## **Supporting Information**

## Facile synthesis of layered $Co(OH)_2$ deposited $g-C_3N_4$ for activating peroxymonosulfate to degrade organic pollutants

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Figure S1. N<sub>2</sub> sorption isotherms curve of g-C<sub>3</sub>N<sub>4</sub>, Co(OH)<sub>2</sub> and Co(OH)<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub>

Table S1. BET surface area and pore volume of  $g-C_3N_4$ ,  $Co(OH)_2$  and  $Co(OH)_2/g-C_3N_4$ .

Catalyst	$S_{BET} (m^2/g)$	pore volum $(cm^3/g)$
Co(OH) <sub>2</sub>	85.5085	0.170488
g-C <sub>3</sub> N <sub>4</sub>	5.1232	0.013123
$Co(OH)_2/g-C_3N_4$	22.8336	0.057799







Figure S3. The electrochemical impedance spectroscopy of  $g-C_3N_4$ ,  $Co(OH)_2$ , and  $Co(OH)_2$ /  $g-C_3N_4$ .



Figure S4. (a) The RhB removal efficiency and (b) Kinetic constants of RhB removal in different systems. Reaction conditions: V=100mL,  $[RhB]_0 = 20.0$  mg/L,  $[Cat.]_0 = 0.15$  g/L,  $[PMS]_0 = 0.50$  g/L, initial pH = 7.



Figure S5. Residual PMS during the reaction system. Reaction conditions: V=100mL, [RhB]0 = 20.0 mg/L, [Cat.]0 = 0.15 g/L, [PMS]0 = 0.50 g/L, initial pH = 7.



Figure S6. Kinetic curves of RhB removal at different reaction conditions.(a) PMS dosage, (b)  $Co(OH)_2$ / g-C<sub>3</sub>N<sub>4</sub> dosage, (c) initial pH value, (d) reaction temperature. Reaction conditions: V=100mL, [RhB]<sub>0</sub> = 20.0 mg/L, [Co(OH)<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub>]<sub>0</sub> = 0.15 g/L (except (a)), [PMS]<sub>0</sub> = 0.50 g/L (except (b)), initial pH = 7 (except (c)).



Figure S7.The TOC removal effect of  $Co(OH)_2/g-C_3N_4$  over time on RhB. Reaction conditions: V = 100 mL, [RhB]\_0 = 20.0 mg/L, [Co(OH)\_2/g-C\_3N\_4]\_0 = 0.15 g/L, [PMS]\_0 = 0.50 g/L, initial pH = 7.0.



Figure S8. (a) The RhB removal efficiency and (b) Kinetic constants of RhB removal in the different initial RhB concentration. Reaction conditions: [Co(OH)2/g-C3N4]0 =0.15g/L, [PMS]0 =0.5g/L, initial pH =7.



Figure S9. The degradation of various emerging organic pollutants. Reaction conditions: V = 100 mL, [organic compounds]<sub>0</sub> = 20.0 mg/L,  $[Co(OH)_2/g-C_3N_4]_0 = 0.15 \text{ g/L}$ ,  $[PMS]_0 = 0.5 \text{ 0g/L}$ , initial pH = 7.0.



Figure S10. Degradation efficiency of RhB after 3 cycles. Reaction conditions: V=100 mL, [organic compounds]<sub>0</sub> =20.0mg/L,  $[Co(OH)_2/g-C_3N_4]_0$  =0.15g/L, [PMS]<sub>0</sub> =0.5g/L, initial pH =7.



Figure S11. The XRD of Co(OH)<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> after using PMS activation.



Figure S12. XPS of Co 2p for Co(OH)<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> after using PMS activation.



Figure S13. The extracted ion chromatography (EIC) of phthalic acid.



Figure S14. The mass spectrogram of phthalic acid.



Figure S15. The extracted ion chromatography (EIC) of phthalic acid.



Figure S16. The mass spectrogram of phthalic acid.



Figure S17. The intermediates obtained by liquid mass spectrometry.

Table S2. Comparison of  $Co(OH)_2/g-C_3N_4$  with other published materials for PMS activation.

Contaminants		Catalyst		PMS	K <sub>obs</sub>	
Type and concentration		Type and concentration		Concentration	(min <sup>-1</sup> )	Ref.
(g L <sup>-1</sup> )		(g L <sup>-1</sup> )				
RhB	0.1	CoFe <sub>2</sub> O <sub>4</sub> /TNTs	0.20	$4.0 \text{ g L}^{-1}$	0.0673	[1]
RhB	0.1	CoFe <sub>2</sub> O <sub>4</sub> /OMC	0.05	1.5 mM	0.0452	[2]
RhB	0.05	CoFe <sub>2</sub> O <sub>4</sub> /diatomite	0.03	1.5 mM	0.572	[3]
RhB	0.01	Mn <sub>3</sub> O <sub>4</sub> / ZIF-8	0.40	$0.3 \text{ g L}^{-1}$	0.913	[4]
MB	0.02	FeCo <sub>2</sub> @ APCFs	0.10	$0.5 \text{ g L}^{-1}$	0.422	[5]
MB	0.02	MnFe <sub>2</sub> O <sub>4</sub> -rGO	0.05	$0.5 \text{ g L}^{-1}$	0.019	[6]
MB	0.02	MnFe <sub>2</sub> O <sub>4</sub>	0.05	$0.5 \text{ g L}^{-1}$	0.012	[6]
MB	0.02	Co(OH) <sub>2</sub> /g-C <sub>3</sub> N <sub>4</sub>	0.15	$0.5 \text{ g L}^{-1}$	0.524	This work
RhB	0.02	Co(OH) <sub>2</sub> /g-C <sub>3</sub> N <sub>4</sub>	0.15	<b>0.5</b> g L <sup>-1</sup>	0.460	This work

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