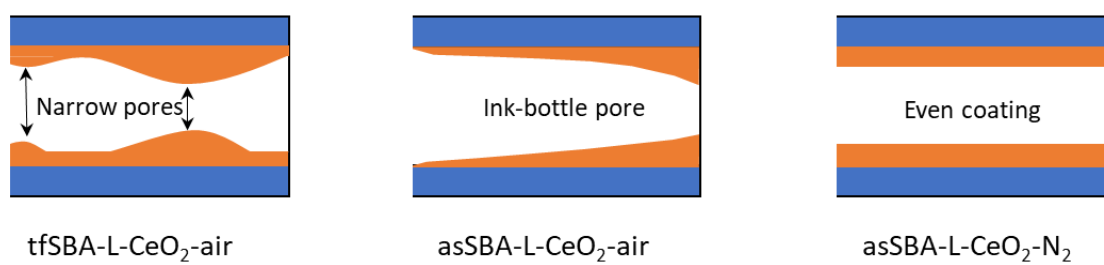


*Electronic Supplementary Information for:*

**Controlling the Dispersion of Ceria Using Nanoconfinement: Application  
to CeO<sub>2</sub>/SBA-15 Catalysts for NH<sub>3</sub>-SCR**

Jun Shen and Christian Hess\*

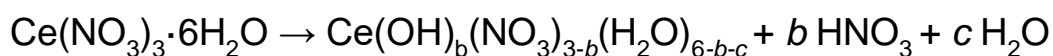
Eduard-Zintl-Institut für Anorganische und Physikalische Chemie, Technical University  
of Darmstadt, Alarich-Weiss-Str. 8, 64287 Darmstadt, Germany. Email: [jun.shen@tu-darmstadt.de](mailto:jun.shen@tu-darmstadt.de); [christian.hess@tu-darmstadt.de](mailto:christian.hess@tu-darmstadt.de)



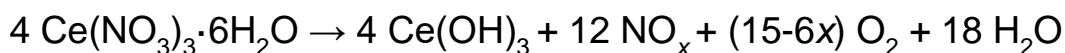
**Figure S1** Schematic diagrams of pore shapes of the three tested samples.

**(a)**

(i) Water-acid azeotrope formation:



(ii)  $\text{NO}_3^-$  thermal decomposition:

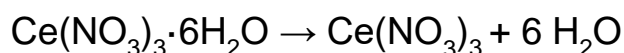


(iii) Cerium hydroxide condensation:

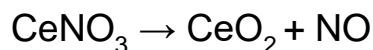
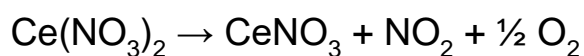


