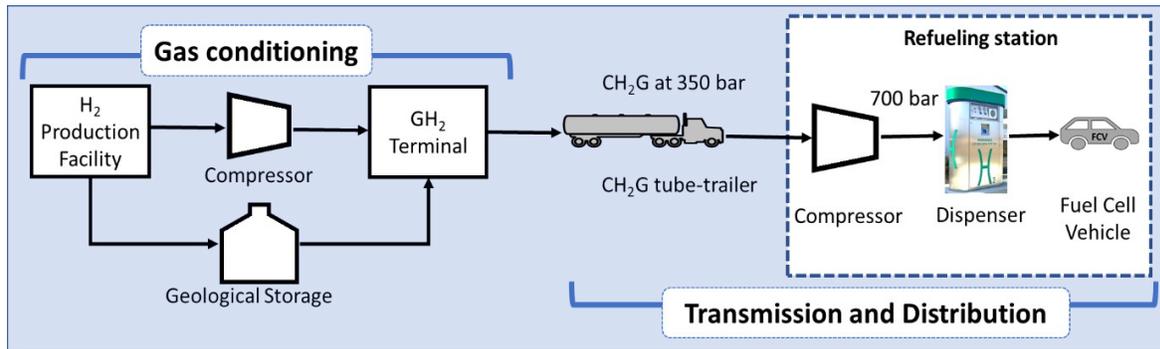


Fig.S 4. Hydrogen delivery as compressed gas by Tube trailer.

Life cycle assessment results of the studied cases.

As shown in Fig. S 5, the green ammonia production process has the highest impact in each environment indicator, which is due to the high amount of electricity used in the water electrolysis process. The breakdown of green ammonia production is also shown in Fig.S 6, which clearly demonstrate that more than 85% of the contribution to each indicator is from the hydrogen production process, as huge amount of electricity is required to produce hydrogen through water electrolysis. As we have also considered the infrastructure so most (more than 90%) of the emissions in hydrogen production are related to the production of electricity from solar PV power plant.

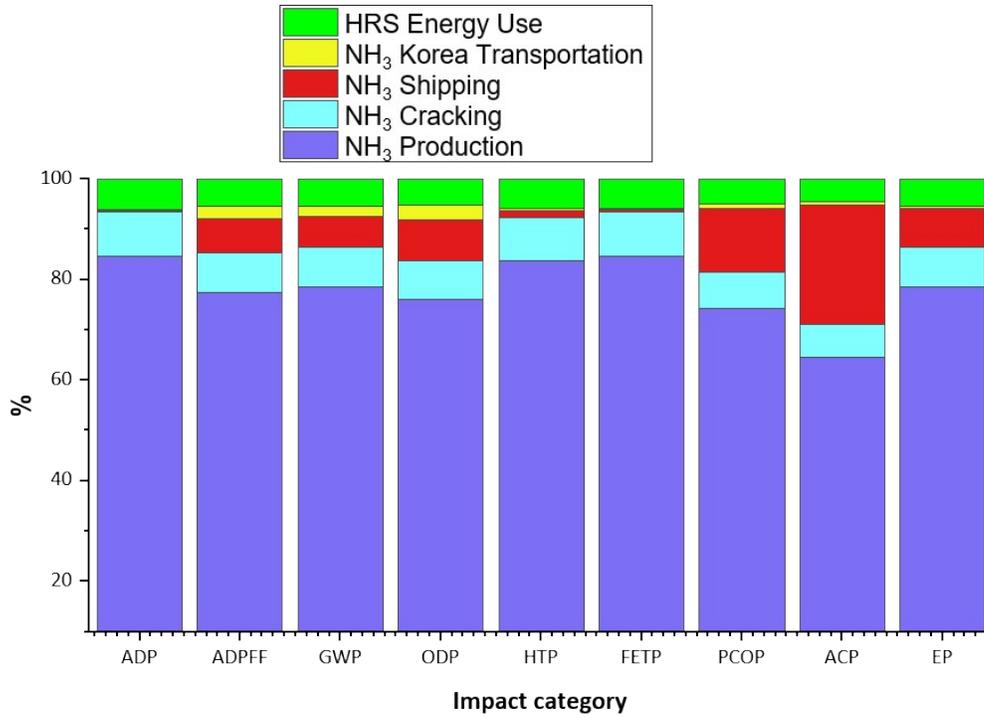


Fig.S 5. Breakdown of LCA results for Case 1.

