

## Supporting Information

### Facet control of manganese oxides with diverse redox abilities and acidities for catalytic removing the hazardous 1,2- dichloroethane

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## S1. Preparation

**$\alpha$ -MnO<sub>2</sub>**: 1.35 g of KMnO<sub>4</sub> and 3.0 mL of HCl (37 wt%) were added to deionized water. After stirring for 30 min, the solution was transferred to a Teflon-lined stainless-steel autoclave, sealed, and maintained at 120 °C for 12 h in an electric oven.

**$\beta$ -MnO<sub>2</sub>**: The mixture of 1.69 g MnSO<sub>4</sub> and 2.28 g (NH<sub>4</sub>)<sub>2</sub>S<sub>2</sub>O<sub>8</sub> was added to deionized water with stirring for 30 min. Then, the solution was transferred to a Teflon-lined stainless-steel autoclave, sealed, and maintained at 140°C for 12 h.

**$\gamma$ -MnO<sub>2</sub>**: The mixture of 6.32 g MnSO<sub>4</sub> and 8.56 g (NH<sub>4</sub>)<sub>2</sub>S<sub>2</sub>O<sub>8</sub> was added to deionized water. After stirring for about 30 min, the solution was transferred to a Teflon-lined stainless-steel autoclave, sealed, and maintained at 90°C for 24 h in oven.

**$\delta$ -MnO<sub>2</sub>**: 1.35 g of KMnO<sub>4</sub> and 1.0 mL of HCl (37 wt%) were added to deionized water, After stirring magnetically for about 30 min, the solution was transferred to a Teflon-lined stainless-steel autoclave and crystallized at 100°C for 12 h.

After the hydrothermal reaction, the autoclave was cooled to room temperature. The sediment was centrifuged, washed with distilled water and ethanol several times, dried at 80°C for 12 h, and then calcined at 300°C for 8 h to obtain the corresponding samples.

## S2. Characterization

The crystallographic information of sample was investigated by X-ray diffraction using a diffractometer equipped with Cu  $K\alpha$  radiation ( $\lambda = 0.15406$  nm, D8FOCUS, Bruker). Diffractograms were collected in the  $2\theta$  range between 10° and 80° by step of 0.1°. Phase identification was made by a comparison with JCPDS database.

The information of specific surface area ( $S_{\text{BET}}$ ) was collected by N<sub>2</sub> sorption isotherm using a Quanta chrome Autosorb IQ analyzer at liquid N<sub>2</sub> temperature (-196 °C). Before analysis, samples were outgassed at 300 °C under vacuum for 10 h. Brunauer-Emmett-Teller (BET) surface area was calculated using experimental points at a relative pressure of  $P/P_0 = 0.05\sim 0.35$ .

H<sub>2</sub>-TPR experiment was carried out in a chemisorption device. Prior to the measurement, the samples were degassed under flowing nitrogen (30 ml/min) at 300 °C for 1 h. After cooling in nitrogen to 100 °C, a 5% H<sub>2</sub>/N<sub>2</sub> flow of 30 ml/min was introduced to pass through a quartz reactor containing the sample (100 mg). The consumption of H<sub>2</sub> along with heating temperature was online recorded by a thermal conductivity detector (TCD, Huasi, China) and the signals of TCD were collected

from 100°C to 600°C in nitrogen flow.

Temperature-programmed desorption of O<sub>2</sub> (O<sub>2</sub>-TPD) was also analyzed with an online mass spectrometer. The concentrations of O<sub>2</sub> and CO<sub>2</sub> were determined using m/z=32 and m/z=44, respectively. For the O<sub>2</sub>-TPD, 0.1 g of catalyst was pretreated at 200 °C with Ar for 30 min, and then 10% O<sub>2</sub>/Ar was introduced on the surface of the catalyst for 60 min at 100 °C. Next, the sample was purged with Ar for 1 h to remove the exterior adsorbed molecular oxygen and the catalyst was cooled down to ambient temperature. Finally, the microreactor was heated from ambient temperature to 650 °C with a heating rate of 5 °C·min<sup>-1</sup> under Ar flow.