**(b)**

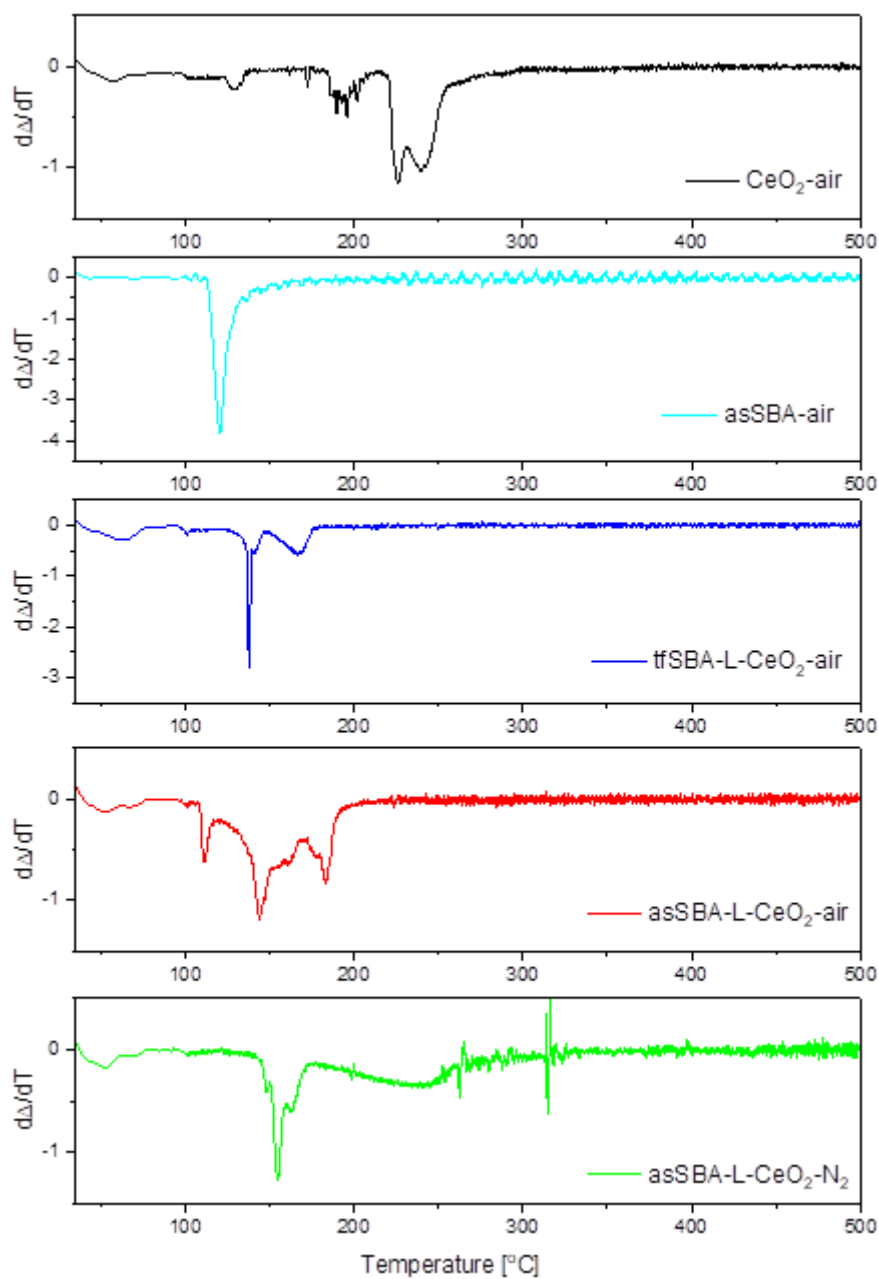
(i) Dehydration:



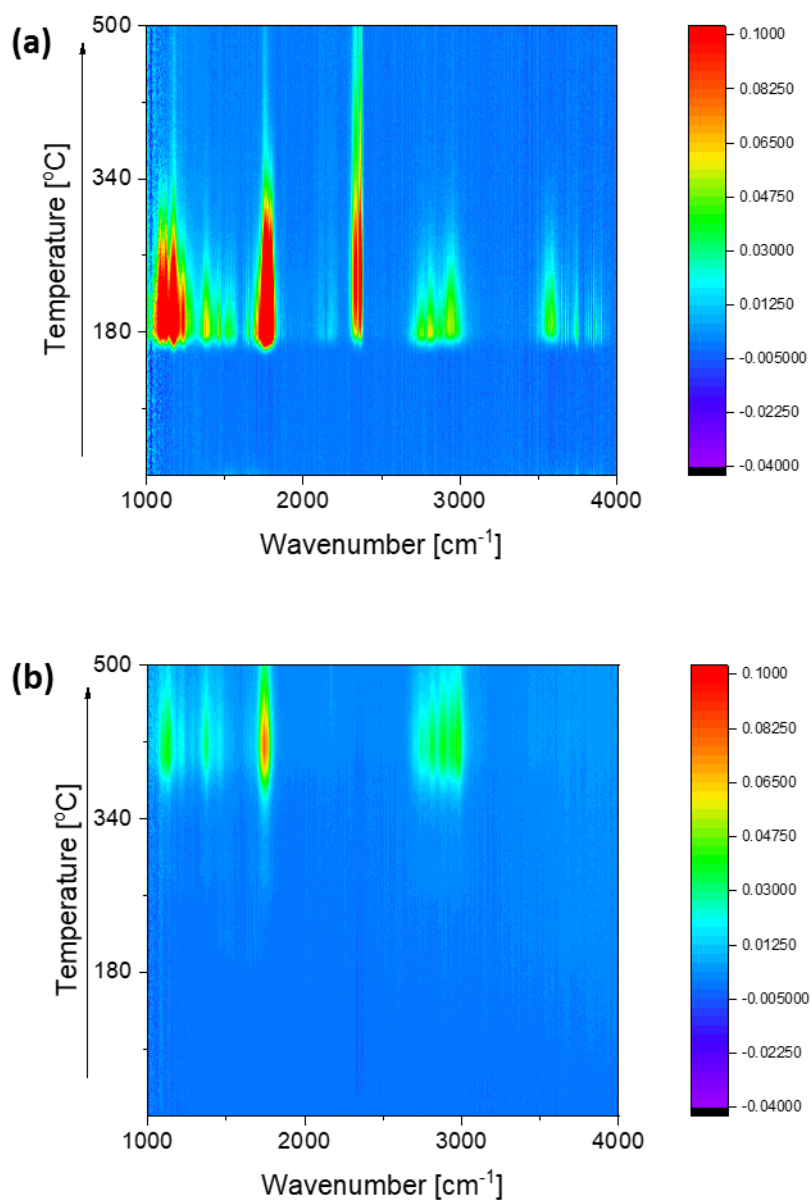
(ii) Decomposition to  $\text{CeO}_2$ :



