

Electronic Supplementary Material (ESI) for New Journal of  
Chemistry

*Electronic Supplementary Information*

**Removal of CO<sub>2</sub> from High-Temperature Flue Gas by PDMS/IL  
composite membranes**

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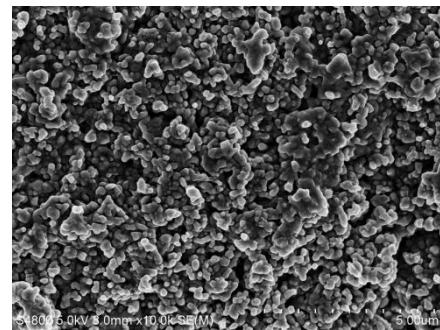
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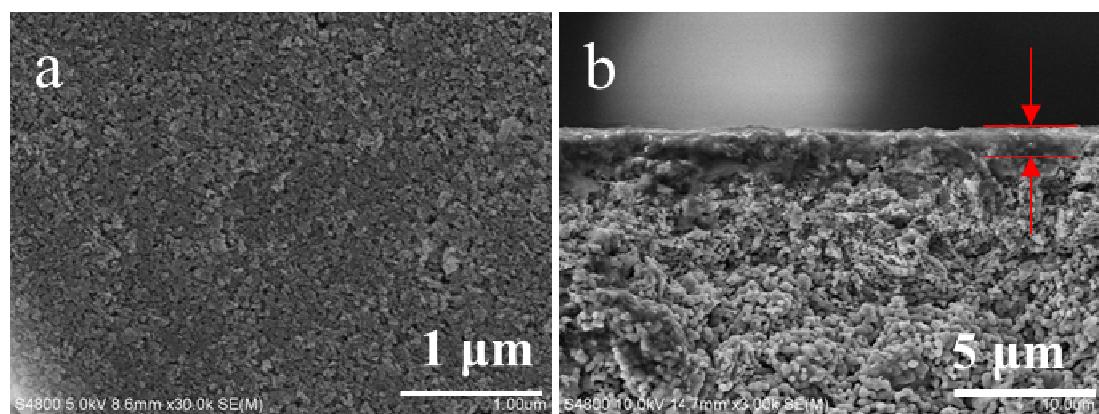
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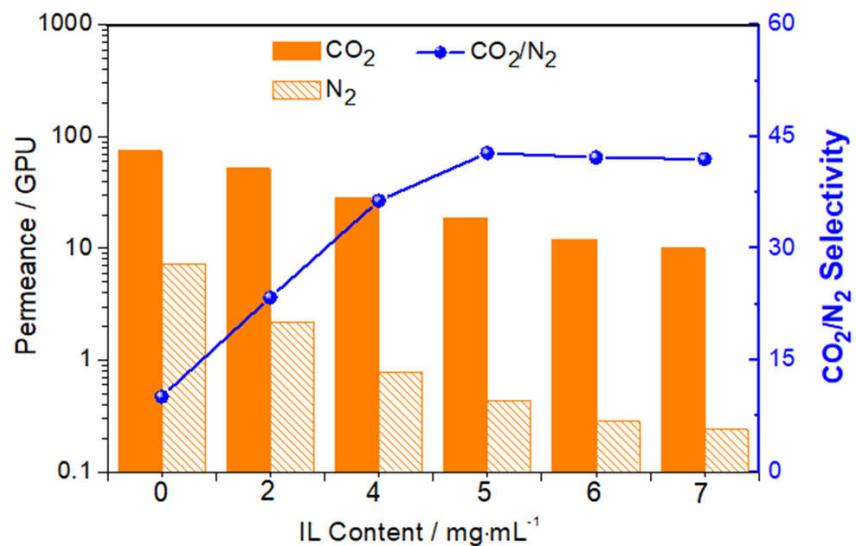
E-mail address: Xiaobing.li@cumt.edu.cn (Xiaobing Li)



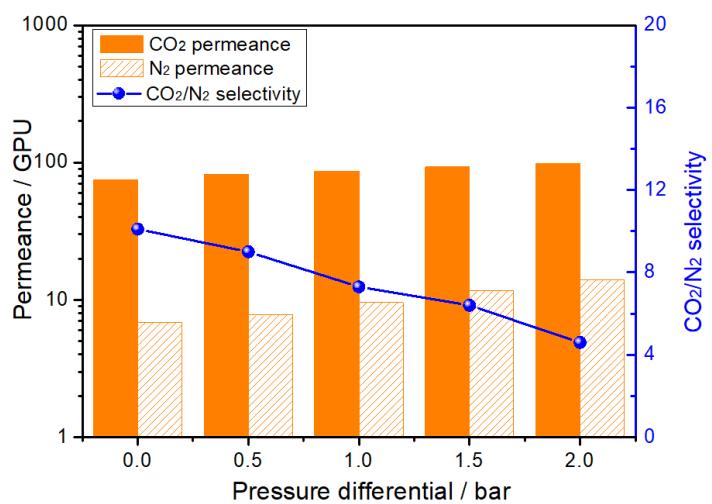
**Fig. S1** SEM image of PDMS/IL composite membrane on a bare  $\alpha$ -alumina substrate.