The NH<sub>3</sub> temperature programmed desorption (NH<sub>3</sub>-TPD) experiment was taken on a device with a thermal conductivity detector (TCD, Huasi, China). The sample (100 mg) was first pretreated at 300°C under nitrogen flow for 0.5 hr. After cooling to 100°C, the sample was saturated in 10% NH<sub>3</sub>/N<sub>2</sub> atmosphere for 1 h and then exposed in nitrogen atmosphere for 0.5 h to eliminate the influence of physisorbed NH<sub>3</sub>. Finally, the signals of TCD were collected from 100°C to 600°C in nitrogen flow.

A S-4800 (Hitachi, Japan) scanning electron microscope (SEM) was employed to characterize the morphology of the prepared MnO<sub>2</sub> solids (the accelerating voltage is 5.0 kV). The powders were coated onto a conductive tape. Besides, a JEM-2100 (Jeol, Japan) high-resolution transmission electron microscopy (HRTEM) was also employed to observe the crystal lattice fringe and internal microstructure (the operating voltage is 200 kV).

X-ray photoelectron spectroscopy (XPS) instrument (Shimadzu, Japan) equipped with a monochromatic Mg/Al K $\alpha$  was used to analyze the superficial layer properties. The binding energy was calibrated by the C 1s peak (B.E.=284.8eV) as a reference. The surface composition and chemical state were determined according to the position and areas of binding energies of Mn 2p, Mn 3s and O 1s peaks.

The *in situ* DRIFTS experiments were performed using an infrared spectrometer (SENSOR 27, BRUKER) that was configured with liquid N<sub>2</sub>-cooled highly sensitive mercury cadmium telluride (MCT) detector. The reaction chamber (Praying Mantis, Harrick) as a diffuse reflection accessory included a diffuse reflectance cell (Harrick) with CaF<sub>2</sub> windows and a heating cartridge that could control the desired temperatures. Before the test, about 50mg finely ground samples were padding in the *in situ*

chamber and heated under flowing Ar at 300 °C for 1 h to remove water from the surface and pores of the catalyst, the samples were then cooled to 50°C in Ar atmosphere. After that, the gaseous mixture of Ar + O<sub>2</sub> + 1, 2-DCE with a flow rate of 40 mL/min and 400 ppm 1, 2-DCE, 20% O<sub>2</sub> in Ar was introduced into the chamber. The spectra were collected in 64 scans at a resolution of 4 cm<sup>-1</sup> within 850–3800 cm<sup>-1</sup>. The sample was tested in the range of 50–300 °C.

### S3. Temperature-programmed oxygen isotopic exchange (OIE) reaction

This experiment is performed on an oxygen isotope device, which includes a vacuum pump, a circulation pump, a heating furnace, an U-shaped micro-reaction tube ( $V = 70 \text{ cm}^3$ ), and many gas pipelines, the signals of reactants were recorded by mass spectrometer (OmniStar, Germany). The sample (100 mg) was pretreated in O<sub>2</sub> atmosphere by heating to 300°C. When the temperature dropped to 200°C, redundant <sup>16</sup>O<sub>2</sub> was removed under the condition of dynamic vacuum for 30 min. Then,  $65.0 \pm 1.5 \text{ mbar}$  of pure Oxygen isotopic (<sup>18</sup>O<sub>2</sub>) was introduced into the reaction system for OIE reaction, and the catalyst was heated to 600°C and the mass spectrometer is turned on at the same time. The concentration changes of <sup>18</sup>O<sub>2</sub> (P36), <sup>16</sup>O<sub>2</sub> (P32), and <sup>16</sup>O<sup>18</sup>O (P34) during the oxygen exchange reaction were recorded by mass spectrometer. Besides, N<sub>2</sub> ( $m/z=28$ ) was also recorded in order to detect possible vacuum system leaks. Figure S1 shows a schematic diagram of an oxygen isotopic exchange device.