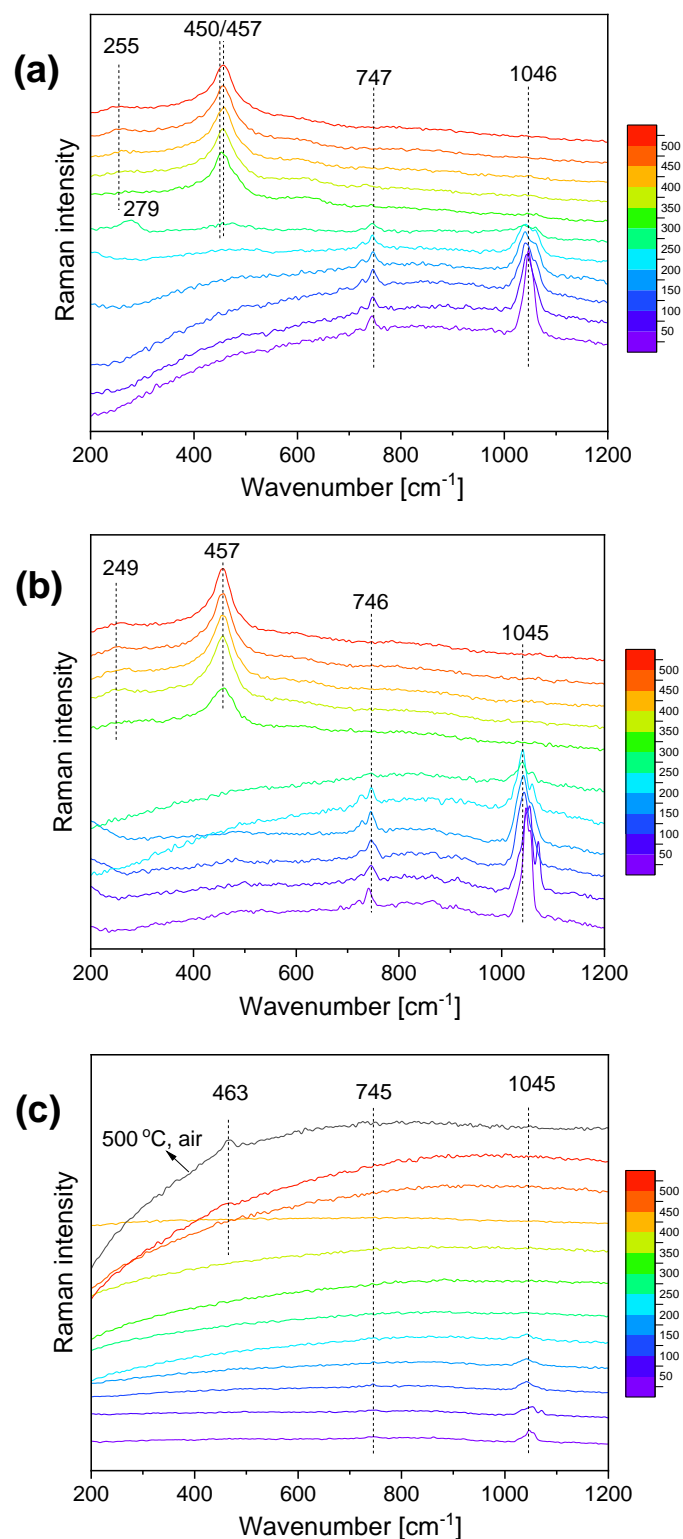
**Figure S2** According to Cochran et al.((a)),<sup>1</sup> the weight loss can be subdivided into three stages: (i) prior to decomposition, the salt melts and releases loosely bound water (<100 °C), or evaporates as aqueous acid azeotrope at a boiling point of about 120 °C; (ii) at higher temperature (>266 °C), residual nitrate thermally decomposes into  $\text{NO}_x$  gas and forms a solid metal hydroxide product; (iii) the resulting cerium hydroxide condenses to form ceria. Kang et al. have proposed a more detailed mechanism for the decomposition of  $\text{Ce}(\text{NO}_3)_3$  ((b)) according to which  $\text{Ce}(\text{NO}_3)_3$  transforms first to  $\text{Ce}(\text{NO}_3)_2$  at about 245 °C, then to  $\text{Ce}(\text{NO}_3)$  at about 270 °C, and finally to  $\text{CeO}_2$  at about 295 °C.<sup>2</sup>