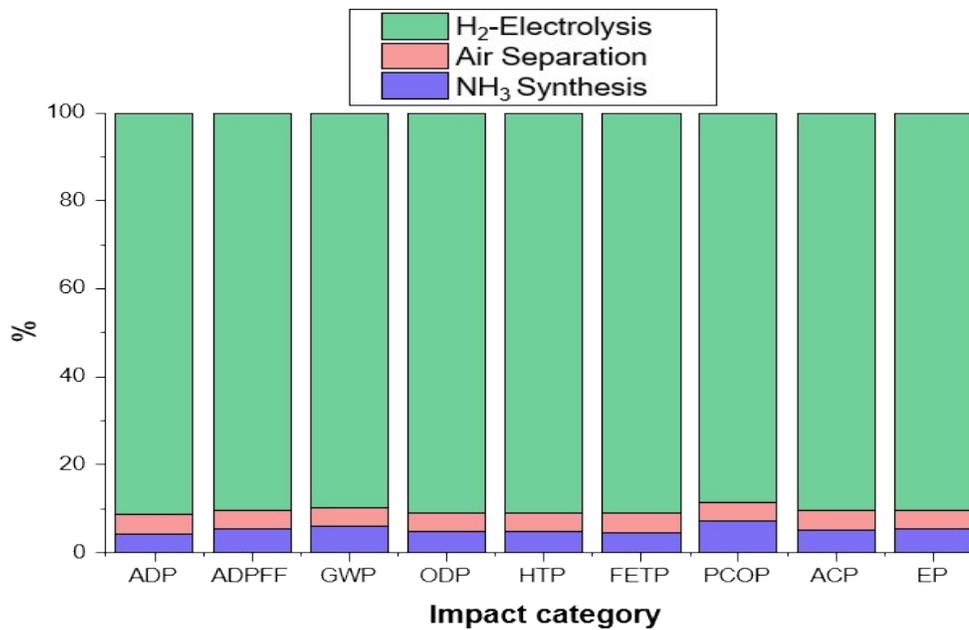


Fig.S 6. Breakdown of LCA results for green NH₃ production.

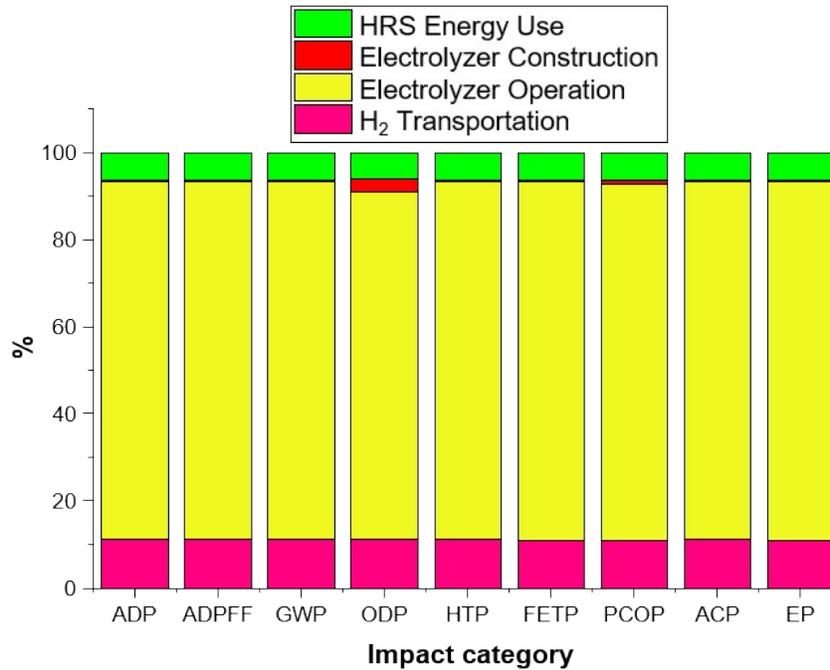


Fig.S 7. Breakdown of LCA results for Case 2.