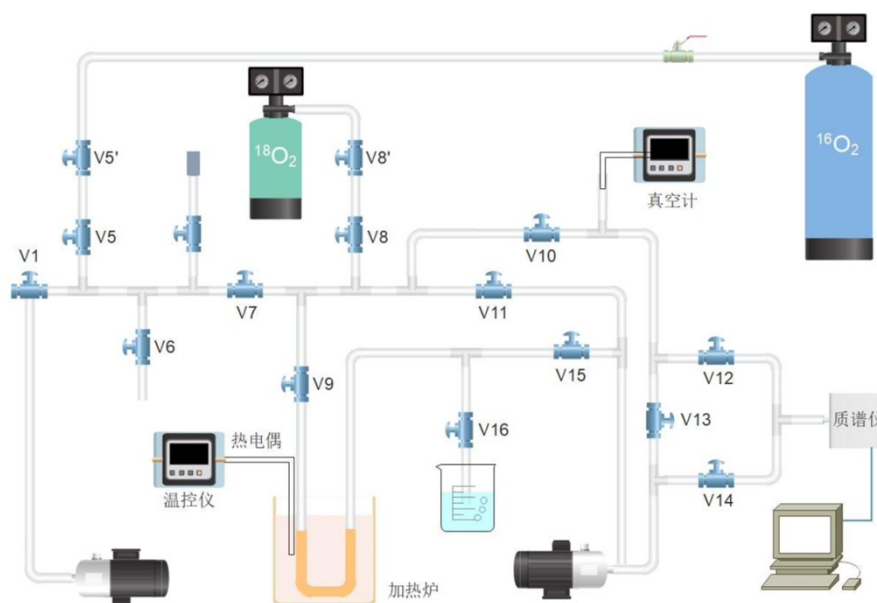


Figure S1: Schematic diagram of the oxygen isotopic exchange experiment

### S4. Computational details

Spin-polarized Periodic Density Functional Theory (DFT) calculations were accomplished with the Vienna simulation package VASP <sup>[S1]</sup>. The projector augmented plane wave (PAW) approach <sup>[S2-S3]</sup> was applied to the electron-ion interaction together with generalized gradient GGA-PW91 <sup>[S4]</sup>.

## S5. Catalytic activity and products yield

The following equations were used to calculate the conversion of 1,2-DCE as well as the CO, CO<sub>2</sub> and HCl yields :

$$1,2 - DCE \text{ conversion } (\%) = \frac{[1,2 - DCE]_{in} - [1,2 - DCE]_{out}}{[1,2 - DCE]_{in}} \times 100$$

(1)

$$CO \text{ yield } (\%) = \frac{[CO]}{[CO] + [CO_2] + x[C_xH_yCl_z]} \times 1,2 - DCE \text{ conversion} \times 100$$

(2)

$$CO_2 \text{ yield } (\%) = \frac{[CO_2]}{[CO] + [CO_2] + x[C_xH_yCl_z]} \times 1,2 - DCE \text{ conversion} \times 100$$

(3)