**Fig. S2** SEM images of  $\gamma$ -alumina buffer layer on  $\alpha$ -alumina substrate: top-view (a) and cross-section (b).



**Fig. S3** The influence of IL contents on the separation performance of the composite membranes.



**Fig. S4** The CO<sub>2</sub>/N<sub>2</sub> separation performance of the PDMS membrane as a function of the trans-membrane pressure.

**Table S1** Ionic liquids tested in the present study and their most relevant properties at °C.

Ionic liquid	Tg <sup>a</sup>	Td <sup>b</sup>	Density <sup>c</sup>	Viscosity <sup>d</sup>
[Bmim][Tf <sub>2</sub> N]	187.15	675.15	1.437	0.069

<sup>a</sup>Tg = glass transition temperature (°C). <sup>b</sup>Td = decomposition temperature (°C). <sup>c</sup>Density at 30 °C(g/cm<sup>3</sup>). <sup>d</sup>Measured viscosity at 30 °C ( $\eta$ , Pa·s).**Table S2** The permeability coefficients, diffusion coefficients and solubility coefficients of CO<sub>2</sub> and N<sub>2</sub> of PDMS membrane by time-lag system under different temperatures.

Temperature	Gas	P (barrer)	D (10 <sup>-6</sup> cm <sup>2</sup> /s)	S (10 <sup>-4</sup> cm <sup>3</sup> (STP)/cm <sup>3</sup> cmHg)	P <sub>CO2</sub> /P <sub>N2</sub>
25°C	CO <sub>2</sub>	74.6	0.43	173.5	10.1
	N <sub>2</sub>	7.38	0.48	15.4	
60°C	CO <sub>2</sub>	77.6	0.62	125.2	8.6
	N <sub>2</sub>	9	0.68	13.2	
90°C	CO <sub>2</sub>	84.7	1.05	80.7	7.8
	N <sub>2</sub>	11.3	1.10	10.3	
120°C	CO <sub>2</sub>	88.1	1.51	58.3	6.7
	N <sub>2</sub>	13.1	1.55	8.45	
150°C	CO <sub>2</sub>	86.8	2.25	38.6	4.9
	N <sub>2</sub>	17.7	2.41	7.35	

**Table S3** The permeability coefficients, diffusion coefficients and solubility coefficients of CO<sub>2</sub> and N<sub>2</sub> of PDMS/IL composite membrane by time-lag system under different temperatures.

Temperature	Gas	P (barrer)	D ( $10^{-6}$ cm <sup>2</sup> /s)	S ( $10^{-4}$ cm <sup>3</sup> (STP)/cm <sup>3</sup> )	P <sub>CO2</sub> /P <sub>N2</sub>
				cmHg)	
25°C	CO <sub>2</sub>	18.9	0.22	85.9	42.8
	N <sub>2</sub>	0.43	0.27	1.59	
60°C	CO <sub>2</sub>	20.1	0.42	47.9	35.6
	N <sub>2</sub>	0.55	0.49	1.12	
90°C	CO <sub>2</sub>	20.9	0.85	24.6	31.5
	N <sub>2</sub>	0.65	0.89	0.73	
120°C	CO <sub>2</sub>	21.3	1.20	17.8	22.5
		0.93	1.32	0.70	
150°C	CO <sub>2</sub>	22.6	1.95	11.6	21.4
	N <sub>2</sub>	1.06	2.19	0.48	

**Table S4** The separation performance of five PDMS/IL composite membranes prepared in the same batch at 150 °C

Membrane	CO <sub>2</sub> permeance (GPU)	N <sub>2</sub> permeance (GPU)	CO <sub>2</sub> /N <sub>2</sub> selectivity	Average selectivity	Standard deviation	RSD
M1	20.9	0.93	22.6	21.9	1.54	7.0%
M2	21.9	1.08	20.2			
M3	21.3	0.89	23.9			
M4	23.0	1.03	22.3			
M5	23.5	1.46	20.5			