

## Supplementary Information

### **Manganese oxide as an alternative to vanadium-based catalysts for effective conversion of glucose to formic acid in water**

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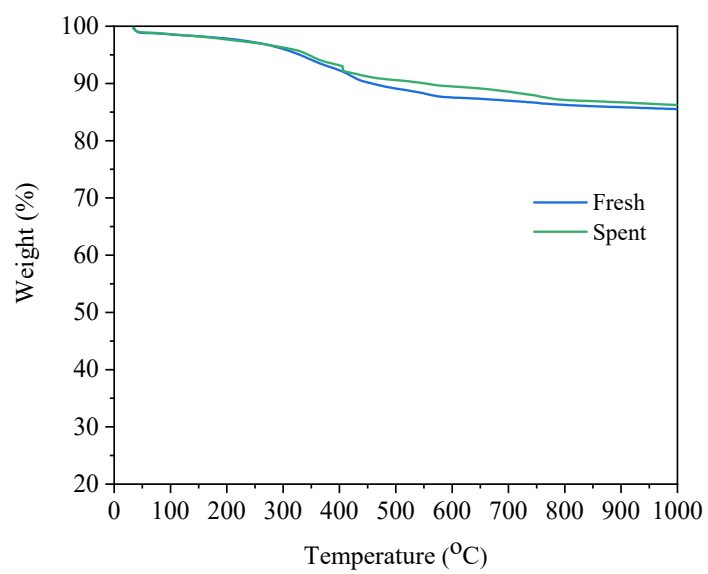
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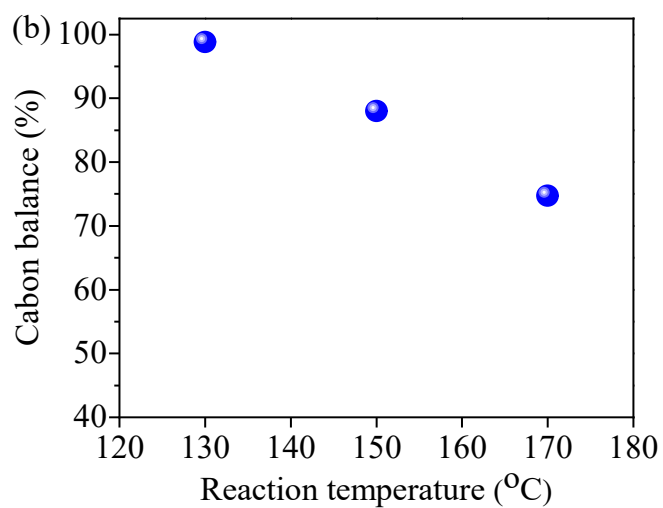
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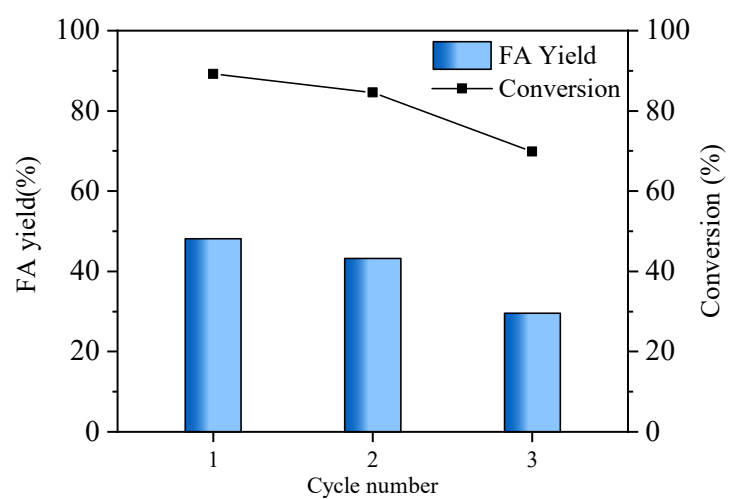
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**Figure S1** Thermal gravimetric analyses (TGA) of fresh MnO<sub>x</sub>-100 and spent MnO<sub>x</sub>-100 after reaction at 170 °C for 150 min.

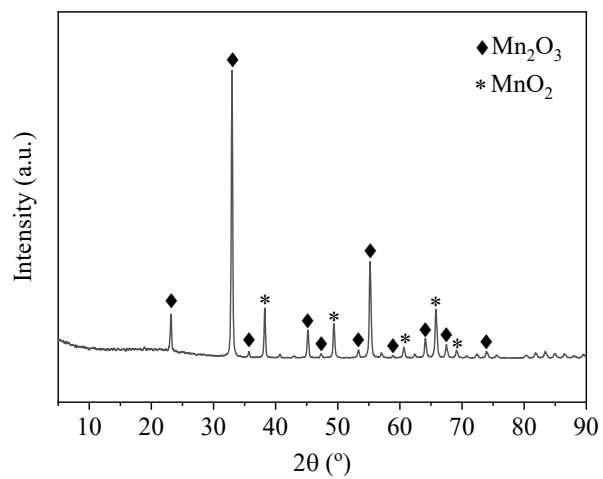


**Figure S2** Carbon balances obtained after oxidation reaction with  $\text{MnO}_x$ -100 catalyst at several temperatures. Reaction conditions: 50 mg catalyst, 100 mg glucose, 5 mL  $\text{H}_2\text{O}$ , 150 min reaction time, 3 MPa  $\text{O}_2$