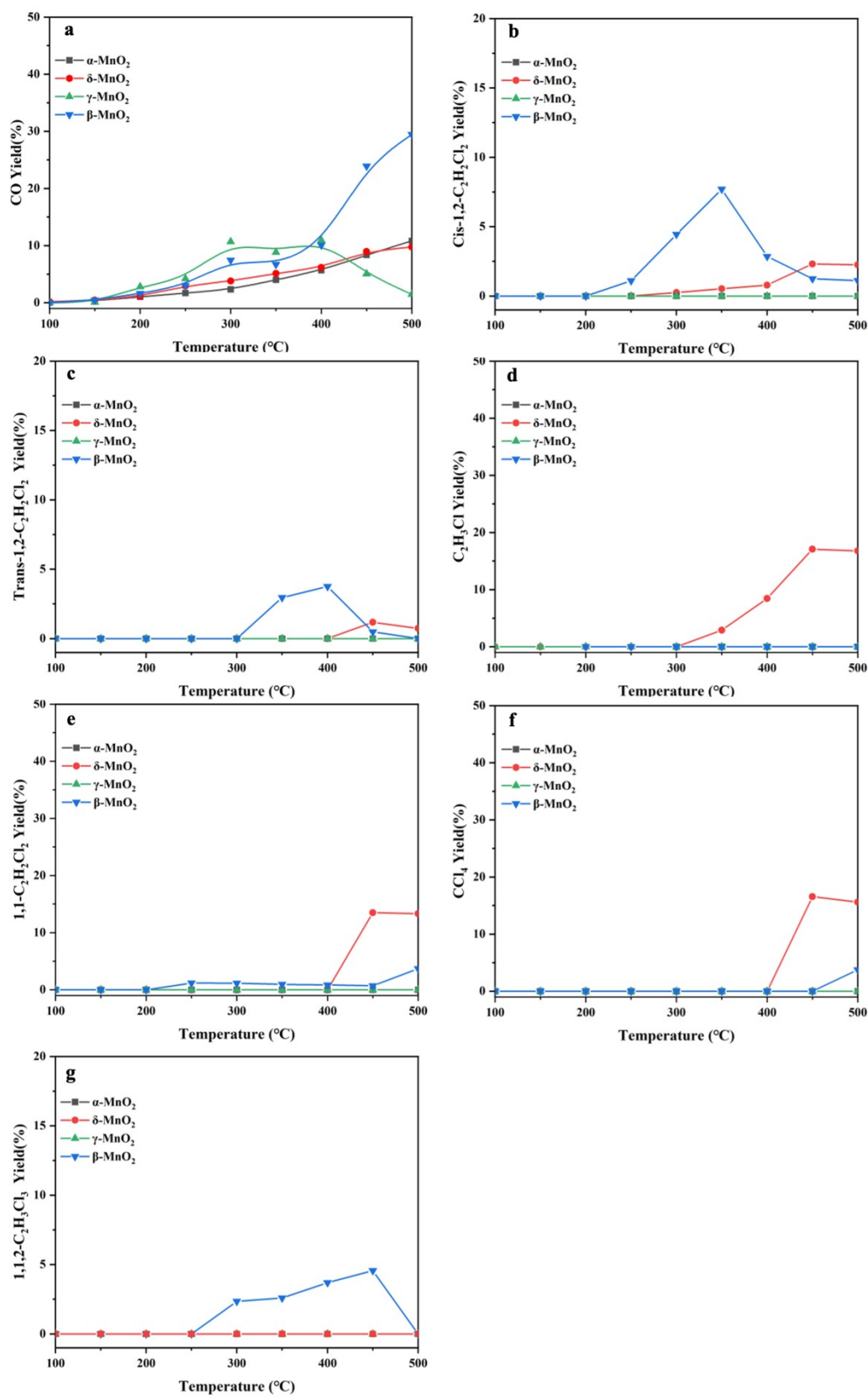
$$HCl \text{ yield } (\%) = \frac{[HCl]}{[HCl] + 2[Cl_2] + z[C_xH_yCl_z]} \times 1,2 - DCE \text{ conversion} \times 100$$

(4)

$$C_xH_yCl_z \text{ yield } (\%) = \frac{x[C_xH_yCl_z]}{[CO] + [CO_2] + x[C_xH_yCl_z]} \times 1,2 - DCE \text{ conversion} \times 100$$

(5)