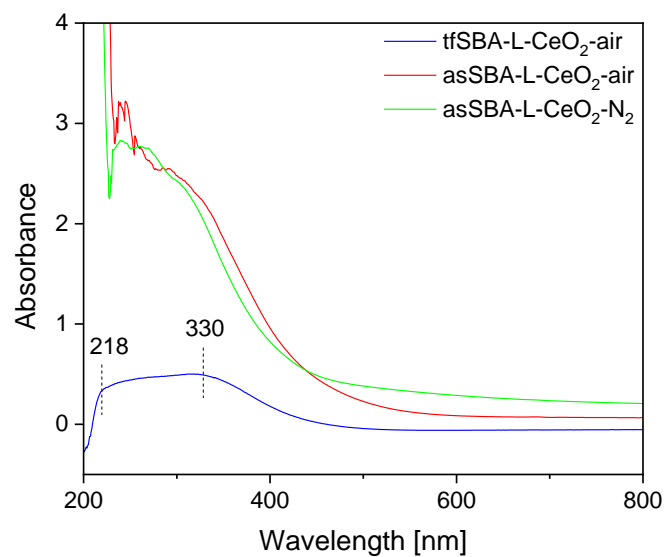
**Figure S3** DTG profiles of pure cerium nitrate, asSBA-15, and mixtures of SBA-15 and cerium nitrate during heating to 500 °C in air or inert  $\text{N}_2$  (heating rate: 1.5 °C/min).



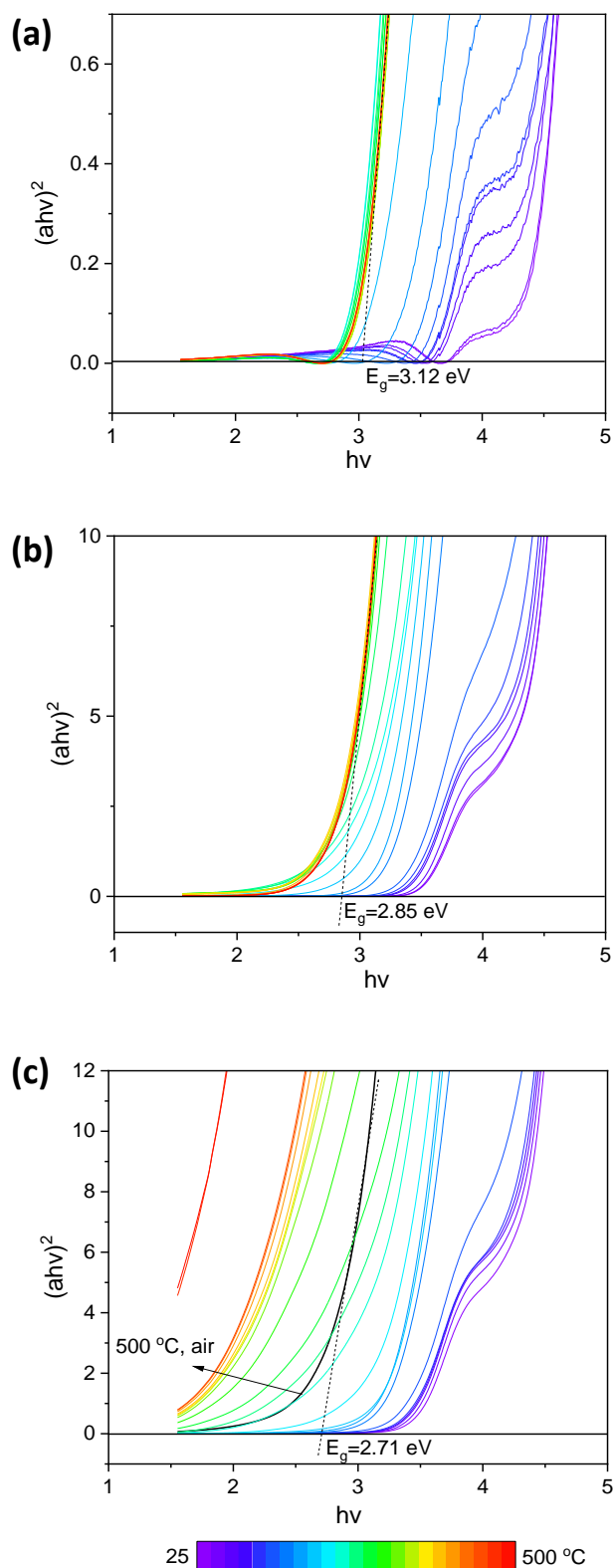
**Figure S4** *In situ* detection of exhaust during calcination of samples (a) asSBA15-air, (b) asSBA15-N<sub>2</sub>.