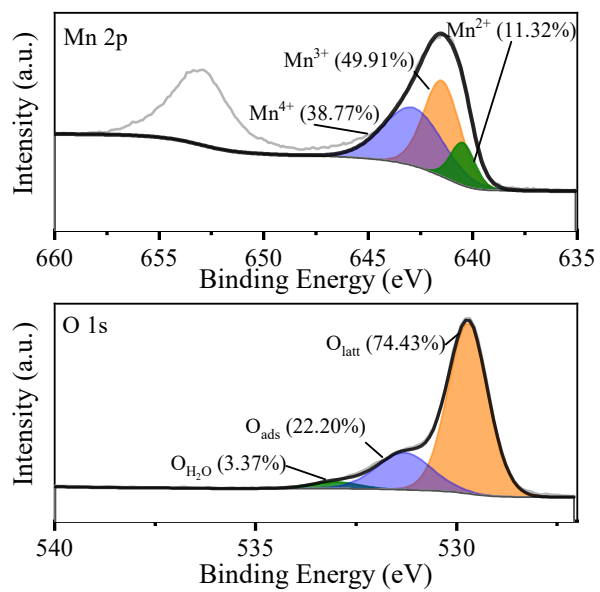
**Figure S3** Recyclability of MnO<sub>x</sub>-100 catalyst for initial catalyst dosage of 50 mg. Reaction

conditions: 100 mg glucose, 5 mL H<sub>2</sub>O, 150 °C, 3 MPa O<sub>2</sub>, 100 min reaction time.



**Figure S4** XRD spectrum of  $\text{MnO}_x$ -100 catalyst after three cycles of use according to conditions

in Fig. S3. ( $\text{MnO}_2$ : JCPDS PDF# 72-1982.  $\text{Mn}_2\text{O}_3$ : JCPDS PDF# 41-1442)



**Figure S5** XPS of spectrum of MnO<sub>x</sub>-100 catalyst after three cycles of use according to conditions

in Fig. S3

**Table S1** Total surface area and pore volume of synthesized catalysts

Catalyst	$S_{\text{BET}}(\text{m}^2 \cdot \text{g}^{-1})$	Pore volume ( $\text{cm}^3 \cdot \text{g}^{-1}$ )
MnO <sub>x</sub> -100	28.0	0.30
MnO <sub>x</sub> -120	16.7	0.08
MnO <sub>x</sub> -140	16.9	0.08

**Table S2** Comparison of maximum formic acid (FA) yields obtained from glucose in aqueous solutions for different homogeneous catalysts

Catalyst	Key reaction conditions				Yield (%)	Ref.
	Glucose concentration (g/L)	Oxidant concentration or O <sub>2</sub> partial pressure	Temperature (°C)	Time (h)		
LiOH	9	2.5 mmol H <sub>2</sub> O <sub>2</sub>	35	8	91.3	1
KOH	-	1 mmol H <sub>2</sub> O <sub>2</sub>	250	1/60	75.0	2
NaOH	-	1 mmol H <sub>2</sub> O <sub>2</sub>	259	1/60	70.0	2
VOSO <sub>4</sub>	9	2 MPa O <sub>2</sub>	140	1	45.0	3
FeCl <sub>3</sub> + H <sub>2</sub> SO <sub>4</sub>	26	3 MPa O <sub>2</sub>	170	5/6	52.3	4
NaVO <sub>3</sub> +H <sub>2</sub> SO <sub>4</sub>	17	3 MPa O <sub>2</sub>	160	1/60	68.2	5
H <sub>4</sub> PVMo <sub>11</sub> O <sub>40</sub>	10	2 MPa O <sub>2</sub>	180	3	54.5	6
H <sub>5</sub> PV <sub>2</sub> Mo <sub>10</sub> O <sub>40</sub>	10	2 MPa O <sub>2</sub>	100	3	55.0	7
H <sub>6</sub> PV <sub>3</sub> Mo <sub>9</sub> O <sub>40</sub>	50	3 MPa O <sub>2</sub>	90	8	56.0	8
H <sub>7</sub> PV <sub>4</sub> Mo <sub>8</sub> O <sub>40</sub>	50	3 MPa O <sub>2</sub>	90	8	52.0	8
H <sub>7</sub> PV <sub>5</sub> Mo <sub>8</sub> O <sub>40</sub>	22	6 MPa O <sub>2</sub>	80	8	58.2	9

**Table S3** Conversion of glucose, arabinose or glyoxylic acid to formic acid (FA) with MnO<sub>x</sub>-100 catalyst. Reaction conditions: 50 mg catalyst, 20 g/L substrate, 5 mL H<sub>2</sub>O, 160 °C, 3 MPa O<sub>2</sub>, 100 min reaction time.

Substrate	Conversion (%)	FA yield (%)
Glucose	94.6	55.7
Arabinose	100	69.8
Glyoxylic acid	100	73.4

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