Fig.S 7 illustrates the breakdown of results for Case 2. Hydrogen transportation also has a significant contribution in each indicator following the electrolyzer operation stage owing to the burning of nonrenewable based fuel used during the transportation. Fig.S 8 presents the breakdown of results for Case 3, showing that the electrolyzer construction contributes little to the emissions, whereas the energy used in the compression and dispensing of hydrogen has a more significant impact; however, hydrogen production is still the highest contributor. The production of electricity is the major contributor (99%) in the operational phase of the electrolyzer owing to the manufacturing of raw materials required for the solar PV power plant.

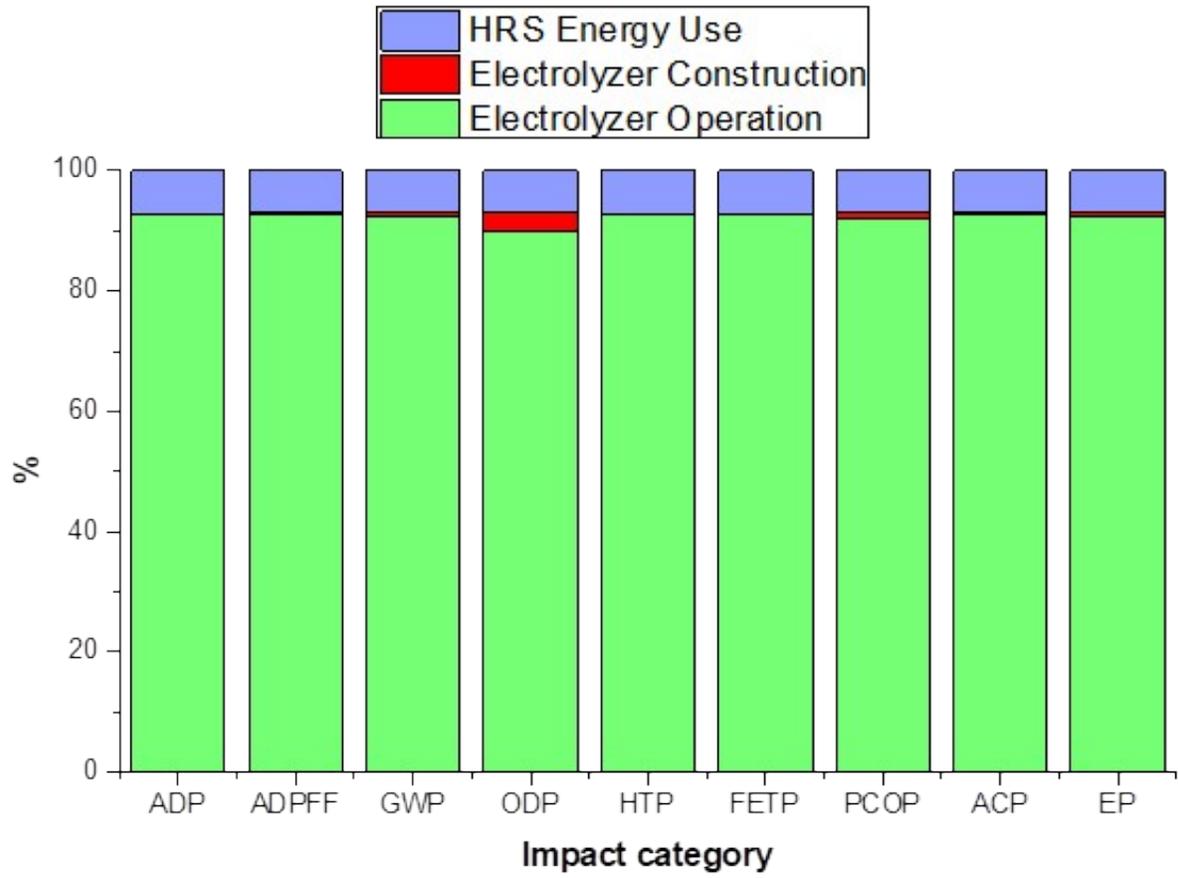


Fig.S 8. Breakdown of LCA results for Case 3.

References

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- 6 B. Madden, E. Chan and S. Alvin, .
- 7 K. M. R. Institute, *KEMRI Electric Power Economy Review*, 2020.