## S6. Byproducts of catalyst combustion

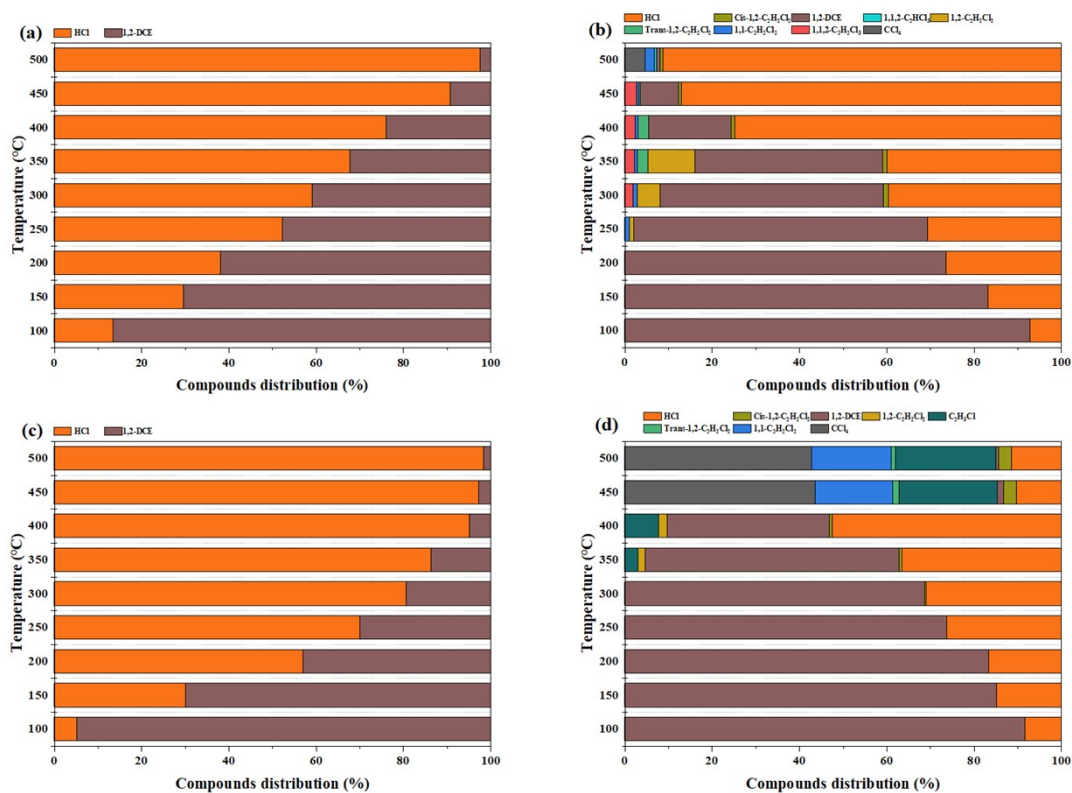


**Figure S2:** Yields of (a) CO, (b) cis-1,2- $\text{C}_2\text{H}_2\text{Cl}_2$ , (c) trans-1,2- $\text{C}_2\text{H}_2\text{Cl}_2$ , (d)  $\text{C}_2\text{H}_3\text{Cl}$ , (e) 1,1- $\text{C}_2\text{H}_2\text{Cl}_2$ , (f)  $\text{CCl}_4$  and (g) 1,1,2- $\text{C}_2\text{H}_3\text{Cl}_3$  over  $\alpha$ -,  $\beta$ -,  $\gamma$ - and  $\delta$ - $\text{MnO}_2$  samples.

Figure S2 shows the byproduct yields of 1,2-dichloroethane (1,2-DCE) combustion

over  $\alpha$ -,  $\beta$ -,  $\gamma$ - and  $\delta$ -MnO<sub>2</sub> samples.  $\alpha$ -MnO<sub>2</sub> presents a gradual increasing trend for CO yield, and cannot observe a decreasing trend.  $\beta$ -MnO<sub>2</sub> exhibits the highest CO yield, owing to the poor redox ability.  $\gamma$ -MnO<sub>2</sub> shows a trend of increasing first and then decreasing, which means CO can be further oxidized at high temperatures. Similar to the  $\alpha$ -MnO<sub>2</sub>,  $\delta$ -MnO<sub>2</sub> also displays the same trend because of the production of too many chlorinated byproducts, which hinders CO further transformation. No obvious chlorinated byproducts are found on  $\alpha$ - and  $\gamma$ -MnO<sub>2</sub>, but there are many chlorinated byproducts are found on  $\beta$ - and  $\delta$ -MnO<sub>2</sub>, especially on  $\delta$ -MnO<sub>2</sub>. Vinyl chloride (C<sub>2</sub>H<sub>3</sub>Cl) (Fig. S2 d) is produced due to the removal of 1,2-DCE by HCl elimination at 300°C. Then at 400 °C, an electrophilic substitution reaction between HCl and vinyl chloride was followed to form *cis*-dichloroethylene and *trans*-dichloroethylene (*cis*-1,2-C<sub>2</sub>H<sub>2</sub>Cl<sub>2</sub> and *trans*-1,2-C<sub>2</sub>H<sub>2</sub>Cl<sub>2</sub>) (Fig. S2 b and c), some of which also become 1,1-dichloroethene (1,1-C<sub>2</sub>H<sub>2</sub>Cl<sub>2</sub>) (Fig. S2 e), part of 1,2-DCE breaks the C-H and C-C bond, gradually becomes CCl<sub>4</sub> (Fig. S2 i) , and this part of the polychlorinated byproducts was formed at last without further transformation, the results show that the yield of HCl at high temperature (> 400°C) was very low. Similar to  $\delta$ -MnO<sub>2</sub>, the overall yield of HCl from  $\beta$ -MnO<sub>2</sub> was also low, and several reaction products (such as *cis*-1,2-dichloroethene, *trans*-1,2-dichloroethene, 1,1-dichloroethene and tetrachloromethane) are found to be identical to  $\delta$ -MnO<sub>2</sub>. Notably, the presence of 1,1,2-trichloroethane (1,1,2-C<sub>2</sub>H<sub>3</sub>Cl<sub>3</sub>) (Fig. S2 g) was noticed on the  $\beta$ -MnO<sub>2</sub>, indicating that the dehydrochlorination and chlorination of vinyl chloride might take place.