**Figure S5** *In situ* Raman spectra (514.5 nm) during the calcination of (a) tfSBA-L-CeO<sub>2</sub>-air, (b) asSBA-L-CeO<sub>2</sub>-air, and (c) asSBA-L-CeO<sub>2</sub>-N<sub>2</sub>, following the protocol given in Fig. 1a. Spectra are offset for clarity. The feature at about 250 cm<sup>-1</sup> has been shown to originate from the longitudinal stretching mode of surface oxygen against cerium ions (Ce-O) as well as a contribution of the 2TA phonon,<sup>3,4</sup> whereas the additional feature at about 279 cm<sup>-1</sup> is tentatively assigned to a nitro species formed during the transformation from cerium nitrate to crystalline ceria.<sup>5</sup>



**Figure S6** DR UV-vis spectra of the samples tfSBA-L-CeO<sub>2</sub>-air, asSBA-L-CeO<sub>2</sub>-air, and asSBA-L-CeO<sub>2</sub>-N<sub>2</sub>, recorded at room temperature after cooling from high temperature calcination in synthetic air.

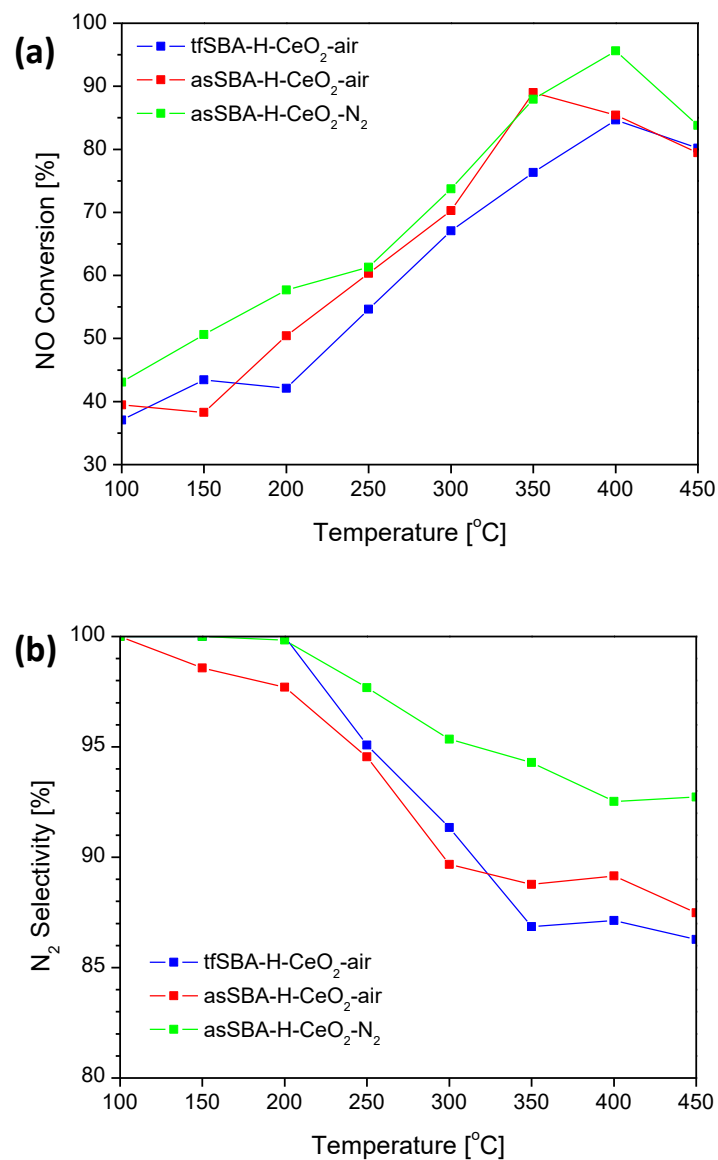


**Figure S7** Calculation of band gap energies according to the *in situ* DR UV-vis spectra by applying Tauc's method. (a) fSBA-L-CeO<sub>2</sub>-air, (b) asSBA-L-CeO<sub>2</sub>-air, and (c) asSBA-L-CeO<sub>2</sub>-N<sub>2</sub>. In (c) the black curve represents the sample calcined in N<sub>2</sub>, followed by calcination in air at 500 °C for 2 hours.

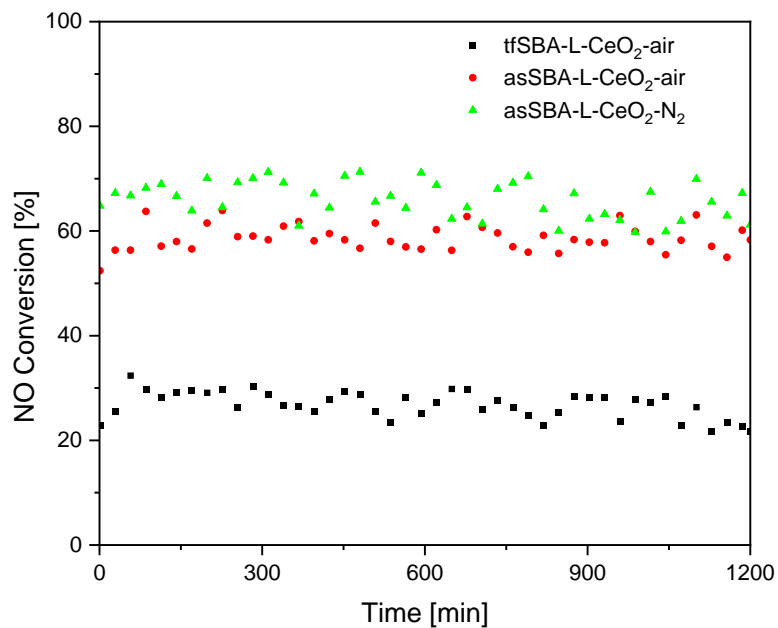


**Table S1** Assignment of the IR features observed by *in situ* DRIFT spectroscopy.

Wavenumber, cm <sup>-1</sup>	tfSBA-CeO <sub>2</sub> -air	asSBA-CeO <sub>2</sub> -air	asSBA-CeO <sub>2</sub> -N <sub>2</sub>	Ref.
1225-1237		Hydrogen carbonates	Hydrogen carbonates	6
1253	Chelate NO <sub>2</sub> <sup>-</sup>			7
1303	Monodentate nitrates			8
1345-1357	Free nitrate ions		Free nitrate ions	8
1458			C-H deformation	9
1539-1543	Bidentate nitrates	Bidentate nitrates		10
1613	Bridging nitrates			10
1625-1636	Adsorbed NO <sub>2</sub>	Adsorbed NO <sub>2</sub>	Adsorbed NO <sub>2</sub>	8
1663	Adsorbed N <sub>2</sub> O <sub>4</sub>			8
1729-1732		C=O	C=O	7
1764-1767	Adsorbed NO	Adsorbed NO	Adsorbed NO	7
1849-1981	Silica framework	Silica framework	Silica framework	8
2290/2341		Adsorbed CO <sub>2</sub>		7
2356-2360	CO <sub>2</sub>	CO <sub>2</sub>	CO <sub>2</sub>	11
2484-2491	C-H	C-H	C-H	12
2809	C-H <sub>2</sub>			13
2867/2933/2976		C-H	C-H	11
2941	CH <sub>2</sub>			9
3176	-OH			14
3266	-OH			13
3200-3500	-OH			13
3700			Ce-OH	15
3740	Si-OH	Si-OH		13