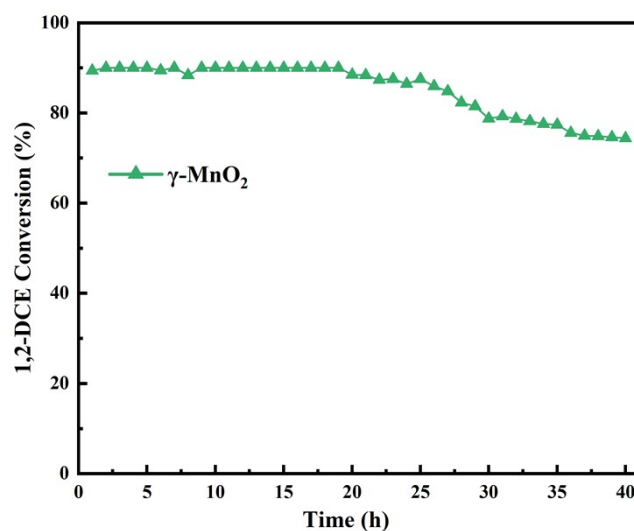
## S7. Cl mass balance of all these products



**Figure S3.** The chlorine mass balance during the 1, 2-DEC oxidation over (a)  $\alpha$ -, (b)  $\beta$ -, (c)  $\gamma$ - and (d)  $\delta$ -MnO<sub>2</sub>

It can be found that the sum of the yields of different detected Cl-containing substances is close to 100% (Figure S3).

## S8. Catalytic stability test



**Fig. S4.** Stability test of  $\gamma$ -MnO<sub>2</sub>



The stability of the best-performing  $\gamma$ -MnO<sub>2</sub> catalyst is investigated as shown in Fig. S4. This catalyst was tested for 1, 2-DCE oxidation at 400 °C for 40 h. After long-term test, the 1, 2-DCE conversion decreased from 89% to 74 %. It is speculated that the accumulation of chlorine over surface caused this deactivation in activity. In general, the investigated sample of  $\gamma$ -MnO<sub>2</sub> exhibited certain stability during activity test.

### S9. Blank experiment

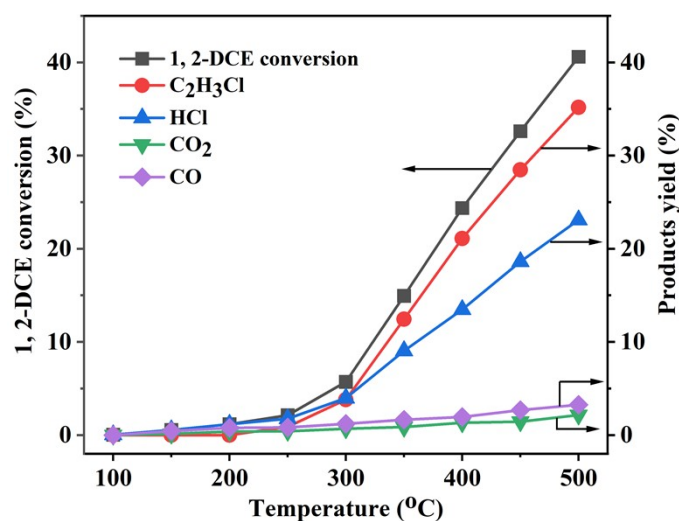


Figure S5. The blank experiment tested for decomposition 1, 2-DCE without catalysts.

A blank experiment in the absence of catalyst under the same experimental atmosphere for 1, 2-DCE oxidation was also conducted (Figure S5). The conversion of 1, 2-DCE was 40% at 500 °C with C<sub>2</sub>H<sub>3</sub>Cl as the main product, whose yield increased with temperature and reached 35% at 500 °C. In addition, the HCl and CO<sub>2</sub> yield were 23% and 2.15%, respectively. Therefore, it is necessary to further eliminate C<sub>2</sub>H<sub>3</sub>Cl using a suitable catalyst as well as improve the HCl and CO<sub>2</sub> yields..

## References

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