**Figure S8** (a) NO conversion and (b) N<sub>2</sub> selectivity of the indicated samples in NH<sub>3</sub>-SCR of NO, using a feed gas consisting of 500 ppm NH<sub>3</sub>, 500 ppm NO, and 5% O<sub>2</sub> (balanced with N<sub>2</sub>) and a total gas flow of 50 ml·min<sup>-1</sup> (GHSV=30000 h<sup>-1</sup>).



**Figure S9** Stability of the indicated samples in NH<sub>3</sub>-SCR of NO at 300 °C, using a feed gas consisting of 500 ppm NH<sub>3</sub>, 500 ppm NO, and 5% O<sub>2</sub> (balanced with N<sub>2</sub>) and a total gas flow of 50 ml·min<sup>-1</sup> (GHSV=30000 h<sup>-1</sup>).

**Table S2** Catalytic performance of cerium-based deNO<sub>x</sub> catalysts synthesized by different methods.

Catalyst	Preparation method	Reaction conditions	NO <sub>x</sub> conversion (temperature range)	GHSV or GWSV	Source
CeO <sub>2</sub>	precipitation method	NO = 600 ppm, NH <sub>3</sub> = 600, ppm, O <sub>2</sub> = 5%	45-60% (225-350 °C)	108000 h <sup>-1</sup>	16
CeO <sub>2</sub>	hydrothermal method	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 3%	50% (300 °C)	120000 ml g <sup>-1</sup> h <sup>-1</sup>	17
CeO <sub>2</sub>	thermal decomposition	NO = 736 mg/m <sup>3</sup> , NH <sub>3</sub> = 417 mg/m <sup>3</sup> , O <sub>2</sub> = 5%	60-65% (300-400 °C)	108000 h <sup>-1</sup>	18
CeO <sub>2</sub>	impregnation	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 5%	15-20 % (350-450 °C)	120000 ml g <sup>-1</sup> h <sup>-1</sup>	19
CeO <sub>2</sub>	thermal decomposition	NH <sub>3</sub> = NO = 600 ppm, O <sub>2</sub> = 5%	40-50% (250-325 °C)	108000 h <sup>-1</sup>	20
CeO <sub>2</sub>	one-pot	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 3%	50-60% (300-400 °C)	45000 h <sup>-1</sup>	21
CeO <sub>2</sub>	spread self-combustion	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 5%	15 % (300-500 °C)	200000 ml g <sup>-1</sup> h <sup>-1</sup>	22
CeO <sub>2</sub> /SiO <sub>2</sub>	wet impregnation	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 5%	70-80% (275-325 °C)	48000 ml g <sup>-1</sup> h <sup>-1</sup>	23
CeO <sub>2</sub> /SBA-15	wet impregnation	NH <sub>3</sub> = 1100 ppm, NO = 1000 ppm, O <sub>2</sub> = 5%	60-70% (200-300 °C)	10000 h <sup>-1</sup>	24
tfSBA-CeO <sub>2</sub> -air	solid-state impregnation	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 5%	30% (300-400 °C)	30000 h <sup>-1</sup> (150000 ml g <sup>-1</sup> h <sup>-1</sup> )	This work
asSBA-CeO <sub>2</sub> -air	solid-state impregnation	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 5%	50-60% (250-400 °C)	30000 h <sup>-1</sup> (150000 ml g <sup>-1</sup> h <sup>-1</sup> )	This work
asSBA-CeO <sub>2</sub> -N <sub>2</sub>	solid-state impregnation	NH <sub>3</sub> = NO = 500 ppm, O <sub>2</sub> = 5%	55-65% (200-450 °C)	30000 h <sup>-1</sup> (150000 ml g <sup>-1</sup> h <sup>-1</sup> )	This work

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